## Angel A.J. Torriero *Editor*

# Electrochemistry in lonic Liquids

**Volume 1: Fundamentals** 



Electrochemistry in Ionic Liquids

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Volume 1: Fundamentals



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## **Preface for First Volume**

Electrochemistry is dominated by the study of species dissolved in solution. The use of a solvent as the reaction medium helps electrochemists to control important reaction conditions such as pH, rate of mass transfer, concentration of reactant, solubility, solvation, etc. Water and organic solvents are the most popular media. However, by using appropriate ionic liquids, reactants and products that are unstable in those media remain stable, and redox reactions that are impossible in water and organic solvents become possible. The reaction environments are markedly wider in some ionic liquids than in other solvent systems. In spite of this, some fundamental electrochemical concepts generally used in conventional solvent systems are not always valid in ionic liquids.

The aim of this book is to present the insights of experts on emerging experimental techniques and theoretical concepts that are or will be in the vanguard of the field of electrochemistry in ionic liquids. The two volumes of this book provides the reader with a broad and self-contained account of electrochemical techniques available to work in ionic liquids. It also gathers and critically discusses the important properties of protic ionic liquids, deep-eutectic solvents, task-specific ionic liquids, polymeric ion gels, and lithium-ion solvation, relevant to electrochemistry.

The two volumes of this book will be of interest for researchers in relevant industries as well as for academics, for scientists, and for the general chemical and electrochemical audience. It also can be given to graduate students and postdoctoral fellows looking for guidance to start working in this research field.

Burwood, VIC, Australia

Angel A.J. Torriero

## **Preface for Second Volume**

The field of electrochemistry in ionic liquids has blossomed in the last decade, since some of these ionic liquids tend to be good electrochemical solvents, exhibit interesting conductive properties, and offer the unique possibility to tune the physicochemical properties. These exclusive properties make them very useful as both the electrolyte and the solvent in electrochemical applications. There are several comprehensive reviews of this field, but none of them have covered the electrochemical applications of ionic liquids to the widest extent. Thanks to the contribution of scientists from different countries with strong expertise in the field, this new book collates the formerly dispersed knowledge into two handy volumes. Readers will find ten chapters gathered in three sections. The book commences with the latest understanding of electrodeposition, and electroless deposition, followed by a critical discussion of voltammetry of adhered microparticles, electrochemistry of organic and organometallic compounds, electrocatalytic reactions, oxygen reduction reaction, and ionic liquids in surface protection and lubrication. The book finishes with an overview on the current industrial application of ionic liquids and the challenges, issues, and recycling methods used in industrial developments.

The two volumes of this book will be of interest to researchers in relevant industries as well as academics, scientists, and anyone interested in general chemistry and electrochemistry. The book can also be used as a guide for graduate students and postdoctoral fellows who wish to start working in this field.

Burwood, VIC, Australia

Angel A.J. Torriero

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## **About the Editor**

#### Dr. Angel A.J. Torriero

Dr. Angel A.J. Torriero is a Lecturer of Chemistry and Electrochemistry at Deakin University, Melbourne, Australia. He has published more than 50-refereed papers (h-index = 18; Scopus, November 2014), six book chapters, several patents, and one book, *Electrochemical Properties and Applications of Ionic Liquids* in 2011.

Dr. Torriero has a broad interest in both fundamental and applied electrochemistry and has made significant contributions in a number of fields, including analytical electrochemistry, biosensor, bioelectrochemistry, organic and organometallic electrochemistry, and most recently internal reference systems for ionic liquids.

## Chapter 1 Introduction

Angel A.J. Torriero

As liquid media at a temperature less than 100 °C that possess some level of ionic conductivity, it is immediately of interest to consider the use of ionic liquids (ILs) as electrolytes to carry out electrochemical processes. This has of course the origins of the modern era of interest in ionic liquids via the work of Wilkes and coworkers in the 1990s [1]. Applications in electrowinning and electrodeposition have developed including processes for a range of metals from copper and zinc to lithium and aluminium [2]. Some metals such as titanium remain, however, stubbornly difficult to electrodeposit [3]. A range of applications in electrochemical devices, including batteries, fuel cells, and solar cells have also emerged and are being thoroughly discussed in Volume 2 (Electrochemistry in ionic liquids. Applications). In parallel to this, there has emerged the need to understand more in detail some important fundamental concepts of electrochemistry as well as the interest on fundamental electrochemical process taking place in an ionic liquid medium and in identifying the ways in which the processes differ, or not, from conventional solvent systems as a result of the highly charged medium [4-6]. Thereby, in this book, special emphasis is placed on showing which aspects of electrochemistry in ionic liquids are different from electrochemistry in conventional solutions. Furthermore, new electrochemical concepts and theories are presented. The book commences with a deep and comprehensive discussion on electrode/electrolyte interface reactions, interface structure, and its critical properties for all electrochemical applications. Chapter 2 discusses these fundamental concepts along with some in situ techniques, such as electrochemical impedance and Fourier transform infrared spectroscopy, cyclic voltammetry, and electrochemical quartz crystal microbalance, suitable for the characterization of electrode/IL interfaces.

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One of the open problems of electrochemistry in ionic liquids nowadays is the choice of a reference electrode. Chapter 3 discusses the latest understanding and practical approaches to the application of reference electrodes and internal reference redox scales in ionic liquids. Problems and limitations of reference systems are presented with the help of experimental examples. Comparison of the behavior of internal reference redox systems in organic solvents with added supporting electrolyte and ionic liquids is provided and new observations critically discussed. This chapter is very important for any experimentalist starting work in the electrochemical and IL fields. Further information about internal reference redox scales can also be found in Volume 2 (Chap. 14).

Chapter 4 describes the specific challenges and opportunities for electrochemists attempting to perform scanning electrochemical microscopic and voltammetric measurements with ultramicroelectrodes in ionic liquids. Meanwhile, Chap. 5 focuses its attention on the electroanalytical application of semiintegral and convolution voltammetry in ionic liquids. This robust and versatile analytical method involves transforming a transient peak-shaped voltammogram into a form that closely resembles a steady-state voltammogram. This transformation is highly advantageous to determine the diffusion coefficient of redox active species, along with other thermodynamic parameters such as the bulk concentration and the stoichiometric number of electrons transferred. Other techniques to quantify these three parameters are summarized in Volume 2 (Chap. 18).

Small-angle X-ray scattering is also a powerful in situ technique that could be used together with electrochemistry to study surfaces and resolve the size and structure of phases on the nanometer scale. Chapter 6 discusses details of the small-angle X-ray scattering technique with special emphasis on the experimental setup and analysis.

Chapter 7 summarizes the synthesis and physical properties of protic ionic liquids and deep eutectic solvents and draws the connection to real-world applications. Further applications of protic ionic liquids can be found in Volume 2 (Chaps. 17 and 20). The "designable" or "tunable" nature of ILs, their physicochemical properties, and high applicability in the electrochemical field is discussed in detail in Chap. 8. The application of deep eutectic solvents presented in Chap. 7, is also discussed in this chapter. Further applications of task-specific ILs can as well be found in Chap. 2.

Chapter 9 summarizes the preparation methods, properties, and applications of ion gels, which are a new type of gels where the liquid phase, percolating throughout the solid phase, is an ionic liquid. The application of these new materials in the development of energy storage systems, in addition to sensors, optoelectronics, catalytic membranes, separation membranes, and in drug release is discussed.

Lithium ions are generally solvated by IL ions to form metal-ion solvation complexes. Electrochemical and physicochemical properties of the lithium-containing IL solutions, such as ionic conductivity, redox reaction behavior, viscosity, and density, strongly depend on the static and dynamic structures of the mentioned solvation complexes. Chapter 10 discusses recent progress in lithium

solvation by imidazolium-containing ionic liquids, a topic that is of both fundamental and practical significance.

This book brings to the scientists, engineers, and students new electrochemical concepts and summarized results in the field of ionic liquid. Of course, as the mentioned research areas are in a constant state of development, this book can hardly be comprehensive, but certainly they will stimulate further the continuing development of *Electrochemistry in Ionic Liquids*.

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## Part I Fundamental Concepts of Electrochemistry in Ionic Liquids

## Chapter 2 Electrode–Electrolyte Interfacial Processes in Ionic Liquids and Sensor Applications

Xiangqun Zeng, Zhe Wang, and Abdul Rehman

## 2.1 Introduction

Electroanalytical methods or electrochemical sensors involve a group of quantitative and qualitative methods in which an electric excitation function is applied to an electrochemical cell and a response function is measured. Based on the properties of the applied excitation function, they are categorized as potentiometry, voltammetry, impedance spectroscopy, etc. All these methods require the use of electrodes where the electron-transfer reactions occur and an electrolyte, an ionically conducting medium, to transport charge within the electrochemical cells, to establish the electrochemical contact of all electrodes effectively, and to solubilize the reactants and products for efficient mass transport. Ionic liquids (ILs) are a class of compounds containing organic cations or anions that melt at or near room temperature. They represent a new type of nonaqueous and biphasic electrolytes that combine the benefits of both solid and liquid systems [1-7]. They are shown to have negligible vapor pressure, high ionic conductivity, wide potential window (up to 5.5 V), high heat capacity, and good chemical and electrochemical stability and have been demonstrated as media in electrochemical devices including super-capacitors, fuel cells, lithium batteries, photovoltaic cells, electrochemical and mechanical actuators, and in electroplating [8-10]. The liquid crystalline structure as well as the solvation properties of ILs has their own significance in many of these applications. In the past, ILs are regarded as completely nonvolatile, but the work of Earle et al. has shown that some ILs may be evaporated and recondensed [11]. However, generally speaking, most ILs have zero vapor pressure at room temperature; thus, there is no drying out of the electrolytes presenting many potential benefits for analytical methods and technique developments in comparison to traditional aqueous and nonaqueous electrolytes/solvents.

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It is well known that the maximum efficiency of electrochemical devices depends upon electrochemical thermodynamics, whereas real efficiency depends upon the electrode kinetics. To understand and control electrode reactions and the related parameters at an electrode and solution interface, a systematic study of the kinetics of electrode reactions is required. When ILs are used as solvents and electrolytes, many of the electrochemical processes will be different and some new electrochemical processes may also occur. For example, the properties of the electrode/electrolyte interface often dictate the sensitivity, specificity, stability, and response time, and thus the success or failure of the electrochemical detection technologies. The IL/electrode interface properties will determine many analytical parameters for sensor applications. Thus, the fundamentals of electrochemical processes in ILs need to be studied in order to have sensor developments as well as many other applications such as electrocatalysis, energy storage, and so on. Based on these insights, this chapter has been arranged into three parts: (1) Fundamentals of electrode/electrolyte interfacial processes in ILs; (2) Experimental techniques for the characterization of dynamic processes at the interface of electrodes and IL electrolytes; and (3) Sensors based on these unique electrode/IL interface properties. And in the end, we will summarize the future directions in fundamental and applied study of IL-electrode interface properties for sensor applications.

## 2.2 Fundamentals of Electrode/Electrolyte Interfacial Processes

Electroanalytical methods and electrochemical sensors are based on changes of electrode-electrolyte interface or the electrochemical reactions occurring at electrode/electrolyte interface for the detection of a specific analyte. The nature of electrode/electrolytic solution interfaces plays a central role in electrochemical surface science. A large number of important reactions take place at the interface between a metal and a solution: metal deposition and dissolution, electron- and proton-transfer reactions, corrosion, film formation, and electro-organic synthesis. If we want to understand and control these processes using ILs, it requires a detailed knowledge of the properties of the electrode/IL interface such as the adsorption of the ILs on electrode surfaces upon the variation of the electric potential, which acts as a driving force for all charge transfer reactions. As shown in Fig. 2.1, a study of electrochemical reaction at an electrode/solution interface is performed in an electrochemical cell. Typically, an electrochemical cell consists of three electrodes. The reference electrode establishes a constant electrical potential and the working electrode is where electrode reaction takes place. The electrical current is expected to flow between the working electrode and the auxiliary electrode, often also called the counter electrode. By holding certain variables of an electrochemical cell constant and applying an external electrical excitation function to the working electrode, information about the analyte can be obtained based on the measurement of how other variables change with the controlled variables. The common electrical



Fig. 2.1 Schematic of electrochemical cell containing the bulk electrolyte, interface and doublelayer regions. *CE* counter electrode, *RE* reference electrode, *WE* working electrode



Fig. 2.2 Schematic of electrode processes at IL/electrode interface (*left*) and interfacial structure (*right*) for the electrochemical sensors at IL modified electrodes

excitation parameters are potential, current, and charge. Electrode kinetics for any electrochemical reactions can be controlled by the electrical excitation parameters (e.g., potential). As shown in Fig. 2.2, the electrode reactions typically involve three major steps: (1) Mass transport step (diffusion, diffusion-convection, and migration); (2) Heterogeneous step (charge transfer, adsorption and desorption, nucleation, crystal growth, and surface diffusion); and (3) Homogeneous step (chemical reactions in solution). The rate of an electron-transfer reaction occurring at the electrode/solution interface mainly depends on the electrical potential. However, other

physical processes may also contribute to the overall kinetics of any particular reaction creating complex electrolysis mechanism. The overall reaction rate will be limited by the slowest step. In particular, the mass transport process (i.e., the transport of the reactant molecules to the electrode surface and the removal of the reaction products from electrode interface when formed) plays significant roles for the kinetics of electrode reactions. Chemical reactions at the electrode or in the solution also affect the mechanisms and kinetics of electrode reactions. The chemical reactions involved in electrolysis mechanisms are not only occurring in the homogenous solution phase (e.g., if the products of the electrode reactions are not chemically stable), but a significant range of heterogeneously coupled chemical reactions can also occur. Furthermore, the chemical processes that occur at electrode/electrolyte interface can also be coupled to mass transport. Finally, electrode materials and properties influence electrochemical reactions. For example, the surface area and the geometry of an electrode could influence the current and may also affect the mass transfer process, as in the case of a rotating disk electrode [12] and an ultramicro electrode [13]. Another area of electrode/electrolyte interface is that an electrode can be modified by the immobilization of a layer of material on to its surface so that the surface character of the immobilized material can control the electrode's performance and can be explored for a wide range of applications. The modified surfaces can offer novel properties such as the ability to hold charge (as in battery), induce novel specific reactions, and act as organic semiconductors or chemical/biosensors. The modification of the electrode greatly expands the application of electrochemistry [14–16] such as the enzyme electrodes that are widely used in biosensors and bio-electrochemistry. Thus, electrode-electrolyte interface processes can be complicated, and understanding these processes will enable the selection of the electrode potential, current density, solvent, supporting electrolyte, solution pH, temperature, deliberate modification of electrode surface or addition of other reagents, etc., based on the requirements of a specific application including sensors. Below we will detail the most important processes at electrode/electrolyte interface.

### 2.2.1 Adsorption

Electrode surface conditions such as roughness and modification are related with the electrochemical active sites and the properties of the electrode/electrolyte interface. Electrode surface conditions also include their single crystal faces. ILs contain organic cations or anions that could adsorb specifically or nonspecifically on the electrode surfaces. The adsorption of organic substances at an electrode/solution interface is of fundamental importance for many chemical and electrochemical processes. For example, adsorption can affect and change the electrode reaction kinetics. Molecules that exhibit structure-sensitive chemisorption are expected to undergo structure-sensitive electrocatalytic reactions. The adsorption of electrochemically active materials could change the peak shape, peak potential, and peak current of a cyclic voltammogram [17]. Depending upon the site of adsorption, electrochemically

active species can be oxidized at different potentials. More complicated adsorption mechanisms exist when surface adsorbed species are not stable in either its charged or uncharged forms, or if they are desorbed during potential cycling. An IL's tremendous diversity in structural and chemical properties will allow various electrode-IL interfaces to be designed to unravel the IL-IL and IL-electrode substrate interaction. Typically, in the case of chemisorptions, the dominant IL-electrode interaction will be due to strong covalent or ionic chemical forces; in the case of physisorption, one often finds that the van der Waals force acting directly between the adsorbates dominates. In this case, the optimum adsorbate-substrate bonding geometry can be overridden by the lateral adsorbate-adsorbate interactions, yielding, for example, incommensurate structures in which the overlayer and the substrate have independent lattices. The IL-IL interactions will include electrostatic interactions, hydrogen bond interactions, orbital-overlapping interactions, and van der Waals interactions. These interactions may be attractive or repulsive depending on the properties of IL and the substrate electrode. Adsorption phenomena in IL-electrode interface are important for understanding the structure of the electric double layer (EDL) and for their various electrochemical applications.

#### 2.2.2 Electrical Double Layer

The double-layer model is used to visualize the ionic environment in the vicinity of a charged surface which can be either a metal under potential control or a dielectric surface with ionic groups. It is easier to understand this model as a sequence of steps that would take place near the surface if its neutralizing ions were suddenly stripped away. The double layer formed, in turn, causes an electrokinetic potential between the surface and any point in the mass of the suspending liquid. This voltage difference is on the order of millivolts and is referred to as the often surface potential. The magnitude of the surface potential is related to the surface charge and the thickness of the double layer (Table 2.1).

Type of interaction	The energy equation	
Ion-dipole	$U_{\text{ion-solvent}} = -(ze\mu\cos\theta)/(4\pi\varepsilon_0)r^2$	
Dipole-dipole	$U_{\text{dipole-dipole}} = -(2\mu_1^2\mu_2^2)/(4\pi\varepsilon_0)3K_{\text{B}}Tr^6$	
Dipole-induced dipole	$U_{\text{dipole-induced dipole}} = -(\alpha_1 \mu_2^2 + \alpha_2 \mu_1^2)/(4\pi\varepsilon_0)r^6$	
Ion-induced dipole	$U_{\text{ion-induced dipole}} = -(z^2 e^2 \alpha)/(4\pi \varepsilon_0) 2r^4$	
Dispersion	$U_{\text{dispersion}} = -(3\alpha_1\alpha_2)(I_1I_2)/(I_1+I_2)2r^6$	

Table 2.1 The molecular interaction forces present in IL solvents

Symbols: *z*—the charge of the ion;  $\theta$ —the dipole angle relative the line joining the ion to the center of dipole; *e*—electric charge of  $-1.602 \times 10^{-19}$  coulomb; *I*—the ionization potential;  $\varepsilon_0$ —the vacuum permittivity; *r* is the separation distance between the charges; *q*—the charge (assuming equal value of charge on each side of the molecule);  $\alpha$ —polarizability of the solvents; *K*<sub>B</sub>—the Boltzmann constant; *T*—the absolute temperature;  $\mu_i$ —permanent dipole moment of solvent

ILs are free of solvents; thus, electrostatic interaction is the predominating force between the electrode and IL electrolyte. The electrode may have interactions with dipole moments of the anion and cation functional groups due to the bulky anions or cations of ILs. Even though the IL-electrode interface structure has some similarity to traditional electrode-electrolyte double layer, the IL-electrified metal interface behaves differently from those described by Gouy-Chapman-Sterns double-layer model. The study shows a well-defined structural organization of IL at Au(111) electrode interface with three structurally distinct regions: the interfacial (innermost) layer composed of ions in direct contact with the electrode; the transition region over which the pronounced interfacial layer structure decays to the bulk morphology; and the bulk liquid region where structure depends on the degree of ion amphiphilicity [18]. The innermost layer which templates ion arrangements in the transition zone is much more structured where the ions form a single layer at the surface to screen the electrode charge [19]. AFM results on gold and graphite in various ILs showed that the double layer at IL-electrified metal interface is not one layer thick, thereby extending the transition zone up to five ion pair diameters from the interface [20, 21]. In addition to the Coulombic short range electrostatic interaction, the ions in ILs are often large in size, flexible, highly polarizable, and chemically complex with a number of interionic forces (such as dispersion forces, dipole-dipole interaction, hydrogen bonding, and pi-stacking forces). Steric effects will contribute to the IL-electrode interface structure as well. Moreover, adsorptions of anions and/or cations are likely to occur at the IL-electrode interfaces. The specific adsorption, ion structures and properties, and the applied potential all influence the structure and thickness of the double layer of ILs near metal surface. For example, multiple sterically hindered allylic functional groups could be incorporated to minimize IL-electrode interactions and maximize compressibility of the solvation layers [22-24]. It was reported that the adsorption and dissolution of gas molecules in the IL-electrified metal interface can lead to the change of the doublelayer structure and thickness and the change of IL viscosity and the dielectric constant (i.e., less organized arrangement of ILs) [25, 26]. The molecular structure of ILs such as alkyl chain length influences the relative permittivity [27]. Capacitance at a fixed potential will depend on double-layer thickness and permittivity of the liquid at the interface. Consequently, varying the structure of IL anions or cations and applied potential can result in the rearrangement of ions and/or adsorbates that enables the modification of the double-layer structure at the IL-electrified metal interface (e.g., thickness and permittivity) [28-30] and subsequently the modification of the IL double-layer capacitance.

### 2.2.3 Chemical Reactions

An electron-transfer process at electrode/electrolyte interface can often have two types of chemical reactions. One is the electron-transfer reaction coupled with heterogeneous chemical reactions including those surface adsorption processes that occur at electrode/electrolyte interface. Another is the electron-transfer reactioncoupled homogeneous reactions such as EC reaction:  $(A+ne\leftrightarrow B; B \rightarrow product)$ , ECE reaction: (A+ne $\leftrightarrow$ B; B $\rightarrow$ C, C+ne $\leftrightarrow$ D), EC' mechanism (A+ne $\leftrightarrow$ B;  $B+Y \rightarrow A+$  product), where the prime (') represents a catalytic process. Among these coupled chemical reactions, catalytic reactions are widely sought after since they often represent a clean and efficient method of enhancing chemical reactivity. The reaction mechanisms change with the solvents. In ILs, the electrophilic (Lewis acid) organic ions can be reduced electrochemically at the cathode or chemically by reducing agents  $(O + e \rightarrow O^{-})$ . On the other hand, many of the nucleophilic (Lewis base) organic ions can be oxidized electrochemically at the anode or chemically by oxidizing agents  $(Q \rightarrow Q^{+} + e)$ . Here, Q<sup>-</sup> and Q<sup>+</sup> are radical anion and cation, respectively, and are extremely reactive if their charges are localized. However, if the charges are more or less delocalized, the radical ions are less reactive. The dynamic properties of ILs can have remarkable influences on the potentials of various types of redox couples and on the mechanisms of the electron-transfer processes that occur either heterogeneously at the electrode or homogeneously in the solution. For example, in high-permittive ILs, ILs can easily dissociate into ions. The anion or cation of ILs can form ion-pair complex with the radical cation or anion, respectively. With the decrease in permittivity of ILs, however, complete dissociation becomes difficult. Some part of the IL electrolyte remains undissociated and forms an ion pair  $(A^++B^-\leftrightarrow A^+B^-)$ . Ion pairs contribute neither ionic strength nor electric conductivity to the solution. Since there is high concentration of anion and cations in ILs, the formation of triple ions  $(A^+ + A^+B^- \leftrightarrow A^+B^-A^+)$  and quadruples can also occur. ILs could also play roles as proton donors to lower the energy needed to oxidize the electroactive materials. In summary, the study of redox processes in ILs can be very complex requiring the adaptation of a diverse range of electrochemical and spectroscopic tools to characterize their properties and mechanisms during electron-transfer processes at electrode/electrolyte interface.

## 2.3 Techniques for Studying Interfacial Properties in ILs

The interfacial properties of IL/electrode interfaces are different from other media (i.e., aqueous or traditional nonaqueous media) because of the unique properties of ILs, especially the electrochemical properties. To understand the electrode/electro-lyte interface chemistry for sensor research, the mechanisms of the electrochemical reactions, and the essential performance-limiting factors, both in the bulk and at the surface of the electrode materials need to be investigated, preferably in situ. In situ analysis is much desired due to the fact that ex situ measurements are usually not able to follow the fast kinetics at electrode interfaces. The past decades have been characterized by a spectacular development of in situ techniques for studying interfacial processes at metal electrodes. Radioactive tracer [31, 32], pulse potentiodynamic [33, 34], and galvanostatic methods [35] have been applied quantitatively to study the adsorption of organic compounds at solid metals. In the study of complex



Fig. 2.3 Methods for characterization of IL-electrode interface

electrode reactions, vibrational spectroscopies, such as Raman [36–40], the infrared (IR) [41–43], and UV–vis spectroscopies [44, 45], have been used to identify adsorbed intermediates and the nature of the chemisorption bond [46]. And the electroreflectance spectroscopies [47] have provided information about the orientation of molecules in adsorbed overlayers. X-ray absorption spectroscopies [48, 49] were employed to determine the coordination numbers of adsorbed species and the substrate–adsorbate and adsorbate–adsorbate bond lengths. Ab initio-based computations on the property of electrode materials and continuum modeling have been incorporated to provide theoretical insights and predictions [50, 51]. Finally, the images of adsorbate-covered electrode surfaces have been obtained using scanning tunneling [52–54] and atomic force microscopies [53, 55].

As shown in Fig. 2.3, many of these techniques have also been used to study the IL/electrode interface properties. Baldelli et al. studied the surface structure at the IL-electrified electrode interfaces by SFG [19, 56–58]. And Endres' group use ATM and SPM to investigate the IL interface morphology and interaction force [59, 60]. As expected, their studies show that the IL/Pt electrode interface has a very thin double-layer structure where the ions form a single layer at the surface to screen the electrode charge. However, it is difficult to obtain high-resolution AFM and SFG and to obtain the dynamics of the interfacial structure of IL real time. Difficulties also exist in how to interpret the AFM, electrochemical impedance spectroscopy (EIS), and SFG results. Additionally, these studies were limited to the non-Faradaic region of the electrode where there are no electron-transfer reactions to occur. Below we will illustrate the principles of electrochemical techniques as well as spectroelectrochemical and microscopic methods that have been used for in situ characterization of the electrochemical processes at IL-electrode interfaces. Combining complementary characterization methods in situ can provide mechanistic understanding of interfacial structure, interfacial dynamics, interfacial chemical composition, etc., and enable the development of new analytical methods based on IL chemistry for the identification and quantitative determination of analytes.

#### 2.3.1 Cyclic Voltammetry

Cyclic voltammetry (CV) is a widely used electrochemical technique to study electrochemical reaction mechanisms and the rates of oxidation and reduction processes. In CV, the current at the working electrode is plotted versus the applied potential to give the cyclic voltammogram traces of an analyte in solution. For studying an electrochemical process using CV, a stable supporting electrolyte and good solubility of analyte in the electrolyte is essential. ILs can offer benefits in both these aspects for CV characterizations. The solubility of the redox active materials in ILs would not be a problem due to the availability of a wide range of ILs with desired functionalities to choose from. ILs have high thermal stability. Most of ILs are stable up to 300 °C [61]. However, the electrochemical stability of an IL electrolyte is important for various electrochemical applications.

#### 2.3.1.1 Electrochemical Stability (Electrochemical Potential Window)

The electrochemical stability of nonaqueous electrolytes is crucial for any electrochemical application. The electrolyte must be electrochemically stable up to the high voltage cutoff (the highest voltage at which cell is allowed to operate), and stable down to the lowest voltage cutoff. Typically, electrochemical potential window lies at a voltage range in which the electrolyte is not oxidized or reduced. The electrochemical potential window is a measure of the electrochemical stability of an electrolyte against oxidation and reduction processes. This value, on one hand, characterizes the electrochemical stability of ILs, i.e., the limits of the potential window correspond to the oxidation limits and the reduction limits of the electrochemical decomposition of the involved ions. On the other hand, the width of the electrochemical window governs the range of potentials available for studying the electrochemical processes that will not be affected by the electrolytes and/or the solvents. One of the important considerations in electrochemical characterization of the potential window is the cell design and reference electrode. In order to avoid contamination to the IL electrolytes due to the reference electrode filling solution (e.g., KCl), a quasi-reference electrodes often used are rather than the saturated Ag/AgCl or calomel electrode. The quasireference electrode often used is Ag, Au, or Pt thin film or wire. The quasi-reference electrode and the auxiliary electrode are placed far apart so that the product at the counter electrode will not diffuse to the reference electrode which can affect its stability. Compared with different reference electrodes in the same IL system, the width of potential window should be consistent. The change of reference electrode materials only affects the absolute value of potential in most of IL systems. And all of them can be calibrated by using stable redox couple, such as Fc+/Fc. Thus, we can compare the potential windows reported using different quasi-reference electrodes.

The structures of ILs make them more electrochemically inert than other solvents such as  $H_2O$  and acetonitrile [62]. The electrochemical window in ILs is much larger than that of most conventional aqueous and nonaqueous electrolytes [63].

RTIL	Potential window (vs. Fc <sup>+</sup> /Fc, ±0.2 V)
[C <sub>2</sub> mim][NTf <sub>2</sub> ]	-2.6 to 3.0 V
[C <sub>4</sub> mim] [CF <sub>3</sub> SO <sub>3</sub> ]	-2.6 to 2.2 V
$[C_4 mim][BF_4]$	-2.8 to 3.2 V
[C <sub>4</sub> mim][PF <sub>6</sub> ]	-2.5 to 3.0 V
[C <sub>4</sub> mim][HSO <sub>4</sub> ]	-2.5 to 3.0 V
[C <sub>4</sub> mim][Cl]	-2.5 to 1.5 V
[C <sub>4</sub> mim][NO <sub>3</sub> ]	-2.5 to 2.0 V
$[P_{4,4,4,4}][NO_3]$	-2.3 to 2.0 V
[N <sub>4,4,4,4</sub> ][NO <sub>3</sub> ]	-3.5 to 2.0 V
$[N_{6,2,2,2}][NTf_2]$	-3.5 to 3.0 V
$[P_{14,6,6,6}][NTf_2]$	-3.4 to 3.0 V
$[P_{14,6,6,6}][FAP]$	-3.5 to 3.0 V
$[C_4mPy][NTf_2]$	-3.2 to 3.0 V

Table 2.2	Potential	windows
of commo	n RTILs	

Table 2.2 lists the potential windows of some commercial ILs, obtained from references [64–67] and also from our own investigations. Here, the purities of all ILs are higher than 95 %. The electrochemical stability of ILs with cations of either quaternary ammonium structures or pyrrolidinium is better than that of imidazolium. However, anion stability is an issue. Halides can be easily oxidized; thus, halidesbased ILs have lower electrochemical stabilities. Additionally, the high chemical activity of halides may result in side reactions during the analyte redox process. The fluorine-containing anions  $(BF_4^- \text{ and } PF_6^-)$  are not as stable and can be decomposed in the presence of trace amounts of water producing HF under electrochemical process, although this reaction usually isn't observable during electrochemical study for short time testing, since both B-F and P-F bonds are weaker than C-F bond [68]. Additionally, for most organic anions, the negative charge is delocalized which increases their stability. It denotes that the electrochemical potential window is sensitive to impurities. Schröder and coworkers have reported that ILs such as [C<sub>4</sub>mim] [BF<sub>4</sub>] can rapidly absorb atmospheric water and that the presence of water has a profound effect on cyclic voltammetric experiments with platinum electrodes [69–71]. Any other impurities such as moisture residues from preparation could give an electrochemical signal during CV characterization. Since the purity of ILs affects the accuracy of the potential window measurement, the potential window obtained experimentally can be regarded to have some uncertainty. Theoretically potential window of ILs was basically dominated by the stability of ions. A general trend for the magnitude of the electrochemical oxidative limit is observed as follows:  $[P_{14,6,6,6}]^+ > [N_{6,2,2,2}]^+ > [C_n mim]^+ \approx [C_4 mPy]^+$  and  $[FAP]^- \approx [NTf_2]^- > [BF_4]^- >$  $[PF_6]^{-}>[MeSO_4]^{-}>[NO_3]^{-}>[CF_3SO_3]^{-}$  [61, 62]. The anodic "breakdown" is presumed to be due to the oxidation of the anionic component of the ILs. In most cases, the stability of the anion determines the anodic potential limits, and stability of the cation determines the cathodic potential limits. But in the practical measurement, the predicted values depend also on the electrode material and current density.

#### 2.3.1.2 Mass Transport

The mass transport of electroactive species plays significant roles in electrode kinetics. The electroactive species can move by diffusion, convection, and migration. The measured mass transport is a combination of these three processes:

- 1. Migration: movement of charged species under the influence of an electric field.
- 2. Diffusion: movement of species because of their concentration gradient.
- 3. Convection: movement of species under the influence of a physical disturbance.

Typically, the contribution of the charged electroactive species which is often in very low concentration to migration process is much smaller than the contribution of inert electrolyte. In conventional electrolyte solutions, ions exist in the form of solvent complexes, and consequently, the solvent molecules are parts of moving ions. As a result, in addition to the flux of ions, there is also a flux of the solvent. This flux leads to the formation of a concentration gradient between the cathodic and anodic compartments during the electrochemical reaction. In the ILs, there is no solvent. ILs can be considered as an excess of inert ions carrying the current; thus, migration of electroactive species can be neglected. In an IL electrolyte, the ionic conduction is related to both the anion and the cation mobility and their transference number. The total cation and anion transference numbers is equal to unity.

$$t_{+} + t_{-} = 1$$
 (2.1)

where  $t_+$  and  $t_-$  are the transference numbers, depicting the portion of charge carried by cations or anions, respectively. Since ILs have much higher viscosities than common electrochemical supporting electrolytes, they have an effect on the diffusion coefficients of species. A previously reported study compares the diffusion coefficients of a neutral molecule and the radical cation produced after an electrochemical reaction in an IL and acetonitrile. The diffusion coefficient of the cation radical was consistently about half that of the value of the neutral molecule. In contrast, in acetonitrile, the ratio of the diffusion coefficients was nearly 60 % or higher [72], providing an indication that viscosity and charge have considerable effects on the transport of diffusing species in ILs [73–75]. We can consider that mass transport is mainly governed by the diffusion process. In this case, the diffusion coefficients, for both the reduced and oxidized forms of the redox species, can be calculated from the slope of the dependence of the peak current  $i_p$  on the square root of the scan rate, according to the Randles–Sevcik equation [76]:

$$i_{\rm p} = 0.446 n F A \left(\frac{nF}{RT}\right)^{1/2} C D^{1/2} v^{1/2}$$
 (2.2)

The Stokes–Einstein equation [77] is generally applicable for molecular liquids and ILs, at least semi-quantitatively, for analyzing the diffusion coefficient D. Water is ubiquitous in the environment. It was shown that water induced accelerated ion diffusion compared to its effect on neutral species in ionic liquids [78]. We also observed that IL conductivity is significantly increased when [Bmim][BF<sub>4</sub>] is

exposed to normal atmosphere for 24 h with 0.25 % wt moisture since fewer cycles are needed to reach a fully conductive polyvinyl ferrocene film [79]. Because of its high molecular weight, the diffusion coefficient of an IL is typically smaller than that of analytes regardless of the medium. However, despite the presence of an additional interaction between the functional group in IL and analytes, this behavior contrasts with the case of a small anion or radical anion; ion-pair formation leads to a marked decrease in the diffusion coefficient.

#### 2.3.1.3 Charging Current in CV

As mentioned before, ILs have a unique double-layer structure, and the doublelayer capacitance can be measured by both cyclic voltammetry and EIS. Our studies and others have shown that the capacitance of IL/electrode interface is potential dependent, and the adsorption of gas on the IL/electrode interface will decrease the double-layer capacitance under a specific DC bias potential [80]. In contrast to the EDL typically observed in dilute aqueous or nonaqueous electrolytes, the ions of ILs are strongly oriented near the electrode into an ordered layer structure with local ion density at maximum possible value [81, 82]. Multiple ion pair layers form at the interface of IL and metal electrode. Due to this heterogeneity, the lattice formation at the interface and the subsequent capacitance variations are not monotonic as described by the Gouy-Chapman-Stern's model [83-85]. Additionally, the hysteresis effects of an IL, where the double-layer capacitance depends on the scan direction of the DC potential, contribute to the slow pseudocapacitive process at the IL-electrode interface [86-88]. Since the change of IL orientation due to applied potential is a very slow process, the resulted charging currents only can be observed at a slow scan rate. Figure 2.4 shows that the small CV peaks related to heterogeneous IL orientations were observed in CV at slow scan rates (e.g., 20 mV/s) in the most of studied ILs. These small peaks will contribute to some uncertainty for the current measured, especially for the Faradaic process, under slow scan rates. Consequently, the double-layer charging current will increase the complexity of CV results. In order to obtain accurate Faradaic current measurement, it is recommended that the peak current of electrochemical processes should be measured under the high scan rate in CV study. The double-layer capacitance measured under this condition can be considered the average capacitance instead of the potential-dependent value.

#### 2.3.1.4 Scan Rate Effects on the IL Double-Layer Charging Currents

In an EC redox process, the Faradaic current depends on the concentration of the analyte and increases monotonically with analyte concentrations. Numerous studies by others and our lab show that the structure and dynamics of the electrochemical double layer in room temperature of ILs are very different from the traditional



**Fig. 2.4** CV of [C<sub>4</sub>mPy][NTf<sub>2</sub>] at 20 mv/s on Pt under air condition. The small peaks (*red circles*) are presenting charging current by the IL orientation during the potential scanning

aqueous and nonaqueous electrolytes. For example, in two separated studies, Gore and Druschler et al. [86, 89] have reported the hysteresis effects in the potential-dependent double-layer capacitance of room temperature ionic liquids at either a Pt electrode or a gold electrode. They explained this hysteresis effect due to the slow pseudocapacitive processes in a frequency range below 10 Hz. We have also observed a similar behavior in our study [90]. It is well known that the first potential cycle is critical to target analyte concentration profile for a Faradaic process in aqueous solutions. However, it is unpredictable in ionic liquid since its pseudocapacitance is scan rate related, and thus the value is highly dependent on the potential and the history of electrode conditions in the IL [91–93]. Currently, there is no method that can obtain the accurate value of pseudocapacitance in an IL consistently. As we know, increasing the scan rate in cyclic voltammetry allows one to decrease the thickness of the diffusion layer, and the pseudocapacitive process caused by the slow orientation of the IL will be negligible. Thus, the hysteresis of the IL double layer will be minimized using higher scan rate. This can help to obtain the reproducible and accurate current values for sensor application. High scan rate could facilitate a steady state of the IL-electrode double layer to be established during the multiple potential cycling. As shown in Fig. 2.5, for the methane-oxygen system [94], the difference of peak currents of methane oxidation (0.9 V) and oxygen redox (-1.2 V/0.9 V) processes in the 6th cycle and 20th cycle at 500 mV/s, is less than 0.2 µA, confirming that the methane and oxygen concentration profile in ionic liquid is reproducible and the double-layer charging current is relatively constant. Thus, electrochemical measurements based on redox processes in IL should be characterized at the high scan rate, and peak current of first cycle should not be used for the analyte quantification.



Fig. 2.5 Cyclic voltammograms of 5 % methane and dry air in [C<sub>4</sub>mPy][NTf<sub>2</sub>] (500 mV/s scan rate)

#### 2.3.1.5 Electrolyte Conductivity

Compared to the conventional aqueous electrolyte, the conductivity of the ILs is at least one order of magnitude smaller. In contrast to the conventional aqueous electrolyte, the higher the concentration of the ILs, the smaller the conductivity of the solution due to their high viscosity. This is expected. At high salt concentrations, all solvent molecules are called "solvent in salt solution," in which the ions primary shell is more complex, and the resulting system shows different properties at the low concentration salt solution [95–97]. In such a case, the conductivity increases with the increasing amount of salt, goes through a maximum, and decreases with a further increase of the salt concentration. However, most of the molecular liquids have relatively low viscosity, and therefore, the dilution of the viscous neat IL with molecular diluents decreases the viscosity of the mixture [98]. Table 2.3 lists the dynamic viscosity ( $\eta$ ) and specific conductivity ( $\kappa$ ) values of common solvents and RTILs [66, 99]. In an IL system, the solution resistance  $(R_{\rm u})$  is high due to higher viscosity and slow ion mobility of ILs. Typically, the solution resistance was calculated from conductivity of the ILs and electrode geometry. In most ILs, the dynamic voltage drop (IR-drop) would not be negligible and can affect the accuracy of the applied electrode potential. The IR-drop is the voltage loss (drop) when current flows through a resistor. IR-drop occurs in most of the electrical circuits and electrochemical systems. In ILs, the solution resistance  $R_u$  could be measured by both AC and DC techniques. In most electrochemical systems, IR-drop could be estimated to be lower than 10 mV. However, in some high capacitance systems and high Faradaic current systems, such as supercapacitor and fuel cell, IR-drop is significant. Although many commercial electrochemical instruments have the capability to compensate IR-drop, it still has to be considered in some analysis of an electrochemical process [100, 101].
	Viscosity	Conductivity
Solvents	(cP)	(mS/cm)
N,N-Dimethylformamide	0.794	4.0ª
Acetonitrile	0.345	7.6ª
Ethanol	1.074	0.6ª
Dimethylsulfoxide	1.987	2.7ª
[C <sub>2</sub> mim][NTf <sub>2</sub> ]	28	8.4
[C <sub>4</sub> mim][NTf <sub>2</sub> ]	44	3.9 <sup>b</sup>
[C <sub>6</sub> mim][NTf <sub>2</sub> ]	59	
[C <sub>8</sub> mim][NTf <sub>2</sub> ]	74	
[C <sub>2</sub> mim][BF <sub>4</sub> ]	43	13.0
[C <sub>2</sub> mim][PF <sub>6</sub> ]		5.2
[C <sub>4</sub> mim][PF <sub>6</sub> ]	275	1.5
[N <sub>6,2,2,2</sub> ][NTf <sub>2</sub> ]	167	0.67
$[N_{6,4,4,4}][NTf_2]$	595	0.16
[C <sub>3</sub> mPy][NTf <sub>2</sub> ]	63	1.4
[C <sub>4</sub> mPy][NTf <sub>2</sub> ]	85	2.2

Unless otherwise stated, T=25 °C <sup>a</sup>Conductivity for organic solvent containing 0.1 M tetrabutylammonium perchlorate at 22 °C <sup>b</sup>20 °C

# 2.3.2 Potential-Step Methods (Chronoamperometry)

Potential-step method is an electrochemical technique in which the potential of the working electrode is either held at constant or stepped to a predetermined value, and the resulting current due to Faradaic processes and double-layer charging processes occurring at the electrode (caused by the potential step) is monitored as a function of time. Especially for practical electrochemical sensor in real-world application, chronoamperometry is preferred due to its simplicity and low cost of instrumentation. Besides its wide use in most electrochemical sensor systems, chronoamperometry has been used in the understanding of the kinetics of the electrochemical processes as well.

#### 2.3.2.1 Kinetics Study for Electrochemical Process

Chronoamperometry was used to determine the electron-transfer kinetics and it could provide information regarding the dynamic model of an electrochemical process. In chronoamperometry, the current is integrated over relatively long time intervals; thus, it gives a better signal to noise ratio in comparison to other voltammetric techniques. The Faradaic current, which is due to electron-transfer events and is most often the current component of interest, decays as described by the Cottrell equation [77] in planar electrodes.

$$i(t) = id(t) = \frac{nFAD_{\rm O}^{1/2}C_{\rm O}^*}{\pi^{1/2}t^{1/2}}$$
(2.3)

In most electrochemical cells, the decay of Faradaic current vs. time is much slower than that of double-layer charging current; however, electrochemical systems with no supporting electrolytes are notable exceptions. ILs are more viscous than traditional organic solvents, thus slowing the diffusion of the electroactive species leads to transient behaviors. While the current behavior in the ILs system could be interpreted using the continuum model, it was recognized that the mechanisms by which an IL-electrode interface responds to an applied electrical field are quite different from a traditional, polar solvent. In the latter, solvent molecules re-orientate, whereas in an IL the molecules must move relative to each other. These differences must impact upon the overall observed rate of electron transfer, even if the free energies of activation are similar. That is, while inner-sphere electrontransfer rates might be expected to be very similar in ILs compared to polar organic solvents, outer-sphere electron transfers will be very different due to the screening response mechanisms [102, 103]. In order to possibly minimize the effect of "IR drop" and "capacitive charging" on the estimation of the heterogeneous electrontransfer rate constant, the microelectrode, scanning electrochemical microscopy (SECM), and other techniques have been used in many investigations by Mirkin, Bard, and Compton [104–107].

#### 2.3.2.2 Faradaic Current Determination

Chronoamperometry (or potential step) can be regarded as an extreme fast potential sweep of CV which is especially beneficial for the practical IL-based sensor development due to its unique double-layer structure as discussed in the earlier section. However, as with all pulsed voltammetric techniques, chronoamperometry generates high charging currents, which decay exponentially with time as in any Randles circuit. As shown in our early work [90], the time-dependent oxygen reduction currents, i(t), in ILs, can be described as the sum of the Faradaic current for EC reaction,  $i_f$ , and the double-layer charging current,  $i_c$ , on the electrode as shown in Eq. (2.4):

$$i(t) = i_{\rm f} + i_{\rm c} = i_{\infty} + \frac{C_{\rm dl} dV_{\rm dl}}{dt} + \frac{C_{\rm bulk} dV_{\rm bulk}}{dt}$$
(2.4)

In this expression, *C* and *V* represent capacitance and electrode potential, with "dl" and "bulk" denoting double layer and bulk solution, respectively. The Faradaic current (e.g., due to oxygen reduction) ordinarily decays much more slowly than the charging current (cells with no supporting electrolyte are notable exceptions). Typically the cell time constant  $\tau = R_u C_d$ , where  $R_u$  is the uncompensated resistance and  $C_d$  is the double-layer capacitance, is very useful to determine the timescale of



Fig. 2.6 Potential step experiment from 0 V to -1.2 V at 100 % air in three ILs. Time constant  $\tau$ =6 s and 50 $\tau$  is about 300 s

a potential step method. As such, it is important that analysis is applied over a sufficiently broad time interval in order to assure the reliability of the results. The charging current can be considered insignificant when current is sampled at times exceeding  $5R_{\mu}C_{d}$ . As shown in Fig. 2.6, the time constant obtained from potential step experiment (step from 0.0 V to -1.2 V in 100 % air) is  $\tau = 6$  seconds (the time required for current decays to 37 % maximum current). Thus, in order to minimize the large double-layer charging current of IL, we measured the current at the 300th second which is  $50\tau$ . The current can be mainly attributed to the Faradaic current of oxygen reduction, and the double-layer charging current is negligible after 300 s, which is much longer than that in aqueous electrolytes (lower than few seconds). And the double-layer capacitance is also potential-dependent [80], because under different potentials the orientations of IL are different and the values of relative capacitances vary as well. Thus, cell time constant  $\tau$  is not a constant and varies in different systems. The value of  $\tau$  is related to the IL structure. Thus, chronoamperometry is not an efficient method to study the dynamic interfacial process in an IL system. For practical electrochemical applications, the significant conditioning process or preconditioning step (>50 $\tau$ ) is required to establish a constant ILelectrode interfacial boundary layers. Obviously, in different ionic liquids, the interface relaxation processes due to potential step vary and these processes have not been fully investigated so far.

# 2.3.3 Electrochemical Impedance Spectroscopy

In CV and potential step, the electrode surface reaction is studied through large perturbation on the system to drive the electrode to a condition far from equilibrium and observe the response. Typically in EIS, the electrochemical reaction is perturbed with an alternating signal (e.g., potential) of small magnitude and the way in which the system follows the perturbation in steady states is measured. The use of low amplitude perturbation in EIS allows the application of a linear model to interpret the results which can yield useful information about the physicochemical properties of the system. Analysis is generally carried out in the frequency domain, although measurements are sometimes made in the time domain and then Fourier transformed to the frequency domain. For the analytical application, EIS is a powerful, informative, and noninvasive method, which can be used to study the interfacial events and trace the blocking behaviors (as complexation and adsorption) or diffusion effects at modified electrodes and serve as a transducer [108], especially in the electrochemical system. EIS has been used to measure the resistance of an electrolyte solution, grain boundary resistance, and interfacial capacitance. The Nyquist plot ( $Z_{im}$  vs.  $Z_{Re}$ ) at high frequency (near 100 kHz) is determined by the solution resistance ( $R_s$ ) and the electrode capacitance. However, for a specific electrochemical process and physical status, EIS is by no means limited to the measurement and the analysis of data at the impedance level (e.g., impedance vs. frequency) but may involve any of the four basic immittance levels; thus, most generally, IS stands for immittance spectroscopy. The signal of the whole system can be equivalent to a combination of certain electric components described by an "equivalent circuit."

#### 2.3.3.1 Randles Circuit

An ideal electrode–electrolyte interface with an electron-transfer process can be described using Randle equivalent circuit shown in Fig. 2.7. The Faradaic electron-transfer reaction is represented by a charge transfer resistance  $R_{ct}$ , and the mass transfer of the electroactive species is described by Warburg element (*W*). The electrolyte resistance  $R_s$  is in series with the parallel combination of the double-layer capacitance  $C_{dl}$  and an impedance of a Faradaic reaction. However, in practical application, the impedance results for a solid electrode/electrolyte interface often reveal a frequency dispersion that cannot be described by simple Randle circuit and simple electronic components. The interaction of each component in an electrochemical system contributes to the complexity of final impedance spectroscopy results. The EIS results often consist of resistive, capacitive, and inductive components, and all of them can be influenced by analytes and their local environment, corresponding to solvent, electrolyte, electrode condition, and other possible electrochemically active species. It is important to characterize the electrode/electrolyte interface properties by EIS for their real-world applications in sensors and energy storage applications.

Fig. 2.7 The typical Randle's circuit



#### 2.3.3.2 Proposed Equivalent Circuit in ILs

The typical IL system could be considered as a solvent-free system, in which it can simplify the EIS analysis significantly which spurs its wide use in the characterization of the IL–electrode interface. However, due to low mobility of ions in an IL and multiple molecular interactions present in an IL, more time is needed to reach to a steady state of IL–electrode interface structure and arrangement, when a potential is applied. Furthermore, the electron-transfer process in ILs is different from that in traditional solvents containing electrolytes. Thus, the interfacial structures of IL are more complex than other systems. Even the electrode geometry could affect the EIS results of IL systems. It is noted that the bulk ILs could not be simply described by a resistor ( $R_s$ ) as in classic electrochemical systems. And the electrode double layer in IL electrolyte couldn't be simply depicted as a capacitor. So the Randle equivalent circuit is not sufficient to describe an IL system. Significant efforts have been made to illustrate the properties of diffusion layer and the bulk ILs with equivalent circuits. However, currently there is no general equivalent circuit model to describe the interface of an IL system.

### 2.3.3.3 EIS Measurement in IL

For practical EIS characterization of IL system, the purity of IL used, the hysteresis effect of IL, and the different experimental measurement conditions can all contribute to the variability of EIS results. Thus, for the EIS measurement: (1) A significant conditioning time for IL–electrode interface is required to minimize the hysteresis effect so that the interfacial boundary layer of IL is at a steady state for each measurement; (2) The electric field applied to the working electrode should be parallel. For sensor applications, the field effect transistor electrode structure in which the voltage applied across the gate and source terminals or the interdigited electrode structure is considered as better electrode designs for IL system using EIS testing. Additionally, EIS has the ability to monitor the ion movement and orientation in real time. However, the presence of the Faradaic process increases the complexity of results; because of the large capacitance of double layer, it is hard to analyze the contributions due to electron-transfer process or the charge transfer processes based only on impedance result. Combining impedance with spectroscopic methods is often used to obtain conclusive results.

# 2.3.4 Infrared Spectroscopy

Spectrometric methods are based on the interactions of electromagnetic radiations with the atomic and molecular species. Among them, IR spectroscopy (with wave-numbers ranging from about 12,800 to  $10 \text{ cm}^{-1}$  or wavelengths from 0.78 to  $100 \text{ }\mu\text{m}$ ) is mostly used to obtain structural information about the molecular species.

IR absorption, emission, and reflection spectra for molecular species either in solid, liquid, or gas phases arise mostly from various changes in energy due to transitions of molecules from one vibrational or rotational energy state to another. The frequency or wavelength of this energy transition is characteristic of the specific chemical bond vibration and/or rotation in the molecule which are determined by the molecular structure, the masses of the atoms, and the associated vibrational energy coupling. Attenuated total reflectance (ATR) and reflection-mode of IR in conjunction with electrochemical methods allow samples to be examined directly in the solid or liquid state without further preparation and are widely used in the characterization of electrode–electrolyte interface properties. Most of ILs are IR-active molecules. Since ILs are stable and chemically inert, the IR characterization can be easily performed on the IL-based system directly.

### 2.3.4.1 IR Signal from IL

ILs have negligible vapor pressure making them not volatile, and this property permits in situ IR characterization of IL systems at various timescales without considering solvent loss generated uncertainties. High solubility of analytes in the ILs enables accurate characterization of their IR spectra in ILs. On one hand, the usage of ILs can eliminate the effect of water, and on the other hand, the signal from IL functional group can complicate the interpretation of Fourier transform infrared spectroscopy (FTIR) results. For example, hydrogen bonding is barely present in highly hydrophobic ILs, and as a result, the relative band shifts caused by the hydrogen bonding are negligible when analyzing the IR results in ILs [100, 109–111]. For those high purity IL systems, the IR spectra could be considered as the sum of the spectra of anion and cation and other species. Most of the methods used for studying the traditional ionic compounds such as ionic melts can be applied to the study of ILs. It is also noted that the IR response in liquid states of IL is different from the one obtained in a crystalline IL, predominantly because of lower energy conformations of the molecules in liquid states. For example, the IR spectra of  $[NTf_2]^-$  in crystalline  $[C_4mim][NTf_2]$  shows intensive bands at 649 and  $\sim$ 600 cm<sup>-1</sup> (Fig. 2.8). Therefore, one may conclude that the anion is in *cis* conformation in this crystal. Furthermore, the intensity of both bands gradually decreases in the premelting region due to the predominance of the *trans* conformation in the liquid state. But they are still detectable [112–115]. Those conformation differences are present in the fingerprint region of IR (under 1,000 cm<sup>-1</sup>), whereas most variability comes from anions. [NTf<sub>2</sub>]<sup>-</sup> has O=S=O (1,100 cm<sup>-1</sup> and 1,400 cm<sup>-1</sup>) and C-F bonding (1,000 cm<sup>-1</sup>) [112–115]. B-F of BF<sub>4</sub> is located at 924 cm<sup>-1</sup> and 1,312 cm<sup>-1</sup>, and P–F of PF<sub>6</sub> is about 843 cm<sup>-1</sup> [116–119]. For cations, the bands are located in the rest of the regions and address the IL structure, such as C-C (around 1,450 cm<sup>-1</sup>), C=C (around 1,600 cm<sup>-1</sup>), and C-N bonding (around 1,450 cm<sup>-1</sup>). Only C-H bonds around 3,000 cm<sup>-1</sup> and 1,200 cm<sup>-1</sup> are highly sensitive to their chemical environment. Typically, the addition of an analyte will change the C-H vibration and hydrogen bonding as well (Fig. 2.8).



Fig. 2.8 FTIR spectra of [C<sub>4</sub>mim][NTf<sub>2</sub>] under a nitrogen atmosphere

Table 2.4 Main IR bands   (cm <sup>-1</sup> ) assigned C–H in ILs	Wavelength of the band (cm <sup>-1</sup> )	Vibration
	3171, 3124	$\nu$ (C–H) aromatic, strong
	2933, 2939, 2878	$\nu$ (C–H) aliphatic, strong
	1575, 1467	v(ring), strong, sym
	1431, 1386	MeC-H, asym
	1170	Ring, strong, sym

A comparison of IR spectra of acidic and basic ILs reveals only a small distortion of the aromatic ring, which is not of such extent as in the case of a salt with a smaller cation. This means that the hydrogen bond between the hydrogen on the carbon atom and a chloride ion is very weak or absent. This kind of bond is seen in the case of [C<sub>4</sub>mim][Cl], where there is a band at 3,088 cm<sup>-1</sup>, and the peaks at 3,100 cm<sup>-1</sup> are considerably smaller [120–123]. The weak absorption from 2,500 cm<sup>-1</sup> to 2,850 cm<sup>-1</sup> may be attributed to the formation of hydrogen bonds between the aromatic protons and the halide ions. In basic ILs, the extent of hydrogen bond acceptor Cl<sup>-</sup> is limited. Hydrogen bonds are weak or even not present. Other anions such as  $[PF_6]^-$ ,  $[BF_4]^-$ , and [NTf<sub>2</sub>]<sup>-</sup> are weakly complexing anions and not expected to participate in strong hydrogen bonding. Indeed, even [C<sub>4</sub>mim][PF<sub>6</sub>] shows no hydrogen bonding bands in the region 3,000–3,100 cm<sup>-1</sup> where C-H...Cl<sup>-</sup> interactions on imidazolium chloride were observed previously. Therefore, IR results are consistent with a lack of hydrogen bonding within weakly complexing anions [124]. This means that cation-anion coulombic attraction is driving the overall structure, with local steric effects influencing the final orientation of ions. Table 2.4 lists the IR response of C–H bond in ILs [112–119].

#### 2.3.4.2 Effects on Dissolved Analytes (Peak Position and Width)

ILs could provide a highly purified environment to monitor the interface reactions, and the species of interests can be localized near the interface because of the high viscosity of the ILs. Both these effects can enhance the observed IR signals. The p-type polarized IR is considered best as the light source for measuring IR-active species through bulk IL. However, typically the strength of signals is attenuated due to the long optical path in ILs.

Inorganic ILs such as the halogen salts of alkali metals provides strong ionic environment. The strong interaction between the analyte and the salt is manifested by peak shift from its position in gaseous state or liquid state of itself. For example,  $\nu_3$  of CO<sub>2</sub> was found with about 150 cm<sup>-1</sup> shift from its position in gaseous state. The shift of  $\nu_2$  of CO<sub>2</sub> is about 40 cm<sup>-1</sup> confirming this fact [125–128]. In an organicbased IL, this effect is not that strong. The position of this band for CO<sub>2</sub> dissolved in IL is very close to that of CO<sub>2</sub> dissolved in glassy polymers, such as poly(methyl methacrylate) (PMMA). The blue-shift is lower than 30 cm<sup>-1</sup> [129–132]. However for H<sub>2</sub>O the polar molecule structure and hydrogen bonding make this effect amplified. The presence of two bands corresponding to the antisymmetric and symmetric stretching modes of water indicated that molecules of water are present in the "free" (not self-aggregated) state bound to the basic anion via H-bonding [133–135]. The blue-shift of the antisymmetric stretching band has been used to correlate the relative strength of the interaction between water and RTILs with different anions. The strength of H-bonding increases in the order  $[PF_6] < [SbF_6] < [BF_4] < [CIO_4] < [CF_3S]$  $O_3$  < [NO<sub>3</sub>] < [CF<sub>3</sub>CO<sub>2</sub>] [110, 111, 136–139].

Another effect is on the IR peak width of the analyte. Since most of the anions in IL are Lewis acids, the IR signal of dissolved analyte could be increased by the interaction. For example, the anions could act as weak Lewis bases, and CO<sub>2</sub> appears to be a useful probe to sense the extent of their basicity. The width of the  $\nu_2$  mode, measured as an effective average width of the split band (the average width represents the width of the doublet at the half maximum of the absorbance), is an estimate of the strength of the interaction of CO<sub>2</sub> with the Lewis bases: the width increases with the increase of the strength of the interaction [113, 130, 140]. This could also be a result of the strength of interaction decreasing with the increase of anion size. Thus, the strength of these interactions cannot be solely responsible for the solubility of CO<sub>2</sub> in these ILs, and, presumably, a free volume contribution in the IL plays a significant role. The strength of anion–cation interaction in the IL affects the available free volume, and one would anticipate that a weaker interacting anion leads to more free volume being available. It makes the result more complex.

#### 2.3.4.3 Interface Signal

For the study of electrochemical processes, the interfacial information is even more important. However, due to the strong bulk absorption of IL, the transmission mode was limited to the electrode design. Using ATR mode may partially eliminate

interference from ILs, ATR-IR spectroscopy overcomes some of the limitations inherent to other techniques when the objective is to gain spectra of molecules dissolved in highly absorbing media. And also the interface information could be collected using the reflection mode as well. But the IR signal is limited by the thickness of the liquid film. The signal/noise ratio is another issue that should be considered. Typically, these methods are limited to verify the products during the electrochemical processes and are not able to provide the information regarding interfacial structure and dynamics. To understand the dynamical electrochemical process in IL and to obtain detailed molecular level information on the interface, the surface-enhanced spectroscopic techniques have to be applied since the bulk adsorption of IL is relatively strong. Among many surface enhanced spectroscopy techniques, SFG has been explored to characterize the electrode-IL interface. The nonlinear laser spectroscopy SFG method has long been recognized as an important tool for deducing the composition, orientation distributions, and some structural information of molecules at gas-solid, gas-liquid, and liquid-solid interfaces without interference from the bulk electrolyte. Thus, the interface is probed in situ, while the electrode potential is changed. Currently, SFG is the most efficient method to directly obtain the interfacial structure from the electrode surface.

SFG measurements of metal/aqueous electrode surfaces have been conducted on Au, Ag, and Pt electrode surfaces. The most extensive studies have been conducted with platinum single-crystalline and polycrystalline surfaces [141–143]. Using a free electron laser, Guyot-Sionnest and Tadjeddine demonstrated the first use of Vibrational Sum Frequency Spectroscopy (VSFS) to study ionic adsorption at an electrified metal/aqueous electrolyte interface [144–146]. Conboy et al. used it to determine the orientation of the imidazolium cation at the RTIL/SiO<sub>2</sub> interface, as well as the structure of the interfacial water molecules [147–149]. Baldelli et al. extended it to investigate the metal/IL interface. It provides solid evidences on the potential-dependant double layer of IL [19, 150]. SFG could determine the ion's location and orientations on the metal surface under variable applied potential via measuring the tilt of the terminal alkyl  $-CH_3$  group on the cation. The results can be compared with those in situ EIS results to obtain an in-depth understanding of IL/solid interface [151, 152].

## 2.3.5 In Situ EQCM Methods

Electrochemical quartz crystal microbalance (EQCM) is a powerful analytical technique for probing electrode–electrolyte interfacial processes by using a quartz crystal electrode. Figure 2.9 shows an integrated EQCM electrode fabricated on a monolithic quartz wafer. AT-cut quartz crystals oscillating in a shear thickness mode exhibit extraordinary high sensitivity to potential-induced changes in the mass at electrode–electrolyte interface via the change of its resonance frequency. In addition to that, the monitoring of the mechanical state of the viscoelastic coatings at a quartz crystal electrode via a change in their shear storage and loss modulus is



**Fig. 2.9** Demonstration of the microfabrication of EIS–QCM electrode chip that was made on a 10 MHz AT cut quartz crystal formed EIS. It has a 2.5 mm disk-working electrode on both sides of 10 MHz AT cut quartz. Ring-shaped counterelectrodes (CE) and quasi-reference electrodes (QRE) are patterned around the circular working electrodes on one side and narrow gaps between disk and ring electrodes to support EIS and QCM

possible. When the coating on the quartz crystal electrode remains rigid, the major component of the OCM depends on the hydrodynamic interactions between the film on the electrode and the contacting electrolyte solution due to potential-induced volume and surface roughness changes in the coating. However, in the case of viscoelastic coatings, there are a variety of ways in which oscillation energy of the coated crystal may dissipate, and a large number of factors affect the change of the resonance frequency which are the indicators of the nature of the physicochemical processes behind the charging processes in the electrode coatings, requiring a careful analysis of the potential dependencies of both resonance frequency shift and resonance bandwidth. In some modern instruments, this damping of the oscillation is expressed through a quantity called dissipation. For a detailed understanding of these quantities and their effects, the readers can be directed to a recent review [153] presenting the main concepts of EQCM in context of its historical development, focusing on the exceptional sensitivity of the method. As described therein, its dynamic capability allows for the real-time monitoring of minute mass changes during electrochemical reactions in electroactive polymers and the accompanying viscoelastic changes [153]. Thus, a QCM used with electrochemistry methods such as EIS and CV allows real-time in situ measurement of the mass changes in the nanogram range during the electrochemical perturbation of the electrode solution interfaces.

ILs are highly viscous media thereby having large viscoelastic effects. Therefore, whether they are used as thin films for absorption-desorption-based phenomena or



Fig. 2.10 Comparison of five-cycle-CV EQCM responses for  $O_2$  (vol. 40 %) electrochemical reduction in the absence and presence of  $CO_2$  in  $[C_4mPy][NTf_2]$ . Scan rate: 20 mV/s

more conventionally used as electrolytes for various electrochemical applications, in situ EQCM technique is quite powerful for characterizing the interfacial phenomena in ILs. For example, we have shown that in situ EOCM enables to answer several very important questions regarding the IL and electrified metal interfaces that have not been addressed before: what are the mechanisms of electrode oxidation and reduction reactions in ILs? Is the adsorption of ILs potential dependent? Is the adsorption of IL specific or nonspecific under potential control? What are the doublelayer structure changes when the electrode changes from a metal to its oxide? These capabilities of EQCM methods facilitate the understanding of the structure/property relationships of electrode reactions in IL electrolytes. For instance, the electrochemical reactions of O<sub>2</sub>, CO<sub>2</sub>, and their mixture were investigated in three structurally different ILs by in situ EQCM [154]. Compared with electrochemical method only, the QCM integrated with the electrochemical method was shown to be significantly more sensitive and powerful for the characterization of the subtle differences (mass change or viscoelastic change) at IL/electrode interface as depicted in Fig. 2.10 showing current, frequency, and resistance responses obtained simultaneously. This led to the conclusion that the CO<sub>2</sub> reduction in ILs is irreversible and forms CO<sub>2</sub><sup>--</sup> adsorbate at electrode interface. With increasing concentrations of CO<sub>2</sub>, the reduction of oxygen is switched from a one electron process to the overall two-electron process, and forms adsorbed  $CO_4^{--}$  intermediate species. Even though the mechanisms of electrochemical reaction between  $CO_2$  and electrochemical-generated superoxide radical  $(O_2^{--})$  in three structurally different ILs are found to be similar, the simultaneous EQCM experimental results show that the different cations in three ILs can modify the kinetics of the electrode reactions of  $O_2$  and  $CO_2$  due to a competition between the ILs' cation and  $CO_2$  to react with  $O_2^{--}$ . The reactivity of  $O_2^{--}$  toward  $CO_2$  follows the order of the stability of the ILs' cation under  $O_2^{--}$  attack. Understanding of such adsorption of redox intermediate at an electrode/electrolyte interface during  $CO_2$  reduction is of fundamental importance for many chemical and electrochemical processes. In this way, EQCM technique can be used for the study of various gaseous molecules' redox processes in ILs in order to characterize the dynamics of the electrode reactions at an electrode and IL interface for a broad range of applications such as electrochemical synthesis, supercapacitor, Li-ion battery solid electrolyte interface, electrolyte interface during conversion, fuel cells, and sensors.

EQCM has also been used to explore the ion-solvent coupling mechanisms in a redox polymer, polyvinylferrocene (PVF) in ILs, and their solutions. From the data of frequency and current values, the mass changes and the moles of electrons transferred can be calculated which can be plotted against each other to obtain very useful information as shown in Fig. 2.11. This study showed that the unique solvation and ionic properties of ILs significantly affected the break-in process and the ion-solvent transport mechanisms of PVF redox switching which is indicated in the form of difference for the significant difference of mass changes during first and fifth cycle of the redox reaction. Due to the existence of strong IL-polymer interaction, not only the anions but also the IL molecules interacted with the PVF matrix. The cations were later removed from the PVF matrix to balance the excessive positive charge in PVF oxidation. This also confirmed that IL was not only an electrolyte but also a



**Fig. 2.11** Mass changes vs. electron transferred during PVF conditioning with  $[C_5mPyr][NTf_2]$  as measured by EQCM. Potential scan rate: 50 mV/s. Scan range: 0–0.6 V. (**A**) The *dots* and the *arrows* correspond to the first potential sweeping cycle and the *solid line* to the following cycles. (**B**) The mass changes during the fifth potential sweeping cycle

solvent in PVF redox switching processes. Various types of interactions between PVF and the IL, including dispersion, dipole induction, dipole orientation, hydrogen bonding, or ionic/charge-charge interactions, could significantly change the PVF redox dynamics. The strong IL–polymer interaction in certain ILs, e.g., methanesulfonate ILs, may change even the polymer sublattice structure. This property was being utilized by preconditioning the PVF films with suitable ILs, such as *N*-alkyl-*N*-methylpyrrolidinium bis(trifluoromethanesulfonyl)imides, which allows PVF film to relax to a state compatible with reversible glycylglycylglycine peptide (GGG<sup>-</sup>) doping/ undoping. In contrast, ILs with structures and properties highly divergent from the target GGG<sup>-</sup> failed to properly condition PVF to a compatible state [155]. These examples further confirmed that IL's tremendous diversity in structural and chemical properties and their distinctive properties offer an excellent opportunity to explore IL–polymer interactions and to dynamically control the conductive polymer relax-ation processes and their redox switching mechanism for various applications.

Another new direction of EQCM-based exploration of ILs is by using in situ admittance mode of EQCM [156] which can characterize the changes in the composition of the ionic part of the EDL during charge/discharge of high surface area electrodes, such as activated carbons. Reliable dynamic information on the rather complicated charging processes in meso- and microporous carbon electrodes can be obtained by the measurement and analysis of the change in the bandwidth of the resonance. It has been shown that EQCM is able to monitor ionic and solvent fluxes [157, 158], and at the same time can reflect the mechanical status of composite activated carbon electrodes, with high sensitivity. The use of this technique provides excellent opportunities for designing new porous electrodes, for the optimization of already existing supercapacitor devices, and for developing effective desalination cells for capacitive deionization (CDI) of water. In situ EQCM frequency-potential responses have also been used for understanding the mechanism of the redox reaction of  $[Au(III)Cl_4]^-$  at the Pt electrode in EmimBF<sub>4</sub> [159]. The results show that a series of 2e<sup>-</sup> and 1e<sup>-</sup> reductions occurs at the Pt electrode. Once metallic Au was formed on the Pt electrode surface, the subsequent reduction of  $[Au(III)Cl_4]^-$  could occur on the Au deposit with a lower over-potential for electrodeposition. In addition, in situ EQCM experiments proved that the Au deposited was produced by the disproportionation of  $[Au(I)Cl_2]^-$  to  $[Au(III)Cl_4]^-$  and Au metal. The dissolution of the Au deposit was also investigated in this work by in situ EQCM method using Pt-QCM, thereby proving it to be a very powerful method in elucidating electrochemical surface phenomena accompanying mass changes in ILs.

# 2.3.6 In Situ Electrochemical–Scanning Probe Microscopy

STM and AFM are powerful tools for the in situ studies of the structure and morphology of electrode interface and have been used to characterize IL electrode interface as well [60]. These techniques are known to routinely achieve atomic resolution images in high vacuum conditions [160] and even in air. However, in situ

measurements in liquids tend to be less well resolved owing to inhibited cantilever resonance and a vast increase in noise [161]. When it comes to ILs, AFM imaging is quite a complicated process, not only in terms of cell designs [162] and arrangement but also in terms of image acquisition [18, 60]. Even for the aqueous and organic electrolytes, electro-viscous effect is quite evident. The viscosity of these solutions when in contact with the electrode increases more than twofold under the influence of an electric field [163]. Compared to other electrolytes, the excellent stability of ILs provides suitability for the long time operation. Moreover, their high purity can make it possible to investigate the molecular level information in IL at the interface. However, an IL represents a dense system of cations and anions with no solvent, so that the individual interactions between neighboring ions create an extraordinary viscosity effect [164]. In addition to this high viscosity, the adsorption of moisture by the ILs also creates challenges for the practical measurements. However, despite these challenges, some fundamental studies have been done in IL systems which can form the basis of new and more relevant discoveries. For instance, AFM measurements have been done to reveal that ILs are strongly adsorbed on solid surfaces and that several layers are present adjacent to the surface [124, 165]. This is consistent with X-ray reflectivity measurements [166] and the proposed theoretical models [167, 168]. But as expected from the diversity of features in ILs, the functional groups as well as the chain lengths can significantly affect the adsorption strength. Study of Atkin and Endres et al. [124] showed that  $[C_4mPy][NTf_2]$  and  $[C_2mim]$ [NTf<sub>2</sub>] behave quite differently on Au(111). Both liquids are adsorbed at the open circuit potential, but the first one adsorbed approximately four times more strongly than the latter. This adsorption of ILs on a solid surface is not at all surprising as water and organic solvents can also be adsorbed [169]. However, the force to rupture IL layers is one order of magnitude higher than for aqueous/organic solvents. Such a strong adsorption must influence the image quality in an in situ STM experiment [170], especially under electrochemical control thereby affecting the electrochemical reactions. This work also emphasizes that ILs should not be regarded as neutral solvents which all have similar properties, particularly regarding the differences in interfacial structure (solvation layers) on metal electrodes which is a function of ionic liquid species. Conventional double layers do not form on metal electrodes in IL systems. Rather, a multilayer architecture is present. The number of these solvation layers is determined by the IL species and the properties of the surface and up to seven discrete interfacial solvent layers are present on electrode surfaces. In a recently published paper [171], the structure and dynamics of the interfacial layers between the air- and water-stable IL [C4mPy][FAP] and Au(111) were investigated using STM, CV, EIS, and AFM measurements. In situ STM measurements reveal that the Au (111) surface also undergoes a reconstruction, forming a "herringbone" superstructure at -1.2 V. AFM force-distance profiles also showed that IL becomes more structured at higher cathodic potentials with an increase in both the solvation layers and the push-through effects. EIS measurements showed a capacitive process at the IL/Au (111) interface which is considerably slower than electrochemical doublelayer formation and seems to be related to the reconstruction of Au(111). In another work from the same group, the anodic regime for the same IL system  $[C_4mPy][FAP]$ and Au(111) was studied. It was again shown that structures form on the nanoscale



Fig. 2.12 Summary of the EC-AFM investigation of electrochemical intercalation–deintercalation of the anions into HOPG in pure  $[C_4mim][HSO_4]$  and  $[C_4mim][NTf_2]$ 

for electrode potentials of up to +2 V which disappear when the electrode potential is returned to the open circuit potential, and the original surface is recovered. Thus, these observed processes on the surface are reversible. Interestingly, the work done in our group has indicated that this heterogeneity of the double-layer structure posed by different ILs and at different potentials is extremely beneficial for designing sensing interfaces. Therefore, the information gathered by the EC-AFM and sole AFM studies can significantly enhance the sensor development process.

Heterogeneity in IL's structure can also influence their interaction with substrate electrodes as well, during the electrochemical reactions and such interaction can also be studied by EC-AFM. Again by understanding these phenomena, more stable and innovative electrochemical systems can be designed both for sensors and fundamental electrochemistry. We have studied [172] such interaction of ILs with highly oriented pyrolytic graphite (HOPG) electrodes using EC-AFM, as summarized in Fig. 2.12. It was observed that electrochemical intercalation-deintercalation processes in pure ILs have caused the morphological changes in HOPG. Such changes due to electrochemical intercalation-deintercalation of ions during electrochemical processes are a common phenomenon occurring in graphite electrodes. HOPG has been widely studied as a model to understand the processes during electrochemical intercalation-deintercalation of ions into graphite. According to the model proposed for aqueous electrolytes, solvent (H<sub>2</sub>O) molecules play an important role during the oxidative reactions on HOPG. Therefore, studying the intercalation-deintercalation process in ILs which are composed entirely of ions is of primary significance. Being composed entirely of ions, morphological changes in HOPG will be mostly due to the intercalation-deintercalation of ions in ILs. Thus, the ionic sizes can have strong influence on intercalation into HOPG. The hydrophobic character of the ILs can also affect the intercalation of the ILs with the hydrophobic HOPG surface. However, these effects may play smaller roles compared to the anionic size effect. Our data proved that these morphological changes are reversible for intercalation and deintercalation,

which are strongly dependent on the anionic size of the ILs used. It was also possible to get the quantitative estimate of the amount of thickness changes on the HOPG surface during the intercalation–deintercalation process. And above a certain voltage, degradation of the steps on the HOPG surface occurs to form carbon nanoparticles. Furthermore, STM results can reveal the relationship of the electrochemical properties and the strength of this interaction. The results of these measurements are used to find out the symmetry and interatomic distances of metal atoms under potential control. Surface diffusion of metal atoms in contact with IL electrolytes has also been explored because of its close relation to the reactivity of the atoms on the surface. Such studies provide a key to understand many kinds of electrochemical processes at an electrode–electrolyte interface, such as anion desorption, electrode-position, corrosion, and surface alloying with a deposit.

As discussed earlier, high viscosity of ILs leads to a complicated situation in terms of AFM measurements that result in much higher signal-to-noise ratios. In order to obtain better spatial resolution in such a scenario, a new EC-AFM technique has been developed which involves independent control of the AFM tip and working electrode substrate and is named as frequency-modulated AFM (FM-AFM) [173]. FM-AFM measures tip–sample interaction very sensitively by detecting changes in the resonant frequency of the oscillating cantilever. This allows the tip–sample interaction stiffness and tip deflection to be monitored simultaneously, providing the atomic resolution images. By utilizing this technique for ILs, not only the topography of the substrate can be accurately ascertained at very high resolution, but the energy dissipation curves for oscillating cantilever can be obtained. Thus, the microscopic information regarding the electrical double layer at the electrode surface can also be attained by the assessment of energy dissipation curves.

# 2.4 New Approaches for Sensor Development Using IL Interface

Following the 1980s PC revolution and the 1990s Internet revolutions, recent decades have experienced a revolution in sensor research which promises to have a significant impact on a broad range of applications including national security, health care, environment, energy, industry and food safety, and manufacturing. The parameters important in the evaluation of sensors can be thought of as the "five S's" of sensor characterization, and include *Sensitivity, Selectivity, Speed of response, Stability*, and *Size/shape/cost*. The unique properties of ILs and IL interface enable a systematic design process across all design layers, with judicious choices in sensing materials, sensing chemistries, and transducers to uniquely overcome all performance challenges, especially those related to sensing capability and miniaturized sensor system implementation. As summarized in Fig. 2.13, (1) ILs' remarkable dissolution properties for organic and inorganic substances enable analyte preconcentration and sensitivity enhancement for the detections; (2) various molecular noncovalent interactions between ILs and the analytes contribute in increasing reversibility; (3) synthetic flexibility of ILs enables selective sensing by



Fig. 2.13 Multifunctional character of ILs as related to different sensing platforms using their highly unique and diverse properties. All these properties help in improving one or more of the performance evaluation parameter of the sensors

constructing ILs' sensor arrays; (4) the high viscosity of ILs allows the formation of stable thin films for mass-based sensors; (5) high thermal stability of ILs enables high-temperature detection; (6) ILs' negligible vapor pressure and nonflammable nature provides stability to the sensing film; (7) ILs' negligible vapor pressure, wide potential windows, high ionic conductivity, and good solubility enable their uses as new electrolytes for many improved electrochemical sensor systems [90, 174–180]; (8) ILs can also serve as a medium or a solvent for dyes and fluorescent compounds to form stable optical matrices, which can be the basis of accurate optical detection systems; (9) ILs can be incorporated into conventional matrices, such as biopolymers, cellulose, carbon nanotubes (CNTs), metal nanoparticles, and sol-gel-based silica matrices [181, 182], to form stable composite materials. These composite materials amalgamate multifunctional properties of materials involved in preparing the composites, thereby enhancing both their utility and their performance for a variety of sensing applications. Moreover, the unique properties of ILs and their miscibility/immiscibility with other solvents can be easily controlled by changing the anions and cations, thereby providing unlimited options for their applications designs, and especially for sensors where cross functionalities are essentially required. In the following sections, we will discuss examples of ILs that have been successfully explored in multiple ways for their chemical and biological sensing capabilities. We will also illustrate the principles of some of the modifications in order to obtain good sensor interfaces which can then generate different types of sensor systems based on ILs.

### 2.4.1 ILs as Electrolytes for Electrochemical Sensors

Most electroanalytical methods are based on the measurements of electrochemical cell potential, current, charge, or impedance at a fixed or controlled external applied function to the electrochemical cell. There are three main types of electrochemical sensors based on either the measurement of a redox current (amperometry), the potential (potentiometry), or the impedance or capacitance (impedance spectroscopy)

at the electrode/electrolyte interface of interests. Both electrode materials and electrolytes play significant roles in the performance of the interface. The analytical detection properties (e.g., sensitivity, selectivity, response time, drift, stability, and interference) are largely determined by the electrode/electrolyte interface properties for all electroanalytical methods. Notably, a majority of the electrochemical sensors developed to date employ aqueous-based electrolytes that suffer from solvent volatility leading to the exhaustion of solvent in a reaction batch. The other option is the nonaqueous electrolyte. Typically, there are three kinds of nonaqueous electrolytes: aqueous salts that could be dissolved in organic solvents (e.g., lithium perchlorate, and other perchlorate compounds, which have good solubility and ionization in particular organic solvents, such as CH<sub>3</sub>CN), organic compounds with charged ion center (e.g., tetra-n-butylammonium perchlorate) or polyelectrolytes (e.g., perfluorosulfonate [183, 184] and Nafion ionomers [185, 186]), and ILs. However, some of the aqueous electrolytes could not be dissolved in the organic solvents or cannot be ionized. The dielectric constants of organic solvents are usually smaller than the aqueous solvents too, which affects the conductivity a lot. So for a certain organic solvent, there are only some particular electrolytes used for a certain kind of solvent. Because of their nonvolatility and much higher ionic conductivity, ILs have the ability to replace almost all conventional electrolytes in all types of electrochemical sensors [174, 175, 187, 188]. Here, we will discuss the principles and examples of the most important analytical applications of ILs where they are used as electrolytes and solvents in electrochemical sensing.

# 2.4.2 Sensory Design Based on the Potentiometry

Potentiometry is a method in which the electrochemical cell potential is measured at equilibrium at which the current is zero. The properties of the interface region differ from the bulk properties. A potential is established at the phase boundaries, e.g., between the solution and the electrode surface. The potential of electrochemical cells is the sum of all interface potentials including electrode/electrolyte interface and liquid/liquid interface (i.e., the two electrolyte solutions of different compositions that are in contact with each other). Ideally the measured potential should depend only on the potential between the interfaces of interest for analytical purpose. This is typically accomplished by keeping all other interfaces constant through a suitable electrode construction. Potentiometric sensors (e.g., ion selective electrodes) usually consist of a membrane that contains ion exchangers, lipophilic salts, and plasticizers, and the transmembrane potential gives the activity of the analyte ion in solution.

#### 2.4.2.1 Sensing Based on the Liquid Junction Potentials

ILs have a broad range of polarity and can be used to design the interface between two immiscible ILs such as water/organic solvent interface to detect ions that are not redox active. The transfer of ions across the interface, as opposed to electron

exchange at solid electrodes, generates a potential which is directly related to the concentrations of the ions of interest. ILs have been explored as an alternative water-immiscible solvent phase for sensing at the liquid/liquid interface by the detection of ions transferring across liquid/liquid interfaces as described in an excellent review by Samec and Kakiuchi [189]. The main advantage of this type of sensing compared to sensing in conventional electrolytes is that the IL is usually pre-saturated with water, so any differences in humidity in the environment will not affect the overall sensor response. The group of Kakiuchi in collaboration with Mirkin has recently reported [105] the kinetics of ion transfer at the IL/water nanointerface. The interface was formed at the tip of a nanopipette, and the transfer of tetrabutylammonium from water to the hydrophobic IL trihexyl(tetracdecyl) phosphonium bis(nonafluorobutylsulfonyl)[P<sub>14,6,6,6</sub>][C<sub>4</sub>C<sub>4</sub>N] was reported. Although this work was not specifically related to sensing, this could have implications in the field due to the use of very small (nano) interfaces that give rise to lower ohmic drop and higher current density, which is highly beneficial for sensing applications. The same group has also highlighted the ultraslow relaxation of the electrical double layer in ILs at millimeter-sized interfaces [190], which may lead to the self-inhibition of the charge-transfer step across the IL-water boundary, limiting the performance of a sensor that relates charge transfer to analyte concentration. More research in this area is needed to understand the impact of the ultraslow relaxation on sensor responses and behavior, using smaller sized interfaces.

#### 2.4.2.2 Ion-Selective Electrodes with ILs

Ion selective electrodes (ISEs) are electrochemical sensors that allow the potentiometric determination of the activity of an analyte ion in the presence of other interfering ions. An ion-selective membrane consists of four major constituents: ionophore [ion carrier, e.g., valinomycin (selective to K<sup>+</sup> over Na<sup>+</sup>)], lipophilic salt as ion exchanger [e.g., K<sup>+</sup>R<sup>-</sup> (where R<sup>-</sup>=lipophilic anion)], plasticizer [e.g., 2-nitrophenyloctylether (NPOE)] as organic solvent, and polymeric substrate matrix such as Polyvinyl chloride (PVC). The different potential response has, as its principal component, the Gibbs energy change associated with permselective mass transfer across a phase boundary. The ionophore in membrane can selectively complex the target ions at membrane interface that causes the interfacial charge separation. The measured potential differences of ISEs are linearly dependent on the logarithm of the activity of a given ion in solution as described in Nicolsky-Eisenman equation (Eq. 2.5).

$$E_{i} = E_{i}^{0} + s_{i} \log \left[ a_{i} + \sum_{i \neq j} K_{i,j}^{\text{pot}} \left( a_{j} \right)^{\frac{z_{i}}{z_{j}}} \right]$$
(2.5)

 $E_i$ : electromotive force (potential) of the cell assembly;  $E_i^{0}$ : cell constant;  $a_i$ : activity of primary ion I in sample solution;  $a_j$ : activity of interfering ion J in sample solution;  $z_i$ ,  $z_j$ : charges of I and J, respectively; and  $K_{i,j}^{\text{pot}}$ : potentiometric selectivity coefficient of primary ion  $\mathbf{I}^{\mathbf{z}_i}$  against interfering ion  $\mathbf{J}^{\mathbf{z}_j}$ . An ideal selective electrode would show all  $K_{i,j}^{\text{pot}} = 0$ .

ILs possess high ion concentration, high conductivity, and good electrochemical stability. So they seem to be natural candidates for liquid ion exchanger membrane electrodes. For these reasons, they have been employed as alternatives to plasticizers and ion exchangers in membranes of ISEs. Most charged carriers applied in conventional ISEs are ion exchangers that do not exhibit specific interactions with the ions to be sensed. As a result, selectivity is determined by the free energy of hydration of the ions and corresponds to the so-called Hofmeister series [191]. However, ILs can be designed by modifying cations such as imidazolium or pyridinium and pendant alkyl groups with functionality; thus increased selectivity or even specificity for a given set of ions can be obtained. This new type of IL-based membrane electrode could be smaller, more portable, and less expensive, with the possibility of conducting simultaneous and continuous analysis of multiple analytes. It is also possible to provide real-time output and higher sensitivity and selectively. Since no sample preparation is required and no secondary labels are needed, these ISEs are very user friendly. For example, low melting ionic solids, i.e., the ILs that melt slightly above room temperature, can be used in ISEs for the potentiometric determination of salicylate, perchlorate, thiocyanate, and iodide ions in water. Three of such ILs  $[N_{66666}]$ [BSB],  $[N_{8888}]$ [BSB], and  $[N_{8881}]$ [BSB] were proved as suitable salts for both liquid-contact and solid-contact ISE membranes, and  $[N_{8888}]$  [BSB] was chosen as the most suitable because of its lowest melting point. A Nernstian response was observed over the range 10<sup>-5</sup> M to 10<sup>-1</sup> M for the four chosen analyte ions, with good reproducibility and reversibility and a fast response time of <10 s. Peng et al. [192] also reported a sulfate ion sensor based on a PVC membrane containing either one of the two ILs  $[C_8mim][C1]$  or  $[P_{14,6,6,6}]$ [CI] as both an anion exchanger and plasticizer, and sulfate ionophore I (1,3-[Bis(3phenylthioureidomethyl)]benzene). Both membranes exhibited ideal Nernstian responses to sulfate over the range 10<sup>-5</sup> M to 10<sup>-1</sup> M and were successfully applied for the analysis of sulfate in drinking water samples. We used two imidazolium-1-butyl-3-methyl-imidazolium bis(trifluoromethanesulfonyl)imide based ILs. [C<sub>4</sub>mim][NTf<sub>2</sub>] and 1,3-dibutylimidazolium bis(trifluoromethanesulfonyl)imide  $[C_4C_4im][NTf_2]$ , to construct PVC liquid membrane electrodes for the detection of [NTf<sub>2</sub>]<sup>-</sup>. As shown in Fig. 2.14, the ISEs we made have improved selectivity and sensitivity as compared to anion-sensitive electrodes based on organic ammonium salts, but we also observed less than Nernstian response due to the partial solubility of the two imidazolium-based ILs in aqueous solutions. The uptake of water is expected for IL membranes being in contact with aqueous samples. The wide potential window is regarded as one of the most important advantages of ILs when they are used as pure electrolytes [189, 193]. This is not the case for IL-modified electrodes used as ISE, because they operate mostly in contact with aqueous solution. Similar to our observation, IL [P<sub>14,6,6,6</sub>][Cl]/PVC membrane-based potentiometric sensor also suffered from severe potential instability due to the tendency of the IL to absorb water, but this was improved by the addition of carbon nanotubes (CNTs) to the membrane, resulting in a stable Nernstian response over the concentration range 10<sup>-5</sup> M to 10<sup>-1</sup> M [194]. Thus, hydrophobic ILs and low melting ionic solid are choices for IL-based new type of ISEs. The solubility of hydrophobic ILs in



Fig. 2.14 EMF time profile of the  $[C_4 mim][NTf_2]$  and  $[C_4 C_4 im][NTf_2]$  PVC membrane at various Li $[NTf_2]$  concentrations

water is much smaller than the solubility of water in IL and in some cases is much below the fraction of percent. This property is crucial from the point of view of stability of IL membrane electrodes, because of the possibility of microliter-sized liquid deposit dissolution in few milliliters of the surrounding aqueous electrolyte. However, IL-membrane electrodes are reported to be stable at least in electrochemical timescale indicating slow dissolution in the case of more hydrophilic ILs. For example, Nishi et al. [195] used the hydrophobic IL methyltrioctylammonium bis(nonafluorobutylsulfonyl)imide  $[N_{8,8,8,1}][C_4C_4N]$  containing the ionophore dicyclohexano-18-crown-6 (DCH18C6) for the potentiometric detection of K<sup>+</sup> in water. Facilitated ion transfer was reported for K<sup>+</sup> and the two-phase system was used for the potentiometric determination of K<sup>+</sup>. A Nernstian response to K<sup>+</sup> (59 mV per decade) was observed over the concentration range 10<sup>-5</sup> M to 10<sup>-1</sup> M with a response time of 20 min. It is clear from these reports that ILs have the ability to be used in membranes of ISEs. However, the long-term stability of such sensors may be restricted by the leaching of IL ions from the membrane into the water phase. At present, the ILs available may not be sufficiently lipophilic to serve as suitable replacements for components in conventional ISEs (e.g., ion exchangers in PVC membranes). This has prompted the researchers to use IL composites in ISEs. For example, polymer/IL/multiwalled CNT composite electrode was developed [194] as an all solid-state potentiometric sensor for various anions (SO<sub>4</sub><sup>2-</sup>, Cl<sup>-</sup>, NO<sub>3</sub><sup>-</sup>, SCN<sup>-</sup>, and ClO<sub>4</sub><sup>-</sup>). Moreover, a potentiometric Er(III) sensor consisting of a multiwalled CNT/[C<sub>4</sub>mim][BF<sub>4</sub>] carbon paste electrode containing 5-(dimethylamino) naphthalene-1-sulfonyl-4-phenylsemicarbazide (NSP) as the sensing material was

also constructed. A Nernstian response of 19.8 mV per decade was observed in the range  $10^{-7}$  M to  $10^{-1}$  M with a detection limit of  $5 \times 10^{-8}$  M for Er(III). This shows that the use of IL as a binder demonstrated improved performance compared to mineral oil (paraffin), and the combination of the three sensing materials gave better sensitivity, selectivity, response time, and stability compared to traditional Er(III) carbon paste sensors. Thus, this strategy is going to be more useful in preparing ISEs until new highly lipophilic ILs are synthesized.

### 2.4.2.3 Nonclassical Potentiometry

In ISE, the equilibrium potential change of the electrode is inversely proportional to the charge of the analyte being detected. Thus, it is not feasible for its use for detecting large, highly charged molecules, due to the very small sensor response to highly charged macromolecules. However, in 1990s, several research groups demonstrated a nonclassical potentiometry [196] for the detection of different macromolecular polyions, including heparin, protamine, carrageenan, and DNA. The response mechanism of nonclassical potentiometry is fundamentally different, employing nonequilibrium, steady-state conditions to generate a useful sensor response. Ionic liquids have also been used in the nonclassical potentiometric electrode fabrication. Langmaier and Samec [197] employed a thin microporous membrane impregnated with valinomycin and the hydrophobic IL [N<sub>12,12,12,1</sub>][TFPB] for the facilitated amperometric detection of  $K^+$  and  $Na^+$ . The use of IL in the membrane in this case provided enhanced stability and selectivity compared to conventional K<sup>+</sup> ISEs. A similar strategy can be applied with the addition of a water-soluble crown ether (18-crown-6) to the aqueous phase, in order to make it possible to distinguish the voltammetric waves of various alkali metal cations (K<sup>+</sup>, Na<sup>+</sup>, Li<sup>+</sup>, and Mg<sup>2+</sup>), and the promising results suggest that the IL membrane may be suitable for application in an amperometric ISE for  $K^+$ . The work of Silvester and Arrigan [198] is quite important in this regard who reported the transfer of several common ions across the interface between water and a commercially available hydrophobic IL  $[P_{14,6,6,6}]$ [FAP] with a melting point of <-50 °C. This was the first report of voltammetry at an array of water/IL microinterfaces, rather than at a single interface or porous polymer-supported interface. The interface array was formed within the micropores of a silicon chip membrane (30 pores and 23 µm diameters) and provided advantages of micron-sized interfaces such as radial diffusion, higher current densities, and lower iR drop, but with larger currents for sensing low concentrations of redoxinactive ions. This work has shown that sensing of various ions is possible at the water-IL interface, but it was limited to the ions that transfer at potentials less negative than the IL anion (e.g., [FAP]<sup>-</sup>) transfers to water. As a result, the synthesis of ILs with extremely hydrophobic cations and anions which are not yet available in the liquid form is required in order to extend the potential windows to those similar to organic solvent/supporting electrolyte systems (e.g., 0.9 V). If this is made possible, this should allow for the observation of species that have been detected at the positive potential limit in water/organic solvent systems, e.g., important biomolecules such as lysozyme and hemoglobin.

It is already known that the contamination of IL with water shrinks potential window to that exhibited in aqueous electrolyte solution [78]. This is also the case of most hydrophobic ILs composed of large 1-alkyl-3-methyl-imidazolium cations and homologs of [NTf<sub>2</sub>] anions. Therefore, the uptake of water is expected for IL deposit being in contact with aqueous electrolyte in the nonclassical potentiometry.

#### 2.4.2.4 Sensing Based on Voltammetry

Voltammetry is a powerful suite of tools that enables qualitative and quantitative information about the analytes to be obtained by the measurement of the current as a function of applied potential. The technique can be applied to any species that can undergo redox transitions on solid electrodes, or any ion that can be transferred across interfaces (in the case of liquid/liquid interface). The analyte species diffuses through the electrolyte to be detected at the working electrode surface. It was also used to monitor the diffusion coefficients of species in solution and to understand their behaviors and electrochemical reaction mechanisms. Voltammetry typically takes place with two- or three electrodes that are connected through an electrolyte medium (e.g., water or organic solvents containing a background electrolyte). There has been a lot of work focused on understanding the reaction mechanisms, kinetics, and thermodynamics of electrochemical reactions in ILs. However, ILs have recently shown much promise as stable and nonvolatile electrolytes, especially in amperometric gas sensors. A typical amperometric gas sensor consists of three electrodes connected through an electrolyte, which is covered by a gas-permeable membrane. The gas passes through the membrane, diffuses through the electrolyte, and is detected at the working electrode. Most commercially available amperometric sensors of gases (e.g., O<sub>2</sub>, CO, SO<sub>2</sub>, H<sub>2</sub>S, NO<sub>2</sub>, and Cl<sub>2</sub>) currently employ conventional solvents (e.g., H<sub>2</sub>SO<sub>4</sub>/ H<sub>2</sub>O mixtures, or organic solvents such as acetonitrile or propylene carbonate) that cannot survive drastic temperature changes or extremely dry or humid conditions. The "lifetime" of a sensor is often determined by how quickly the electrolyte dries up and the solvent often has to be replaced every few days/weeks in the most extreme conditions. ILs possess negligible volatility and high chemical stability, making them ideal electrolyte media in robust gas sensors for potential application in more extreme operating conditions (e.g., up to 300 °C), with no possibility of solvent evaporation or degradation. This, combined with the intrinsic conductivity (no need for supporting electrolyte), wide potential windows (to investigate compounds that may have been inaccessible otherwise), and, in some cases, increased gas solubility in ILs, makes them ideal electrolyte media for gas detection. Furthermore, ILs can stabilize the radical cation or radical anions which enables new redox chemistry of many analytes that are quasi reversible. However, the high viscosity of ILs often results in slow and less reproducible response [199] that have limited their direct use in practical sensors regarding the response time and sensitivity. To increase response speed and circumvent the high viscosity of ILs, we introduced an innovative electrochemical cell (Fig. 2.15) with a porous Teflon membrane as the support for ILs that facilitate diffusional transport through the pores and provide two levels of selectivity (i.e., the size of the pore and the IL membrane) [90]. Analytes entering from the back side



Fig. 2.15 Schematic diagram (not to scale) of the Clark-type oxygen sensing cell with the analyte flow from the back side to circumvent the high viscosity of ILs, and the current transients recorded at -1.2 V for different oxygen concentrations using three different ILs. Nitrogen was used as the carrier gas

were able to quickly reach the electrode/electrolyte interface without passing through the IL diffusion barrier, reducing response time to mere seconds. Figure 2.15 also shows the amperometric response of three  $[NTf_2]$ -based ILs to oxygen and illustrates a strong dependence on the choice of cation, as desired. High sensitivity, complete reversibility, long-term stability (less than 0.3 % potential shift over 90 days), rapid response, and strong selectivity (selectivity coefficient ~0.01 % for CO<sub>2</sub>, NO, NO<sub>2</sub>, SO<sub>2</sub>) of this IL oxygen sensor were observed.

Recent advances in voltammetry-based gas sensing involving ILs have been reviewed by Rogers et al. [200] who describe the electrochemistry of various gases including oxygen, carbon dioxide, hydrogen, ammonia, hydrogen sulfide, sulfur dioxide, and nitrogen dioxide in ILs. From these studies, it appears that the most logical step forward in this area is to employ thin IL layers to overcome the slow diffusion often associated with viscous ILs. This may result in decreased response times, on the order of minutes or seconds, which is ideal for most gas sensor device requirements. Microelectrodes fabricated on a silicon chip can be an important advancement in this regard as shown by Compton's group [179]. The use of small (micron-sized) working electrodes can minimize any iR/Ohmic drop limitations that are often associated with voltammetry in highly resistive ILs on larger electrodes (larger currents). Also from these studies, the electrochemical reaction mechanisms of carbon dioxide, hydrogen sulfide, and chlorine gas in ILs can be explored. For example, the electrochemical reduction of CO<sub>2</sub> in the RTIL [C<sub>4</sub>mim] [Ac] was studied on a Pt microelectrode using cyclic voltammetry. CO<sub>2</sub> undergoes a chemically irreversible one-electron reduction to the radical anion CO<sub>2</sub><sup>--</sup> and subsequent followup chemistry including interaction/complexation with the IL. The behavior was found to be irreversible due to strong absorption of  $CO_2$  in the IL, suggesting that this system may not be suitable for real-time sensing of CO<sub>2</sub>; however, the high solubility (>1.5 M) of CO<sub>2</sub> in [C<sub>4</sub>mim][Ac] suggests a method for sequestration of the greenhouse gas. We have also used voltammetry in ILs in combination with QCM technique [154] as described in in situ EQCM section proving that the CO<sub>2</sub> reduction in ILs is irreversible and forms CO<sub>2</sub><sup>-</sup> adsorbate at electrode interface. In the presence of O<sub>2</sub> and with increasing concentrations of CO<sub>2</sub>, the reduction of oxygen is switched from a one-electron process to overall two-electron process, and forms adsorbed CO<sub>4</sub><sup>--</sup> intermediate species. Such information about the mechanisms of the reaction is highly beneficial for the development of the sensor systems.

#### 2.4.2.5 IL Redox Chemistry Enabled Reliable Voltammetric Sensing

Study focusing on understanding the reaction mechanisms and comparing behavior to that in conventional electrolyte systems is an active research area and always establishes the foundation of reliable sensing before the actual sensing protocols are developed. In some cases, reactions and mechanisms have been found to be the similar in ILs as those in conventional solvents, however, in some cases, notable differences and unusual behavior have also been observed. It is extremely important to understand the atypical behavior in ILs before they can be employed as direct replacements for conventional molecular solvents (containing supporting electrolytes) in sensor devices. Compton's group [201], for example, has reported the twoelectron reduction of 100 % chlorine gas to chloride on a Pt microelectrode in a range of ILs ( $[C_2mim][NTf_2]$ ,  $[C_4mim][NTf_2]$ ,  $[C_4mPy][NTf_2]$ ,  $[C_4mim][BF_4]$ ,  $[C_4 mim][PF_6]$ ,  $[C_4 mim][CF_3SO_3]$ ,  $[N_{6,2,2,2}][NTf_2]$ , and  $[C_6 mim][C1]$ ). The behavior of the voltammetry at various scan rates was highly unusual, with limiting currents observed to decrease with increasing sweep rate. This intriguing observation was assigned to a mechanism of adsorption of chlorine gas on the Pt electrode surface. The adsorbed chlorine itself cannot be reduced, but must undergo desorption before the electron-transfer step. At slower scan rates with longer timescales, there is more desorption resulting in more surface available for electron transfer, thereby resulting in higher currents at slower scan rates. The large voltammetric currents observed suggest that Cl<sub>2</sub> has a very high solubility (1–10 M) in ILs, making these solvents attractive for the purposes of  $Cl_2$  gas sensors. The authors did not report the effect of varying concentrations of Cl<sub>2</sub> on the current response, but this seems like the next logical step especially given the unusual adsorption mechanism. If the current scales linearly with concentration, ILs may prove to be a useful medium for robust Cl<sub>2</sub> gas sensing.

Although IL electrolytes provide partial selectivity, the primary selectivity of an IL–electrochemical sensor comes from the redox properties of the analyte observed using amperometric methods, wherein the electrical current generated by reaction of an analyte at an electrode at a fixed or variable potential is measured [22]. We have shown redox chemistry that occurs only in ILs and can be exploited to enhance sensor performance [202]. As shown in Fig. 2.16, we discovered that at platinum electrode in [NTf<sub>2</sub>]-based ionic liquids (ILs), facile methane electro-oxidation is observed suggesting a unique catalytic Pt-[NTf<sub>2</sub>] interface for electron-transfer reaction of methane at room temperature. Little methane electro-oxidation signals are observed in ILs with other anions. In this experiment, an oxygen reduction process

was included; as a result, the incomplete methane oxidation product CO was fully oxidized to  $CO_2$  in the presence of superoxide ions, since superoxide can quickly adsorb on the electrode surface to form the active species, and  $[C_4mPv][NTf_2]$  is one of the best solvents to stabilize superoxide. In contrast to many methane oxidation systems reported, there are no incomplete oxidation products such as CO or COOH detected and the final methane oxidation products in [C<sub>4</sub>mPy][NTf<sub>2</sub>] are confirmed to be CO<sub>2</sub> and water by in situ infrared spectroscopy and electrochemistry. The electrochemical oxidation of methane at  $Pt/[C_4mPy][NTf_2]$  interface depends on the methane concentration linearly (from 1 % to 10 vol% methane concentration). As shown in Fig. 2.16, taking advantage of the unique coupled chemical reactivity of superoxide with the methane electrode oxidation product CO<sub>2</sub> that takes place in [C<sub>4</sub>mPy][NTf<sub>2</sub>] at room temperature, we introduce an innovative internally referenced electrochemical method for methane detection that increases the reliability of the measurements by determining these two ambient gases within a single sample matrix in real time, with cross-validation occurring for a single sensory element. The coupled reactions facilitate the complete oxidation of methane to  $CO_2$  and water in [C<sub>4</sub>mPy][NTf<sub>2</sub>] and the in situ generated CO<sub>2</sub> was used as an internal standard for oxygen detection which addresses the fundamental limitations to accuracy and the long-term stability and reliability in chemical analysis. We have validated this ionic liquid-based methane sensor employing both conventional solid macroelectrodes and flexible microfabricated electrodes using single- and double-potential step chronoamperometry and the analytical parameters [202]. Figure 2.16 shows the amperometric response of a methane sensor with the IL  $[C_4mPv][NTf_2]$ , as methane concentration is increased and oxygen concentration is decreased. Both analytes can be selectively quantified by alternating the bias potential. Oxygen can be reduced to superoxide radical which was used for oxygen sensor development (-1.2 V) as shown in Fig. 2.16. High sensitivity, complete reversibility, long-term stability (less than 0.3 % potential shift over 90 days), rapid response, and strong selectivity (selectivity coefficient ~0.01 % for CO<sub>2</sub>, NO, NO<sub>2</sub>, and SO<sub>2</sub>) of this IL oxygen sensor were observed. The simplicity of detection using low-power and low-cost potential step chronoamperometry and microfabricated electrodes provides strong foundation for their easy integration with engineering advancements such as portable electronics, networked sensing, and next-generation monolithic implementation for autonomous, maintenance-free sensor operation with a long lifetime for the detection of methane with high sensitivity and specificity using smaller, inexpensive, and low-power transducers for their applications for monitoring the methane emissions.

# 2.4.3 Electrified IL/Electrode Interface and Related Sensor Based on Impedance Technique

EIS, which involves the application of a sinusoidal electrochemical perturbation (potential or current) over a wide range of frequencies, allows for the measurement of impedance changes in the forms of double-layer capacitance and the



**Fig. 2.16** (a) In situ FT-IR study of methane oxidation in  $[C_4mPy][NTf_2]$ ; (b) plots of methane anodic currents at 0.9 V applied vs. methane concentration and (c) plots of normalized oxygen reduction currents at -1.2 V vs. oxygen concentration. (d) Scheme of methane oxidation and coupled oxygen reduction in  $[C_4mPy][NTf_2]$ 

charge-transfer conductance that originate from the change of polarization of ILelectrode interface. The current signals and the impedance signals are all related to the active area of the electrodes. Thus, EIS-based sensors not only provide orthogonal detection modes to amperometric sensors but they also permit self-monitoring of the sensor's stability and automated calibration for drift mechanisms. We have demonstrated an innovative capacitance sensor based on the change of the surface charge at IL-electrified metal interfaces either due to the change of ion or electron transport in ILs resulted from the redox process of analyte or the polarization reaction due to adsorption/dissolution of analyte in ILs [80]. At room temperature, ILs have high viscosity, and the diffusion and conductivity of ions are normally lower in ILs than in aqueous electrolyte solutions. Thus, they can be regarded as a solid and liquid interface simultaneously. As a result, ILs are ideally suited for applications that require a thin or intensely concentrated layer of ionic charge, such as capacitance sensor development. Compared with molten salts at room temperature, the ions comprised of ILs are often large, flexible, highly polarizable, and chemically complex with a number of interionic forces (such as dispersion forces, dipole-dipole interaction, hydrogen bonding, and pi-stacking forces) in addition to coulombic forces present. Additionally, adsorption of anions and/or cations is likely to happen at the interfaces with ILs. Specific adsorption of IL on solid surface depends on the chemistry of the ions and applied potential. Varying the applied potential can result in the rearrangement of adsorbed ions which allows the modification of the IL double-layer capacitance. Capacitance at a fixed potential will depend on double-layer thickness and permittivity of the liquid at the interface. Ion size and applied potential influences the double-layer thickness, and alkyl chain length influences the relative permittivity. Consequently, varying the structure of IL anions or cations and applied potential enables the modification of the double-layer structure at the IL-electrified metal interface (e.g., thickness).

The double-layer structures in ILs are highly dependent on IL physicochemical properties and the applied potential. When exposed to an analyte especially small gaseous molecules, the molecular interaction events that occur at the IL interface can lead to polarization reaction at interface via redox reaction, binding, or dissolution of the analyte in ILs. For example, the analyte can displace or rearrange the IL order in the double layer to a new orientation. Removing analyte allows the IL double layer return to its original orientation. For example, the IL  $[C_4mPy][NTf_2]$ , which has a double-layer structure favoring small gas molecule adsorption, can sensitively and selectively measure concentrations of CH<sub>4</sub> (Fig. 2.17) using EIS with a -0.3 V DC bias [80]. Figure 2.17c also clearly shows that the sensor returns to its baseline value when the analyte is removed, demonstrating the reaction is fully reversible with less than 0.1 % drift. The selectivity comes from the unique highly ordered arrangement of ions in the innermost layer of IL-electrode interface which is potential dependent. The degree of ordered structure at IL-electrode interface can be tuned by the applied bias (e.g., -0.3 V for CH<sub>4</sub>) and by the unique molecular structure of the IL ions. The high viscosity of ILs that is usually considered a limitation to practical electrochemical applications due to slow rate of mass transport is an advantage in capacitance [203] measurement due to a more ordered



**Fig. 2.17** (a) Plots of real part of complex capacitance at different methane concentrations. (b) Change of real part of complex capacitance ( $C_{re}$ ) at 1 Hz vs. methane concentrations. [C<sub>4</sub>mPy] [NTf<sub>2</sub>] is the IL and DC bias is -0.3 V; (c)  $C_{re}$  measured over five cycles of alternate exposure to 5 % methane (N<sub>2</sub> carrier gas at 200 sccm). DC potential is -0.3 V vs. Au quasi reference electrode. AC frequency is at 1 Hz

and concentrated double layer. Thus, impedance measurements provide an orthogonal detection mode to amperometric measurement, enhancing measurement sensitivity and improving sensor robustness.

## 2.4.4 IL Electrochemical Microarrays

For real-time multiple analyte monitoring, a group of sensors must be brought together, typically in an array format. We have demonstrated small arrays of IL sensors using both amperometric and impedance approaches. An array of four IL-coated glassy carbon electrodes was tested for the voltammetric detection of DNT and TNT, and a correlation (with 100 % classification accuracy) between the redox properties and the physiochemical parameters of the species involved was revealed (Fig. 2.18) [204]. Detection limits in liquid phase of 190 nM and 230 nM for TNT and DNT, respectively, and a linear range up to 100  $\mu$ M were obtained.



Fig. 2.18 Square wave voltammograms of 0.1 mM of TNT and DNT in four different ILs

Interference from water was eliminated by calibrating with a redox peak that was not proton related. Gas phase analysis showed strong redox signals for TNT and DNT and demonstrated that ILs serve as a preconcentrator to improve the sensitivity of very low vapor pressure analytes. These examples demonstrate that the combination of IL materials and electrochemical transducers overcomes many obstacles in forming an effective sensor system. IL–electrochemical sensors are also well suited for miniaturization and can be fabricated with very low cost. In contrast to nonspecific transducers such as a surface acoustic wave device, arrays of amperometric and EIS transducers allow a secondary perturbation (e.g., potential) that enhances selectivity and increases analytical information content without increasing the number of physical sensor elements.

## 2.4.4.1 Microarray Fabrication

To improve current density and to overcome iR/Ohmic drop common in resistive ILs, small-sized working electrodes and eventually "lab-on-a-chip" type systems are being investigated. Microfabrication technologies, particularly thin film deposition of microelectrodes and formation of microfluidic channels, have been widely applied to analytical systems [205, 206]. Electrode arrays, both macro- and microscale, are now commonly fabricated using thin film metal deposition and photolithography [207–210]. For example, Fig. 2.19 shows an interdigitated electrode (IDE), which was fabricated using thin film deposition of gold on porous Teflon. Figure 2.19 also shows the data using this electrode for the measurement of oxygen concentrations. These miniaturized sensors yield similar sensitivity to results shown before. Similar fabrication techniques can be applied to optimize electrodes for the sensor interfaces developed within this project and design array structures. As fabrication of these electrodes relies on photolithography, the size and geometry of the electrode can easily be varied to meet the needs of the sensor interfaces, and different electrode configurations can be utilized within the same array to improve analytical performance.



Fig. 2.19 Amperometric sensing of oxygen using (inset) micro-fabricated concentric ring disk electrode on porous Teflon

An ethylene gas sensor employing a thin layer of the IL [C<sub>4</sub>mim][BF<sub>4</sub>] on a "lab-on-a-chip" sensor was proposed by Zevenbergen et al. [177] The sensor consisted of a 1-mm diameter Au working electrode surrounded by a Pt ring-shaped quasi-reference electrode and a Pt rectangular counter electrode. CV curve of ethylene in the IL revealed an oxidation peak before the onset of gold oxidation. Interestingly, the ethylene oxidation peak was only visible when water was present in the IL; no response was observed with humidity levels less than 20 %. As a result, the authors studied the dependence on humidity and observed larger responses when the humidity level was higher. A detection limit of 760 ppb and a linear response (current vs. concentration) up to 10 ppm were achieved. This suggests that amperometric ethylene detection in ILs is possible; however, it is limited only to environments with sufficient humidity levels (more than 40 %), which limits the application of such a sensor in extremely dry environments.

# 2.4.5 IL as Component for New Electrode Materials

Besides using ILs as electrolytes for electrochemical sensor development, their low melting points and low tendency to crystallize, realized by the combination of large, usually asymmetric cation and smaller anion, make them good candidates for electrode modifications that can lead to a diverse set of applications in sensing fields. These modifications can be done in many different ways as shown in Fig. 2.20; however, the choice of modification is entirely based on the application requirements. For example, IL/CNT-based composite materials, consisting of highly electroactive carbon nanotubes and fluid electrolyte, can be utilized for a wide variety of electrochemical applications, such as sensors, capacitors, and actuators. In electrochemical biosensors, these composite materials can also be used as an immobilizing matrix to entrap proteins and enzymes, which provide a favorable microenvironment



Fig. 2.20 Most common modes of the electrode modifications using ILs for different sensing applications

for redox proteins and enzymes to retain their bioactivity and perform direct electrochemistry and electrocatalysis. In the following sections, we will discuss some of the most common modifications for IL-based electrodes for sensing applications.

### 2.4.5.1 Electrodes Modified with IL Droplets or IL Films

Among many different types of electrode modifications possible for sensor applications, electrodes modified with IL droplets or films are the most commonly employed. In this method, electrodes are prepared by direct deposition of IL on the electrode surface [211] or from its diluted solution in volatile solvent [212]. These two procedures may provide different geometry of the deposit. Thin liquid film geometry is most important for sensors which can be enforced by surface coverage with porous Teflon membranes. The preparation of IL-modified electrode in situ by the adsorption of IL from aqueous solution has also been reported [213]. The appropriate selection of electrode substrate and IL is important in this case to obtain stable liquid deposit in contact with aqueous solution. Although research on ILmodified electrodes started from electrode substrate covered by droplets or liquid film, in the absence of other film components, now the focus has been shifted to film electrodes with organic or inorganic polymers, nanoparticles, nanotubes, and other micro- or nano-objects as other components. Their complexity ranges from simple ones as polymer film plasticized with IL to multicomponent films. The electrodes consisting of polymer membrane saturated with IL-based ionophore solution exhibit ion selectivity and were applied as ion-selective electrode. By using similar strategy with Ag/AgCl substrate, reference electrodes can be prepared. In particular, gel composed of poly(vinylidene fluoride-co-hexafluoropropylene) and viscous IL (1-methyl-3-octylimidazolium bis-(trifluoromethyl-sulfonyl)imide) allows to obtain solid state and easy to miniaturize devices.

In many of these cases of direct modification, ILs, especially the imidazolium based, can also be appended to demonstrate functionalities which are related to their immobilization onto the electrodes to generate different types of modified electrodes. These functionalities include self-assemblies of IL on the electrode surface, covalent bonding of IL to the electrode surface, IL functions that can be used for the preparation of IL-based polymer (PILs) films, and IL used for the functionalization of conductive elements of the film. When the electrode is ready, the counter ions are electrostatically attracted to positively charged functionalities and they can be exchanged after immobilization on the electrode surface. Such small modifications can be highly suitable for incorporating the desired characteristics to the electrode materials. But most importantly, the electrodes modified by any of these methods can then be utilized for various sensing applications. For example, Ng et al. [214] employed a nanocomposite gel consisting of a three-dimensional graphene material and the IL  $[C_4 mim][PF_6]$  for the amperometric detection of nitric oxide (NO). A linear response of current vs. concentration over the range  $1-16 \mu M$  NO was observed, with a fast response time of less than 4 s and a low detection limit of 16 nM. The improved response of this modified electrode is attributed to the porous graphene material that has a high specific surface area and superior conductivity which generated a 3-D graphene/IL nanocomposite to provide a novel platform for sensitive NO detection.

Although the generic combinations of IL with other electrode materials as shown in case of NO sensing have proven quite useful for sensing applications, the results are again generic in most cases with much less selectivity than required. Therefore, the focus is now shifting to use more task-specific ILs in the electrode modifications. Lu et al. [215] have shown that a task-specific IL in combination with bismuth oxide (Bi<sub>2</sub>O<sub>3</sub>) can be used for the electrochemical detection of heavy metal oxides including cadmium oxide (CdO), copper oxide (CuO), and lead oxide (PbO). The IL contained an  $[NTf_2]^-$  anion and a tetraalkylammonium cation with one carbon chain functionalized with a carboxylic acid group. The presence of the acid group allowed for the solubilization of metal oxides into the IL. The IL was coated as a thin layer onto a surface containing three indium tin oxide (ITO) printed electrodes and acted as the selective solubilization medium and electrolyte. It is envisioned that more analyte species may begin to be detected by employing newly synthesized ILs with specific functional groups.

#### 2.4.5.2 Carbon Paste Electrodes with IL as Binder

The high viscosity of ILs can also be employed to enhance the performance of the modified electrodes, for example, ILs as binders in carbon paste electrodes (CPE) which can then be used as sensing materials as well. In most cases, hydrophobic ILs are used for IL-based carbon paste electrodes (IL-CPE). Contrary to classic CPEs, their binder is composed of charged species and exhibits ionic conductivity which

enhances the electrochemical sensing capabilities of these modified electrodes. Typically, IL-CPEs are prepared as classic CPEs by mixing or grinding the graphite particles with IL and placing the mixture in a cavity of the polymer or glass tube. After polishing, the electrode is ready to use. The IL/graphite particles ratio has to be optimized from the point of view of not only mechanical stability but also capacitive current, resistance, and specific electrode process, and 7:3 graphite-to-IL ratio has become a popular composition. Imidazolium-type ILs also tend to form physical gel when ground with SWCNTs by physical cross-linking of the nanotube bundles, mediated by local molecular ordering of ILs. Recently, ILs have been found to be efficient binders in the preparation of carbon composite/carbon paste electrodes. They are prepared by mixing or grinding graphite particles with the IL, followed by the transfer of this mixture into a cavity of a polymer. Higher currents (both Faradaic and capacitive) are often observed at IL-CPEs compared to traditional CPEs. This is believed to be due to the larger electroactive area for electron transfer in the IL-CPEs due to the conductive IL medium. In traditional oil-based CPEs, electron transfer can only take place at the carbon/aqueous electrolyte interface. Other reasons for the higher currents may also be due to the changes in paste morphology, better solubility of polar analytes in the IL (compared to the binder), or the presence of additional interface where transfer across the liquid/liquid interface can occur.

From all this discussion, it is quite clear that ILs can be easily employed as a modifying component of the electrodes, and in whatever way it is done, they come up with good responses for analyte detection in synthetic and real-world samples. In particular, the higher currents at IL-CPEs compared to oil-CPEs have huge advantages for sensing applications. Task specificity renders high selectivity, if employed in this modification. Otherwise, many of the sensing performance parameters are enhanced up to certain extents, even if the ILs are used randomly. The ease of preparation and the low cost of such sensing systems suggest that this could be a very active field for future sensing of species in the food/drink industry and for environmental monitoring of soil/water samples.

# 2.4.6 Adsorption and Absorption-Based Chemical Sensing Using IL Thin Films

In contrast to electrochemical sensor, the high viscosity of ILs is beneficial for adsorption based sensor since they can be cast into a thin film which makes them suitable for many chemical sensing applications. Being highly volatile, solvents are seldom used as sensing elements. In contrast, ILs have no significant volatility, allowing chemical processes to be carried out with essentially zero emission of toxic organic solvents and enabling their utilization as recognition elements. In these applications, ILs behave as both solid and liquid interfaces simultaneously, thus overcoming the issues associated with the interchangeable use of solid and liquid phases and the requirement of solvents to generate these phases. Depending on the physical phenomenon involved for the solvation of analytes in ILs, a coating of IL can swell, shrink, or undergo a viscosity change. The solvation in ILs is controlled by the variable contributions of adsorption-desorption and partition phenomena depending upon IL and analyte properties to furnish additional selectivity, thus opening up excellent opportunities to design different arrays of chemically selective IL films. Such characteristics make these ILs suitable for the detection of analytes in liquid or atmospheric environments via mass sensing approaches such as Quartz Crystal Microbalance (QCM) or MEMS.

#### 2.4.6.1 IL-Based QCM Mass Sensor

QCM is a mass sensing transducer, the key component of which is quartz that functions for signal transduction and substrate for sensing materials. Applying alternating current to the gold electrodes coated on the quartz wafer induces mechanical oscillations modifiable by interfacial mass changes according to the Sauerbrey's equation:

$$\Delta f = -\frac{\Delta m f_0^2}{A \sqrt{\mu_a \rho_a}} \tag{2.6}$$

Here  $\Delta f$ =frequency shift,  $\Delta m$ =mass changes,  $f_0$ =fundamental frequency, A=electrode area,  $\mu_q$ =quartz shear modulus, and  $\rho_q$ =quartz density. This principle assumes that the foreign mass is strongly coupled to the resonator making it quite straightforward for gas phase operations, where the added mass binds tightly to the surface, and the films are stiff and thin. However, density and viscosity strongly impact the nonrigid systems such as ILs, for which the following expression is used:

$$\Delta f = -f_0^{3/2} \left( \frac{\eta_{\rm L} \rho_{\rm L}}{\pi \mu_{\rm q} \rho_{\rm q}} \right)^{1/2} \tag{2.7}$$

Here  $\eta_L$  = viscosity and  $\rho_L$  = density of the liquid in contact with the crystal. ILs form stable layers just like the polymer matrices; however, being liquids, they bound firmly but not rigidly. QCM is capable of measuring the change of mass as well as the energy dissipation properties of thin films simultaneously, upon analyte adsorption/desorption or partition processes in thin films, thus providing rich information of the dynamic processes occurring during the adsorption–desorption events as depicted in Fig. 2.21. Dai and coworkers [216] first developed a sensor for organic vapors based on QCM using ILs as sensing materials. When analytes were dissolved in an IL, the viscosity of this IL changed rapidly which generated a frequency shift of the QCM device. The response of the QCM depended on the nature of both the analyte and the IL. Some of these ILs also have strong affinities for selected chemical species. Sensors comprising multiple of these sensors, each with a different IL coating, thus can not only detect target analytes but also help identify chemical speciation. In most of these cases, ILs are solely used as sensing films which interact with targets through ion and dipole forces, hydrogen bonding, and



van der Waals interactions on various spatial and temporal scales. All these interactions depend upon variations in ionic composition and structure of ILs, thereby generating a criterion for selective incorporation and interaction of analytes. In addition, great solvation ability of ILs enables the rapid and reversible incorporation of gases, as shown in the work done by our group for detecting different explosive gases [176]. We have also shown that the very different solubilities of ILs for specific reactant gases create a membrane-like selectively to enhance or suppress (preconcentrate) the transport of specific reactants and provide a mechanism for selectivity [90]. Using this principle, we have successfully classified four volatile organic compounds (benzene, hexane, methylene chloride, and ethanol) via seven IL film-based mass sensors, where the unique selectivity of the ILs results from strong hydrogen bond basicity and significant capacity for dipole-type interactions with the analytes [217].

## 2.4.6.2 IL-Thin Film Formation

For the sorption-based sensor too, thin films on the electrodes are usually formed by employing the methods in the electrode modification sections. However, the effectiveness of most thin film-based sorption sensors relies on high sensitivity and specificity of the detection interface. The obvious approach to increase the sensitivity of
OCM sensors is to increase the thickness/amount of the sensing material. Pure ILs inherently possess certain limitations in this regard, especially for low molecular weight analytes, where sensitivity enhancement by thicker IL films can substantially influence the reproducibility through temperature-controlled variations in IL-layer thickness and the spreading out effects. Nonrigidity of thicker films makes the Sauerbrey's equation invalid in addition to slower responses, requiring a strategy to achieve higher IL loading while maintaining the IL-film integrity. For these situations, IL composite films are usually employed. Several approaches have been developed for fabricating IL-composite sensing films. In one such example, ILs are trapped as nanodroplets into the cylindrical cavities of solid alumina matrix, thus avoiding liquid wetting and softness [218]. Although this matrix can hold more IL than planar gold surface, the detection limits were not low enough for selected analytes. Contrarily, conducting polymers (CPs) and polyelectrolytes have charges, which make them ideal template materials to make IL-composite films. The proof of the concept was provided with the example of methane [219], a highly inflammable gas with very low molecular weight, and hence an evidential candidate for higher sensitivity in mass sensing devices requiring abundant total absorption/partition into the films. An ideal template for this purpose should be a porous and stable scaffold that can be modified to generate the required surface area and wettability for IL immobilization. Polyaniline (PAN) can provide this dimensionality. Four different oxidation states of PAN including the doped and undoped ones can be tested for the analytical response with an IL, e.g., 1-ethyl-3-methylimidazolium camphorsulfonate  $[C_2mim][CS]$ , which can form hydrogen bonds through the sulfonate group; however, the doped PAN showed the highest sensitivity being highly charged, facilitating IL wettability through electrostatic interactions, in addition to hydrogen bonding. This increased IL surface area exposed to the analyte. The IL distribution into the nanosized channels of the PAN film helped to increase the response owing to the increase of IL film coverage. UV-vis and FT-IR data in this case confirmed [220] the formation of hydrogen bonds between camphorsulfonate and the nitrogen sites of protic acid-doped PAN. These bonds force the anions to align along the polymer backbone in a comb-like manner so as to enhance the long-range  $\pi$ -orbital conjugation. The interacting methane molecules can fit into these comb spaces and thus an enhanced sensitivity was observed. The enthalpy and entropy of the dissolution were shown to be higher than those in pure IL or PAN which further supported the existence of methane inside the composite generating a more ordered structure. Molecular mechanics simulation agreed with these results as well. This example and others indicate that CPs often have fairly rigid structures with tunable porosity and charge states, which can promote the rational development of the CP/IL interface alongside the IL-controlled parameters. The chemical selectivity can be provided by varying the oxidation states of CP and ionic structure of IL.

Besides this, many useful approaches are available for IL-composite formation both for their use in QCM sensors, biosensors, and even for their electrochemical sensing applications. The most widely used techniques include direct mixing, casting and rubbing, physical adsorption, electrodeposition, layer-by-layer assemblies, and sol-gel encapsulation. Physical adsorption of the IL onto a solid support is most often used to prepare the sensing films, which is based on binding forces including ionic interactions, hydrogen bonds, van der Waals forces, hydrophobic interactions, and so on. However, the more sophisticated methods for this immobilization are electrodeposition, sol-gel encapsulation, and layer-by-layer assembly. In electrodeposition, a clean electrode is immersed in a bath containing the supporting electroactive material and corresponding IL which are then electrochemically deposited onto the electrodes [221, 222]. Electrodeposition of metal nanoparticles onto IL/CNT is another well-studied technique to prepare AuNP/IL/CNT nanocomposite-based sensors [223]. In sol-gel encapsulation, an IL-silica sol is synthesized which is then mixed with different types of interesting molecules to form the films [224], whereas in layer-by-layer method, a sequential deposition of multiple layers is achieved [225], one being the IL and the other one that is supporting material, onto the electrode surface by electrostatic, van der Waals, hydrogen bonding, and charge transfer interactions. From all these approaches, merits and demerits can be identified for any of them; however, the selection is highly related to the particular application in which the approach is going to be applied.

### 2.4.6.3 IL High Temperature Sensor

We have also demonstrated that the IL sensors show great promise for hightemperature gas sensing [226]. For that purpose, a polar IL, trihexyl(tetracdecyl) phosphonium dodecylbenzenesulphonate [ $P_{14,6,6,6}$ ][DBS], was prepared via the alcohol-to-alkyl halide conversion method and coated onto QCM from its ethanol solution. This sensor was studied for the exposure of both polar (ethanol, dichloromethane) and nonpolar (heptane, benzene) vapors even at 200 °C showing linear response pattern and clear signals as shown in Fig. 2.22. As expected thermodynamically, the sensor signal decreased with increasing temperature, but still we could achieve a 5 % detection limit, which is encouraging because most solid surfaces are unable to adsorb vapors at temperatures that much higher than their boiling points. Additionally, there was an excellent reversibility for adsorption–desorption processes, requiring no experimental manipulation for sensor regeneration. The data for the damping resistance showed that physiochemical parameters such as Henry's constant can be more accurately determined at higher temperatures because of the lowered viscosity of the ILs.

### 2.4.6.4 IL Solvation and Other Sensing Platform

Although in many mass sensing applications, IL films play the role of solvents to dissolve the target analytes thereby having a partition coefficient, their roles as solvating species can be best described from the examples of optical sensing. Here, they dissolve many important optical substances to form stabilized optical matrices. For instance, Oter et al. reported [227] an optical CO<sub>2</sub> sensor using the ILs ([C<sub>4</sub>mim] [BF<sub>4</sub>] or [C<sub>4</sub>mim][Br]) as the matrix with 8-hydroxypyrene-1,3,6-trisulfonic acid



Fig. 2.22 Responses shown by IL-sensors from ambient to elevated temperatures for different volatile organic compounds (VOCs)

trisodium salt (HPTS). The detection of  $CO_2$  is based on the fluorescence signal change of HPTS when pairing to  $CO_2$ . More recently, the same group reported [228] that IL modification of an ethyl cellulose matrix extended the detection range to 0-100 % pCO<sub>2</sub>. In comparison to conventional solid matrix or liquid optical sensors, which have leaching problems, short life times because of evaporation of solvents, and poisoning issues from the ambient air and interfering gases, IL-based sensor showed much better performance due to IL's unique properties and better CO<sub>2</sub> adsorption than polymeric materials. Similar principles have been applied for temperature sensors, in which temperature indicators are dissolved in IL matrix to monitor temperatures in microregions, such as in case of microfluidics [229]. A hybrid electrochemical-colorimetric sensing platform for detecting explosives was also developed [230]. The product of the electrochemical reaction was detected by a colorimetric device. A thin layer of [C<sub>4</sub>mim][PF<sub>6</sub>] played an important role in this platform: the IL coating selectively preconcentrated explosives by its solvation power and quickly transported them to the electrodes, and it facilitated the formation of reduction products.

### 2.4.6.5 Detection of Explosives and Chemical Warfare Agents

Although many of the new developments in this area can be covered by one of the previous headings, it seems appropriate to give this topic a separate section to highlight the importance of this area. With the increasing need of sensors for explosive materials at airports and security installations which may be at risk from improvised explosive devices, the interest in developing electrochemical and absorptive sensors for the detection of explosives is growing rapidly, and in the past few years, there have been several reports on the detection of explosive and toxic materials using ILs as solvent/supporting electrolytes. ILs are conductive and have low volatility, allowing them to be deployed in many types of extreme environments (e.g., hot/dry/arid conditions) where other sensor electrolytes would fail. In the prospects of such huge importance, the researchers have even used a combination of different sensing methodologies for these detections. For example, Forzani et al. proposed a hybrid electrochemical-colorimetric sensing platform for the detection of explosive trinitrotoluene (TNT) vapors [230]. A thin layer of the IL [C<sub>4</sub>mim][PF<sub>6</sub>] was found to selectively preconcentrate the explosive materials and quickly transport the analytes to the electrodes. The explosive vapors were detected by electrochemical (cyclic voltammetry) and colorimetric (absorbance change) methods at the working electrode. The observed currents and distinct color changes provide a fingerprint for the identification and quantification of TNT. The same group later employed a conducting polymer nanojunction that was sensitive only to the reduction products of TNT and was able to discriminate from other redox-active interferents found in ambient air. The sensor simultaneously measured the current for the reduction of TNT and the resulting conductance change of the polymer, such as poly(ethylenedioxythiophene) (PEDOT). A linear response (current vs. concentration) was observed at concentrations of 30 pM to 6 nM TNT and the sensor was capable of detecting extremely low levels of TNT within 1-2 min.

Carbon materials have got a real interest in this sense, as they possess high surface area which can enhance the IL distribution in the film as well as help in improving the sensitivity which is critically required for explosive detections. Graphene is even special and, in conjunction with ILs, has been employed for highly selective sensing of explosive TNT by Guo et al. [231]. The IL  $[C_4mim][PF_6]$  was combined with three-dimensional graphene to make an IL-graphene paste electrode with a large surface area, low background current, and pronounced mesoporosity. A linear relationship was observed between peak current using absorptive stripping voltammetry and concentration from 2 to 1,000 ppb, with a low detection limit of 0.5 ppb for TNT. This performance was superior to that demonstrated by IL-CNT and IL-graphite composites. We have also shown for many of explosive targets and employing electrochemical [204], piezoelectric [176], and EQCM platforms that by using IL materials, certain performance parameters can be achieved which are not usually possible with conventional materials.

These interesting works have shown that it is possible to selectively detect highly dangerous explosive and toxic species using an IL as an electrolyte and/or preconcentration medium. In many cases, the IL has been combined with other materials

(e.g., nanomaterials), or the electrochemical technique has been combined with a complementary technique. It seems that the high viscosity of ILs compared to conventional solvent/electrolyte systems (resulting in slower mass transport, smaller diffusion coefficients, and therefore lower currents) may prevent the detection of trace quantities of explosives that are required for a viable real-world sensor. However, perhaps one of their most useful applications could be as electrolytes in sensors that can be deployed directly after an explosion in an enclosed area where temperature could still be high and other electrolytes would volatilize. This would allow for the fast identification of "hot," "warm," and "cold" zones, allowing forensic personnel to determine the areas that are safe to enter for postexplosion analysis.

# 2.5 Future Directions and Concluding Remarks

This chapter gives a brief highlight of the current state of knowledge of IL-electrode interface study and the notable contributions to the sensor fields using IL materials from our laboratories and others. ILs bring in several benefits as nonvolatile and stable electrolytes and solvents for electrochemical sensor as well as sensing materials for adsorption-based mass sensor developments. By synergistically utilizing IL interface electrochemistry as well as molecular design and control of IL composites, ILs-based electrochemical and mass sensors are shown to enable multiple gas detections with multiple modes detection principles that can address many gas sensors challenges, especially for sensors that can operate in unconventional and hostile environments (i.e., elevated temperature, low pressure) or in the presence of typically interfering substances (e.g., high humidity, pyrophorics) as well as for sensor miniaturization and robustness. However, in order to further the developments of ILs for the sensor applications discussed here, many aspects of the behavior of ILs need urgent investigation as well: the fundamental electrochemical issues such as the structure of the double layer and diffusion layer at electrode/ionic liquid interface; the speciation of solute ions such as metal ions and polymerized ions; transference numbers and how these are influenced by speciation; dielectric properties and how these merge with conduction properties as a function of surface chemistry and the wetting phenomena of ILs at gas/liquid/solid interfaces; the thermodynamic quantities such as chemical potentials of solutes in ILs, and how these influence redox potentials and redox reversibility; ion association and its effect on thermodynamic and transport properties; and interactions of ILs with solutes and interfaces. Additionally, ILs have been shown as promising alternative solvents in a variety of applications. However, only a few processes are commercialized due to the relatively high cost of ILs. The recovery and reuse of ILs play an important role in the commercialization of processes employing ILs. The understanding of recyclability of ILs based on the available literature in various application fields is still in its infancy stage which was recognized by ILs' research communities. With ever flourishing research and applications of ILs in the future, the study toward thermal stability of ionic liquids for engineering applications should analyze the ILs with thoughts

on evaporation or temperatures at which evaporation kinetics are known. The temperature-dependent properties and the high dependency of the results on the experimental factors need to be investigated in the comparison of different conditions. In summary, many fundamental aspects of the physical chemistry and electrochemistry of ILs need to be thoroughly investigated, and they promise to further improve the potential of their various electrochemical and chemical applications.

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# **Chapter 3 Reference Systems for Voltammetric Measurements in Ionic Liquids**

Angel A.J. Torriero

# 3.1 Introduction

One of the open problems of electrochemistry in ionic liquids (ILs) nowadays is the choice of a reference electrode. In order to carry out reliable electrochemical measurements in ILs, a robust and stable reference electrode is required. Unfortunately, many literature reports describe the use of poorly chosen, unreliable reference electrodes or the use of quasi-reference electrodes of unknown potential versus any standard potential scale, so they could not be reproduced, being therefore, of little or no value [1]. In addition, the potential differences of reliable reference electrodes in ILs have rarely been measured, preventing the comparison of potential data measured by different research groups in the same IL. A similar situation was reported by IUPAC almost 30 years ago for nonaqueous systems [2]. As a consequence, it is necessary to agree for ILs systems on some procedures and limitations to measure and report electrode potentials versus generally accepted standards. There are in general two possible ways: (a) to use a reference electrode or (b) to refer all potentials versus internal reference redox systems.

# 3.2 Reference Electrodes

The use of quasi-reference (or pseudo-reference) electrodes, QRE, is a common practice in electrochemical studies in nonaqueous solvents, where, as is the case with ionic liquid investigations, well-defined reference electrodes are difficult to

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prepare and stabilize. In most ionic liquids, volatility is not an issue compared to the situation prevailing in some organic solvents in which evaporation can vary the composition of the reference electrode half cell. However, the small volume of IL typically used, in general several tenth or hundred of microliters, in order to perform simple and cost-efficient research, justifies the use of this kind of reference system. The majority of reports that employ QRE in ILs are based on silver [3–12] or platinum wire [13–16] immersed directly into the working solution. Lithium, zinc, and magnesium [17, 18] are less commonly used.

As discussed by Snook and Bond, the function of silver or platinum wire as a ORE is based on the presence of various compounds (most likely oxides) on the metal surface, where the exact identity of those "redox couples" is never known with any confidence [1]. In addition, the amount of the oxidized component(s), which is very small when compared with properly constructed reference electrodes, is also unknown [19]. Therefore, the potential of the QRE is likely to change greatly in the event of (i) reaction with the IL components or impurities present in the media; (ii) dissolution of the oxidized compounds (present onto the metal surface) in the IL; (iii) polarization, due to a lack of potentiostatic control, or (iv) its recent history [20]. These changes can occur dynamically throughout the time period when the wire is immersed in the IL system during, or even as a consequence of, the electrochemical experiment. Therefore, the assumption that the potential(s) of the electrochemical processes of interest recorded against a QRE can be calibrated, at some stage (or before and after the experiment), against a suitable reference electrode or a standard redox compound, cannot always be relied upon to provide an accurate potential value over the entire range of potentials measured.

To illustrate this, the electrochemistry of cobaltocenium, Cc<sup>+</sup>, and ferrocene, Fc, in the protic ionic liquid triethylammonium acetate,  $[HN_{222}][CH_3CO_2]$ , was studied on a glassy carbon electrode (GC, Fig. 3.1) under low water content (<100 ppm) by using an argon-filled glove box. The QRE used in this setup was a silver wire, which together with the platinum wire used as a counter electrode was immersed directly into the working solution. For cobaltocenium (Fig. 3.1a), the mid-point potential,  $E_m$  {where  $E_m$  was calculated from the average of the oxidation ( $E_{\text{peak}}^{\text{anodic}}$ ) and reduction ( $E_{\text{peak}}^{\text{cathodic}}$ ) peak potentials  $\left[E_m = \left(E_{\text{peak}}^{\text{anodic}} + E_{\text{peak}}^{\text{cathodic}}\right)/2\right]$ } is -0.763 V vs. Ag QRE at 0.1 V s<sup>-1</sup>, which systematically shifts to more positive potentials during consecutive scans with increased scan rates, up to a value of -0.623 V vs. Ag QRE at 1.0 V s<sup>-1</sup>. Immediately after this experiment, a solution of 1.9 mM Fc in [HN<sub>222</sub>] [CH<sub>3</sub>CO<sub>2</sub>] was evaluated under identical experimental conditions, and the result is shown in Fig. 3.1b. Here, although there was no systematically increased from 0.1 to 1.0 V s<sup>-1</sup> (0.463 V at 0.1 V s<sup>-1</sup>, and 0.470 V at 0.1 V s<sup>-1</sup>).

The electrochemistry of Fc and Cc<sup>+</sup> was also studied in 1-butyl-3-methylimidazolium hexafluorophosphate,  $[C_4mim][PF_6]$ , 1-butyl-3-methylimidazolium trifluoromethane-sulfonate,  $[C_4mim][CF_3SO_3]$ , and 1-ethyl-3-methylimidazolium tetracyanoborate,  $[C_2mim][B(CN)_4]$ , using an argon-filled glove box [20]. The QRE used in this experiment was a platinum wire, which together with a second platinum wire used as a



**Fig. 3.1** Cyclic voltammograms for (**a**) the reduction of 2.1 mM CcPF<sub>6</sub> and (**b**) oxidation of 1.9 mM Fc in  $[HN_{222}][CH_3CO_2]$  on a GC electrode (diameter = 1 mm) at scan rates of 0.1, 0.2, 0.3, 0.4, 0.5, 0.7, 1.0 V s<sup>-1</sup> and using Ag wire as a QRE.  $T=21\pm1$  °C

counter electrode was immersed directly into the working solution. For cobaltocenium (Fig. 3.2a), the  $E_m$  measured after the Pt wire was immersed for 7 min in [C<sub>4</sub>mim][PF<sub>6</sub>] was –1.082 V at 0.1 V s<sup>-1</sup> (curve *a*). This value systematically shifted to more positive potentials with time, up to a value of –0.829 V after 45 min (curve *c*). This indicates a drift in the QRE potential of around 0.250 V during this timeframe. Figure 3.2b shows voltammograms of 10.3 mM Cc<sup>+</sup> in [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>], where a drift in the  $E_m$  of 0.034 V between two consecutive potential scans is observed. Similar observations were previously reported by Huber and Roling, where a drift of 0.330 V in the Pt wire potential was reported after the QRE was immersed for 10 min in 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide, [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] [21].

For reversible processes, such as Fc and Cc<sup>+</sup> couples, the separation between the potentials of the forward and reverse peaks (called peak-to-peak potential separation),  $\Delta E_{\rm p}$ , at 25 °C, is expected to be 0.059 V. A departure of 20–30 mV from the theoretical value (especially at relatively high scan rates) does not compromise the criterion of reversibility in ILs, as both the slower heterogeneous electron transfer rate constant observed for redox compounds in ILs with respect to organic solvents [22] and the eventual presence of solution resistances not compensated by the electrochemical instrumentation tend to simultaneously "spread" the forward and reverse peaks of Fc and Cc<sup>+</sup>, thus increasing the relative  $\Delta E_{p}$  value. It is worth noting that this is strictly true only if a stable reference system is being used. Figure 3.2c shows voltammograms obtained under the same experimental conditions (including a constant distance between the QRE and the working electrode) in order to avoid changes in the solution resistance. The peak-to-peak potential separation changes from 0.078 V(a) to 0.066 (b) in two consecutive potential scans. As observed in this figure, the ferrocenium reduction peak (Ic) drifts from 0.152 (curve a) to 0.164 V (curve b) vs. Pt QRE, while the oxidation peak (Ia) is unaltered. Therefore, the around 0.006 V error in the mid-point potential determination in Fig. 3.2c, curve a, is directly related to a drift in the Pt QRE potential during the potential scan instead



**Fig. 3.2** Cyclic voltammograms of 10.3 mM Cc<sup>+</sup> (**a** and **b**) and 10.3 mM Fc (**c** and **d**) on a glassy carbon electrode (diameter 1 mm) at scan rate of 0.1 (**a**, **b**, and **d**) and 0.05 V s<sup>-1</sup> (**c**) and using Pt wire as a QRE. (**a**) voltammograms after cleaning the Pt QRE and immersion for (*a*) 7 min, (*b*) 10 min, and (*c*) 45 min in [C<sub>4</sub>mim][PF<sub>6</sub>]. (**b**–**d**) Two consecutive voltammetric scans after Pt QRE cleaning and its immersion (**b**) in [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>], and (**c**, **d**) in [C<sub>4</sub>mim][PF<sub>6</sub>]. Voltammograms were recorded in a homemade argon glove box (H<sub>2</sub>O<100 ppm). Reproduced from [20] with permission from Elsevier

of modification in the uncompensated resistance magnitude. Figure 3.2d shows an extreme experimental situation observed in the same solution when the potential sweep rate was 0.05 V s<sup>-1</sup>. Voltammogram *a* in this figure shows a  $\Delta E_p$  of 0.074 V, however, an important drift in the Pt QRE potential was produced during the consecutive potential sweep scan (curve *b*) affecting the potential of peak Ic, which introduced an error of 0.055 V in the calculated  $E_m$  value.

The most common drift in the QRE potential is shown in Fig. 3.2b, where both cathodic (IIc) and anodic peak (IIa) potentials drift similarly in two consecutive scans, leading to the  $\Delta E_p$  value of around 0.077 V in both voltammograms. Examples of Pt QRE potential drift could also be observed in Fig. 3.2a, where a  $\Delta E_p$ =0.104, 0.127, and 0.112 V is observed in voltammograms *a*, *b*, and *c*, respectively [20].

This series of experiments clearly illustrates the problems associated with the use of QREs, where a variety of influences, including the nature of the IL cation and anion as well as time-dependent changes (most likely related to changes at the surface of the QRE), lead to a variety of different outcomes in terms of the absolute position of the QRE on the potential scale.

Figure 3.3a illustrates cyclic voltammograms obtained at a GC electrode for ferrocene (peaks Ia and Ic) and cobaltocenium (peaks IIc and IIa) redox processes in  $[C_2mim][B(CN)_4]$  using a Ag/AgCl,  $[C_2mim][B(CN)_4]$  reference system separated from the test solution via a glass frit. Using this setup, the potential of the reference system was stable enough to confirm that the distance between the  $E_m$  of Fc and Cc<sup>+</sup> ( $\Delta E_m$ ) in this IL is  $1.325 \pm 0.002$  V and independent of the direction of the scan potential [20]. For comparison, voltammograms obtained under similar conditions in  $[C_2mim][B(CN)_4]$  using a platinum wire QRE showed a  $\Delta E_m$  of 1.293 V and 1.263 V (Fig. 3.3b, curves *a* and *b*, respectively). This indicates an error in the potential measurement of 0.032 V and 0.062 V, respectively. To easily visualize the Pt wire QRE drifts during (and not just between) the voltammetric experiments, all voltammograms in Fig. 3.3 were calibrated against the cobaltocenium/cobaltocene, Cc<sup>+/0</sup>, potential scale. Figures 3.3c and 3.3d display different error magnitudes in



**Fig. 3.3** Two consecutive cyclic voltammograms obtained for the oxidation of Fc and reduction of Cc<sup>+</sup> at a GC electrode (diameter = 1 mm) at  $25 \pm 1$  °C. (**a**) 5.70 mM Cc<sup>+</sup> and 5.55 mM Fc in [C<sub>2</sub>mim] [B(CN)<sub>4</sub>] using a AglAgCl, [C<sub>2</sub>mim][B(CN)<sub>4</sub>] reference electrode; (**b**) 10.1 mM Cc<sup>+</sup> and 10.3 mM Fc in [C<sub>2</sub>mim][B(CN)<sub>4</sub>] using Pt wire as a QRE; (**c**) 10.3 mM Cc<sup>+</sup> and 10.3 mM Fc [C<sub>4</sub>mim][PF<sub>6</sub>] using Pt wire as a QRE; and (**d**) 10.3 mM Cc<sup>+</sup> and 10.5 mM Fc in [C<sub>4</sub>mim][N(Tf)<sub>2</sub>] using Pt wire as a QRE. Voltammograms were recorded in a homemade argon glove box (H<sub>2</sub>O < 100 ppm) at a scan rate = 0.1 V s<sup>-1</sup>. Reproduced from [20] with permission from Elsevier

the  $\Delta E_{\rm m}$  determination in [C<sub>4</sub>mim][PF<sub>6</sub>] and 1-butyl-3-methylimidazolium bis(trifluoro-methylsulfonyl)imide, [C<sub>4</sub>mim][N(Tf)<sub>2</sub>], respectively [20].

Silvester et al. also reported results related with the stability of silver and platinum QREs [23]. The QRE was inserted into a glass tube and separated from the test solution via a vycor tip. The reference electrode was, prior to recording the respective voltammogram, preoxidized for different times by holding the potential at a predetermined value. From this experiment, platinum QRE showed a shift of around 90 mV when the preoxidizing time was increased from 5 to 40 min. Meanwhile, the shift in potential from experiment to experiment in the silver wire QRE was minimized by introducing the wire into a compartment filled with the same IL present in the working solution and separated from this solution by a glass frit [6, 19, 23]. However, even when the behavior of this system may appear to be stable, comparison of day-to-day potential stability indicates a relatively large variability [19].

Activated carbon (AC) has been proposed recently as an alternative ORE for use in ionic liquids [24]. This electrode was tested in 1-ethyl-3-methylimidazolium tetrafluoroborate, [C<sub>2</sub>mim][BF<sub>4</sub>], 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide, [C<sub>2</sub>mim][N(Tf)<sub>2</sub>], 1-ethyl-3-methylimidazolium trifluorotris(pentafluoroethyl)phosphate, [C<sub>2</sub>mim][FAP], and 1-methyl-1-propylpyrrolidinium bis(trifluoromethylsulfonyl)imide, [C<sub>3</sub>mPyr][N(Tf)<sub>2</sub>], using ferrocene (50 mM) as the redox probe. Although the AC ORE is stable for more than 40 h and it is not affected by impurities, the electrode showed a potential of  $0.190 \pm 0.010$  V vs. Fc<sup>0/+</sup> independently of the IL used. This last point is a real concern, because recent studies have proven that  $Fc^{0/+}$  redox process is sensible to the solvation effect of ILs, and a difference in the  $E_m$  of Fc of approximately 0.092 V was observed when the IL was changed from [C<sub>2</sub>mim][FAP] to 1-butyl-3-methylimidazolium tetrafluoroborate,  $[C_4 mim][BF_4]$  (see below) [25]. Consequently, a variation on the potential of  $Fc^{0/+}$ vs. AC QRE is expected by changing the nature of the IL. It is worth noting that the last-mentioned ILs are similar to those used to validate the AC ORE. Consequently, more studies are required to prove the applicability of this new ORE to IL solvent systems.

A highly stable reference system in IL was described by Snook et al., which was formed by immersing a silver wire in a fixed concentration of silver trifluoromethanesulfonate (Ag[CF<sub>3</sub>SO<sub>3</sub>]) dissolved in [C<sub>4</sub>mPyr][N(Tf)<sub>2</sub>] and separated by a porous junction from the test solution [19]. This reference electrode, when stored in an argon-filled glove-box away from light, was found to be stable for 3 weeks, but it drifts significantly at longer times. The reproducibility of this electrode was studied by repeated preparations of the AglAg<sup>+</sup>(10 mM Ag[CF<sub>3</sub>SO<sub>3</sub>], [C<sub>4</sub>mPyr] [N(Tf)<sub>2</sub>]) electrode, which gave a variation in potential of  $\pm 2$  mV. Once prepared, the reproducibility intra- and interday was of  $\pm 0.001$  V, for up to about 3 weeks [19].

Even when this electrode was proven to be useful in different ILs, in situations where a large number of experiments are to be performed in the same IL, it is recommended to prepare the  $Ag|Ag^+$  reference electrode using the IL under study as the solvent in the reference system and evaluate its potential against a standard redox compound.

Table 3.1 shows that the potential of an AglAg<sup>+</sup> system is highly dependent on the ionic liquid used in the reference electrode compartment and varies by more than 0.600 V vs. Fc<sup>0/+</sup>. In order to overcome this issue, Lewandowski et al. have proposed the use of cryptand reference electrodes, which are prepared by immersing a silver wire in a solution of 0.01 M silver perchlorate and 0.1 M cryptand 222 ligand (4,7,13,16,21,24-hexaoxa-1,10-diazobicyclo[8,8,8]hexacosane) in an IL or with the use of an organic solvent ([AglAg<sup>+</sup> 222, R] where R represents the IL or the organic solvent used) [26, 30, 31]. The  $E_m$  of Fc<sup>0/+</sup> vs. [AglAg<sup>+</sup> 222, CH<sub>3</sub>CN] varies by around 0.110 V in different ILs, and between 0.240 and 1.000 V when compared with a AglAg<sup>+</sup>(10 mM Ag[CF<sub>3</sub>SO<sub>3</sub>], IL) system in the same IL (Table 3.1).

$E_{\rm m}$ (V)	Reference electrode	Ref
-0.39	Ag 10 mM Ag[CF <sub>2</sub> SO <sub>2</sub> ]	[19]
-0.45	Agl100 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]	[19]
0.55	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.04	Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]	[20]
0.40	AglAgCl, [Bu <sub>4</sub> N]Cl(0.1 M), CH <sub>3</sub> CN <sup>b</sup>	[27]
-0.58	Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]	[20]
0.46	AglAgCl, [Bu <sub>4</sub> N]Cl(0.1 M), CH <sub>3</sub> CN <sup>b</sup>	[27]
-0.51	AglAg[BF <sub>4</sub> ] <sub>(sat)</sub>	[28]
-0.25	Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]	[20]
0.26	Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]	[20]
0.50	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
-0.37	Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]	[20]
0.20	Agl10 mM Ag[N(Tf)2]	[21]
0.52	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.46	AglAg <sup>+</sup> Kryptofix22, CH <sub>3</sub> CN <sup>c</sup>	[29]
0.45	AglAgCl, [Bu <sub>4</sub> N]Cl(0.1 M), CH <sub>3</sub> CN <sup>b</sup>	[27]
-0.49	d	[28]
0.57	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.52	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.53	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.55	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.56	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.48	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.44	AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>	[26]
0.39	AglAg <sup>+</sup> Kryptofix22, CH <sub>3</sub> CN <sup>c</sup>	[29]
	$\begin{array}{c} E_{\rm m}\left({\rm V}\right) \\ -0.39 \\ -0.45 \\ 0.55 \\ 0.04 \\ 0.40 \\ -0.58 \\ 0.46 \\ -0.51 \\ -0.25 \\ 0.26 \\ 0.50 \\ -0.37 \\ 0.20 \\ 0.52 \\ 0.46 \\ 0.45 \\ -0.49 \\ 0.57 \\ 0.52 \\ 0.53 \\ 0.55 \\ 0.56 \\ 0.48 \\ 0.44 \\ 0.39 \\ \end{array}$	$E_{\rm m}$ (V)Reference electrode-0.39Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]-0.45Agl100 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]0.55AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.04Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]0.40AglAgCl, [Bu <sub>4</sub> N]Cl(0.1 M), CH <sub>3</sub> CN <sup>b</sup> -0.58Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]0.46AglAgCl, [Bu <sub>4</sub> N]Cl(0.1 M), CH <sub>3</sub> CN <sup>b</sup> -0.51AglAg[BF <sub>4</sub> ] <sub>(sat)</sub> -0.52Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]0.26Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]0.50AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> -0.37Agl10 mM Ag[CF <sub>3</sub> SO <sub>3</sub> ]0.50AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> -0.37Agl10 mM Ag[N(Tf) <sub>2</sub> ]0.52AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.46AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.45AglAgCl, [Bu <sub>4</sub> N]Cl(0.1 M), CH <sub>3</sub> CN <sup>b</sup> -0.49d0.57AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.52AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.53AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.55AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.56AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.56AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.48AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.44AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup> 0.45AglAg <sup>+</sup> 222, CH <sub>3</sub> CN <sup>a</sup>

 Table 3.1 Mid-point potentials of the ferrocene/ferrocenium redox process against different

 Ag-based reference electrodes

<sup>a</sup>AglAgClO<sub>4</sub>(0.01 M) 222(0.1 M), acetonitrile

 $^{b}50 \ \mu\text{L}$  of a 1 M [Bu<sub>4</sub>N]Cl acetonitrile solution was mixed with 450  $\mu\text{L}$  of the respective IL to give a final concentration of 0.1 M [Bu<sub>4</sub>N]Cl in the reference compartment

<sup>c</sup>AglAgNO<sub>3</sub>(0.01 M) Kryptofix<sup>®</sup>22(0.1 M) (Kryptofix<sup>®</sup>22=1,7,10,16-tetraoxa-4,13-diazacyclo-octadecane)

<sup>d</sup>AglAg[N(Tf)<sub>2</sub>] reference electrode, where the Ag[N(Tf)<sub>2</sub>] concentration was not reported

Consequently, different factors such as (i) silver ion coordination or solvation by the IL anions and/or cryptand 222 ligand, (ii) junction potential, and (iii) effect of IL nature on the  $E_m$  of Fc (discussed below) could simultaneously be operative and responsible for the observed potential variation [20]. The stable lifetime of the [AglAg<sup>+</sup> 222, CH<sub>3</sub>CN] reference electrode is about 4 weeks and, thereby, similar to that reported by Snook et al. [19], even when the silver(I) stability is increased by the formation of the Ag<sup>+</sup>-222 inclusion complex [30].

Rogers et al. have studied the kinetics of the Ag|Ag<sup>+</sup> system in  $[C_4 mPyr][N(Tf)_2]$ and found that the interconversion of Ag and Ag<sup>+</sup> is slow, with a charge transfer rate constant  $(k^{0'})$  of 2.0 cm × 10<sup>-4</sup> s<sup>-1</sup> when using the Ag[CF<sub>3</sub>SO<sub>3</sub>] salt [32]. It is even slower when  $[N(Tf)_2]^-$  is used as the counter ion  $(1.5 \times 10^{-4} \text{ cm s}^{-1})$  and yet again slower with nitrate as the counter ion  $(1.0 \times 10^{-5} \text{ cm s}^{-1})$ . This means fast measurements such as a fast scan rate cyclic voltammetry if a two-electrode system is utilized and high-frequency electrochemical impedance spectroscopy (EIS) if a three-electrode system is utilized could be limited [32]. Even in aqueous systems using a AglAgCl reference electrode in a three-electrode setup, the use of EIS is limited to frequencies below 10 kHz. Above this range, artifacts (e.g., inductive loops) due to the sluggish kinetics of the reference half-cell reaction will begin to dominate. To minimize this kinetic limitation with the reference electrode, Rogers et al. [32] have introduced the TMPD/TMPD<sup>++</sup> couple (TMPD=N,N,N',N'tetramethyl-p-phenylenediamine) as a reference electrode of the third kind (Type III or reference electrodes of the third kind involve immersing an inert metal (e.g., platinum) in a solution containing both halves of a redox couple). In this case,  $k^{0'}$  is an order of magnitude higher  $(2.6-2.8 \times 10^{-3} \text{ cm s}^{-1})$  but does depend on the counter ion used. However, a true TMPD/TMPD+\* reference electrode was not actually constructed. Rather, the voltammetry of a solution of TMPD and of TMPD<sup>+\*</sup> was measured using a quasi-reference electrode in the form of a silver wire, in order to carry out charge transfer rate constant calculations. The authors recognize that the availability, solubility, and stability of the TMPD radical cation salt may limit the use of TMPD/TMPD<sup>+•</sup> in the construction of a reference electrode of the third kind [32].

In a work by Andriyko et al., an AgCl-coated Ag wire (or AglAgCl reference electrode) was immersed in  $[C_4 dmim][BF_4]$  containing a saturated solution of AgCl [33]. The reference electrode was contained in a Vycor fritted separate compartment for studies in  $[C_4 dmim]^+$ -based ionic liquids. A similar reference electrode configuration was employed by Ikeda and colleagues [34]. However, even when this AglAgCl system could, in principle, be used to construct reference electrodes in many ionic liquids, the AgCl coating is prone to being stripped off from the Ag wire, as it is often partly soluble or sparingly soluble in many ionic liquids [35], thereby introducing instability in the reference electrode system, which in addition acts as a source of impurities in the general electrochemical setup.

Saheb et al. described an AglAg<sup>+</sup> reference electrode (for use in an imidazolium-based ionic liquid) in which the concentration of silver ion was established by addition of silver(I) nitrate in acetonitrile [27]. A problem noted with the use of this system is that the potential of the reference half cell varies significantly with the volume fraction of acetonitrile, which is likely to vary after extended periods of use [27]. Lordermeyer et al. also used an acetonitrile-based reference electrode to study the electroplating of dysprosium from an ionic liquid [36]. Other studies have described the use of the saturated calomel electrode (aqueous based) in electrochemical investigations in ionic liquids [37–40]. However, a problem with these and related approaches is that large junction potentials may exist between the two very different media (molecular solvent in the reference compartment and IL in the working solution compartment) and a contamination of the IL with the molecular solvent part of the reference system is unavoidable [20].

# 3.3 Internal Reference Redox Scales

Internal reference redox scales or internal reference redox systems, IRRS, are reversible or nearly reversible redox systems used to provide a known and stable reference point in nonaqueous solvents in conditions where reliable reference electrodes are difficult to be established and/or stabilized [20]. In general, IRRS is used in conjunction with a QRE [18, 41–44].

The establishment of a solvent-independent reference electrode for the comparison of redox potentials in nonaqueous systems has a long story. It began with the concept of RblRb<sup>+</sup> or Rb(Hg)lRb<sup>+</sup>, followed by the proposal of using organometallic redox couples [2]. In order to limit the number of redox systems used and then make the comparison easier, IUPAC recommended that the systems ferrocenelferrocenium,  $Fc^{0/+}$ , and bis(biphenyl)chromium(0)lbis(biphenyl)chromium(I), BCr<sup>0/+</sup>, need to be used as internal reference redox systems in nonaqueous media [2]. These two complexes were selected arbitrarily from several published redox systems [2].

An effective IRRS must possess a number of properties, many of which were suggested by Gritzner and Kuta in their IUPAC recommendation, and most of which can be deduced by common sense [2]. We recently suggested the following to be essential properties of an IRRS [45]:

- 1. The  $OX_{IRRS}/RED_{IRRS}$  redox couple ( $OX_{IRRS} + e \leftrightarrows RED_{IRRS}$ ; being  $OX_{IRRS}$  and  $RED_{IRRS}$  the oxidized and reduced form of IRRS, respectively) must be reversible or nearly reversible under the operative measurement conditions. It is advantageous for the IRRS electron transfer to be a simple one-electron outer-sphere electron transfer.
- 2. It is very important that the IRRS redox moieties do not specifically interact with the working electrode (e.g., they do not adsorb on the working electrode).
- 3. The mid-point potential for IRRS should not overlap the active potential zone of the analyte (ANS) under study.
- The initially present IRRS redox component, OX<sub>IRRS</sub> or RED<sub>IRRS</sub>, must be stable over the time period of experimentation; it should not react with the solvent, supporting electrolyte or ANS.
- IRRS redox moiety, OX<sub>IRRS</sub> or RED<sub>IRRS</sub>, which is not initially present, must be stable on the timescale required to execute the slowest cyclic voltammetry (CV).

6. The molecule or salt that is the source of the selected IRRS component should be pure, easily synthesized, or otherwise, readily available and should have a long shelf life.

There are also some constraints and requirements for ANS [45]:

- 1. ANS is initially present as either an oxidizable moiety ( $RED_{ANS}$ ) or reducible moiety ( $OX_{ANS}$ ). It is worth noting that  $RED_{ANS}$  and  $OX_{ANS}$  species may or may not be redox partners, and the oxidation of  $RED_{ANS}$  and reduction of  $OX_{ANS}$  may be complicated.
- 2. The initially present ANS moiety should be stable and should not react with IRRS.

It is necessary to notice that IUPAC recommendation has been proposed for organic solvents and their mixtures. By extrapolation from those systems, the  $Fc^{0/+}$  redox couple is also being used as an IRRS in ionic liquids [18, 26, 46, 47].

Nowadays, it is well known that Fc is not an "ideal" redox process as mentioned in the IUPAC recommendation, as its formal potential is highly dependent on the solvation effects of the organic solvent and supporting electrolyte used [48, 49]. There are two types of solvation around the Fc molecule, which includes the electrostatic interaction of solvent/electrolyte with (i) the iron center and (ii) the cyclopentadienyl ring [48]. Yang et al. has recently computed the molecular electrostatic potential (MEP) for ferrocene and ferrocenium ion (Fig. 3.4) [50]. As seen in



**Fig. 3.4** Isovalue molecular electrostatic potential surface for Fc and Fc<sup>+</sup> at the B97-D/6-311++G<sup>\*\*</sup> level. *Red* is for the positive potential, and *blue* is for the negative potential. (a) Isovalues of -0.013 a.u. (*blue*) and 0.030 a.u. (*red*) are presented for Fc; (b) isovalues of 0.10 a.u. (outer surface) and 0.15 a.u. (inner surface) are presented for Fc<sup>+</sup>. Reproduced from [50] with permission from the PCCP Owner Societies

Fig. 3.4a, negative electrostatic potentials are observed on the top of the Fc cyclopentadienyl rings and as a planetary distribution on a plane going through the central iron atom, which favor the electrostatic interaction between Fc and positively charged molecules and ions (including electron–acceptor moieties). Meanwhile, an interaction with electron–donor moieties from the solvent and/or electrolyte is also possible from the side of the cyclopentadienyl rings, due to the presence of a positive electrostatic potential. A different situation can be observed for the ferrocenium ion MEP (Fig. 3.4b), where only positive electrostatic potentials are observed. In this last situation, the electrostatic interaction between Fc<sup>+</sup> and either negatively charged ions or molecules with electron–donor moieties is favored. The MEP difference between Fc and Fc<sup>+</sup> is very important to understand the dissimilarities in the mass transport properties of Fc and Fc<sup>+</sup> observed experimentally in different ionic liquids (see below).

Decamethylferrocene (DmFc or  $[Fe^{II}(\eta^5-C_5(CH_3)_5)_2]$ ) shows at least an order of magnitude weaker solvent–solute interaction (in organic solvent systems) compared to ferrocene, as the methyl-substituent groups in the cyclopentadienyl rings prevent both specific (previously mentioned for Fc) and nonspecific interactions by hindering the access of organic solvent and supporting electrolyte molecules to the metal center and to the cyclopentadienyl ring [48, 51–54]. This observation was also confirmed after analysis of the X-ray diffraction patterns of decamethylferrocene, which indicate that the inter-ring methyl groups of DmFc are within Van der Waals distances [55]. Consequently, DmFc is better suited than Fc as an IRRS in organic solvents.

Decamethylferrocene is oxidized in organic solvents in a reversible, one-electron transfer process to decamethylferrocenium (DmFc<sup>+</sup> or  $[Fe^{III}(\eta^5-C_5(CH_3)_5)_2]^+$ ) and reduced back to DmFc according to Eq. (3.1). The  $E_m$  value of this redox couple is more negative than that of Fc as a consequence of the electron-donating effect of the methyl groups (inductive effect) which, by pushing electron density toward the metal ion, facilitates electron removal by the electrode. As given in Table 3.2, the difference in the  $E_m$  values between Fc<sup>0/+</sup> and DmFc<sup>0/+</sup> varies from a low of 0.413±0.005 V in tetrahydrofuran/0.1 M [Bu<sub>4</sub>N][BF<sub>4</sub>] to a high of 0.614±0.005 V in dichloromethane/0.1 M [Bu<sub>4</sub>N][TFAB] ([TFAB] =  $[B(C_6F_5)_4]^-$ ), which represents a difference of 0.201 V. Furthermore, a variation of about 0.152 V can be observed by changing the organic solvent form tetrahydrofuran to 2,2,2-trifluoroethanol and keeping constant the supporting electrolyte nature and concentration (0.1 M  $[Bu_4N]$ [ClO<sub>4</sub>]). To minimize uncertainties in the comparison of mid-point potentials in Table 3.2, all potentials quoted are relative to the  $DmFc^{0/+}$  potential scale. Consequently, since the values presented in this table represent the difference in  $E_{\rm m}$ , the variations in the absolute values of  $E_m$  of the Fc<sup>0/+</sup> and DmFc<sup>0/+</sup> IRRS may probably be larger than those indicated here.

$$\left[\operatorname{Fe}^{\mathrm{II}}\left(\eta^{5}-\operatorname{C}_{5}\left(\operatorname{CH}_{3}\right)_{5}\right)_{2}\right] \leftrightarrows \left[\operatorname{Fe}^{\mathrm{III}}\left(\eta^{5}-\operatorname{C}_{5}\left(\operatorname{CH}_{3}\right)_{5}\right)_{2}\right]^{+}+e^{-}$$
(3.1)

The solvent–Fc interaction is also present in ILs. This issue was addressed by studying the effect of ionic liquid structure on the mid-point potentials of Fc and DmFc in 11 different ILs as well as in dichloromethane with added IL as the

Solvent	Electrolyte	Fc <sup>0/+</sup> vs. DmFc <sup>0/+</sup> (V)	Ref
Diethyl ether	0.1 M [Bu <sub>4</sub> N][BArF <sub>24</sub> ] <sup>a</sup>	$0.550 \pm 0.005$	[ <b>49</b> ]
	0.1 M Na[BArF <sub>24</sub> ] <sup>a</sup>	$0.583 \pm 0.005$	[49]
Anisole	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.518 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.607 \pm 0.005$	[49]
Methanol	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.497 \pm 0.002$	[48]
Ethanol	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.473 \pm 0.005$	[48]
2,2,2-Trifluoroethanol	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.575 \pm 0.004$	[48]
2-Propanol	0.1 M [Bu <sub>4</sub> N][CF <sub>3</sub> SO <sub>3</sub> ]	$0.455 \pm 0.003$	[48]
Tetrahydrofuran	0.1 M [Bu <sub>4</sub> N][BF <sub>4</sub> ]	$0.413 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][CF <sub>3</sub> SO <sub>3</sub> ]	$0.438 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.423 \pm 0.005$	[ <b>49</b> ]
		$0.427 \pm 0.002$	[48]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.446 \pm 0.005$	[ <b>49</b> ]
	0.1 M [Bu <sub>4</sub> N][BPh <sub>4</sub> ]	$0.485 \pm 0.005$	[ <b>49</b> ]
	0.1 M Na[BArF <sub>24</sub> ] <sup>a</sup>	$0.502 \pm 0.005$	[ <b>49</b> ]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.484 \pm 0.005$	[ <b>49</b> ]
	0.1 M [Bu <sub>4</sub> N][BArF <sub>24</sub> ] <sup>a</sup>	$0.521 \pm 0.005$	[ <b>49</b> ]
Pyridine	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.517 \pm 0.004$	[48]
Dichloromethane	0.1 M [Bu <sub>4</sub> N]Cl	$0.534 \pm 0.005$	[ <b>49</b> ]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.532 \pm 0.002$	[48]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.548 \pm 0.003$	[56]
	0.1 M [Et <sub>4</sub> N][BF <sub>4</sub> ]	$0.541 \pm 0.003$	[57]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.614 \pm 0.005$	[ <b>49</b> ]
	0.1 M [C <sub>4</sub> mPyr][FAP]	$0.589 \pm 0.003$	[57]
	0.1 M [C <sub>2</sub> mim][FAP]	$0.590 \pm 0.003$	[57]
	0.1 M [C <sub>2</sub> mim][B(CN) <sub>4</sub> ]	$0.588 \pm 0.003$	[57]
	0.1 M [C <sub>4</sub> mim][N(Tf) <sub>2</sub> ]	$0.570 \pm 0.003$	[57]
	0.1 M [C <sub>4</sub> mPyr][N(Tf) <sub>2</sub> ]	$0.568 \pm 0.003$	[57]
	0.1 M [C <sub>2</sub> mim][FSI]	$0.569 \pm 0.003$	[57]
	0.1 M [C <sub>3</sub> mim][FSI]	$0.568 \pm 0.003$	[57]
	0.1 M [C <sub>4</sub> mPyr][N(CN) <sub>2</sub> ]	$0.564 \pm 0.003$	[57]
	0.1 M [C <sub>4</sub> mim][PF <sub>6</sub> ]	$0.556 \pm 0.003$	[57]
	0.1 M [C <sub>4</sub> mim][BF <sub>4</sub> ]	$0.557 \pm 0.003$	[57]
	0.1 M [C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	$0.556 \pm 0.003$	[57]
1,2-Dichloroethane	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.532 \pm 0.001$	[48]
1,2-Dibromoethane	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.475 \pm 0.007$	[48]
Benzonitrile	0.1 M [Bu <sub>4</sub> N]Cl	$0.524 \pm 0.005$	[ <mark>49</mark> ]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.523 \pm 0.001$	[48]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.530 \pm 0.005$	[ <mark>49</mark> ]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.543 \pm 0.005$	[ <b>49</b> ]
Bromobenzene	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.489 \pm 0.005$	[48]

**Table 3.2** Redox potentials of ferrocene versus decamethylferrocene $^{0/+}$  redox couple in differentorganic media

(continued)

Solvent	Electrolyte	Fc <sup>0/+</sup> vs. DmFc <sup>0/+</sup> (V)	Ref
Chlorobenzene	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.497 \pm 0.001$	[48]
1,2-Dichlorobenzene	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.535 \pm 0.001$	[48]
Benzyl alcohol	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.508 \pm 0.003$	[48]
Nitrobenzene	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.514 \pm 0.002$	[48]
Aniline	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.527 \pm 0.004$	[48]
Toluene	$[Bu_4N][BF_4]^c$	$0.430 \pm 0.005$	[49]
Acetone	0.1 M [Bu <sub>4</sub> N]Cl	$0.451 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.479 \pm 0.004$	[48]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.487 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.504 \pm 0.005$	[49]
Propylene carbonate	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.495 \pm 0.002$	[48]
Acetonitrile	0.1 M [Bu <sub>4</sub> N]Cl	$0.501 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.505 \pm 0.002$	[48]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.509 \pm 0.003$	[56]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.517 \pm 0.005$	[49]
Nitromethane	0.1 M [Bu <sub>4</sub> N]Cl	$0.505 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.516 \pm 0.004$	[48]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.510 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.516 \pm 0.005$	[49]
Formamide	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.510 \pm 0.003$	[48]
N-methylformamide	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.510 \pm 0.002$	[48]
N,N-dimethylformamide	0.1 M [Bu <sub>4</sub> N]Cl	$0.475 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.458 \pm 0.003$	[48]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.478 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.493 \pm 0.005$	[49]
N,N-dimethylacetamide	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.455 \pm 0.008$	[48]
Dimethyl sulfoxide	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$0.486 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][TFAB] <sup>b</sup>	$0.493 \pm 0.005$	[49]
	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.468 \pm 0.001$	[48]
Chloroform	0.1 M [Bu <sub>4</sub> N][ClO <sub>4</sub> ]	$0.483 \pm 0.001$	[48]

Table 3.2 (	continued)
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 $^{a}[BArF_{24}] = [B(C_{6}H_{3}(CF_{3})_{2})_{4}]^{-}$ 

 ${}^{b}[TFAB] = [B(C_{6}F_{5})_{4}]^{-}$ 

°The toluene:[Bu<sub>4</sub>N][BF<sub>4</sub>] electrolyte is of the 3:1 stoichiometry

supporting electrolyte [57]. As evidenced in Table 3.3, a variation in the  $E_{\rm m}$  of Fc vs. DmFc<sup>0/+</sup> of about 0.100 V is observed when the IL was changed from [C<sub>4</sub>mim] [CF<sub>3</sub>SO<sub>3</sub>] to [C<sub>2</sub>mim][FAP] under neat conditions (water content <100 ppm). Similarly, when DmFc and Fc were simultaneously present in dichloromethane with added IL as the supporting electrolyte—conditions under which DmFc is less sensitive to solvation effects—a variation in the  $E_{\rm m}$  of Fc vs. DmFc<sup>0/+</sup> of about 0.050 V was observed when the supporting electrolyte was changed from 0.1 M [Et<sub>4</sub>N][BF<sub>4</sub>] to 0.1 M [C<sub>2</sub>mim][FAP] (Table 3.2). A variable potential difference

		$E_{\rm m}$ vs. DmFc <sup>0/+</sup> (V)		$E_{\rm m}$ vs. Fc <sup>0/+</sup> (V)	
IL	Electrode	Fc	Cc <sup>+</sup>	Cc <sup>+</sup>	Ref
[C <sub>4</sub> mPyr][FAP]	GC	0.575ª	-0.747ª	-1.322ª	[20, 57]
[C <sub>2</sub> mim][FAP]	GC	0.574ª	-0.749ª	-1.323ª	[20, 57]
[C <sub>2</sub> mim][B(CN) <sub>4</sub> ]	GC	0.526ª	-0.799ª	-1.325 <sup>a</sup>	[20, 57]
[C <sub>2</sub> mim][N(Tf) <sub>2</sub> ]	Au, Pt, GC	0.520ª	-0.820ª	-1.330ª	[21, 58]
[C <sub>4</sub> mim][N(Tf) <sub>2</sub> ]	GC	0.514ª	-0.813ª	-1.327ª	[20, 57]
$[C_3mPyr][N(Tf)_2]$	Pt	-	-	-1.325 <sup>b</sup>	[59]
	GC	-	-	-1.327 <sup>b</sup>	[59]
$[C_4 mPyr][N(Tf)_2]$	GC	0.511ª	-0.816ª	-1.327ª	[20, 57]
	Au	-	-	-1.363 <sup>b</sup>	[ <b>59</b> ]
	Pt	-	-	-1.333°	[19]
$[S_{221}][N(Tf)_2]$	Au	-	-	-1.348 <sup>b</sup>	[ <b>59</b> ]
[S <sub>222</sub> ][N(Tf) <sub>2</sub> ]	Au	-	-	-1.354 <sup>b</sup>	[59]
[C <sub>3</sub> mpip][N(Tf) <sub>2</sub> ]	Au	-	-	-1.362 <sup>b</sup>	[ <b>59</b> ]
[HmimSC <sub>4</sub> ][N(Tf) <sub>2</sub> ]	Au, Pt, GC	0.510ª	-0.830ª	-1.330 <sup>a</sup>	[58]
[C <sub>2</sub> mim][FSI]	GC	0.512ª	-0.820ª	-1.332ª	[20, 57]
[C <sub>3</sub> mPyr][FSI]	GC	0.510ª	-0.822ª	-1.332ª	[20, 57]
[C <sub>2</sub> mim][N(CN) <sub>2</sub> ]	GC	-	-	-1.332 <sup>b</sup>	[59]
	Pt	-	-	-1.355 <sup>b</sup>	[59]
[C <sub>4</sub> mPyr][N(CN) <sub>2</sub> ]	GC	0.505ª	-	-	[20, 57]
[C <sub>4</sub> mim][PF <sub>6</sub> ]	GC	0.478ª	-0.851ª	-1.329ª	[20, 57]
[C <sub>2</sub> mim][BF <sub>4</sub> ]	GC	-	-	-1.336 <sup>d</sup>	[60]
[C <sub>4</sub> mim][BF <sub>4</sub> ]	GC	0.478ª	-0.848ª	-1.326ª	[20, 57]
[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	GC	0.474ª	-0.854ª	-1.328ª	[20, 57]
	Au	-	-	-1.362 <sup>b</sup>	[59]
[C <sub>4</sub> mPyr][CF <sub>3</sub> SO <sub>3</sub> ]	GC	-	-	-1.347 <sup>b</sup>	[59]

 Table 3.3 Redox potentials of transition-metal sandwich complexes obtained by cyclic voltammetry in different ionic liquids

<sup>a</sup>Potentials were obtained using a scan rate of 0.1 V s<sup>-1</sup>.  $E_m$  values were obtained with an accuracy of ±0.003 V (n=5)

<sup>b</sup>No experimental error was reported

 $^{\circ}E_{\rm m}$  value was obtained with an accuracy of ±0.001 V

 ${}^{d}E_{\rm m}$  values were obtained with an accuracy of ±0.002 V

which increases from 0.014 V in the case of  $[C_4mPyr][FAP]$  to 0.082 V in the case of  $[C_4mim][CF_3SO_3]$  is noticed from the comparison of the  $E_m$  of Fc vs. DmFc<sup>0/+</sup> between neat ILs and diluted conditions (dichloromethane with added IL as the supporting electrolyte) [57].

This interaction between Fc and IL ions has been theoretically studied by Yang et al. [50]. According to their MEP predictions, the possible interactions of ferrocene with 1,3-dimethylimidazolium tetrafluoroborate ( $[C_1mim][BF_4]$ , used as an IL model system) are shown in Figs. 3.5 and 3.6. In Fig. 3.5, it is possible to observe that the IL cation binds to Fc both on the top and from the side. Meanwhile, the IL anion is only able to interact with Fc from the side (Fig. 3.6).



**Fig. 3.5** Optimized geometries for Fc– $[C_1mim]^+$  complexes. Distances are in Å, and angles are in degrees. Molecules are rendered in CPK style, with carbon in *cyan*, nitrogen in *blue*, hydrogen in *white*, and iron in *pink*. The sphere for ion atom is lightly shrunk for clearer geometrical parameters labeling. (**a**)  $[C_1mim]^+$  is perpendicular to the Cp plane of Fc (*left*: side view; *right*: top view). The *purple arrow* shows the H2–Cp distance; (**b**)  $[C_1mim]^+$  is tilted on top of the Cp plane (*left*: side view; *right*: top view); (**c**)  $[C_1mim]^+$  "orbits" around Fc, with H2–Fe distance of 2.64 Å (*left*: side view; *right*: top view). Reproduced from [50] with permission from the PCCP Owner Societies

As shown in Fig. 3.4b, ferrocenium ion only has positive electrostatic potentials. Thereby, a strong and exclusive interaction between the +1 charged ferrocenium ion with the IL anion is expected [50]. This interaction could form a stable and tight first solvation shell of anions, around which the IL cation could occupy the second solvation shell by strong electrostatic interactions with the anionic shell [50]. Consequently, the hydrodynamic radius of the diffusing Fc<sup>+</sup> species will be largely affected (increased), decreasing the mass transport rate of this oxidized species with respect to that of Fc. This implies the appearance of an inequality in the values of the diffusion coefficient for the reduced ( $D_R$ ) and oxidized ( $D_0$ ) component of the Fc<sup>0/+</sup> redox couple (Table 3.4) and a net effect in the  $E_m$  (Eq. 3.2) and in the half-wave potential,  $E_{1/2}$  (Eq. 3.3), experimentally obtained [25]. For example, the  $E_{1/2}$  obtained with the use of ultramicroelectrodes is larger by (RT/nF) ln ( $D_R/D_o$ ) than the  $E^{\theta'}$ , the value of which is between 0.007±0.001 and 0.017±0.002 V depending on the IL used (Table 3.4).

$$E_m = E^{\theta'} + \frac{RT}{nF} \ln \sqrt{\frac{D_R}{D_O}}$$
(3.2)



**Fig. 3.6** Optimized geometries for the  $Fc-[BF_4]^-$  complex. Distances are in Å, and angles are in degrees. Molecules are rendered in the same scheme as in Fig. 3.5. The complex structure is shown from the different perspectives in (a)–(c). Reproduced from [50] with permission from the PCCP Owner Societies

Table 3.4 Effect of diffusion coefficient inequality on the mid-point potential observed between  $DmFc^{0/4}$  and  $Fc^{0/4a}$ 

IL	$\frac{D_{\rm Fc}}{D_{\rm Fc+}}$	$\frac{D_{\rm DmFc}}{D_{\rm DmFc+}}$	$\frac{RT}{nF} \ln \frac{D_{Fc}}{D_{Fc+}}$ (10 <sup>-3</sup> V)	$\frac{RT}{nF}\ln\frac{D_{\rm DmFc}}{D_{\rm DmFc+}}$ (10 <sup>-3</sup> V)	$E_{m(Fc+)} \text{ vs.}$ $DmFc^{0/+}$ (V)	$E_{(\rm Fc+)}^{ heta^{\prime}}$ vs. DmFc <sup>0/+</sup> (V)
[C₄mim] [PF <sub>6</sub> ]	1.64±0.16	$1.56 \pm 0.20$	13±2	11±3	0.478	0.478
[C <sub>2</sub> mim] [FAP]	$1.73 \pm 0.06$	$1.00 \pm 0.10$	14±1	0±2	0.574	0.567
[C <sub>4</sub> mim] [CF <sub>3</sub> SO <sub>3</sub> ]	$1.31 \pm 0.08$	1.36±0.14	7±1	8±2	0.474	0.475
$[C_4 mim] \\ [N(Tf)_2]$	1.35±0.07	1.09±0.05	8±1	2±1	0.513	0.510
[C <sub>4</sub> mPyr] [FAP]	1.98±0.29	1.07±0.16	17±3	2±2	0.575	0.567
[C <sub>4</sub> mim] [BF <sub>4</sub> ]	2.01±0.34	1.59±0.10	18±3	12±2	0.478	0.475

<sup>a</sup> Optimal diffusion coefficient values were determined by numerical and digital fit of the experimental chronoamperometric and voltammetric data (n=5). Values obtained from [25]

#### 3 Reference Systems for Voltammetric Measurements in Ionic Liquids

$$E_{1/2} = E^{\theta'} + \frac{RT}{nF} \ln \frac{D_R}{D_Q}$$
(3.3)

It is worth noting that when the ratio of the diffusion coefficient for  $D_{\rm R}$  and  $D_{\rm O}$  components of a particular redox couple is close to unity, the difference between  $E_{1/2}$ ,  $E_{\rm m}$ , and  $E^{\theta'}$  is not experimentally significant. However, this condition is not always true in the case of ILs. Thereby, in those ILs where  $D_{\rm R}/D_{\rm O} \neq 1$ , the  $E_{1/2}$  obtained with the use of an ultramicroelectrode may differ from the  $E_{\rm m}$  obtained with a macroelectrode. This is because the second term in Eq. (3.3) contains the first power of the diffusion coefficient, rather than the square root as in Eq. (3.2). Consequently, the experimentally obtained  $E_{1/2}$  is larger by  $(RT/nF)\ln(D_{\rm R}/D_{\rm O})$  with respect to  $E_{\rm m}$ . For example, the experimental  $E_{1/2({\rm Fc})}=0.582\pm0.003$  V vs. DmFc<sup>0/+</sup> obtained in [C<sub>4</sub>mPyr][FAP] and with the use of a carbon fiber ultramicroelectrode (6.2 µm diameter) is larger with respect to  $E_{\rm m}=0.575\pm0.003$  V vs. DmFc<sup>0/+</sup> obtained with a glassy carbon macroelectrode (1 mm diameter) under the same experimental conditions. This difference is consistent, within the experimental error, to the calculated  $(RT/nF)\ln(D_{\rm R}/D_{\rm O})$  value of 0.008 V in this IL.

The  $E_{\rm m}$  of Fc vs. DmFc<sup>0/+</sup>, as well as the  $E^{\theta'}$  obtained after correction for inequality in the respective diffusion coefficients of the charged and neutral species by using Eq. (3.2), is presented in Table 3.4. From this table, it is possible to observe that the inequality in the diffusion coefficients introduces negligible differences between the experimental  $E_{\rm m}$  and  $E^{\theta'}$  values when Fc and DmFc have a similar inequality ratio (e.g., in [C<sub>4</sub>mim][PF<sub>6</sub>] and [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>]). Meanwhile, the mentioned difference becomes larger than 0.003 V (consider a typical experimental error) as the inequality ratio difference increases. For example, a difference of 0.007 V and 0.008 V is observed for [C<sub>2</sub>mim][FAP] and [C<sub>4</sub>mPyr][FAP], respectively. For comparison, a difference of about 0.016 V between  $E_{1/2}$  and  $E^{\theta'}$  is observed in these ILs [25].

Figure 3.7 shows typical cyclic voltammograms for the oxidation of saturated solution of DmFc in  $[C_4mim][N(Tf)_2]$  and  $[C_4mPyr][FAP]$  on a 6.2 µm diameter carbon fiber ultramicroelectrode at a scan rate of 10 mV s<sup>-1</sup> and under an argon atmosphere. Decamethylferrocene is oxidized in a reversible, one-electron transfer process to DmFc<sup>+</sup> and reduced back to DmFc according to Eq. (3.1). The  $E_{1/2}$  for this redox reaction was arbitrarily set at 0.0 V.

As expected for a reversible process, a well-defined response with  $|E_{3/4}-E_{1/4}|$  values of 56 and 52 was observed in  $[C_4mim][N(Tf)_2]$  and  $[C_2mim][FAP]$ , respectively, which are close to the theoretical value of 56 mV at 21 °C. Values below 50 mV were observed in  $[C_4mim][PF_6]$ ,  $[C_4mim][CF_3SO_3]$ ,  $[C_4mPyr][FAP]$ , and  $[C_4mim][BF_4]$  ILs. This departure from ideality could be attributed to a voltam metric behavior intermediate to that observed at micro- and macroelectrodes due to the very low diffusivity of DmFc and DmFc<sup>+</sup> in these ILs and the value of potential scan rate selected for this experiment. For example, Fig. 3.7a shows the voltammogram



**Fig. 3.7** Comparison of experimental (*black solid line*) and digitally simulated (*open red circles*) cyclic voltammograms obtained for the oxidation of saturated solution of DmFc in (**a**) [C<sub>4</sub>mim] [N(Tf)<sub>2</sub>] and (**b**) [C<sub>4</sub>mPyr][FAP], respectively, under argon atmosphere and using a carbon fiber ultramicroelectrode ( $d=6.2 \ \mu$ m) as the working electrode. Scan rate=10 mV s<sup>-1</sup>;  $T=21\pm1$  °C. Reproduced from [25] with permission from Elsevier

of DmFc in  $[C_4mim][N(Tf)_2]$ . The potential scan rate of 10 mV s<sup>-1</sup> used experimentally is smaller than the 20 and 18 mV s<sup>-1</sup> predicted by the following inequality

$$v \ll \frac{RTD}{nFr^2} \tag{3.4}$$

and required to observe a near-steady-state voltammetric behavior for the oxidation of DmFc and the following reduction of DmFc<sup>+</sup>, respectively ( $D_{\text{DmFc}}=0.76 \times 10^{-7}$ and the  $D_{\text{DmFc}+}=0.70 \times 10^{-7} \text{ cm}^2 \text{ s}^{-1}$ ). Meanwhile, Fig. 3.7b shows the cyclic voltammogram of DmFc in [C<sub>4</sub>mPyr][FAP]. According to Eq. (3.4) and assuming  $D_{\text{DmFc}}=0.30 \times 10^{-7}$  and  $D_{\text{DmFc}+}=0.28 \times 10^{-7} \text{ cm}^2 \text{ s}^{-1}$  in this IL, near-steady-state behavior at the microdisk electrode is expected to be achieved at scan rates of  $\ll 8 \text{ mV s}^{-1}$  and 7 mV s<sup>-1</sup> for the oxidation of DmFc and the following reduction of DmFc<sup>+</sup>, respectively. Consequently, the scan rate of 10 mV s<sup>-1</sup> used experimentally allows observing peak-shaped voltammograms, which is characteristic for more planar diffusion behaviors [25].

To further confirm the reversibility of the DmFc<sup>0/+</sup> redox process, a comparison of digital simulations of the cyclic voltammograms and experimental data was performed (Fig. 3.7). Simulations based on the reversible mechanism outlined in Eq. (3.1) give excellent agreement to experimental data for DmFc in all the ILs evaluated [25].

Table 3.4 shows the  $D_{\text{DmFc}}/D_{\text{DmFc}}$  ratio obtained in different ILs. In contrast with Fc, where the *D* ratio is within the range of 1.31–2.01, the  $D_{\text{DmFc}}/D_{\text{DmFc}}$  ratio is  $\approx 1$ , except for [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>], [C<sub>4</sub>mim][PF<sub>6</sub>], and [C<sub>4</sub>mim][BF<sub>4</sub>], which have a higher ratio of  $1.36 \pm 0.14$ ,  $1.56 \pm 0.20$ , and  $1.59 \pm 0.10$ , respectively. This result suggests that neutral DmFc species diffuse at the same rate than positively charged decamethylferrocenium species through the [C<sub>4</sub>mim][FAP], [C<sub>4</sub>mim][N(Tf)<sub>2</sub>], and [C<sub>4</sub>mPyr][FAP] media. Thereof, the  $E_{1/2} \approx E^{0'}$  (within the experimental error) for DmFc in these ILs. Although this is not a ubiquitous property, the behavior observed
in the latest mentioned ILs is consistent with that observed in traditional organic solvents with added supporting electrolyte and where DmFc is considered to be a less solvent-dependent internal reference redox system with respect to Fc [48].

It has been previously discussed that the formal potential of redox couples obtained in ILs could be affected by at least two factors [20]: (i) the different IL solvation effects on DmFc/DmFc<sup>+</sup> and Fc/Fc<sup>+</sup> couples and (ii) the inequality ratio between the  $D_R$  and  $D_O$  of these redox couples. An analysis of Table 3.4 shows that an increase in experimental  $E_m$  of Fc vs. DmFc<sup>0/+</sup> of about 0.101 V is observed when the IL is changed from [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>] to [C<sub>4</sub>mPyr][FAP]. The increase in the  $E^{\theta'}$  of Fc vs. DmFc<sup>0/+</sup> is equal to 0.092 V after the correction for inequality in the diffusion coefficients of both redox couples in the mentioned ILs. It is instructive to mention that the mentioned increase in the experimental  $E_{1/2}$  of Fc vs. DmFc<sup>0/+</sup> is of 0.110 V by changing from [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>] to [C<sub>4</sub>mPyr][FAP]. These differences between  $E_m$ ,  $E_{1/2}$ , and  $E^{\theta'}$  could easily be explained by considering the differences between Eqs. (3.2) and (3.3). Furthermore, from these values it is possible to see that even when both previously mentioned factors (i and ii) are present in the obtained potential difference, the solvation property of the ILs as a function of the chemical structure is the predominant reason for the observed variations.

The cobaltoceniumlcobaltocene,  $Cc^{+/0}$  (also known as  $[Co^{III}(\eta^5-C_5H_5)_2]^+/[Co^{II}(\eta^5-C_5H_5)_2])$ , redox couple is used in organic solvent and ILs as an alternative IRRS. It was suggested by Strehlok et al. in 1960 as an IRRS for organic solvent systems [61]. Although it was not considered by IUPAC as an alternative to the Fc<sup>0/+</sup> couple, it shows negligible volatility and high stability and solubility in some organic solvents [62] and ILs [6, 47, 58, 63]. If the cathodic potential window of the solvent is large enough, two chemically reversible, one electron reduction processes can be observed (Eqs. 3.5 and 3.6).

$$\left[\operatorname{Co}^{\mathrm{III}}\left(\eta^{5}-\operatorname{C}_{5}\operatorname{H}_{5}\right)_{2}\right]^{+}+\operatorname{e}^{-} \leftrightarrows \left[\operatorname{Co}^{\mathrm{II}}\left(\eta^{5}-\operatorname{C}_{5}\operatorname{H}_{5}\right)_{2}\right]$$
(3.5)

$$\left[\operatorname{Co}^{II}\left(\eta^{5}-\operatorname{C}_{5}\operatorname{H}_{5}\right)_{2}\right]+e^{-} \Longrightarrow \left[\operatorname{Co}^{I}\left(\eta^{5}-\operatorname{C}_{5}\operatorname{H}_{5}\right)_{2}\right]^{-}$$
(3.6)

The mid-point potential for the  $Cc^{0/-}$  couple (Eq. 3.6) was found to be considerably solvent dependent and can not always be determined accurately at room temperature, mainly due to the overlap and interaction of this process with the electrochemical response of the organic solvent used [62]. Thereby, only the  $Cc^{+/0}$ redox couple (Eq. 3.5) has been extensively used in organic solvents to provide a known and stable reference point. As an extrapolation of the concept, it is also used in IL systems. Surprisingly, little is known about the solvation effect of either different organic solvents with added supporting electrolytes or IL structure on the  $Cc^{+/0}$ formal potential.

Table 3.3 reports the IL effect on the  $Cc^{+/0}$  process using both  $Fc^{0/+}$  and  $DmFc^{0/+}$  as IRRS. In the first case, the  $E_m$  of  $Cc^{+/0}$  is almost constant and could be represented by a value of  $1.327 \pm 0.005$  V vs.  $Fc^{0/+}$  in 14 different ILs and using glassy carbon as the working electrode (exceptions are  $[C_2mim][BF_4]$  and  $[C_4mPyr][CF_3SO_3]$ , where

Solvent	Electrolyte	Cc <sup>+/0</sup> vs. Fc <sup>0/+</sup> (V)	Ref
Acetonitrile	0.1 M [Et <sub>4</sub> N][ClO <sub>4</sub> ]	$-1.350 \pm 0.003$	[62]
	0.1 M [Bu <sub>4</sub> N][BF <sub>4</sub> ]	$-1.348 \pm 0.003$	[62]
	0.1 M [Bu <sub>4</sub> N][PF <sub>6</sub> ]	$-1.337 \pm 0.005$	
Dichloromethane	0.1 M [Et <sub>4</sub> N][ClO <sub>4</sub> ]	$-1.359 \pm 0.007$	[62]
	0.1 M [Bu <sub>4</sub> N][BF <sub>4</sub> ]	$-1.355 \pm 0.007$	[62]
Ethanol	0.1 M [Et <sub>4</sub> N][ClO <sub>4</sub> ]	$-1.351 \pm 0.004$	[62]
	0.1 M [Bu <sub>4</sub> N][BF <sub>4</sub> ]	$-1.356 \pm 0.004$	[62]
Water	0.1 M Li[ClO <sub>4</sub> ]	$-1.367 \pm 0.002$	[62]
Toluene	0.4 M [P <sub>66614</sub> ][FAP]	$-1.340 \pm 0.005$	[64]

Table 3.5 Redox potentials of cobaltocenium hexafluorophosphate vs.  $Fc^{0+}$  in different organic media

 $[P_{66614}]$ [FAP] = trihexyl(tetradecyl)phosphonium tris(pentafluoroethyl)trifluorophosphate

a value of 1.336 V and 1.347 V was reported, respectively). Meanwhile, when  $DmFc^{0/+}$  is used as IRRS, an increase of 0.107 V in the potential separation between  $Cc^{+/0}$  and  $DmFc^{0/+}$  couples is observed upon changing the IL from [C<sub>4</sub>mPyr][FAP] to [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>] and using GC as the working electrode.

To further understand this observation, we need to compare the variation in the  $E_{\rm m}$  of Cc<sup>+/0</sup> vs. Fc<sup>0/+</sup> in organic solvents with added supporting electrolyte. It is well known that Fc is highly sensitive to solvation effects under these conditions (see above). As seen in Table 3.5, the  $E_{\rm m}$  of Cc<sup>+/0</sup> in nine different solvent/supporting electrolyte combinations can be represented by an almost constant value of about  $1.352\pm0.015$  V vs. Fc<sup>0/+</sup>. As given in Table 3.2, the  $E_{\rm m}$  value of the Fc<sup>0/+</sup> redox process varies from  $0.437\pm0.005$  V in ethanol/0.1 M [Bu<sub>4</sub>N][ClO<sub>4</sub>] to a value of  $0.532\pm0.002$  V in dichloromethane/0.1 M [Bu<sub>4</sub>N][ClO<sub>4</sub>], which represents a difference of 0.095 V. Meanwhile, the obtained Cc<sup>+</sup>  $E_{\rm m}$  values vs. Fc<sup>0/+</sup> in the same two organic solvent systems (with 0.1 M [Bu<sub>4</sub>N][ClO<sub>4</sub>] as the supporting electrolyte) show a variation of just 0.008 V (Table 3.5).

The comparison of data reported in Tables 3.2, 3.3, and 3.5 is of significant value as they suggest that the mid-point potentials of both  $Cc^{+/0}$  and  $Fc^{0/+}$  couples are dependent on the solvation properties of organic solvents (with added supporting electrolyte) as well as the solvation properties of ILs, particularly under the assumption that  $DmFc^{0/+}$  redox couple is a less solvent dependent process [57]. Consequently, potentials reported versus  $Cc^{+/0}$  and  $Fc^{0/+}$  might need to be corrected using the reported values in case of comparison of experimental data obtained in different organic solvents (Tables 3.2 and 3.5) and/or ILs (Table 3.3).

Decamethylcobaltocenium (DmCc<sup>+</sup> or  $[Co^{III}(\eta^5-C_5(CH_3)_5)_2]^+$ ) was studied to throw light further on this matter [65]. Figure 3.8 shows typical cyclic voltammograms for the reduction of a 4.36 mmol/kg DmCc<sup>+</sup> solution in  $[C_4mPyr][N(Tf)_2]$  on a 1.0 mm diameter GC electrode at varying scan rates. Decamethylcobaltocenium is reduced by one electron to decamethylcobaltocene, DmCc, at a peak potential of *ca*. -1.424 V vs. DmFc<sup>0/+</sup>, and oxidized back to DmCc<sup>+</sup> at a potential of *ca*. -1.359 V vs. DmFc<sup>0/+</sup>, according to Eq. (3.7). The second reduction process, related to the one-electron reduction of decamethylcobaltocene (Eq. 3.8), however, was not observed in all ILs studied [65].

$$\left[\operatorname{Co}^{\mathrm{III}}\left(\eta^{5}-\operatorname{C}_{5}\left(\operatorname{CH}_{3}\right)_{5}\right)_{2}\right]^{+}+\operatorname{e}^{-} \leftrightarrows \left[\operatorname{Co}^{\mathrm{II}}\left(\eta^{5}-\operatorname{C}_{5}\left(\operatorname{CH}_{3}\right)_{5}\right)_{2}\right]$$
(3.7)

$$\left[\operatorname{Co}^{\mathrm{II}}\left(\eta^{5}-\operatorname{C}_{5}\left(\operatorname{CH}_{3}\right)_{5}\right)_{2}\right]+\mathrm{e}^{-} \leftrightarrows \left[\operatorname{Co}^{\mathrm{I}}\left(\eta^{5}-\operatorname{C}_{5}\left(\operatorname{CH}_{3}\right)_{5}\right)_{2}\right]^{-}$$
(3.8)

As expected for reversible processes,  $E_{\rm m}$  values obtained from the cyclic voltammograms are independent of the scan rates (0.1–0.7 V s<sup>-1</sup>, Fig. 3.8) and concentrations (3–4.5 mmol/kg) studied. The peak current for the reduction of DmCc<sup>+</sup> varies linearly with the square root of the scan rate (0.1–0.7 V s<sup>-1</sup>), characteristic of diffusion-controlled electrode processes [65].

To examine the influence of IL constituents on the redox potential of  $DmCc^+$ , ionic liquids containing the same anion but different cations, e.g.,  $[C_4mim][N(Tf)_2]$ and  $[C_4mPyr][N(Tf)_2]$ , and the same cation but different anions, e.g.,  $[C_4mim][N(Tf)_2]$  and  $[C_4mim][CF_3SO_3]$ , were selected. From Fig. 3.9 and Table 3.6, it is noted that the substitution of the ten hydrogen atoms of the cyclopentadienyl ring of cobaltocenium with ten methyl groups decreases the redox potential of the reduction process by 0.579 V, 0.583 V, and 0.541 V in  $[C_4mPyr][N(Tf)_2]$ ,  $[C_4mim][N(Tf)_2]$ , and  $[C_4mim][CF_3SO_3]$ , respectively [65]. This effect may be attributed to the



**Fig. 3.8** Cyclic voltammetry for the reduction of 4.36 mmol/kg DmCc<sup>+</sup> in  $[C_4mPyr][N(Tf)_2]$  on a 1 mm diameter GC electrode at varying scan rates (0.1, 0.2, 0.3, 0.4, 0.5, 0.7 V s<sup>-1</sup>). Reproduced from [65] with permission from the PCCP Owner Societies



**Fig. 3.9** Voltammetric responses for the oxidation of 1.39 mmol/kg Fc and reduction of 4.33 mmol/kg Cc<sup>+</sup> and 4.36 mmol/kg DmCc<sup>+</sup> in  $[C_4mPyr][N(Tf)_2]$  on a GC electrode (diameter=1 mm) at a scan rate of 0.1 V s<sup>-1</sup>. Reproduced from [65] with permission from the PCCP Owner Societies

electron-donating effect of the methyl groups, which leads to the pushing of the electron density toward the metal center and, thereby, obstructing the electron addition to the  $DmCc^+$  by the electrode.

Table 3.6 shows a subtle variation of the  $E_m$  of DmCc<sup>+</sup>, Cc<sup>+</sup>, and Fc vs. DmFc<sup>0/+</sup> upon changing the IL from  $[C_4mim][N(Tf)_2]$  to  $[C_4mPyr][N(Tf)_2]$ . Magnitude changes of around 0.040 V, nonetheless, are observed for Cc<sup>+</sup>, and Fc by keeping the  $[C_4mim]$  cation constant and changing the anion from  $[N(Tf)_2]^-$  to  $[CF_3SO_3]^-$ . The observed variation in the Cc<sup>+</sup> and Fc  $E_m$  values vs. DmFc<sup>0/+</sup> when the weakly coordinating  $[N(Tf)_2]$  anion is replaced with  $[CF_3SO_3]^-$ can be rationalized in terms of the ion-pairing tendencies of small versus large anions and the differences in their donor abilities [66, 67]. This tendency also justifies the Cc<sup>+</sup> and Fc  $E_m$  values vs. DmFc<sup>0/+</sup> observed with the bulky  $[FAP]^-$ -containing IL,  $[C_2mim][FAP]$ , and in comparison with the previously mentioned ILs, where for example, the Cc<sup>+</sup>  $E_m$  value vs. DmFc<sup>0/+</sup> shifts in the cathodic direction by *ca*. 0.100 V by changing the IL from  $[C_2mim][FAP]$  to  $[C_4mim][CF_3SO_3]$ . Surprisingly, the difference in the  $E_m$  between DmCc<sup>+</sup> and DmFc<sup>0/+</sup> remains almost constant in all four ILs.

Other alternatives, such as 1,1'-dimethylferrocene, 1,1-diacetylferrocene, ferrocenecarboxaldehyde, etc., could be used to provide a stable redox potential [6, 58, 68]. However, these systems have not been fully characterized for this role in ILs as yet.

		$E_{\rm m}$ vs. DmFc <sup>0/+</sup> (V)		$E_{\rm m}$ vs. Fc <sup><math>0/+</math></sup> (V)		
IL	Electrode	Fc	Cc+	DmCc+	Cc+	Ref
[C <sub>2</sub> mim][FAP]	GC	0.574	-0.749	-1.392	-1.323	[65]
[C <sub>4</sub> mPyr][N(Tf) <sub>2</sub> ]	GC	0.511	-0.816	-1.395	-1.327	[65]
[C <sub>4</sub> mim][N(Tf) <sub>2</sub> ]	GC	0.514	-0.813	-1.396	-1.327	[65]
[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	GC	0.474	-0.854	-1.395	-1.328	[65]

 Table 3.6 Redox potentials of transition-metal sandwich complexes obtained by cyclic voltammetry in different ionic liquids<sup>a</sup>

<sup>a</sup>Potentials were obtained by cyclic voltammetry and using a scan rate of 0.1 V s<sup>-1</sup>.  $E_m$  values were obtained with an accuracy of ±0.003 V (n=5)

#### 3.3.1 Limitations in the Application of IRRS in Ionic Liquids

- Poor solubility of Fc in some ionic liquids, mostly in those with high viscosity [63],
- Moderate volatility of Fc [25, 69, 70],
- Reactivity of Fc<sup>+</sup> with the IL components: generally observed when the anodic potential window of the IL is close to the formal redox potential of Fc<sup>0/+</sup> [58, 63].
- The  $E_m$  of  $Fc^{0/+}$  redox process differs from the  $E^{0'}$ : this effect is related to the inequality in the diffusion coefficients of Fc and Fc<sup>+</sup> in almost all known ILs [25, 46].
- Poor solubility of decamethylcobaltocene in some ILs: Fig. 3.10 shows a voltammogram of  $DmCc^{+/0}$  in  $[C_4mim][PF_6]$  and  $[C_4mim][BF_4]$  ILs. An almost symmetrical, bell-shaped anodic peak is observed in the positive going potential scan at -1.310 V vs.  $DmFc^{0/+}$  in  $[C_4mim][PF_6]$  (Fig. 3.10a). This is a consequence of the poor solubility of the reduction product, DmCc, which translates to important electrode adsorption effects. Meanwhile, stronger electrode adsorption processes of  $DmCc^+$  and its oxidation product can be observed in  $[C_4mim][BF_4]$  (Fig. 3.10b), where the adsorption process can be observed both in the reduction and oxidation voltammetric scan direction. This adsorption process prevents the accurate determination of the  $E_m$ , and consequently, the application of this redox system as a reliable IRRS in these particular ILs.
- *Limited solubility of decamethylferrocene in ILs:* Table 3.7 shows the solubility of DmFc and Fc in different ILs. As possible to be seen, the solubility of DmFc is much smaller (0.5–5.6 mM) than that of ferrocene in the same ILs.
- Reactivity of decamethylferrocene in the presence of oxygen: Fig. 3.11a-a shows a picture of a 2.19 mmol/kg DmFc solution in [C<sub>4</sub>mPyr][N(Tf)<sub>2</sub>] under argon atmosphere. Under this experimental condition, the DmFc solution was yellow and stable over time, even with the addition of different water concentrations [57, 65]. However, after the exposure to an O<sub>2</sub> and H<sub>2</sub>O saturated atmosphere (atmospheric condition), the IL solution turns green (Fig. 3.11a-b). This reaction was followed by UV–Vis spectroscopy, where an absorption band due to the



**Fig. 3.10** Cyclic voltammetry for the reduction of (a) 4.27 mmol/kg DmCc<sup>+</sup> in  $[C_4mim][PF_6]$  and (b) 4.71 mmol/kg DmCc<sup>+</sup> in  $[C_4mim][BF_4]$  on a 1 mm diameter GC electrode at scan rate of 0.02 V s<sup>-1</sup>. Reproduced from [65] with permission from the PCCP Owner Societies

	DmFc solubility	Fc solubility
IL	$(\mathbf{m}\mathbf{M})^{\mathrm{a}}$	(mM) <sup>b</sup>
[C <sub>4</sub> mim][PF <sub>6</sub> ]	1.10±0.21	$38.2 \pm 1.5$
[C <sub>2</sub> mim][FAP]	$2.80 \pm 0.12$	-
[C <sub>4</sub> mim][CF <sub>3</sub> SO <sub>3</sub> ]	$1.90 \pm 0.09$	$58.3 \pm 0.1$
[C <sub>4</sub> mim][N(Tf) <sub>2</sub> ]	$5.26 \pm 0.14$	77.4±0.5
[C <sub>4</sub> mPyr][FAP]	3.50±0.17	-
[C <sub>4</sub> mim][BF <sub>4</sub> ]	0.52±0.09	27.5±0.2

Table 3.7 Solubilities of DmFc and Fc in various ILs

<sup>a</sup>Data obtained from [25]

<sup>b</sup>Data obtained from [46]

DmFc<sup>+</sup> centered at 776 nm develops, whereas the absorption peak for DmFc centered at 428 nm is replaced by a very large absorbance in the UV range with peaks at 242, 278, and 315 nm and the appearance of an isosbestic point, IP, at 258 nm. An almost identical spectrum can be observed from a 1.15 mM DmFc solution in acetonitrile (0.1 M [Bu<sub>4</sub>N][PF<sub>6</sub>]) during its oxidative electrolysis at 0.2 V vs. DmFc<sup>0/+</sup> [65]. These observations confirm the occurrence of DmFc oxidation to DmFc<sup>+</sup> in the IL solution.

The spontaneous reaction observed between DmFc and oxygen brings important consequences in the establishment of conditions under which DmFc should be used. Indeed, it is a suitable IRRS to work under inert atmospheres, such as those present inside argon or nitrogen-filled glove boxes. However, the application of this redox system as IRRS should be avoided when the experiments are being conducted under atmospheric conditions. Moreover, DmFc sample preparation in ILs should be also performed under an inert atmosphere.



**Fig. 3.11** (a) Comparison of a 2.19 mmol/kg DmFc in  $[C_4mPyr][N(Tf)_2]$  solution under argon (a) and atmospheric (b) conditions. (b) UV–Vis spectra of the  $[C_4mPyr][N(Tf)_2]$  solution shown in A-a exposed to atmospheric condition and recorded in function of time. Inset: magnification of (b) to show the differences in the spectra before (*green*) and after (*blue*) 400 min exposition to atmospheric condition. Adapted from [65] with permission from the PCCP Owner Societies

### 3.3.2 Selection of an Internal Reference Redox Scale for Voltammetric Measurements

The appropriated selection of IRRS to provide a known and stable reference point in voltammetry is very important both in organic and IL solvent systems. The objective is to choose IRRS (either the OX<sub>IRRS</sub> or RED<sub>IRRS</sub> component of a reversible redox couple) so that the cyclic voltammetric response for the simultaneously present electroactive ANS can be observed independently of the IRRS response. This means that if ANS to be studied is in the oxidized form, then the reduced form of IRRS must be added to the system. Conversely, if ANS is in the reduced from, then the oxidized form of IRRS must be added to the system. However, it is possible to see a large number of published works, which do not follow this basic rule. This matter was recently addressed and three fundamental paradigms describing the relative positioning of IRRS and ANS on the potential scale, the operative redox components for IRRS and ANS, and the starting potential ( $E_{start}$ ), reversing potential ( $E_{rev}$ ), and ending potential ( $E_{end}$ ) for a cyclic voltammetric scan have been identified [45]. These paradigms are as follows:

Paradigm A	an optimal paradigm, which can produce completely independent
	voltammetric responses for ANS and for IRRS.
Paradigm B	a less-than-optimal paradigm which can produce an independent
	CV response for ANS or a mixed response for IRRS with that response
	on top of ANS response.
Paradigm C	a problematic paradigm that can produce an independent CV
	response for IRRS or a mixed response for ANS with that response on
	top of the IRRS response.

Any mixed response produces a thermodynamically favored redox-cross-reaction which couples the IRRS and ANS systems and which can complicate the analysis of ANS and IRRS responses [45].

The various paradigmatic arrangements along a potential axis are shown in Table 3.8. For the purposes of illustration of the concepts, we will assume that cyclic voltammetry is the operative experimental protocol.

The paradigms A-1a and A-1b have identical arrangement of the  $OX_{ANS}$  and  $RED_{IRRS}$  along the potential scale. They only differ in the initial scan direction and  $E_{rev}$ . The paradigm A-1a produces the independent CV response for ANS (Eq. 3.9). Meanwhile, the paradigm A-1b produces the independent CV response for IRRS (Eq. 3.10). A cross-reaction (Eq. 3.11) is not being established, as the necessary reactants are never simultaneously present in the diffusion layer. An analogous situation can be seen with the paradigms A-2a and A-2b, the oxidation state of the electroactive species (RED<sub>ANS</sub> and OX<sub>IRRS</sub>) being the major difference between A-1 and A-2 paradigm [45].

$$\mathbf{A} - \mathbf{1a}: \quad OX_{ANS} + e \Leftrightarrow RED_{ANS} \quad (OX_{ANS} \text{ initially present})$$
 (3.9)

$$\mathbf{A} - \mathbf{lb}$$
:  $OX_{IRRS} + e \Leftrightarrow RED_{IRRS}$  (RED<sub>IRRS</sub> initially present) (3.10)

$$\operatorname{RED}_{ANS} + \operatorname{OX}_{IRRS} \Leftrightarrow \operatorname{OX}_{ANS} + \operatorname{RED}_{IRRS} \qquad \left(K_{cross} = 2.82 \times 10^8\right) \quad (3.11)$$

 $K_{\rm cross}$  being the equilibrium constant for a simple outer-sphere second-order cross-reaction.

$$K_{\rm cross} = \exp\left[\frac{F}{RT} \left| E_{\rm ANS}^{\theta'} - E_{\rm IRRS}^{\theta'} \right| \right]$$
(3.12)

Figure 3.12 shows simulated voltammograms related to the paradigms A-1a and A-1b, and following the mechanism depicted in Eqs. (3.9)-(3.11). Setting

Paradigm	Potential zone	CV response for	Cross- reaction
A-1a	$E_{ANS_{OOD}}^{O'} E_{IRRS_{OUTD}}^{O'}$	ANS	NO
A-1b	$-E \qquad \qquad$	IRRS	NO
A-2a	$E = \begin{bmatrix} E_{IRRS_{(0X)}}^{\theta'} & E_{ANS_{(0X)}}^{\theta'} \\ \vdots & \vdots & \vdots \\ -E & \vdots & \vdots & \vdots \\ \vdots & \vdots & \vdots & \vdots \\ \vdots & \vdots & \vdots$	ANS	NO
A-2b	$E \xrightarrow{0'}_{IRRS_{(OX)}} E \xrightarrow{0'}_{ANS_{(OXI)}}$	IRRS	NO
B-1a	$E_{ANS_{OUD}}^{0'} E_{IRRS_{OUD}}^{0'}$	ANS	NO
B-1b	$E_{ANS_{OUTED}}^{0'} E_{IRRS_{OUTED}}^{0'}$	IRRS+ANS	YES
B-2a	$-E \qquad \qquad$	ANS	NO
B-2b	$E \xrightarrow{\phi'_{IRRS_{(00)}}} E_{ANS_{(00)}}^{\phi'}$	IRRS+ANS	YES

Table 3.8 The three fundamental paradigms (A, B, and C) characterizing the cyclic voltammetric responses for IRRS and ANS compounds [45]

(continued)



#### Table 3.8 (continued)

 $\leftarrow$  or  $\rightarrow$ : The potential zone where a given CV scan is initiated ( $E_{\text{start}}$ ) and the initial direction of the scan (following the IUPAC sign convention: negative scan:  $\leftarrow$ ; positive scan:  $\rightarrow$ ). This potential zone should be chosen so that the current is initially zero before the scan commences.  $\frown$  or  $\rightarrow$ : The potential zone where a scan is reversed ( $E_{\text{rev}}$ ).  $\leftarrow$  or  $\rightarrow$ : The potential zone where a given CV scan is finished ( $E_{\text{end}}$ ).  $E_{\text{IRRS}}^{\theta'}$ : The formal potential zone where IRRS is electroactive.  $E_{\text{rev}}^{\theta'}$ . The formal potential zone where ANS is electroactive. Adapted from [45] with permission from RSC

 $E_{\text{start}} = -0.25 \text{ V}$ ,  $E_{\text{rev}} = -0.75 \text{ V}$ , and  $E_{\text{end}} = E_{\text{start}} = -0.25 \text{ V}$  produces the independent voltammogram for ANS. Meanwhile, by setting  $E_{\text{start}} = -0.25 \text{ V}$ ,  $E_{\text{rev}} = 0.25 \text{ V}$ , and  $E_{\text{end}} = E_{\text{start}}$ , the independent voltammogram for IRRS is obtained. Note that there are no conditions where there will be significant concentrations of both RED<sub>ANS</sub> and OX<sub>IRRS</sub> generated within the diffusion layer. Of course, one could execute multiple CV cycles over the entire potential range (e.g., between -0.75 and 0.25 V) and generate the full menu of species and a cross-reaction [45].

Paradigms B-1a (Eq. 3.13) and B-1b (Eq. 3.14) have identical arrangements of the RED<sub>IRRS</sub> and RED<sub>ANS</sub> but differ in the choice of the reversal zone. The B-2a and B-2b paradigms are analogously related, the oxidation state of the electroactive species (OX<sub>ANS</sub> and OX<sub>IRRS</sub>) being the major difference. Depending upon the initial scan direction and reversing potential the B-paradigm will produce independent CV responses for ANS and will also produce the mixed CV response for ANS and IRRS (Eqs. 3.13–3.15). In this particular case scenario, the CV response for IRRS is on top of the CV response for ANS [45].



**Fig. 3.12** Simulations of the CV responses for ANS (*open red circles*, paradigm A-1a) and IRRS (*black solid line*, Paradigm A-1b) with electrode area = 1.0 cm<sup>2</sup>, scan rate = 1.0 V s<sup>-1</sup>, T = 298.2 K,  $c_{\text{OX}_{\text{ANS}}} = 1 \times 10^{-3} \text{ M}$ ,  $D_{\text{OX}_{\text{ANS}}} = D_{\text{RED}_{\text{ANS}}} = D_{\text{OX}_{\text{IRRS}}} = D_{\text{RED}_{\text{IRRS}}} = 1.0 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ,  $E_{\text{ANS}}^{\theta'} = -0.5 \text{ V}$ ,  $c_{\text{RED}_{\text{IRRS}}} = 1 \times 10^{-3} \text{ M}$ ,  $E_{\text{IRRS}}^{\theta'} = 0 \text{ V}$ ,  $k_{\text{s,ANS}} = k_{\text{s,IRRS}} = 1.0 \times 10^{4} \text{ cm s}^{-1}$ ,  $K_{\text{cross}} = 2.82 \times 10^{8}$ , rate constant for a simple outer-sphere second-order cross-reaction ( $k_{\text{cross}} = 1.0 \times 10^{7} \text{ M}^{-1} \text{ s}^{-1}$ ,  $E_{\text{start}} = -0.25 \text{ V}$ ). Reproduced from [45] with permission from the RSC

$$\mathbf{B} - \mathbf{1a} : OX_{ANS} + e \Leftrightarrow RED_{ANS} \qquad (RED_{ANS} \text{ initially present}) \qquad (3.13)$$

$$\mathbf{B} - \mathbf{1b} : OX_{IRRS} + e \Leftrightarrow RED_{IRRS} \quad (RED_{IRRS} \text{ initially present}) \quad (3.14)$$

$$\operatorname{RED}_{ANS} + \operatorname{OX}_{IRRS} \Leftrightarrow \operatorname{OX}_{ANS} + \operatorname{RED}_{IRRS} \left( K_{cross} = 2.82 \times 10^8 \right)$$
(3.15)

Simulated examples of the B-1a and B-1b voltammograms are shown in Fig. 3.13. Setting  $E_{\text{start}} = -0.75$  V,  $E_{\text{rev}} = -0.25$  V, and  $E_{\text{end}} = E_{\text{start}} = -0.75$  V produces the independent voltammogram for ANS; setting  $E_{\text{start}} = -0.75$  V,  $E_{\text{rev}} = 0.25$  V, and  $E_{\text{end}} = E_{\text{start}}$  produces the mixed response with IRRS response on top of ANS response. Note that as soon as an increasingly positive potential begins to drive Eq. (3.14) to the left, thereby producing OX<sub>IRRS</sub>, Eq. (3.15) will proceed to the right creating an additional path for the generation of OX<sub>ANS</sub> [45].

Paradigm C will produce an independent CV response for IRRS (Eq. 3.16) and will also produce the mixed CV response for IRRS and ANS (Eqs. 3.16–3.18). In this case, the CV response for ANS is on top of the CV response for IRRS. Please note that paradigm C cannot produce an independent CV response for ANS.

$$\mathbf{C} - \mathbf{1a} : OX_{IRRS} + \mathbf{e} \Leftrightarrow RED_{IRRS} \qquad (RED_{IRRS} \text{ initially present}) \quad (3.16)$$

$$\mathbf{C} - \mathbf{lb} : OX_{ANS} + e \Leftrightarrow RED_{ANS}$$
 (RED<sub>ANS</sub> initially present) (3.17)



**Fig. 3.13** Simulations of the CV responses for ANS (*open red circles*, paradigms B-1a) and IRRS/ANS (*solid black line*, paradigms B-1b) with electrode area = 1.0 cm<sup>2</sup>, scan rate = 1.0 V s<sup>-1</sup>, *T* = 298.2 K,  $c_{\text{RED}_{ANS}} = 1 \times 10^{-3} \text{ M}$ ,  $D_{\text{OX}_{ANS}} = D_{\text{RED}_{ANS}} = D_{\text{OX}_{IRRS}} = D_{\text{RED}_{RRS}} = 1.0 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ,  $E_{\text{ANS}}^{\theta \prime} = -0.5 \text{ V}$ ,  $c_{\text{RED}_{IRRS}} = 1 \times 10^{-3} \text{ M}$ ,  $E_{\text{IRRS}}^{\theta \prime} = 0 \text{ V}$ ,  $k_{\text{s,ANS}} = k_{\text{s,IRRS}} = 1.0 \times 10^{4} \text{ cm} \text{ s}^{-1}$ ,  $K_{\text{cross}} = 2.82 \times 10^8$ ,  $k_{\text{cross}} = 1.0 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ ,  $E_{\text{start}} = -0.75 \text{ V}$ . Reproduced from [45] with permission from the RSC

$$OX_{ANS} + RED_{IRRS} \iff RED_{ANS} + OX_{IRRS} \qquad \left(K_{cross} = 2.82 \times 10^8\right) \quad (3.18)$$

$$OX_{ANS} \Leftrightarrow P \qquad \left(K_{d} = 1.0 \times 10^{5}; \quad k_{d} = 10.0 \,\mathrm{s}^{-1}\right) \tag{3.19}$$

Figure 3.14 shows simulated examples of the C-1a and C-1b voltammograms. Setting  $E_{\text{start}} = -0.25$  V,  $E_{\text{rev}} = 0.25$  V, and  $E_{\text{end}} = E_{\text{start}} = -0.25$  V produces the independent voltammogram for IRRS; setting  $E_{\text{start}} = -0.25$  V,  $E_{\text{rev}} = 0.75$  V, and  $E_{\text{end}} = E_{\text{start}}$  produces the mixed response with the ANS response on top of the IRRS response.

Any ANS/IRRS mixed response (see Table 3.8, paradigms B-1b, B-2b, C-1b, and C-2b) is potentially problematic in that the CV response is a combination of the responses for the two electroactive systems [45]. Extracting an accurate estimate of that potential from a mixed response may not be that difficult (see Figs. 3.13 and 3.14) even when the ANS response is more complicated than a simple outer-sphere one-electron transfer. There is, however, an additional complication: every mixed response produces a thermodynamically favored cross-reaction (see Eqs. 3.15 and 3.18). Under certain conditions (both IRRS and ANS are perfectly reversible-electron transfers, a simple second-order cross-reaction and identical diffusion coefficients for all species) the cyclic voltammetric response is completely independent of the value of  $k_{cross}$  (see the analysis of Andrieux and Savéant [71] for the closely related sequential electron transfer, EE, mechanism [41]). Of course, it is



**Fig. 3.14** Simulations of the CV responses for IRRS (*solid black line*, paradigm C-1a) and ANS/IRRS (*open red circles*, paradigm C-1b) with electrode area=1.0 cm<sup>2</sup>, scan rate=1.0 V s<sup>-1</sup>, T=298.2 K,  $c_{\text{RED}_{\text{ANS}}} = 1 \times 10^{-3} \text{ M}$ ,  $D_{\text{OX}_{\text{ANS}}} = D_{\text{RED}_{\text{ANS}}} = D_{\text{RED}_{\text{IRRS}}} = 1.0 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ,  $E_{\text{ANS}}^{\theta \prime} = -0.5 \text{ V}$ ,  $c_{\text{RED}_{\text{IRRS}}} = 1 \times 10^{-3} \text{ M}$ ,  $E_{\text{IRRS}}^{\theta \prime} = 0 \text{ V}$ ,  $k_{\text{s,ANS}} = k_{\text{s,IRRS}} = 1.0 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ,  $K_{\text{cross}} = 2.82 \times 10^8$ ,  $k_{\text{cross}} = 1.0 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ ,  $E_{\text{start}} = -0.25 \text{ V}$ . Reproduced from [45] with permission from the RSC

unlikely that the preconditions will be precisely met. Furthermore, when oxidation of  $\text{RED}_{\text{ANS}}$  or reduction of  $\text{OX}_{\text{ANS}}$  is not a mechanistically simple redox process, the cyclic voltammetric response can be quite sensitive to the magnitude of the rate constant for the cross-reaction,  $k_{\text{cross}}$  [45].

Figure 3.15 shows an example of this situation, where a C-paradigm system comprising the previously discussed ANS and IRRS reactions (Eqs. 3.16–3.18) and the added homogeneous reaction (Eq. 3.19) are present [45]. In this figure, voltammograms with  $k_{cross}=0$  and  $k_{cross}=1.0\times10^7$  M<sup>-1</sup> s<sup>-1</sup> and  $k_d=10.0$  s<sup>-1</sup> are compared. The presence of the first-order reaction (Eq. 3.19) amplifies the effect of the cross-reaction. Based on these results, it could be suggested that a conservative but wise experimental protocol is to use the paradigm A as the first option. If this is impossible, then paradigm B may be used. Both can produce independent responses for ANS.

We noted earlier that under certain, precisely defined conditions the cyclic voltammetric response is perfectly independent of the value of  $k_{cross}$  when paradigms B and C are operative [45]. However, the insensitivity of the electrochemical response to the value of  $k_{cross}$  does not mean that nothing is happening: even when those preconditions prevail (and when  $K_{cross} \gg 1$ ), the composition of the diffusion layer is dramatically sensitive to the value of  $k_{cross}$  and that can be seen spectroelectrochemically [72]. If  $k_{cross}$  is large enough the highly favored cross-reaction can produce what Amatore et al. refer to as an acute reaction front [73]. Thus, certainly for spectroelectrochemical measurements the analysis of ANS spectroelectrochemical response should be limited to paradigms A and B.



**Fig. 3.15** Simulations of the CV responses for  $k_{\text{cross}}=0$  (*solid black line*) and  $k_{\text{cross}}=1.0 \times 10^7 \text{ M}^{-1} \text{ s}^{-1}$ (*solid red line*); electrode area = 1.0 cm<sup>2</sup>, scan rate = 1.0 V s<sup>-1</sup>, T=298.2 K,  $c_{\text{RED}_{\text{ANS}}} = 1 \times 10^{-3} \text{ M}$ ,  $D_{\text{OX}_{\text{ANS}}} = D_{\text{RED}_{\text{ANS}}} = D_{\text{OX}_{\text{IRRS}}} = D_{\text{OX}_{\text{IRRS}}} = 1.0 \times 10^{-5} \text{ cm}^2 \text{ s}^{-1}$ ,  $E_{\text{ANS}}^{\theta \prime} = -0.5 \text{ V}$ ,  $c_{\text{RED}_{\text{IRRS}}} = 1 \times 10^{-3} \text{ M}$ ,  $E_{\text{IRRS}}^{\theta \prime} = 0 \text{ V}$ ,  $k_{\text{s,ANS}} = k_{\text{s,IRRS}} = 1.0 \times 10^4 \text{ cm s}^{-1}$ ,  $K_{\text{cross}} = 2.82 \times 10^8$ ,  $K_{\text{d}} = 10^5$ ,  $E_{\text{start}} = -0.25 \text{ V}$ . Reproduced from [45] with permission from the RSC

#### 3.4 Recommendations

As a conclusion, good practice for electrochemistry in ILs dictates that

- If anything other than qualitative data is sought, the use of QRE needs to be avoided. If impossible, the potential of the QRE must be calibrated against an IRRS. The key requirement under this situation is that the voltammetric response for ANS must be independent of the IRRS response (paradigms A or B). As we noted above, the selection of the optimal IRRS is based, to a great extent, on common sense. Errors associated with the QRE drift during the voltammetric experiments must be considered.
- In situations where a large number of experiments are to be performed in the same IL, it is recommended to prepare a Agl0.01 M Ag[CF<sub>3</sub>SO<sub>3</sub>] reference electrode using the IL under study as the solvent in the reference system. If the solubility of Ag[CF<sub>3</sub>SO<sub>3</sub>] in the IL becomes an issue, this can be substituted by a silver salt that contains the same anion as the IL (e.g., in an IL in which the anion is [BF<sub>4</sub>]<sup>-</sup>, silver(I) could be introduced as Ag[BF<sub>4</sub>]). Cryptane-based reference electrodes (AglAg<sup>+</sup> 222, R) could be useful if the electrochemical experiment is exposed to a source of light. However, a precaution should be taken if R = acetonitrile, as it could be a source of impurity in long time experiments. Irrespective of which of these reference electrodes is used, it must be calibrated against an IRRS before and after the experiment, in order to evaluate possible drifts of the reference system during the electrochemical experiment.

- The redox potentials of Fc and Cc<sup>+</sup> are sensitive to the solvation properties of the IL components. Consequently, the use of Fc<sup>+/0</sup> and Cc<sup>+/0</sup> couples as IRRS is expected to be adequate only when a single IL system is being studied; however, corrections may be required in conditions that require comparison between different IL systems.
- Even though DmFc is not freely soluble in ILs, the results presented throughout this chapter suggest that the DmFc<sup>0/+</sup> redox process is a suitable IRRS for voltammetric studies in ionic liquids, as it is less dependent on the IL nature in comparison to what is observed for ferrocene and cobaltocenium.
- If DmFc is not soluble in the IL under study, or if the Fc<sup>+/0</sup> and/or Cc<sup>+/0</sup> couples are preferred, the experimentally obtained  $E_m$  needs to be corrected to eliminate the errors associated with the inequality in the diffusion coefficients as well as the solvation effect of ILs ions.
- The spontaneous reaction observed between DmFc and oxygen brings important consequences in the establishment of conditions under which DmFc should be used. Indeed, it is a suitable IRRS to work under inert atmospheres, such as those present inside argon- or nitrogen-filled glove boxes. However, the application of this redox system as IRRS should be avoided when the experiments are being conducted under atmospheric conditions. Moreover, DmFc sample preparation in ILs should be also performed under an inert atmosphere.

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## Chapter 4 Ultramicroelectrode Voltammetry and Scanning Electrochemical Microscopy in Room Temperature Ionic Liquids

Darren A. Walsh

#### 4.1 Introduction

This year (2014) marks the 25th anniversary of the invention of SECM in the Bard lab at the University of Texas [1, 2]. Such is the impact of its development that the scanning electrochemical microscope (SECM-the same abbreviation is used for the instrument and the method) is now a "textbook" electroanalytical tool used in a wide variety of applications, ranging from fundamental studies of mass and charge transfer dynamics to molecular transport across biological cell membranes, corrosion analysis and electrocatalyst screening [3, 4]. Given the increasing popularity of room-temperature ionic liquids (RTILs) in electrochemical studies and devices [5, 6], it was perhaps inevitable that SECM measurements would also be carried out in RTILs and a number of such studies have appeared in the recent literature [7-10]. However, the unique physicochemical properties of RTILs can lead to very unusual behaviour being observed during SECM. For example, drastic differences in the rates of diffusion of charged and uncharged species can arise in RTILs and such phenomena have been studied using SECM [11]. The high viscosities of RTILs also mean that unusual SECM responses are often obtained in RTILs, unless one carefully controls the experimental parameters [9].

In this chapter, those studies that have involved performing SECM in RTILs will be discussed. As we will see, a relatively small number of such studies have been carried out to date, but unique electrochemical insights have been obtained. In attempting to fully describe how the properties of RTILs affect SECM in these media, the voltammetric behaviour of UMEs must also be described as the operation of the SECM depends on the behaviour of UMEs during electrolytic reactions. The chapter begins with a brief description of the principles of UME voltammetry and

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SECM. The origin of the unusual voltammetric and SECM responses obtained in RTILs is discussed and the effects of a range of electrochemical parameters on the responses are then described. Following this discussion, some of the electrochemical insights that have come from UME voltammetry and SECM in RTILs are discussed.

#### 4.2 Principles of Ultramicroelectrode Voltammetry

UMEs are often defined as electrodes with critical dimensions in the range 1–25  $\mu$ m. Compared to conventional "macroelectrodes" with mm (or larger) dimensions, UMEs exhibit faster double-layer charging, lower ohmic losses and higher rates of mass transport, and these advantages have allowed electrochemists to use UMEs to explore a wide array of phenomena inaccessible to study using macroelectrodes [12–14]. One of the key advantages of UMEs is their ability to carry steady-state (time-independent) currents during the electrolysis of redox-active species, a phenomenon that has been exploited in the development of the SECM. In describing why steady-state currents are often observed at UMEs and not usually at macroelectrodes, we consider first the electrochemical reduction of species Ox to species Red at a spherical electrode of radius  $r_0$  in a solution containing only dissolved Ox and an inert supporting electrolyte. A spherical electrode is considered here because its surface is uniformly accessible and a rigorous mathematical treatment leads to a closed-form solution of the mass transport equation. Reduction of Ox occurs by the addition of *n* electrons to each molecule:

$$Ox + ne^- \rightarrow Red$$
 (4.1)

and, if the potential of the electrode is stepped from an initial potential where the reduction of Ox does not occur to one where Ox is reduced at the diffusion-controlled rate, the concentration gradient is given by integration of Fick's second law:

$$\frac{\partial c_{\text{Ox}}\left(r,t\right)}{\partial t} = D_{\text{Ox}}\left[\frac{\partial^{2} c_{\text{Ox}}\left(r,t\right)}{\partial r^{2}} + \frac{2}{r}\frac{\partial c_{\text{Ox}}\left(r,t\right)}{\partial r}\right]$$
(4.2)

where  $c_{Ox}(r,t)$  is the concentration of Ox at a distance *r* from the centre of the sphere and time *t* after the potential step and  $D_{Ox}$  is the diffusion coefficient of Ox. The boundary conditions for the potential-step experiment are

$$\lim_{r \to \infty} c_{\text{Ox}}\left(r,t\right) = c_{\text{Ox}}^{\infty} \tag{4.3}$$

$$c_{\rm Ox}(r,0) = c_{\rm Ox}^{\infty} \text{ for } r > r_0$$
 (4.4)

$$c_{\text{Ox}}(r_0, t) = 0 \text{ for } t > 0$$
 (4.5)

where  $c_{0x}^{\infty}$  is the bulk solution concentration of Ox. Equation (2) can be solved using Laplace transform methods to give the faradaic current, *i*, flowing through the electrode as a function of *t* [14]:

$$i(t) = \frac{nFAD_{Ox}c_{Ox}^{\infty}}{r_0} + \frac{nFAD_{Ox}^{1/2}c_{Ox}^{\infty}}{\pi^{1/2}t^{1/2}}$$
(4.6)

where F is the Faraday constant (96,485 C/mol) and A is the electrode area. Therefore, the current flowing through a spherical electrode during the reduction of Ox is the sum of time-independent (steady-state) and time-dependent (transient) contributions. At large spherical electrodes (i.e. when  $r_0$  is large), the timeindependent term (first term on the right of Eq. 4.6) is negligible, the electrode can be considered planar, linear diffusion of Ox to the electrode surface dominates and *i* decays with  $t^{1/2}$ . However, at spherical UMEs (i.e. when  $r_0$  is small), the timeindependent term can become significant depending on the experimental conditions. If, for example, the timescale of the experiment is very short (i.e. t is small), the diffusion field remains small relative to the electrode radius, the second term on the right side of Eq. (4.6) dominates and the current decays with  $t^{1/2}$  as expected for linear diffusion to a planar electrode (Fig. 4.1a). However, at long timescales, the diffusion field becomes large relative to  $r_0$ , the second term on the right side of Eq. (4.6) decays such that its contribution to *i* becomes negligible and the spherical character of the diffusion field becomes important (Fig. 4.1b). In this case, a steadystate current,  $i_{ss}$ , flows through the UME, which is given by

$$i_{\rm ss} = 4\pi n F D_{\rm Ox} c_{\rm Ox}^{\infty} r_0 \tag{4.7}$$

where the area of the electrode, A, is given by  $4\pi r_0^2$ .

By far, the most common UME geometry is that of a microdisc inlaid in an insulating sheath but, unlike spherical electrodes, the surface of an inlaid microdisc UME is not uniformly accessible as electrolysis at the edges of the microdisc diminishes diffusion to the disc centre. A rigorous mathematical treatment of the steady-state current at a microdisc is not possible but similar considerations to those described above apply. The faradaic current flowing at a microdisc UME during the electrolysis of a redox-active species contains contributions from a transient component



Fig. 4.1 (a) Linear diffusion to the surface of a spherical electrode at short timescales and (b) spherical diffusion to the electrode surface at long timescales



**Fig. 4.2** (a) Hemispherical diffusion to a microdisk ultramicroelectrode. (b) A steady-state cyclic voltammogram recorded using an ultramicroelectrode. (c) A transient cyclic voltammogram recorded at a macroelectrode

and a steady-state component. The steady-state component arises due to hemispherical diffusion to the microdisc surface (Fig. 4.2a), which leads to a steady-state current given by

$$i_{\rm ss} = 4nFD_{\rm Ox}c_{\rm Ox}^{\infty}a\beta \tag{4.8}$$

where *a* is the radius of the microdisc and  $\beta$  depends on the geometry of the UME. When the ratio of the radius of the non-conducting sheath to that of the microdisc  $(R_g = r_g/a, \text{ where } r_g \text{ is the radius of the sheath})$  is large (>20),  $\beta = 1.00$ , but  $\beta$  increases until it equals 1.43 at  $R_g = 1$  [15]. This means that  $i_{ss}$  at a microdisc UME with a very small  $R_g$  is approximately 40 % larger than that at a microdisc with large  $R_g$  due to the diffusion of redox species from behind the plane of the microdisc surface. A typical sigmoidal, steady-state cyclic voltammogram (CV) obtained at a microdisc UME is shown in Fig. 4.2b and differs from the peaked responses usually obtained at macroelectrodes (Fig. 4.2c), where linear diffusion dominates and the peak height,  $i_p$ , increases as the voltammetric scan rate, v, increases  $(i_p \propto v^{1/2} \text{ at macroelectrodes})$ .

It is clear from the discussion above that diffusion of redox-active species to a disc UME can be dominated by a transient component or a steady-state component depending on the timescale of the experiment (which in a cyclic voltammetry experiment is controlled through v). It can be shown that steady-state CVs should be recorded when [16]

$$\upsilon << \frac{RTD}{nFa^2} \tag{4.9}$$

where *R* is the universal gas constant, *T* is the absolute temperature and *D* is the diffusion coefficient of the redox species under study. Figure 4.3 shows a number of simulated CVs showing the effects of increasing *v* during cyclic voltammetry at a 10-µm-radius UME (note that the diffusion coefficients  $D_{0x}$  and  $D_{Red}$  used to generate the CVs in Fig. 4.3 are typical of those observed in "conventional" aqueous or organic electrolytes). At 0.01 V/s, a steady-state CV is obtained, demonstrating that



**Fig. 4.3** Simulated CVs showing the effects of increasing the voltammetric scan rate during cyclic voltammetry using a 10- $\mu$ m-radius UME. The responses were simulated for a reversible (Nernstian) reaction with n = 1,  $D_{\text{ox}} = D_{\text{Red}} = 10^{-5} \text{ cm}^2/\text{s}$ ,  $c_{\text{ox}} = 1.0 \text{ mM}$ , and T = 25 °C. Steady-state responses are observed at v = 0.01 V/s but at 0.1 V/s and above peaks begin to appear in the CVs. Reprinted with permission from Bard, A J; Faulkner, L R (2001) Electrochemical Methods: Fundamentals and Applications; 2nd ed. Copyright 2001 John Wiley and Sons

the steady-state component dominates at this *v*. While the steady-state component is still dominant as *v* increases to 1 V/s (note, for example, the high current at the switching potential), peaks emerge in the CV, illustrating that the transient component is significant at 1 V/s. In general, UME voltammetry is performed either at low or high scan rates, when the steady-state or transient component, respectively, dominates the observed behaviour [17, 18]. Equation (9) also illustrates why steady-state CVs cannot readily be recorded at macroelectrodes at reasonable timescales; if, for example, *a* is 1 mm and other experimental conditions are as in Fig. 4.3, a steady-state response should be observed at  $v \ll 25 \,\mu$ V/s, a scan rate that corresponds to an experimental "time window" longer than 10<sup>3</sup> s, in which convective effects will be significant and mass transport will no longer occur primarily by diffusion [16].

#### 4.3 Principles of Scanning Electrochemical Microscopy

In SECM, the UME (which is usually called the SECM tip) can be moved in three dimensions, usually under piezo-control. The most common mode of SECM is the amperometric mode, in which a redox-active species is oxidised or reduced at the SECM tip and the effects of moving the tip close to the surface of a second electrode (which is usually called the substrate) are studied. To describe the operation of the amperometric mode of SECM, we again consider the reduction of species Ox to species Red at a disc-shaped SECM tip (Eq. 4.1), which results in the flow of a steady-state current through the tip (Eq. 4.8). In the SECM literature, the

steady-state current at the tip (when the tip is far from any substrate) is usually identified as  $i_{T,\infty}$  rather than  $i_{ss}$  and this convention will be used in the remainder of this chapter. If the SECM tip is brought close to the surface of the substrate, a number of effects can be observed depending on the composition of the substrate. If the substrate is made from an insulating material, diffusion of Ox to the SECM tip surface becomes hindered as the tip approaches the substrate and the tip current,  $i_{\rm T}$ , decreases with decreasing tip-substrate distance, d (Fig. 4.4a). This effect is called negative feedback. Conversely, if the substrate is made from a conducting material, regeneration of Ox occurs at the substrate surface leading to an enhancement in the flux of Ox to the SECM tip as it approaches the substrate (Fig. 4.4b). This enhancement causes an increase in  $i_{\rm T}$  as d decreases and this effect is called positive feedback. The curves shown in Fig. 4.4 are called SECM feedback approach curves and, when presenting such data, d is usually normalised to a and expressed as L and  $i_{\rm T}$  is usually normalised to  $i_{T,\infty}$ . The theoretical basis for SECM is well developed [3, 4, 15, 19] and, while no exact analytical expressions have been found for positive or negative feedback, a number of approximate analytical equations describing the effect of L on  $i_T/i_{T,\infty}$  have been developed. In 2006, an approximate equation describing the effect of positive feedback on the normalised current at a microdisc SECM tip, which included as variables  $R_g$  and L, was developed (earlier equations did not include  $R_{g}$  as a variable) [20]. The general expression, which is accurate to better than 2 % for any L and  $R_s$ , is as follows:

$$\frac{i_{\rm T}}{i_{\rm T,\infty}} = \alpha \left(R_{\rm g}\right) + \frac{\pi}{4\beta \left(R_{\rm g}\right) \arctan L} + \left(1 - \alpha \left(R_{\rm g}\right) - \frac{1}{2\beta \left(R_{\rm g}\right)}\right) \frac{2}{\pi} \arctan L \quad (4.10)$$

where  $\alpha$  and  $\beta$  are given by Eqs. (4.11) and (4.12), respectively:

$$\alpha\left(R_{g}\right) = \ln 2 + \ln 2\left(1 - \frac{2}{\pi}\arccos\frac{1}{R_{g}}\right) - \ln 2\left[1 - \left(\frac{2}{\pi}\arccos\frac{1}{R_{g}}\right)^{2}\right] \quad (4.11)$$

$$\beta(R_g) = 1 + 0.639 \left(1 - \frac{2}{\pi} \arccos \frac{1}{R_g}\right) - 0.186 \left[1 - \left(\frac{2}{\pi} \arccos \frac{1}{R_g}\right)^2\right] \quad (4.12)$$

In the case of negative feedback at an insulating substrate, the following expression is accurate to better than 1 % [21]:

$$\frac{i_T}{i_{r,\infty}} = \frac{\frac{2.08}{R_g^{0.358}} \left(L - \frac{0.145}{R_g}\right) + 1.585}{\frac{2.08}{R_g^{0.358}} \left(L + 0.0023R_g\right) + 1.57 + \frac{\ln R_g}{L} + \frac{2}{\pi R_g} \ln \left(1 + \frac{\pi Rg}{2L}\right)}$$
(4.13)



**Fig. 4.4** SECM feedback approach for (**a**) negative feedback as an SECM tip approaches an insulating substrate and (**b**) positive feedback as an SECM tip approaches a conducting substrate. Reprinted with permission from Fan, F R; Fernández, J L; Liu, B; Mauzeroll, J (2007) Scanning Electrochemical Microscopy. In Zoski, C. G., Ed. Handbook of Electrochemistry. Copyright 2007 Elsevier BV

SECM feedback approach curves such as those shown in Fig. 4.4 are obtained when the rate of the substrate reaction is negligibly small (negative feedback) or very high (positive feedback). In the case of finite heterogeneous electron transfer (ET) kinetics at the substrate, intermediate SECM feedback approach curves are obtained, and theoretical kinetic SECM curves also exist that can be used to obtain kinetic information about the substrate reaction [4, 15]. The kinetics of the ET reaction occurring at an SECM tip can also be studied by positioning the SECM tip very close to the substrate and recording tip CVs and fitting the resulting data to theoretical voltammograms [22]. SECM is often also used in the amperometric imaging mode by scanning the tip across the surface and recording  $i_T$  as the tip passes over regions of varying conductivity or electrochemical activity [4]. Several alternative modes of SECM have also been developed that differ from the amperometric feedback modes described above. In generation-collection mode SECM, a redox-active species is electrochemically "generated" at either the tip or the substrate and is then "collected" at the opposing electrode by oxidising or reducing it. Generation-collection modes of SECM are especially useful for studying homogeneous reactions [23]. Chronoamperometric SECM, in which  $i_T$  is recorded as a function of time, is particularly useful for studying mass transport effects [24]. In alternating current (AC) mode SECM, an AC signal is superimposed onto the potentiostat input signal, which generates an alternating current signal that depends on *L* and the substrate properties [25]. A relatively recent advance is the development of a number of novel modes of SECM based on the use of hollow pipet tips filled with solutions. These new modes of SECM have allowed users to expand the applications of SECM to areas inaccessible to study using conventional SECM. For further information on these methods, the interested reader is directed to the cited works and references therein [26–29].

### 4.4 Instrumentation for Scanning Electrochemical Microscopy

A schematic of a typical SECM is shown in Fig. 4.5. The main components are the bipotentiostat, tip-positioning system, electrochemical cell and data acquisition/ output system. While these basic components are common to almost all SECMs, the SECM tip can differ significantly depending on the particular system under investigation. Due to the ease of fabrication and polishing, microdisc SECM tips are most common. Microdisc tips are constructed by sealing microwires of metals such as Pt



Fig. 4.5 A schematic diagram of a typical SECM

or Au into soft glass tubing and exposing and polishing the cross section of the wire. To ensure that the tips formed using this approach can be positioned close to substrate surfaces, they are usually sharpened to reduce  $R_g$  to below 10 (note that this sharpening affects  $i_{T,\infty}$ ; see discussion above). For some applications, it is necessary to use SECM tips with  $a \ll 10 \ \mu m$  (e.g. for studying rapid charge transfer kinetics or for imaging sub- $\mu m$  features on substrates) and fabricating, polishing and sharpening such very small SECM tips by hand are difficult. The most common method used for fabricating very small tips is to seal a metal microwire into quartz tubing and then to pull the quartz/microwire assembly to a fine point using a laser pipette puller [30, 31]. Other methods include insulating the sides of sharp tips with electrophoretic paint [32] and pushing sharpened wires through wax to leave just the tip exposed [33].

# 4.5 Steady-State Voltammetry at Ultramicroelectrodes in RTILs

If we consider again the parameters used to generate the CVs shown in Fig. 4.3, Eq. (4.9) suggests that steady-state CVs should be recorded in this system at  $v \ll 0.25$  V/s and, indeed, Fig. 4.3 illustrates that linear diffusion to the UME affects the response at almost half that value. However, when performing electrochemical measurements in RTILs, one must consider that diffusion coefficients in RTILs are typically 2–3 orders of magnitude smaller than in conventional aqueous and organic electrolytes. If the diffusion coefficients used to generate the curves shown in Fig. 4.3 were typical of that expected in RTILs (e.g.  $10^{-8}$  cm<sup>2</sup>/s), Eq. (4.9) suggests that steady-state responses would only be recorded at  $\upsilon \ll 0.3$  mV/s at a 10-µm-radius UME. This brief calculation suggests that transient responses may be obtained in RTILs at UMEs under typical UME voltammetry conditions (i.e.  $v \sim 1-10$  mV/s and  $a \sim 5-12.5 \,\mu\text{m}$ ). In an early investigation into such phenomena, Bond and co-workers showed that peak-shaped responses were obtained in the RTIL 1-butyl-3-methylimidazolium hexafluorophosphate, [C<sub>4</sub>mim][PF<sub>6</sub>], during ferrocene (Fc) oxidation at a 5-µm-radius Pt disc UME, even at 1 mV/s (Fig. 4.6a-c) [34]. The transient responses obtained in  $[C_4 mim][PF_6]$  are due to the relatively high viscosity of the RTIL ( $\eta$  = 381 mPa s) [35], which leads to a diffusion coefficient of Fc,  $D_{\rm Fc}$ , of  $6 \times 10^{-8}$  cm<sup>2</sup>/s in this RTIL [36]. By moving to a smaller UME ( $a = 1 \mu m$ ), the authors recorded CVs that resembled a steady-state response, but there was some hysteresis between the forward and reverse sweeps (Fig. 4.6d) [34]. As well as decreasing the UME dimensions, another strategy for moving between transient and steady-state responses in RTILs is to move to a less viscous RTIL. Figure 4.7 shows CVs recorded in  $[C_4 \text{mim}][BF_4]$  ( $\eta = 120 \text{ mPa s and in which } D_{Fc} = 9 \times 10^{-8} \text{ cm}^2/\text{s}$  [36]). Note that the CVs were simulated with a  $D_{\rm Fc}$  of  $5 \times 10^{-7}$  cm<sup>2</sup>/s, an earlier estimate of  $D_{\rm Fc}$  in this RTIL [34]. In this case, an approximately steady-state CV (that showed some hysteresis) was recorded at the 5-µm-radius Pt disc UME at 1 mV/s but not at higher scan rates (Fig. 4.7a-c). However, at the 1-µm-radius UME, a steady-state CV was obtained at 10 mV/s.



**Fig. 4.6** Experimental (*solid line*) and simulated (*open circles, open triangles, open squares*) CVs recorded at a 5-µm-radius Pt microdisk UME at scan rates of (**a**) 50, (**b**) 10 and (**c**) 1 mV/s, and (**d**) at a 1-µm-radius microdisk at a scan rate of 10 mV/s during oxidation of 7 mM ferrocene (Fc) in  $[C_4mim][PF_6]$  at 25 °C. Potentials are vs. Fc/Fc<sup>+</sup> and the simulated voltammograms represent those calculated for a reversible process with a diffusion coefficient of  $6 \times 10^{-8}$  cm<sup>2</sup>/s. Reprinted with permission from Carano, M; Bond, A M (2007) Aust. J. Chem. 60:29–34. Copyright 2007 CSIRO

Walsh and co-workers also analysed the effects of the tip dimensions and voltammetric scan rates during cyclic voltammetry in a range of imidazolium-based RTILs with widely varying viscosities. Fc was again used as the redox species and the data are shown in Fig. 4.8. In this study, a relatively large UME ( $a=12.5 \mu$ m) and a small UME ( $a=1.5 \mu$ m) were used. Figure 4.8a shows the CVs recorded at the 12.5-µm-radius UME at 1 mV/s  $\leq v \leq 50$  mV/s in [C<sub>4</sub>mim][PF<sub>6</sub>]. Transient responses were obtained at each v due to linear diffusion of Fc to the UME surface. The application of Eq. (4.9) to this system indicates that transient responses should indeed have been observed at v > 1 mV/s. Figure 4.8b shows the responses obtained at the 12.5-µm-radius UME in the less viscous RTIL 1-ethyl-3-methylimidazolium bis[trifluoromethanesulfonyl]imide, [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] (which has  $\eta=27$  mPa s and in which  $D_{Fc}=4 \times 10^{-7}$  cm<sup>2</sup>/s). According to Eq. (4.9), steady-state CVs should be



**Fig. 4.7** Experimental (*solid line*) and simulated (*open circles, open triangles, open squares*) CVs recorded at a 5-µm-radius Pt microdisk UME at scan rates of (**a**) 50, (**b**) 10 and (**c**) 1 mV/s, and (**d**) at a 1-µm-radius microdisc at a scan rate of 10 mV/s during oxidation of 7 mM Fc in [C<sub>4</sub>mim][BF<sub>4</sub>] at 25 °C. Potentials are vs. Fc/Fc<sup>+</sup> scale and the simulated voltammograms represent those calculated for a reversible process with a diffusion coefficient of  $5 \times 10^{-7}$  cm<sup>2</sup>/s. Reprinted with permission from Carano, M; Bond, A M (2007) Aust. J. Chem. 60:29–34. Copyright 2007 CSIRO

recorded in this RTIL at  $v \ll 6 \text{ mV s}^{-1}$  at a 12.5-µm UME and Fig. 4.8b shows that a steady-state CV (although with hysteresis between the forward and reverse sweeps) was recorded at v=1 mV/s, but, as the scan rate increased, peak-shaped responses were clearly obtained, demonstrating that linear diffusion became significant at higher scan rates.

Figure 4.8c, d shows the CVs recorded using the 1.5- $\mu$ m UME at 1, 10 and 50 mV/s in [C<sub>4</sub>mim][PF<sub>6</sub>] and [C<sub>2</sub>mim][N(Tf)<sub>2</sub>]. Equation (9) predicts that steady-state CVs should be observed at  $v \ll 70$  mV/s in [C<sub>4</sub>mim][PF<sub>6</sub>] and Fig. 4.8c shows that such responses were recorded at v < 10 mV/s. However, when v = 50 mV/s, slightly peak-shaped responses were obtained, demonstrating that linear diffusion



**Fig. 4.8** Cyclic voltammograms obtained at a 12.5- $\mu$ m-radius Pt disk UME in (**a**) 3.20 mM Fc in [C<sub>4</sub>mim][PF<sub>6</sub>] and (**b**) 1.56 mM Fc in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>]. (**c**) and (**d**) Responses obtained at a 1.5- $\mu$ m-radius Pt disk UME in 3.20 mM Fc in [C<sub>4</sub>mim][PF<sub>6</sub>] and 1.56 mM Fc in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>], respectively. The voltammetric scan rates were 1, 10 and 50 mV/s and additionally 5 mV/s for (**d**). Reprinted with permission from Lovelock, K R J; Cowling, F N; Taylor, A W; Licence, P; Walsh, D A (2010) J. Phys. Chem. B 114:4442–4450. Copyright 2010 American Chemical Society

became significant as the voltammetric scan rate approached 70 mV/s, in agreement with the expected behaviour. In the case of the CVs recorded in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>], Eq. (4.9) suggests that steady-state CVs should be obtained at  $\upsilon \ll 400$  mV/s at a 1.5-µm UME and Fig. 4.8d shows that true steady-state CVs could be recorded at  $\upsilon < 10$  mV/s. At 50 mV/s (green line in Fig. 4.8d), the shape of the CV changed slightly and the current at the switching potential increased above those observed at lower scan rates, suggesting that a purely steady-state response may not have been recorded at this scan rate.

In summary, the UME voltammetry that has been performed in RTILs has illustrated the crucial roles that the UME dimensions, the RTIL viscosity (and consequently the diffusion coefficient of the redox species) and the voltammetric scan rate play in such measurements. If one wants to record truly steady-state CVs in RTILs, it is important to consider each effect and, for electroanalysis in especially viscous RTILs, much smaller UMEs may be required to record steady-state currents.

#### 4.6 Scanning Electrochemical Microscopy in RTILs

Prior to carrying out SECM experiments in "conventional" organic and aqueous electrolytes, one usually records steady-state CVs (with the tip positioned far from any substrate) to ensure that the tip is "behaving" as expected. Such measurements are usually not problematic, assuming that the SECM tip has been prepared carefully and does not allow, e.g. a leak of the electrolyte into the electrode interior. In conventional electrochemical solvents, such CVs are usually recorded at a scan rate of a few mV/s. However, the discussion in the previous section illustrated some of the challenges that one faces when attempting to record steady-state currents using UMEs in RTILs and the crucial roles that  $a, \eta$  and v play during such measurements. During SECM measurements in RTILs, not only must a and  $\eta$  be considered, the fact that the SECM tip is usually moving within the RTIL must also be considered. The effects of moving an SECM tip within an RTIL were first explored by Bond and co-workers who recorded SECM feedback approach curves during Fc oxidation in  $[C_4 mim][BF_4]$  using a 5-µm-radius microdisc SECM tip at a tip approach speed,  $\nu_0$ , of 0.1 µm/s (main frame of Fig. 4.9) [34]. Note that under these conditions the experimental curve agreed with that predicted by conventional SECM theory. However, in the more viscous  $[C_4 mim][PF_6]$ , the experimental feedback approach curves deviated from the theoretical curves. During the positive feedback experiment,  $i_{T}$  was lower than that predicted by theory at all L values, and during the negative feedback experiment,  $i_{\rm T}$  was higher than that predicted by theory at all L values (except at L>8).

Hapiot and co-workers also performed SECM measurements in a viscous RTIL and recorded unusual SECM feedback approach curves. In this case, SECM was performed in the pure ferrocenyl RTIL [FcC<sub>1</sub>mim][N(Tf)<sub>2</sub>] at 50 °C (the high temperature was necessary due to the high melting point of this RTIL), and the results are shown in Fig. 4.10 [8]. The diffusion coefficient of [FcC<sub>1</sub>mim][N(Tf)<sub>2</sub>] is  $3.3 \times 10^{-8}$  cm<sup>2</sup>/s. In this RTIL, similar results to those observed by Bond and co-workers were observed. At  $\nu_0 = 1 \mu m/s$ , a negative feedback was observed as the tip approached an insulating substrate, but the curve did not fit the conventional SECM theory satisfactorily ( $i_T$  was higher than that predicted by theory at all *L*). During the positive feedback approach curve experiment,  $i_T$  was lower than that predicted by theory. Interestingly, at high  $\nu_0$  (10 µm/s),  $i_T$  increased as the tip approached an insulating substrate, an effect that has been attributed to convective mass transfer to the tip surface.



**Fig. 4.9** Comparison of theoretical (*open circles*) and experimental SECM approach curves obtained using 5 mM Fc dissolved in  $[C_4mim][BF_4]$  (*solid line*) and  $[C_4mim][PF_6]$  (*dashed line*) at a 5-µm-radius Pt SECM tip with a tip speed of 0.1 µm/s. The equilibration time before commencing each approach was 50 s. The potential applied at the SECM tip was 0.6 V vs. Ag wire. The positive feedback curve was obtained by approaching a conducting Pt disk biased at 0.0 V vs. the Ag wire quasi-reference electrode and the negative feedback curve was obtained by approaching a glass slide. Inset: Theoretical (*open squares*) and experimental (*solid line*) data obtained in  $[C_4mim][PF_6]$  using a 1-µm-radius SECM tip and tip speed of 0.05 µm/s. Reprinted with permission from Carano, M; Bond, A M (2007) Aust. J. Chem. 60:29–34. Copyright 2007 CSIRO

LeSuer performed SECM in deep eutectic solvents (DES), which constitute a sub-class of RTILs, consisting of choline chloride and either trifluoroacetamide or malonic acids as the hydrogen-bond donor [37]. In LeSuer's DESs, the shape of the negative feedback approach curves differed as  $\nu_0$  was altered (Fig. 4.11) and the responses were reminiscent of those recorded by Bond in [C<sub>4</sub>mim][PF<sub>6</sub>] using a 5-µm-radius SECM tip (Fig. 4.9), i.e. in the positive feedback experiment,  $i_T$  was lower than that predicted by theory at all *L*, and during the negative feedback experiment,  $i_T$  was higher than that predicted by theory at all *L*.

In Bond's, Hapiot's, and LeSuer's negative feedback experiments,  $i_T$  was higher than that expected from theory at all *L* due to convective mass transfer of the redox species to the moving tip. In the case of the positive feedback approach curve experiments, sluggish diffusion of the redox species to the SECM tip meant that  $i_T$  was



**Fig. 4.10** SECM feedback approach curves at 1  $\mu$ m/s at insulating (*open diamonds*) and conducting (*cross symbols*) substrates in [FcC<sub>1</sub>mim][N(Tf)<sub>2</sub>] at 50 °C. *Dashed lines* show the theoretical feedback approach curves. Reprinted with permission from Fontaine, O; Lagrost, C; Ghilane, J; Martin, P; Trippe, G; Fave, C; Lacroix, J C; Hapiot, P; Randriamahazaka, H N (2009) J. Electroanal. Chem. 632:88–96. Copyright 2009 Elsevier BV



**Fig. 4.11** (a) Positive feedback and (b) negative feedback approach curves in a 1:2 choline chloride/trifluoroacetamide deep eutectic solvent containing 15 mM Fc as the redox mediator. The *x*-axis represents normalised distance only for theoretical curves (*dashed lines*). Experimental curves were normalised by assuming that tip/substrate contact occurred at L=0. The diffusion coefficient of Fc in the DES is  $2.7 \times 10^{-8}$  cm<sup>2</sup>/s. Reprinted with permission from Nkuku, C A; LeSuer, R J (2007) J. Phys. Chem. B 111:13271–13277. Copyright 2007 American Chemical Society

lower at all *L* than that expected from theory. However, just as one can preferentially record steady-state CVs at UMEs in RTILs by moving to smaller electrodes, one can change the dimensions of the SECM tip in order to record steady-state SECM feedback approach curves. The inset of Fig. 4.9 shows that by decreasing the radius of their SECM tip from 5 to 1  $\mu$ m and reducing  $\nu_0$  from 0.1 to 0.05  $\mu$ m/s, Bond and co-workers could ensure that steady-state currents flowed during the feedback approach curve experiment in [C<sub>4</sub>mim][PF<sub>6</sub>] and that the experimental curves agreed with theory [34].

The magnitudes of convective and diffusive mass transport to a moving SECM tip are related to the SECM tip dimensions by a dimensionless parameter known as the Péclet number,  $Pe = \nu_0 a/D$  [38]. When  $Pe \le 0.01$  (i.e. low  $\nu_0$ , small a and high D), convection does not contribute significantly to mass transport to the tip [37]. At Pe > 1 (i.e. high  $\nu_0$ , large a and low D), convection contributes significantly to mass transfer to the tip surface, and feedback approach curves do not fit conventional SECM theory. Hapiot and co-workers calculated Pe values of 1.5 and 15 for their work on  $[FcC_1mim][N(Tf)_2]$  at 50 °C at  $\nu_0 = 1 \mu m/s$  and the curves shown in Fig. 4.10 confirm that the feedback approach curves did not fit conventional steady-state SECM theory at this  $\nu_0$  [8]. Walsh and co-workers have explored the effects of experimental parameters during SECM in [C<sub>n</sub>mim][N(Tf)<sub>2</sub>] RTILs and compared the observed behaviour with that expected from calculating Pe values. By increasing the length of the alkyl chain on the RTIL cation, they synthesised a series of RTILs of increasing viscosities. Figure 4.12 shows that steady-state negative feedback approach curves were recorded at small  $\nu_0$  values using a 1.5-µm-radius SECM tip in  $[C_4 mim][N(Tf)_2]$ ,  $[C_6 mim][N(Tf)_2]$  and  $[C_8 mim][N(Tf)_2]$  but not in  $[C_4 mim]$  $[PF_6]$  due to its especially high viscosity. In those experiments that did yield steadystate SECM feedback approach curves, Pe was less than 0.01, in agreement with the expected behaviour.

As well dealing with (presumably unwanted) convective effects during SECM in RTILs by changing the experimental parameters, one can incorporate convective effects into the model used to describe the SECM feedback approach curves. LeSuer has developed a method in which Pe can be incorporated as an adjustable parameter into the simulation of SECM feedback approach curves [37]. Figure 4.13 shows experimental feedback approach curves recorded in a DES at a range of  $\nu_0$  values and the accompanying simulations that describe the observed behaviour very well. Good agreement between simulated curves that incorporate Pe into the model and feedback approach curves recorded by Walsh and co-workers during the oxidation of ferrocenemethanol in [C<sub>8</sub>mim][PF<sub>6</sub>] (for which Pe=2) has also been demonstrated [10].

In summary, it is clear that SECM in RTILs can be complicated by the high viscosity of the liquids. Sluggish diffusion within RTILs, combined with convective effects that can become apparent at moving SECM tips in RTILs, can yield non-steady-state feedback approach curves. If one wants to combat such effects and record steady-state SECM feedback approach curves in RTILs, one can consider



**Fig. 4.12** Negative feedback SECM approach curves obtained in (**a**) 3.20 mM Fc in  $[C_4mim][PF_6]$  ( $\eta = 203$ ), (**b**) 3.50 mM Fc in  $[C_4mim][N(Tf)_2]$  ( $\eta = 43$ ), (**c**) 3.30 mM Fc in  $[C_6mim][N(Tf)_2]$  ( $\eta = 59$ ) and (**d**) 4.35 mM Fc in  $[C_8mim][N(Tf)_2]$  ( $\eta = 84$ ) as a 1.5-µm SECM tip approached a PTFE substrate. The tip was held at (**a**) +0.43 V, (**b**) +0.47 V, (**c**) +0.38 V and (**d**) +0.38 V vs. Fc/Fc<sup>+</sup>. In each case, the viscosities were measured using a falling ball viscometer and the *dashed line* shows the theoretical negative feedback approach curve generated for an SECM tip with RG=10 (RG=8 in **d**). Reprinted with permission from Lovelock, K R J; Cowling, F N; Taylor, A W; Licence, P; Walsh, D A (2010) J. Phys. Chem. B 114:4442–4450. Copyright 2010 American Chemical Society

changing the tip dimensions, the RTIL viscosity (if possible) and the tip approach speed. However, it may well be that the fabrication and the use of especially small SECM tips will be necessary as users attempt to perform steady-state SECM in highly viscous RTILs. An alternative strategy, as proposed by LeSuer [37], is to incorporate convective effects into the model used to describe the shape of SECM feedback approach curves, and from the few studies in which such models have been used, this appears to be a very promising approach.


**Fig. 4.13** Experimental (*solid lines*) and simulated (*squares*) SECM feedback approach curves recorded during oxidation of 15 mM Fc in a choline chloride/trifluoroacetamide DES. Reprinted with permission from Nkuku, C A; LeSuer, R J (2007) J. Phys. Chem. B 111:13271–13277. Copyright 2007 American Chemical Society

# 4.7 Effects of Non-equal Diffusion Coefficients on Scanning Electrochemical Microscopy

Due to the high density of charges within RTILs, the reduced and oxidised forms of a redox mediator can exhibit drastically different diffusion coefficients, a phenomenon that is less significant in organic solvents [11, 39]. An example of the effects of such an inequality was reported by Compton and co-workers who used cyclic voltammetry to study the  $O_2/O_2^{--}$  system in the RTIL [N<sub>2226</sub>][N(Tf)<sub>2</sub>], where [N<sub>2226</sub>] is the triethylhexylammonium ion [40]. In this RTIL, the diffusion coefficient of  $O_2$  is more than an order of magnitude larger than that of  $O_2^{--}$ . Remarkably, the effects of this difference in diffusion coefficients can be observed in a single CV (Fig. 4.14) [41]. This CV shows that hemispherical diffusion of  $O_2$  to the Au UME dominated during the reduction sweep (due to diffusion of  $O_2$  from the RTIL from an expanding hemispherical diffusion field), while linear diffusion of  $O_2^{--}$  dominated during the oxidation sweep (due to the formation of a relatively thin diffusion field).

Hapiot and co-workers studied the  $O_2/O_2^{-\epsilon}$  system using SECM and the feedback approach curves obtained using  $O_2/O_2^{-\epsilon}$  in  $[N_{2224}][N(Tf)_2]$ , where  $[N_{2224}]$  is the triethylbutylammonium ion, are shown in Fig. 4.15 [11]. At  $\nu_0=5 \mu$ m/s, an unusual negative feedback approach curve was observed as the tip approached the conducting Pt substrate due to the low diffusion coefficient of  $O_2^{-\epsilon}$ , which hindered the regeneration of  $O_2$  at the substrate. However, at a slower  $\nu_0$  (0.2  $\mu$ m/s), positive feedback was observed because tip movement was slow enough to allow sufficient time for



**Fig. 4.14** A cyclic voltammogram showing the reduction of  $O_2$  in  $[N_{2226}][N(Tf)_2]$  at an Au microdisk UME with  $a=5 \ \mu m$ ,  $v=0.5 \ V/s$  and  $T=308 \ K$ . Inset is a schematic indicating the dominant mode of diffusion to the electrode surface responsible for dictating the shape of the forward and reverse waves. Reprinted with permission from Buzzeo, M C; Evans, R G; Compton, R G (2004) ChemPhysChem 5:1106–1120. Copyright 2004 Wiley VCH



**Fig. 4.15** SECM feedback approach curves obtained at an Au SECM tip as it approached a Pt substrate in  $[N_{2224}][N(Tf)_2]$  in the presence of O<sub>2</sub>. The substrate potential was -0.1 V vs. the saturated calomel electrode (SCE) and the tip potential was -1.1 V vs. SCE.  $\nu_0 = 5 \mu m/s$  (*open squares*).  $\nu_0 = 0.2 \mu m/s$  (*filled squares*). Reprinted with permission from Ghilane, J; Lagrost, C; Hapiot, P (2007) Anal. Chem. 79:7383–7391. Copyright 2007 American Chemical Society

the diffusion of  $O_2^-$  to the substrate and regeneration of  $O_2$ . This example shows that SECM feedback approach curves can become complicated when the ratio of  $D_{red}$  to  $D_{ox}$  ( $\gamma = D_{red}/D_{ox}$ ) is far from unity but are possible if  $\nu_0$  is sufficiently low. The effect of adding varying concentrations of dimethylformamide (DMF) as a co-solvent was also studied by SECM using the  $O_2/O_2^-$  system in  $[N_{2224}][N(Tf)_2]$  [42].  $D_{ox}$ and  $D_{red}$  increased drastically with increasing DMF concentration, due to a decrease in the viscosity of the electrolyte. However,  $\gamma$  also increased exponentially with the addition of DMF, demonstrating that higher concentrations of DMF had a far greater effect on  $D_{red}$  than on  $D_{ox}$  and that the addition of the DMF reduced the strength of the interactions between the cation of the RTIL and  $O_2^-$ .

# 4.8 Studying Electron Transfer in RTILs Using SECM

When an SECM tip is positioned close (within about 1-tip radius) to a substrate, the mass transfer coefficient, m, is equal to D/d. By decreasing d, it is possible to achieve extremely high rates of mass transfer to the tip surface and measure the kinetics of very fast reactions [43]. For example, Mirkin and co-workers have fabricated SECM tips with radii as small as 10 nm and studied kinetics of fast ET reactions in aqueous and non-aqueous solutions [22]. Furthermore, using this approach, they estimate that rate constants as large as 200 cm/s may be measurable using nm-sized SECM tips.

For a simple quasi-reversible redox reaction at a disc-shaped SECM tip, coupled with the diffusion-controlled regeneration of the mediator at the substrate, the normalised tip current at potential E is given by [22]:

$$I_{\rm T}(E,L) = \frac{k_2}{L(\theta+1/\kappa)} + \frac{k_1 + k_3 \exp(k_4/L)}{\theta \left[1 + \frac{\pi}{\kappa\theta} \frac{2\kappa\theta + 3\pi}{4\kappa\theta + 3\pi^2}\right]}$$
(4.14)

where  $k_1, k_2, k_3$  and  $k_4$  are constants.  $\theta$  and  $\kappa$  for an oxidation reaction are given by

$$\theta = 1 + \exp\left[\frac{F}{RT} \left(E^{\circ'} - E\right)\right] \frac{D_{\text{ox}}}{D_{\text{red}}}$$
(4.15)

$$\kappa = \pi \lambda \, \exp\left[\frac{(1-\alpha)F}{RT} \left(E - E^{\circ'}\right)\right] / 4I_{\rm T}^{\circ} \tag{4.16}$$

where  $E^{0'}$  is the formal potential,  $\alpha$  is the transfer coefficient and the kinetic parameter,  $\lambda = k^0 a/D$ , where  $k^0$  is the standard heterogeneous electron transfer rate constant.  $I_{\rm T}^{\rm c}$  is the normalised diffusion-limiting tip current for the same *L* above a conducting substrate. By positioning SECM tips close to substrate surfaces, recording tip CVs, and fitting the resulting data to Eq. (4.14), Walsh and co-workers have



**Fig. 4.16** Experimental voltammograms (*solid lines*) obtained at a 1.5-µm-radius Pt SECM tip at distances of L=0.12, 0.15, 0.20, 0.30, 0.54 and  $L \rightarrow \infty$  from a 1-mm-radius Pt-disk substrate. The solution was 9 mM [FcC<sub>1</sub>mim][N(Tf)<sub>2</sub>] in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] and the substrate potential was -0.6 V vs. Ag/Ag<sup>+</sup>. The theoretical voltammograms at each distance (*open circles*) were calculated using Eq. (4.14) in the text. Reprinted with permission from Taylor, A W; Qiu, F L; Hu, J P; Licence, P; Walsh, D A (2008) J. Phys. Chem. B 112:13292–13299. Copyright 2008 American Chemical Society

measured  $k^0$  values for a number of electrochemical reactions. For example, Fig. 4.16 shows tip CVs recorded at a range of *L* values in a solution of [FcC<sub>1</sub>mim] [N(Tf)<sub>2</sub>] when dissolved in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] [44]. In this case, the  $k^0$  value obtained from fitting the experimental data to Eq. (4.14) (7.6×10<sup>-3</sup> cm/s) was slightly higher than that obtained using cyclic voltammetry (4.25×10<sup>-3</sup> cm/s) and was also slightly higher than that determined by Hapiot and co-workers for the same system using cyclic voltammetry and electrochemical impedance spectroscopy [8]. Walsh and co-workers have also used the same method to determine  $k^0$  for Fc oxidation in a series of imidazolium-based RTILs with varying viscosities [9]. In general, the  $k^0$ values determined using SECM were higher than those determined using cyclic voltammetry [45], suggesting that the use of cyclic voltammetry for kinetic measurements in RTILs can lead to significant underestimations of  $k^0$ . In this study, the  $k^0$ values determined for Fc oxidation using SECM were also correlated with the RTIL viscosity, revealing an inverse relationship between  $k^0$  and  $\eta$  (Fig. 4.17) [9].

Studies of ET, as well as ion and molecule transfer, across the interface between two immiscible electrolyte solutions (ITIES) have been of interest for a number of years. Traditionally, the phases involved are water and a water-immiscible organic solvent. However, in recent years a number of researchers have replaced the organic phase in such experiments with a water-immiscible RTIL. This approach has been



**Fig. 4.17** Graph of the heterogeneous electron transfer rate constant,  $k^0$ , vs. viscosity for Fc oxidation in [CnC<sub>1</sub>Im][Tf<sub>2</sub>N] RTILs, where n = 2-8. The *error bars* represent the standard deviation of four measurements of  $k^0$ . Reprinted with permission from Lovelock, K R J; Cowling, F N; Taylor, A W; Licence, P; Walsh, D A (2010) J. Phys. Chem. B 114:4442–4450. Copyright 2008 American Chemical Society

described by Mirkin and co-workers, who compared the rate of ET across the RTIL/ water interface with that of ET across the organic/water interface using the  $[Fe(CN)_6]^{4-}/[Fe(CN)_6]^{3-}$  system as the redox probe (Fig. 4.18) [46]. In this experiment, the upper aqueous phase contained  $[Fe(CN)_6]^{4-}$ , which was oxidised to  $[Fe(CN)_6]^{3-}$  at a Pt SECM tip. The electrogenerated  $[Fe(CN)_6]^{3-}$  diffused to the  $[C_8mim][N(Tf)_2]/water(w)$  interface where it was reduced by interfacial ET from Fc dissolved in the RTIL:

$$\operatorname{Fc}(\operatorname{RTIL}) + \left[\operatorname{Fe}(\operatorname{CN})_{6}\right]^{3-}(w) \to \operatorname{Fc}^{+}(\operatorname{RTIL}) + \left[\operatorname{Fe}(\operatorname{CN})_{6}\right]^{4-}(w) \quad (4.17)$$

The rate of ET across the RTIL/water interface was drastically higher than that across the 1,2-dichloroethane/water interface. In a later study using the same RTIL, the authors showed that Fc partitioning from the RTIL into the aqueous phase was significant and that there was a large contribution to the tip current from oxidation of Fc at the tip in the water phase [47]. This phenomenon is known as SECM-induced transfer (SECMIT) as Fc is transferred from the RTIL to the aqueous phase (Fig. 4.19). To study the kinetics of ET across the RTIL–water interface, the authors developed a method for separating the current due to partitioned Fc oxidation from the total current, allowing accurate measurement of the kinetics of interfacial



**Fig. 4.18** Schematic diagram of the measurement of electron transfer kinetics between Fc dissolved in  $[C_8mim][N(Tf)_2]$  and  $Fe(CN)_6^{3-}$  dissolved in water. Reprinted with permission from Laforge, F O; Kakiuchi, T; Shigematsu, F; Mirkin, M V (2004) J. Am. Chem. Soc. 126:15380–15381. Copyright 2004 American Chemical Society



**Fig. 4.19** Scheme of an SECMIT/feedback experiment at the water/ $[C_8mim][N(Tf)_2]$  interface. Reprinted with permission from Laforge, F O; Kakiuchi, T; Shigematsu, F; Mirkin, M V (2006) Langmuir 22:10705–10710. Copyright 2006 American Chemical Society

ET. The same authors also studied ET reactions involving the  $[IrCl_6]^{3-/2-}$  and  $[Ru(CN)_6]^{4-/3-}$  systems, which were dissolved in the aqueous phase [47].

Wittstock and co-workers have used SECM to explore the kinetics of dye regeneration in dye-sensitised solar cells (DSSCs) using an RTIL electrolyte [48]. In this experiment, I<sup>-</sup> was electrogenerated from I<sub>3</sub><sup>-</sup> at a Pt SECM tip (Fig. 4.20). As the tip approached a TiO<sub>2</sub> substrate, which was coated with a DSSC dye (in this case *cis*-*di*(thiocyanato)bis(2,2'-bipyridyl-4,4"-dicarboxylate)ruthenium, which is usually



**Fig. 4.20** Schematic diagram of the feedback-mode SECM experiment used to measure the rate of dye regeneration in dye-sensitised solar cells. Reprinted with permission from Tefashe, U M; Nonomura, K; Vlachopoulos, N; Hagfeldt, A; Wittstock, G (2012) J. Phys. Chem. C 116:4316–4323. Copyright 2012 American Chemical Society

labelled N719),  $I_3^-$  was regenerated by ET from I<sup>-</sup> to the oxidised dye. Regeneration of  $I_3^-$  at the dye-coated substrate increased the flux of  $I_3^-$  to the tip which increased  $i_{\rm T}$  above that expected for pure negative feedback. Using this method, the authors showed that dye regeneration kinetics are faster in acetonitrile-based electrolytes than in the exemplar RTIL  $[C_2 mim][N(TF_2)]$ . By adding various ions to the RTIL, the group identified drastic decreases in the effective rate constant for dye regeneration,  $k_{\text{eff}}$ , with increasing cation concentration. For example, Fig. 4.21a shows SECM feedback approach curves recorded in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] containing varying amounts of  $Li[N(Tf)_2]$ . At the highest concentration of  $Li[N(Tf)_2]$ , the feedback approach curve overlapped with the curve expected for the hindered diffusion of  $I_3^-$  to the tip (i.e. pure negative feedback). However, as the concentration of  $Li[N(Tf)_2]$  decreased, the rate of  $I_3^-$  regeneration increased resulting in an increase in  $i_{\rm T}$  at all L values. By fitting the entire feedback approach curves to theoretical kinetic SECM feedback approach curves, the group extracted effective rate constants,  $k_{\rm eff}$ , for dye regeneration and Fig. 4.21b shows the effect of the concentration of Li<sup>+</sup>, as well as that of the 1,2,-dimethyl-3-propylimidazolium and tetrabutylammonium cations, on  $k_{\text{eff}}$ . In each case, increasing the concentration of the cations within the RTIL decreased  $k_{\text{eff}}$  and the effect was most prominent for the Li<sup>+</sup> cation. These effects were attributed to (1) cation adsorption onto the substrate, which can shift the energy of the conduction band of the  $TiO_2$  (in the case of Li<sup>+</sup>), (2) possible changes in the local I<sup>-</sup> concentration near the substrate due to cation adsorption and (3) possible changes in the substrate structure due to interactions between the dye and the cations. For those interested in the development of new electrolytes for DSSCs, such insights are extremely valuable and could lead to the development of new RTIL electrolytes for DSSCs, which would benefit from the non-volatility of the RTILs and overcome the problem of solvent loss in DSSCs. The advantage of using the "photo-SECM" method for determining kinetic parameters is that the measurements are performed at a single sensitised electrode rather than within a complete DSSC, offering a potentially simpler route to kinetic data on such devices.



**Fig. 4.21** (a) SECM feedback approach curves recorded using a Pt SECM tip ( $a=12.5 \ \mu\text{m}$ ) as it approached a TiO<sub>2</sub>/N719 film illuminated with green LED with an intensity of  $25.5 \times 10^{-9} \ \text{mol/} \ \text{cm}^2/\text{s}$  and in solutions containing 0.064 mM [I<sub>3</sub><sup>-</sup>]\* and various concentration of Li[N(Tf)<sub>2</sub>] in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>]. The Li[N(Tf)<sub>2</sub>] concentrations were (1) 2.5 M, (2) 2.02 M, (3) 1.51 M, (4) 1.05 M, (5) 0.5 M and (6) 0.01 M. (b) Plot of  $k_{\text{eff}}$  as a function of cation concentration for three different electrolytes compositions varying only in terms of cation counter ions (1) Lil/I<sub>2</sub>/Li[N(Tf)<sub>2</sub>], (2) [mmpim][I/I<sub>2</sub>/[mmpim][N(Tf)<sub>2</sub>] and (3) [TBA]I/I<sub>2</sub>/[TBA][N(Tf)<sub>2</sub>] in [C<sub>2</sub>mim] [N(Tf)<sub>2</sub>], where [mmpim]<sup>+</sup> is the 1,2,-dimethyl-3-propylimidazolium cation and [TBA]<sup>+</sup> is the tetrabutylammonium cation. Reprinted with permission from Tefashe, U M; Nonomura, K; Vlachopoulos, N; Hagfeldt, A; Wittstock, G (2012) J. Phys. Chem. C 116:4316–4323. Copyright 2012 American Chemical Society

# 4.9 SECM Imaging in Ionic Liquids

The resolution that can be achieved during SECM imaging is predominantly governed by the magnitudes of *a* and *d* so surface features ~10 µm in diameter can be imaged by SECM routinely. To date, there are only a couple of reports on the use of SECM imaging in RTILs. In one example of SECM imaging in RTILs, Bond and co-workers imaged an Ag substrate using Fc dissolved in [C<sub>4</sub>mim][BF<sub>4</sub>] at a 5-µm-radius tip and a lateral tip speed of 0.2 µm/s [34]. Mirkin and co-workers imaged the surface of a compact disc using Fc dissolved in [C<sub>8</sub>mim][N(Tf)<sub>2</sub>] as the redox species with a 0.19-µm-radius tip and lateral tip speed of 0.5 µm/s (Fig. 4.22) [49].

# 4.10 Conclusions

While the number of papers describing the use of UME voltammetry and SECM in RTILs is relatively small, it is clear that these methods are very useful for studying electrochemical phenomena in RTILs. Given that this field is relatively young, it is



**Fig. 4.22** Constant-height SECM image of a 3.5  $\mu$ m ×3.5  $\mu$ m portion of a gold CD surface obtained using a 190 nm Pt tip in [C<sub>8</sub>mim][N(Tf)<sub>2</sub>] containing 50 mM Fc. The lateral scan rate was 500 nm/s. Reprinted with permission from Laforge, F O; Velmurugan, J; Wang, Y X; Mirkin, M V (2009) Anal. Chem. 81:3143–3150. Copyright 2009 American Chemical Society

perhaps not surprising that much of the work done thus far is quite "fundamental" in nature, focusing on phenomena such as mass and charge transport in RTILs. The sluggishness of mass transport in RTILs, and how it affects voltammetry and SECM, is a particularly common theme and the effects of experimental parameters on mass transport to ultramicroelectrodes are now well understood. Even in modestly viscous RTILs, SECM feedback approach curves can be complicated by convective mass transport to the moving tip and the use of the Péclet number can guide users towards the appropriate tip dimensions and speeds to ensure that steady-state responses are obtained. However, as electrochemists move to especially viscous RTILs, it is likely that very small (nm-sized) SECM tips will be required to record steady-state responses, and it is fortunate that there are now several methods available for fabricating nanoscopic SECM tips. An interesting development is the recent availability of a model for producing SECM feedback approach curves, which includes the Péclet number as an adjustable parameter. In those RTILs that are too viscous for steady-state SECM to be performed, even using nm-sized SECM tips, this model can provide useful information about mass transport in RTILs.

There is little doubt that, as this field develops, new insights into the electrochemical behaviour of RTILs will be revealed by UME voltammetry and SECM. SECM has already been used to study the kinetics of electron transfer between RTILs and solid electrodes, and the use of SECM to probe the kinetics of dye regeneration in RTIL-based solar cells has demonstrated the power of these methods. As the electrochemical applications of RTILs now extend to sensors, batteries and fuel cells, it is likely that UME voltammetry and SECM will be used to study processes occurring within these devices and contribute to the development of the next-generation electrochemical technologies. 4 Ultramicroelectrode Voltammetry and Scanning...

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# Chapter 5 Electroanalytical Applications of Semiintegral and Convolution Voltammetry in Room-Temperature Ionic Liquids

Cameron L. Bentley, Alan M. Bond, Anthony F. Hollenkamp, Peter J. Mahon, and Jie Zhang

# 5.1 Introduction

Room-temperature ionic liquids (RTILs) are intrinsic ionic conductors which have been successfully employed as nonflammable/nonreactive electrolytes in a range of electrochemical devices, including dye-sensitized solar cells [1, 2], lithium batteries [3], fuel cells [4], and supercapacitors [5]. The quantification of mass transport is of interest in any solvent, particularly those employed in electrochemical devices, as it affects the ultimate rate/speed at which the device can operate. The diffusivity or diffusion coefficient (D) of a redox active species, along with other thermodynamic parameters such as the bulk concentration (c) and the stoichiometric number of electrons (n) that are of fundamental significance in any study of an electrode reaction, can be determined experimentally using a range of electroanalytical techniques [6].

As with any analytical method, the ideal electroanalytical technique for parameter characterization should be accurate, reproducible, selective, and robust. In many respects voltammetric methods meet these requirements, since they can be

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successfully applied to a diverse range of electroactive species in a wide range of electrolyte media. In conventional low-viscosity molecular solvents such as water or acetonitrile containing added supporting electrolyte, steady-state techniques such as microelectrode voltammetry or rotating disk electrode (RDE) voltammetry are generally advantageous over transient methods for quantifying the mass transport parameters associated with an electrochemical system, since the magnitude of the steady-state mass transport limited current ( $I_L$ ) is unaffected by sluggish heterogeneous kinetics and/or uncompensated resistance ( $R_u$ ). In practice, this means D, c, or n can be determined straightforwardly from the voltammetric  $I_L$  plateau at a microdisk electrode or RDE using well-established analytical theories [6].

By contrast, RTILs possess viscosities that are typically 10 to 10,000 times higher than that of conventional molecular solvent (electrolyte) media. The Stokes–Einstein relationship [7] predicts that diffusivity is inversely proportional to the viscosity of the medium. As a result, mass transport is considerably slower in RTILs, with *D* often being in the range of  $10^{-7}$  to  $10^{-9}$  cm<sup>2</sup> s<sup>-1</sup> compared to  $10^{-5}$  to  $10^{-6}$  cm<sup>2</sup> s<sup>-1</sup> in molecular solvents. This means that in RTIL media, particularly those with high viscosity, it is much more difficult to achieve a true steady state at a microdisk electrode, preventing *D*, *c*, or *n* from being determined from the mass transport limited current [8–10]. It has also been shown that it is similarly difficult to achieve a true steady state at an RDE in RTILs, arising from the difficulty in rotating the electrode at sufficiently high rates under highly viscous conditions [9–11].

In theory, *D*, *c*, or *n* can be calculated from the peak current  $(I_p)$  of a dc linearsweep or cyclic voltammogram by employing the relationships described by the Randles–Sevcik equation for a reversible electron-transfer process of the kind  $Ox + ne^- \Rightarrow Red$ , when the effect of  $R_u$  is negligible [6]. When working in a viscous RTIL, however, very few of the electrochemical systems of interest fulfill these criteria, which severely limits the direct application of dc voltammetry for this purpose. Assuming the Randles–Sevcik equation is not applicable, a best-fit approach with numerical simulation may be a viable alternative, although even this method has its limitations, as mechanistic complexities or other uncertainties can make the modeling process difficult [10].

Through data processing, transient peak-shaped voltammetric (*I–E*) curves can be transformed into a form which closely resembles that of a sigmoidal steady-state voltammogram; this outcome can be highly advantageous for further analysis [6]. Transforming the data in this manner is achieved using a convolution procedure [12], which, when applied under conditions where mass transport occurs solely by semi-infinite planar (1D) diffusion, is known as semiintegration [13]. This new form of data presentation provides the same advantages as outlined above for steady-state techniques (i.e., insensitivity to sluggish heterogeneous kinetics and  $R_u$ ). Furthermore, an extension of this technique, convolution voltammetry, allows the method to be applied even when mass transport includes a contribution from nonplanar (2D) diffusion, permitting the use of a wide range of electrode geometries and voltammetric scan rates [14]. The convolutive transformation also allows the parameters *D* and *nc* to be determined simultaneously from two sets of *I–E* data obtained using two distinctly different voltammetric scan rates applied at the same electrode [15]. In this chapter, the difficulties associated with applying conventional electroanalytical techniques, such as steady-state microelectrode voltammetry, RDE voltammetry, and dc cyclic voltammetry with numerical simulation for the purpose of quantifying diffusivity in RTILs, are highlighted. In developing a strategy for overcoming these issues, we first outline the fundamentals of convolution voltammetry and then discuss a range of situations where electroanalytical applications of these techniques in RTILs have been employed successfully.

### 5.2 Conventional Voltammetric Techniques

#### 5.2.1 Steady-State Microelectrode Voltammetry

Under true steady-state conditions, D can be calculated from the value of  $I_L$  measured at a microdisk electrode using the expression [6]:

$$I_{\rm L} = 4nFcr_0 D \tag{5.1}$$

where  $r_0$  is the radius of the microdisk electrode and *F* is Faraday's constant. In order to approach a true steady state at a microdisk electrode during potential sweep voltammetry, the following inequality must be satisfied [16, 17]:

$$v \ll \frac{RTD}{nFr_0^2} \tag{5.2}$$

where  $\nu$  is the voltammetric scan rate, T is the temperature, and R is the universal gas constant. Since D is inversely proportional to viscosity as per the Stokes-Einstein relationship [7], one consequence of this inequality is that relatively slow voltammetric scan rates and/or small electrode geometries are required to approach a true steady state in highly viscous RTILs [8, 9]. In practice, satisfying the inequality shown in Eq. (5.2) may not be feasible, as is demonstrated from the cyclic voltammograms shown in Fig. 5.1, obtained from the one-electron reduction of the cobaltocenium cation ( $[Co(Cp)_2]^+$ , where Cp=cyclopentadienyl) at a platinum microdisk electrode in the highly viscous RTIL 1-methyl-3-octylimidazolium hexafluorophosphate ( $[C_8 mim][PF_6]$ ,  $\eta = 866$  cP at 20 °C [18]). The shape of the voltammogram is intermediate between sigmoidal and peak-shaped, implying that radial diffusion contributes significantly to mass transport under these conditions. Despite the small electrode size ( $r_0 = 5 \text{ }\mu\text{m}$ ) and slow voltammetric scan rate ( $\nu = 5 \text{ }\text{mV s}^{-1}$ ), near steady-state conditions have not been attained and therefore Eq. (5.1) cannot be applied, making it very difficult to quantify D without resorting to a "best-fit" approach with numerical simulation. It follows that under these conditions, an impractically small electrode (difficulty in both electrode fabrication and current measurement [19]) or slow scan rate would be required to achieve a good approximation to true steady-state measurements [10].



**Fig. 5.1** Cyclic voltammogram obtained from the reduction of 10 mM  $[Co(Cp)_2]^+$  in  $[C_8mim]$   $[PF_6]$  using a 10 µm diameter Pt microdisk electrode with a scan rate of 5 mV s<sup>-1</sup>. Reprinted with permission from Bentley et al., *Anal. Chem.* 2012, *85*, 2239–2245 [10]. Copyright 2013, American Chemical Society

#### 5.2.2 Rotating Disk Electrode Voltammetry

With this technique, under true steady-state conditions, D can be calculated from the value of  $I_L$  measured at an RDE using the Levich equation [20]:

$$I_{\rm L} = 0.620 n FA \left(\frac{d}{\eta}\right)^{1/6} D^{2/3} \omega^{1/2} c$$
 (5.3)

where A is the active electrode area, d is the density of the solvent (electrolyte),  $\eta$  is the hydrodynamic viscosity of the solvent (electrolyte), and  $\omega$  is the angular rotation rate of the electrode. Much higher rotation speeds are required to approach steady-state conditions at an RDE in RTILs compared to conventional molecular solvents (electrolytes) due to the relative insensitivity of high-viscosity fluids to forced convection. This requirement is evident from the cyclic voltammograms shown in Fig. 5.2, obtained from the one-electron reduction of  $[Co(Cp)_2]^+$  at a platinum RDE in  $[C_8mim][PF_6]$ . The shape of the voltammogram obtained with a rotation rate of 500 rpm is almost identical to that obtained at a stationary electrode (0 rpm), implying that mass transport is governed predominantly by planar diffusion. Once again, because steady-state conditions have not been attained, Eq. (5.3)



**Fig. 5.2** Cyclic voltammograms obtained from the reduction of 10 mM  $[Co(Cp)_2]^+$  in  $[C_8mim]$   $[PF_6]$  using a 3.0 mm diameter Pt RDE with a scan rate of 50 mV s<sup>-1</sup> and rotation speeds of 0 rpm (*solid line*) and 500 rpm (*dashed line*). Reprinted with permission from Bentley et al., *Anal. Chem.* 2012, 85, 2239–2245 [10]. Copyright 2013, American Chemical Society

is not applicable, making it very difficult to quantify *D* without resorting to a "best-fit" approach with numerical simulation [10].

In principle, much higher rotation speeds could be employed in order to approach true steady-state conditions in highly viscous  $[C_8mim][PF_6]$ . Indeed, numerical simulations performed for the reduction of  $[Co(Cp)_2]^+$  in the room-temperature protic ionic liquid (RTPIL) diethanolamine acetate ( $\eta$  = 336 cP at 25 °C) revealed that rotation speeds in excess of 5,000 rpm would be required to approach a true steady state at an RDE [11]. In practice, this approach is not feasible, as air bubbles become trapped at the electrode–electrolyte interface at high rotation speeds (>500 rpm), giving rise to noisy and non-reproducible RDE voltammetric data [10, 11].

# 5.2.3 DC Cyclic Voltammetry

The peak current  $(I_p)$  for a simple reversible process under purely planar diffusion conditions can be described by the Randles–Sevcik equation [6] when it is assumed that  $R_u$  is negligible:

$$I_{\rm p} = 0.4463nFAc \left(\frac{nFDv}{RT}\right)^{1/2}$$
(5.4)



**Fig. 5.3** (a) Cyclic voltammograms obtained from the reduction of 10 mM  $[Co(Cp)_2]^+$  in  $[C_8mim]$   $[PF_6]$  at a 1.6 mm diameter Pt macrodisk electrode with scan rates (from *top* to *bottom*) of 50, 25, and 10 mV s<sup>-1</sup>. (b) Comparison of an experimental voltammogram (*solid line*) and simulated voltammograms for a reversible process with  $R_u = 0\Omega$  (*dashed line*) and  $R_u = 13 \text{ k}\Omega$  (*dotted line*). Other simulation parameters used were  $\nu = 50 \text{ mV s}^{-1}$ ,  $D_{ox} = 9.1 \times 10^{-9} \text{ cm}^2 \text{ s}^{-1}$ ,  $D_{red} = 1.5 \times 10^{-8} \text{ cm}^2 \text{ s}^{-1}$  (where the subscripts 'ox' and 'red' refer to the oxidised and reduced forms of the electroactive species, respectively),  $k_s = 1 \text{ cm s}^{-1}$ ,  $\alpha = 0.5$ ,  $C_{dl} = 2 \times 10^{-7}$  F,  $E^0 = -1.104$  V, and T = 297 K. Reprinted with permission from Bentley et al., *Anal. Chem.* 2012, *85*, 2239–2245 [10]. Copyright 2013, American Chemical Society

In reality, very few electrochemical systems fulfill the above criteria, as is demonstrated by the cyclic voltammograms shown in Fig. 5.3a, obtained from the oneelectron reduction of  $[Co(Cp)_2]^+$  at a platinum macrodisk electrode in  $[C_8mim]$  $[PF_6]$ . Despite the fact that  $[Co(Cp)_2]^{+/0}$  is a well-known reversible process, peak-topeak separations ( $\Delta E_p$ ) were larger than expected (56.8 mV at 24 °C) and increased significantly with scan rate, attributable to the high level of uncompensated resistance ( $R_u \approx 13 \text{ k}\Omega$ ) in this highly viscous RTIL [10].

The value of *D* directly estimated from the slope of the  $I_p$  vs.  $\nu^{1/2}$  plot (obtained by linear regression of the experimental data), 7.6 (±0.2)×10<sup>-9</sup> cm<sup>2</sup> s<sup>-1</sup>, is expected to be somewhat smaller in magnitude than the true value due to the ohmic distortion in the voltammetric *I*–*E* data. A more accurate value for *D* can be obtained using a "best-fit" approach with numerical simulations that accommodate the contribution from  $R_u$ , as shown in Fig. 5.3b. As expected, the *D* value estimated from simulation/ experiment comparison, 9.0 (±0.2)×10<sup>-9</sup> cm<sup>2</sup> s<sup>-1</sup>, is significantly greater than the value obtained from the direct use of peak currents. Although this approach is straightforward in the present case (the [Co(Cp)<sub>2</sub>]<sup>+/0</sup> process is reversible, simple, and well characterized), application to electroactive species undergoing more complex mechanisms may be problematic, due to uncertainties with the simulation, as will be demonstrated in Sect. 5.3.2.2.

# 5.3 Convolution Voltammetry

# 5.3.1 Theory

Post-measurement data processing techniques which can be applied to voltammetric *I*-*t* or *I*-*E* data can greatly enhance the ability to extract information from the raw data. One such data transformation approach makes use of the general convolution procedure initially described by Savéant and coworkers [12, 21–28], where semiintegral voltammetry [13] is a subset of a range of techniques collectively known as convolution voltammetry. As described by Oldham and coworkers [13, 29–38], semiintegration is specific to conditions under which mass transport occurs by semi-infinite planar diffusion and gives rise to a function, M(t), which is the 1/2 order fractional integral of current, I(t), where:

$$M(t) = \frac{d^{-1/2}I}{dt^{-1/2}}(t) = I(t) * \frac{1}{\sqrt{\pi t}}$$
(5.5)

and the asterisk represents the convolution operation. In Eq. (5.5), the current, I(t) is said to have been semiintegrated with respect to time or convolved with the function  $1/\sqrt{\pi t}$ . The function, M(t), known as the semiintegral of the current, is related to the concentration of electroactive species at the electrode surface:

$$c(0,t) = c(\infty,t) - \frac{M(t)}{nAF\sqrt{D}}$$
(5.6)

where c(x,t) denotes the concentration of electroactive species at distance *x* from the electrode surface at time *t*. It follows that under purely diffusion-controlled conditions [i.e., c(0,t)=0], M(t) reaches its maximum or limiting value,  $M_L$ :

$$M_L = nAFc\sqrt{D} \tag{5.7}$$

Therefore, semiintegrating a peak-shaped transient voltammogram (I-E) gives rise to a sigmoidal M-E curve which resembles a steady-state voltammogram, which in some circumstances is more amenable to data analysis [6]. Indeed, just like the  $I_L$ plateau of a steady-state voltammogram, the magnitude of the  $M_L$  plateau is unaffected by sluggish heterogeneous kinetics or  $R_u$ . The semiintegral at the time  $t=J\Delta$ is calculable from current data evenly spaced in time,  $I(0), I(\Delta), I(2\Delta), ..., I(j\Delta), ..., I(J\Delta)$ , using the easily programmed formula [39–41]:

$$M(t) = M(J\Delta) = \frac{4}{3}\sqrt{\frac{\Delta}{\pi}} \left[ I(J\Delta) + \sum_{J=1}^{j=1} \left\{ \frac{(J-j+1)^{3/2} - 2(J-j)^{3/2}}{+(J-j-1)^{3/2}} \right\} I(j\Delta) \right]$$
(5.8)

or by equivalent methods [12, 20, 42, 43], where  $\Delta$  is a small increment of the total time. A Microsoft Excel macro containing a semiintegration algorithm is available free online [44].

The fully planar diffusion restrictions associated with semiintegral voltammetry can be relaxed by replacing the function,  $1/\sqrt{\pi t}$ , in Eq. (5.5) with the generalized function, g(t), whose form is dependent upon the details of the mechanism (e.g., electron transfer with coupled chemical reactions) and the geometry of the electrode [45]:

$$M(t) = I(t) * g(t)$$
(5.9)

Herein M(t) will be referred to as the *semiintegrated current* when calculated based on Eq. (5.5) under planar diffusion conditions and as the *convolved current* for other electrode geometries when calculated more generally based on Eq. (5.9) taking into account the contribution of radial diffusion to the mass transport. Although the function library for g(t) is quite extensive and can deal with first-order homogeneous mechanisms at a range of electrode geometries [45]; herein the discussion is restricted to diffusion limited conditions at an inlaid disk electrode [14, 46]. In order to accommodate radial or edge effects, the formalization applied to the inlaid disk geometry is the bipartite expression which at short times is given by [47]:

$$g(t) = \frac{\sqrt{D}}{r_0} \sum_{j=1}^{5} a_j \theta^{(j-2)/2}$$
(5.10)

and at long times is given by:

$$g(t) = \frac{\sqrt{D}}{r_0} \left( b_2 \theta^{-3/2} + \sum_{j=4}^8 b_j \theta^{(3-2j)/2} \right)$$
(5.11)

where  $\theta$  is the dimensionless time parameter equal to  $Dt / r_0^2$  with the coefficients  $a_j$  and  $b_j$  listed in Table 5.1 and the transition from the short to the long time expression occurring when  $\theta = 1.304$ . The convolved current is readily calculable from current data evenly spaced in time using the programmable convolution algorithm [48]:

$$M(t) = \left[I(t) * g(t)\right]_{t=J\Delta} = \frac{1}{\Delta} \left(I_J G_1 + \sum_{j=1}^{J-1} I_{J-j} \left(G_{j-1} - 2G_j + G_{j+1}\right)\right)$$
(5.12)

where  $G(t) = \iint_{\substack{0 \\ 0 \\ 0}}^{t} g(t) dt dt$  and the abbreviations  $I_j$  and  $G_j$  refer to  $I(j\Delta)$  and  $G(j\Delta)$ . The *double* integral of g(t) at short times for use in the convolution algorithm is obtained from:

$$G(t) = \frac{r_0^3}{D^{3/2}} \sum_{j=1}^5 a_j \theta^{(j+2)/2}$$
(5.13)

	g(t)		G(t)	
j	$a_j$	$b_j$	$a_j$	$b_j$
1	$\frac{1}{\pi^{1/2}}$	0	$\frac{4}{3\pi^{1/2}}$	$\frac{\pi}{4}$
2	-1	$\frac{1}{4\pi^{1/2}}$	$\frac{-1}{2}$	$\frac{-1}{\pi^{1/2}}$
3	$\frac{3}{2\pi^{1/2}}$	0	$\frac{2}{5\pi^{1/2}}$	0.26180
4	-0.38584	$-4.7016 \times 10^{-2}$	$-6.4307 \times 10^{-2}$	$-6.2688 \times 10^{-2}$
5	$7.8535 \times 10^{-2}$	$4.7019 \times 10^{-3}$	$8.9754 \times 10^{-3}$	$1.2538 \times 10^{-3}$
6		$1.6079 \times 10^{-2}$		$1.8376 \times 10^{-3}$
7		$-2.2686 \times 10^{-2}$		$-1.4404 \times 10^{-3}$
8		$1.2948 \times 10^{-2}$		$5.2315 \times 10^{-4}$
	$\theta = 1.304$		$\theta = 1.368$	

Table 5.1 Values of important polynomial coefficients used in Eqs. (5.10), (5.11), (5.13), and (5.14)

and for the long time series:

$$G(t) = \frac{r_0^3}{D^{3/2}} \left( \sum_{j=1}^3 b_j \theta^{(3-j)/2} + \sum_{j=4}^8 b_j \theta^{(7-2j)/2} \right)$$
(5.14)

with transition occurring when  $\theta = 1.368$ . The coefficients  $b_1$  and  $b_3$  are integration constants obtained from Aoki et al. [49]. The double integral of the long-time expression contains eight terms due to the addition of the integration constant for each integration step. Again, the values for the  $a_j$  and  $b_j$  coefficients are listed in Table 5.1.

The complex time dependence of the diffusion process to an inlaid disk electrode is described by Eqs. (5.10) and (5.11), which are defined in terms of the dimensionless time parameter  $\theta$ . It follows that under a specific set of experimental conditions, a unique ratio of  $\sqrt{D} / r_0$  will apply and this ratio can be defined as a single parameter,  $\rho$ . In order to obtain the convolved current, M(t), an initial estimate for  $\rho$  must be inputted into the convolution algorithm. If c is known and  $M_L$  can be obtained from the limiting convolved current plateau, then it is possible to iteratively refine  $\rho$ based on Eq. (5.7) for a known value of  $r_0$ :

$$\rho = \frac{M_{\rm L}}{nF\pi r_0^3 c} \tag{5.15}$$

or *D*:

$$\rho = \frac{nFD^{3/2}c}{M_{\rm L}} \tag{5.16}$$

Successive refinements of  $\rho$  oscillate and converge on an optimized value that can then be used to calculate either *D* or  $r_0$  depending on which is known. Furthermore, if voltammograms are obtained using two distinctly different scan rates at the same electrode, then it is possible to calculate both *D* and *nc* simultaneously, as both voltammograms should result in identical  $M_L$  plateaus even though different time dependencies are involved. This approach assumes  $r_0$  is known, as the optimized value of  $\rho$  provides *D* and this is then substituted into Eq. (5.7) in order to estimate the product of *n* and *c*. The discussed convolutive methods can effectively be thought of as "black box" data analysis methods, as the required transformations can be readily performed off-line on voltammetric *I*-*t* or *I*-*E* data using programmable digital algorithms [shown in Eqs. (5.8) and (5.12)].

In order to apply convolutive analysis to a particular set of experimental data, it is necessary to ensure that certain criteria apply, with uniformity of concentration across the electrode surface being the key requirement [14, 45, 46, 50] for the voltammetry to be describable by a temporal convolution integral and there are three circumstances where this might occur. The first case involves an electrode that is geometrically uniformly accessible. This is an electrode where symmetry dictates that the rate of transport be equal at all points on the surface (i.e., under conditions where mass transport to the electrode surface occurs solely by semiinfinite planar diffusion). When a diffusion limited current occurs at such an electrode, then a uniform concentration distribution will result at the electrode surface if the initial concentration distribution is uniform and this is the situation in most electrochemical experiments. In practice, the only such geometries are a suitably shrouded (or very large) plane, a capped cylinder, an isolated sphere, or a sessile hemisphere. Secondly, if the electrochemical reaction is reversible, then the uniformity of the potential and Nernst's law conspire to ensure that the ratio of activities for the substrate and product is also uniform across the electrode surface. The third situation is when the polarization is so intense that the concentration of the electroactive species at the electrode surface is virtually zero; this will lead to a uniform distribution of the product across the electrode surface even if the reaction is not reversible. In this case, conservation laws ensure that the product is generated uniformly.

A commonly encountered experimental scenario arises when an inlaid disk electrode is used and the electron-transfer kinetics are quasireversible. The implication in this circumstance is that the convolved current will no longer be directly proportional to the surface concentration in the vicinity of the standard potential as described by Eq. (5.6), because the current is kinetically limited in this potential region. However, once the diffusion limited plateau is attained, then the convolved current is once again directly proportional to the surface concentration, and Eq. (5.7), which is the limiting form of Eq. (5.6), is applicable [46, 50].

# 5.3.2 Applications of Semiintegral Voltammetry

# 5.3.2.1 [Co(Cp)<sub>2</sub>]<sup>+/0</sup> Process in [C<sub>8</sub>mim][PF<sub>6</sub>]

The merits of semiintegration as an analytical technique can be tested by comparing the diffusivity of  $[Co(Cp)_2]^+$  determined using this method to the value previously determined in Sect. 5.2.3 using numerical simulation. Linear-sweep semiintegral voltammograms obtained from the one-electron reduction of  $[Co(Cp)_2]^+$  at a platinum macrodisk electrode in  $[C_8 \text{mim}][PF_6]$  are shown in Fig. 5.4. The *M*-*E* curves resemble true steady-state voltammograms, possessing a sigmoidal shape with a well-defined  $M_{\rm L}$  plateau. However, there is a significant slope in the  $M_{\rm L}$  plateau prior to background subtraction, attributable to the charging of the electrical double layer at the stationary electrode (i.e., nonfaradaic current) [10, 29]. Background subtraction can be easily performed by measuring the residual current in the absence of  $[Co(Cp)_2]^+$  and subtracting this from the total current prior to semiintegration. The value for D, 9.4  $(\pm 0.3) \times 10^{-9}$  cm<sup>2</sup> s<sup>-1</sup>, estimated from the background subtracted  $M_{\rm L}$  plateau by substituting the appropriate values for known parameters into Eq. (5.7), is, as expected, significantly larger than the value previously estimated by direct use of the Randles-Sevcik method (underestimated due to  $R_{\mu}$  effects) and in good agreement with the value determined using numerical



**Fig. 5.4** Linear-sweep semiintegral voltammograms obtained from the reduction of 10 mM  $[Co(Cp)_2]^+$  in  $[C_8mim][PF_6]$  using a 1.6 mm diameter Pt macrodisk electrode with a scan rate of 50 mV s<sup>-1</sup> before (*dashed line*) and after (*solid line*) background subtraction. Reprinted with permission from Bentley et al., *Anal. Chem.* 2012, *85*, 2239–2245 [10]. Copyright 2013, American Chemical Society

simulation. Despite the significant ohmic distortion present in the voltammetric I-E data (previously shown in Fig. 5.3), the diffusivity of  $[Co(Cp)_2]^+$  has been successfully determined with high accuracy using the semiintegral method.

#### 5.3.2.2 I<sup>-</sup>/I<sub>3</sub><sup>-</sup>/I<sub>2</sub> Processes in [C<sub>8</sub>mim][PF<sub>6</sub>]

In aprotic solvents such as acetonitrile [51, 52] and analogously in a range of RTILs [53–57], iodide has been shown to be oxidized to molecular iodine on platinum in two steps, giving rise to two resolved voltammetric processes:

$$3I^- \rightleftharpoons I_3^- + 2e^-$$
 (5.17)

$$I_{3}^{-} \rightleftharpoons \frac{3}{2}I_{2} + e^{-}$$
(5.18)

The reaction mechanism is complicated by the following homogeneous equilibrium process:

$$\mathbf{I}^- + \mathbf{I}_2 \rightleftharpoons \mathbf{I}_3^- \tag{5.19}$$

Cyclic voltammograms obtained from the oxidation of iodide (from 1-ethyl-3-methylimidazolium iodide, ([C<sub>2</sub>mim]I) at a platinum macrodisk electrode in [C<sub>8</sub>mim][PF<sub>6</sub>] are shown in Fig. 5.5a. Evidently, the iodide oxidation process possesses much greater mechanistic complexity than the previously investigated [Co(Cp)<sub>2</sub>]<sup>+/0</sup> process. In addition, the I<sup>-</sup>/I<sub>3</sub><sup>-</sup> process [reaction shown in Eq. (5.17)] is reportedly kinetically sluggish [54–56], evidenced by the large  $\Delta E_p$  values associated with this process in the cyclic voltammograms.

The sluggish heterogeneous electron-transfer kinetics of the iodide oxidation process precludes the direct application of the relationships described by the Randles-Sevcik equation and mechanistic complexities make numerical simulation difficult. Fortunately, the  $M_{\rm I}$  plateau of a linear-sweep semiintegral voltammogram is insensitive to both sluggish heterogeneous kinetics and  $R_{u}$ ; *M*–*E* curves obtained from the oxidation of iodide at a platinum macrodisk electrode in [C<sub>8</sub>mim][PF<sub>6</sub>] are shown in Fig. 5.5b. Once again, the M-E curves resemble steady-state voltammograms, possessing a sigmoidal shape with two  $M_{\rm L}$  plateaus corresponding to the two oxidation processes shown in Eqs. (5.17) and (5.18), respectively. The diffusion coefficient of iodide can be estimated from the background subtracted  $M_{\rm L}$  plateau by substituting the appropriate values for known parameters into Eq. (5.7); the determined value, 7.3  $(\pm 0.3) \times 10^{-9}$  cm<sup>2</sup> s<sup>-1</sup>, is comparable to the diffusivity of  $[Co(Cp)_2]^+$  previously determined in this highly viscous RTIL. Semiintegral voltammetry has successfully been employed to determine the diffusivity of an electroactive species under conditions where all of the "conventional voltammetric techniques" discussed in Sect. 5.2, including numerical simulation, are either not valid or unavailable, further highlighting the benefits of convolutive techniques for electroanalytical applications.



**Fig. 5.5** (a) Cyclic voltammograms obtained from the oxidation of 14 mM I<sup>-</sup> in  $[C_8mim][PF_6]$  using a 1.6 mm diameter Pt macrodisk electrode with scan rates (from *top* to *bottom*) of 50, 25, and 10 mV s<sup>-1</sup>. (b) *M*–*E* curves obtained by semiintegrating the forward sweep of the voltammogram obtained at a scan rate of 50 mV s<sup>-1</sup> shown in (a) before (*dashed line*) and after (*solid line*) background subtraction. Reprinted with permission from Bentley et al., *Anal. Chem.* 2012, *85*, 2239–2245 [10]. Copyright 2013, American Chemical Society

## 5.3.2.3 Electro-oxidation of Iodide on a Glassy Carbon Electrode in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>]

The discussions below pertain to the  $I^{-}/I_{3}^{-}/I_{2}$  redox processes in RTILs, a subject which has led to significant research interest in recent years [1, 53, 57–64] due to the integral role that the  $I^{-}/I_{3}^{-}$  process plays in the operation of dye-sensitized solar cells (DSSCs). A DSSC, in essence, has three fundamental components: a semiconductor photoanode (TiO<sub>2</sub>) with an adhered photoactive dye, a platinized cathode (counter electrode), and an electrolyte containing a suitable redox shuttle. As previously alluded to, the electrolyte is most commonly composed of the iodide/triiodide ( $I^{-}/I_{3}^{-}$ ) couple dissolved in a volatile organic solvent, such as acetonitrile [2]. RTILs have shown promise as alternative electrolytes in DSSCs as they circumvent the long-term safety/stability problems associated with the traditional organic solvent-based electrolytes [1, 2, 65].

Platinum is the most commonly employed cathode material in DSSCs because it acts as an electrocatalyst for the  $I^-/I_3^-$  redox shuttle mechanism shown in Eq. (5.17). However, the high cost of noble metals is a significant driving force for the development of more cost-efficient cathode materials, notably carbon-based ones [2, 66, 67]. Cyclic voltammograms obtained for the oxidation of [C<sub>2</sub>mim]I on platinum and glassy carbon macrodisk electrodes in the relatively fluid RTIL 1-ethyl-3-methyl-imidazolium bis(trifluoromethanesulfonyl)imide ([C<sub>2</sub>mim][N(Tf)<sub>2</sub>],  $\eta$ =34 cP at 20 °C [9]) are shown in Fig. 5.6a. On platinum, two sets of peaks are observed,



**Fig. 5.6** (a) Cyclic voltammograms obtained from the oxidation of 10 mM I<sup>-</sup> in  $[C_2mim][N(Tf)_2]$  with a scan rate of 250 mV s<sup>-1</sup> using a 1.6 mm diameter Pt macrodisk electrode (*solid line*) or a 3.0 mm diameter glassy carbon macrodisk electrode (*dashed line*). (b) *M*–*E* curves obtained by semiintegrating the forward sweep of the voltammograms shown in (a) after background subtraction. Reprinted with permission from Bentley et al., *Electrochim. Acta* 2013, *109*, 554–561 [53]. Copyright 2013, Elsevier

corresponding to the  $I^{-}/I_{3}^{-}$  process and  $I_{3}^{-}/I_{2}$  process at less and more positive potentials, respectively, as shown in Eqs. (5.17) and (5.18). On a glassy carbon electrode, two sets of peaks also are observed, albeit with significant overpotentials when compared with the behavior at platinum. Unfortunately, it is not obvious from the transient voltammograms whether the number of electrons associated with each process (and hence, the overall redox mechanism) is the same on both electrode materials.

This information would be readily available from a sigmoidal steady-state voltammogram ( $I_L$  plateau magnitudes are proportional to *n*). However, performing these additional experiments is unnecessary, as the same information is available through semiintegration, as shown in Fig. 5.6b. As expected, on platinum, the relative magnitude of the background subtracted  $M_L$  plateaus is clearly proportional to the ratio of number of electrons involved in each process (i.e., 2:1). On glassy carbon, even though the  $I^-/I_3^-$  plateau is not as well defined, the two processes still convincingly exhibit a 2:1 ratio, strongly suggesting that the overall iodide oxidation processes are analogous on both electrode materials. The diffusion coefficient of iodide is estimated to be  $2.68 \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup> and  $2.61 \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup> from the background subtracted  $M_L$  plateaus on platinum and glassy carbon, respectively, in excellent agreement with each other and with the literature value of  $2.68 \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup> [53, 57]. This study clearly demonstrates that the information available from the semiintegrated  $M_{-E}$  data is superior to that available from the unprocessed *I*–*E* data, further expanding upon the electroanalytical utility of cyclic voltammetry.

# 5.3.2.4 Electro-oxidation of Iodide on a Gold Electrode in [C<sub>2</sub>mim] [N(Tf)<sub>2</sub>]

The limited number of studies available on the electro-oxidation of iodide on gold electrodes in conventional solvents such as water [68, 69] and acetonitrile [70] indicates that unique interactions between the  $I^-/I_2$  couple and gold occur. Cyclic voltammograms obtained from the oxidation of  $[C_2mim]I$  on platinum and gold macrodisk electrodes in  $[C_2mim][N(Tf)_2]$  are shown in Fig. 5.7a. As expected, two sets of peaks are observed on platinum, corresponding to the  $I^-/I_3^-$  and  $I_3^-/I_2$  processes as per Eqs. (5.17) and (5.18), respectively. Two sets of peaks are also observed on gold. However, unlike at a glassy carbon electrode, the positions of the peaks are comparable to those observed on platinum. Once again, it is difficult to ascertain whether the number of electrons associated with each process is identical on each material from the unprocessed transient cyclic voltammograms.

M-E curves obtained by semiintegrating the forward sweeps of the respective voltammograms (after background subtraction) are shown in Fig. 5.7b. Remarkably, the magnitude of the  $M_L$  plateaus relative to each other is different on platinum and gold; while platinum displays the expected 2:1 magnitude ratio, gold clearly exhibits a 1:1 magnitude ratio, indicative of a different oxidation mechanism for iodide. The magnitudes of the area-normalized  $M_L$  plateaus on gold and platinum are comparable, indicating the overall number of electrons involved in the electro-oxidation of each iodide ion (i.e., n = 1) is identical on both electrode materials. Therefore, the difference in the iodide oxidation mechanism



**Fig. 5.7** (a) Cyclic voltammograms obtained from the oxidation of 10 mM I<sup>-</sup> in  $[C_2mim][N(Tf)_2]$  with a scan rate of 250 mV s<sup>-1</sup> using a 1.6 mm diameter Pt macrodisk electrode (*solid line*) or a 3.0 mm diameter Au macrodisk electrode (*dashed line*). (b) *M*–*E* curves obtained by semiintegrating the forward sweep of the voltammograms shown in (a) after background subtraction. Reprinted with permission from Bentley et al., *Anal. Chem.* 2013, *85*, 11319–11325 [60]. Copyright 2013, American Chemical Society

on gold and platinum must arise from a disparity in the intermediate formed after the initial oxidation process, which is well known to be triiodide  $(I_3^-)$  on platinum [see the reaction shown in Eq. (5.17)]. Indeed, by performing further investigations with other electroanalytical techniques such as electrogravimetry and EQCM, it can be shown that iodide oxidation on gold in  $[C_2mim][N(Tf)_2]$  proceeds predominantly via a diiodoaurate  $([AuI_2]^-)$  intermediate [60]:

$$2I^{-} + Au \rightleftharpoons [AuI_{2}]^{-} + e^{-}$$
(5.20)

$$\left[\operatorname{AuI}_{2}\right]^{-}\rightleftharpoons \operatorname{I}_{2} + \operatorname{Au} + e^{-}$$
(5.21)

The 1:1 electron stoichiometry shown in Eqs. (5.20) and (5.21) is in agreement with the 1:1  $M_L$  plateau magnitude ratio observed on gold, as demonstrated in Fig. 5.7b. This study and the study previously discussed in Sect. 5.3.2.3 clearly highlight the utility of the semiintegral technique to provide valuable quantitative (i.e., *D* and *n*) information about an electrochemical system, achievable simply through off-line data processing, transforming a peak-shaped transient *I*–*E* curve into a sigmoidal *M*–*E* curve.

# 5.3.3 Applications of Convolution Voltammetry

#### 5.3.3.1 Electro-oxidation of Iodide at a Platinum Microdisk Electrode

The requirement of semiintegration that mass transport due to nonplanar (radial) diffusion must be negligible, limits the use of this technique to relatively large planar electrodes and/or high scan rates, as demonstrated in Sect. 5.3.2. Unfortunately, when working with a macrodisk electrode in RTILs, nonfaradaic current makes a significant contribution to the total measured current, manifesting as a severely sloped  $M_L$  plateau, making background subtraction essential for quantitative semi-integral work. As addressed in Sect. 5.3.1, the strictly planar diffusion requirement of semiintegration can be relaxed through the extension available via. Eqs. (5.10) and (11). This allows the convolution algorithm to be applied when working with microdisk electrodes, while retaining all of the advantages of the original semiintegration approach. Changing from a macrodisk to a microdisk electrode has obvious benefits, as it minimizes difficulties with potential control (i.e.,  $IR_u$  distortion) and reduces the capacitive background current contribution [71–74].

The advantages of convolution voltammetry are illustrated in Fig. 5.8, obtained from the oxidation of  $[C_2mim]I$  on a platinum microdisk electrode in  $[C_2mim]$   $[N(Tf)_2]$ . In Fig. 5.8a, the shape of the voltammogram is intermediate between sigmoidal and peak-shaped, implying mixed planar/radial diffusion conditions,



**Fig. 5.8** (a) Cyclic voltammogram obtained from the oxidation of 4.3 mM I<sup>-</sup> in  $[C_2mim][N(Tf)_2]$  using a 25 µm diameter Pt microdisk electrode with a scan rate of 50 mV s<sup>-1</sup>. (b) The convolved current of the voltammogram (forward sweep) shown in (a) before (*dashed line*) and after (*solid line*) background subtraction. Reprinted with permission from Bentley et al., *Anal. Chem.* 2014, 86, 2073–2081 [15]. Copyright 2014, American Chemical Society

and as a result, steady-state microdisk electrode theory is not valid and semiintegration is not applicable. Nonetheless, convolution with Eq. (5.9) taking into account the contribution of radial diffusion to the mass transport is applicable, as illustrated in Fig. 5.8b. The convolved current voltammogram is sigmoidal in shape and features two well-defined, scan rate independent, diffusion-controlled  $M_L$  plateaus with the expected size ratio (i.e., 2:1). Under these conditions, the charging current is negligible and therefore background subtraction is not required. The diffusion coefficient of iodide is estimated to be 2.70  $(\pm 0.03) \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup> from the  $M_L$  plateau, in excellent agreement with the values previously determined on platinum/glassy carbon macrodisk electrodes using the semiintegration technique (after background subtraction).

Use of the technique known generally as convolution voltammetry is obviously advantageous over the previously discussed semiintegration method, as avoiding the need to background subtract greatly simplifies the analytical procedure. Although [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] is sufficiently fluid to allow a true steady state to be approached at a microdisk electrode over a practical experimental timescale (i.e., substituting T=298 K,  $D=3 \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup>, n=1, and  $r_0=0.00025$  cm into Eq. (5.2) results in  $\nu \ll 123$  mV s<sup>-1</sup>), convolution voltammetry remains an attractive alternative. This is because, unlike steady-state microelectrode voltammetry, there are no  $r_0$  or  $\nu$  restrictions associated with the convolution technique, therefore avoiding the practical difficulties associated with measuring small currents over extended experimental timescales.

# 5.3.3.2 [Fe(Cp)<sub>2</sub>]<sup>0/+</sup> Process in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>]: Determination of *D* and *nc*

In Sects. 5.3.2 and 5.3.3.1, it was shown how the value of *D* may be determined from the  $M_L$  plateau after semiintegration/convolution of the experimental *I*–*E* data when the parameters  $r_0$ , *n*, and *c* are known. As highlighted in Sect. 5.3.1, convolution can also be employed to determine the constants *D* and *nc* simultaneously from two *I*–*E* datasets obtained under conditions with differing sphericity factors ( $\sigma$ ):

$$\sigma = \sqrt{\frac{RTD}{nFvr_0^2}}$$
(5.22)

where the dimensionless sphericity factor describes the relative contribution of planar and radial diffusion to an inlaid disk electrode under a given set of voltammetric conditions.  $\sigma$  is varied in practice simply by changing either the electrode dimensions (i.e.,  $r_0$ ) or the experimental timescale (i.e.,  $\nu$ ) [46, 75]. This convolutive technique is most sensitive in the "mixed diffusion region" (0.012< $\sigma$ <40) where the contributions from both planar and radial diffusion are significant.

Ferrocene ([Fe(Cp)<sub>2</sub>]) is a suitable redox species to test the merits of this convolutive technique because while it is reasonably soluble in a range of RTILs [76], it dissolves at a very slow rate, making quantitative preparation of solutions (i.e., where c is known) problematic and time-consuming [8]. The need to prepare solutions of known ferrocene concentration can be avoided entirely if the constants D and c are determined simultaneously, and since in the present case n is known, the convolution method is ideal. Cyclic voltammograms (I-E) and the corresponding convolved current voltammograms (M-E) obtained from the one-electron oxidation of an unknown concentration of  $[Fe(Cp)_2]$  in  $[C_2mim][N(Tf)_2]$  on a platinum microdisk electrode are shown in Fig. 5.9. Once again, the shape of the cyclic voltammograms indicates mixed planar/radial diffusion conditions, ideal circumstances to apply the convolutive transformation. Due to the reversible nature of the  $[Fe(Cp)_2]^{0/+}$  process and the negligible effects of  $C_{dl}$  and  $R_{u}$ , the resulting M-E curves at the two investigated scan rates almost perfectly coincide, possessing identical  $M_{\rm L}$  plateaus. Using the convolution method described in Sect. 5.3.1, the values for D and c are estimated to be  $4.49 \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup> and 10.5 mM, respectively.

Since the  $[Fe(Cp)]^{0/+}$  electrode mechanism parameters are known, their accuracy can be confirmed by checking the "goodness of fit" with numerical simulation of the cyclic voltammograms, as shown in Fig. 5.10. The excellent agreement between the experimental and simulated data indicates that the values determined for *D* and *c* are valid. This method has also been applied successfully to determine the parameters *D* and *n* simultaneously (i.e., when *c* is known) for more complex



**Fig. 5.9** (a) Cyclic voltammograms and (b) linear-sweep convolved current voltammograms obtained from the oxidation of an unknown concentration of  $[Fe(Cp)_2]$  in  $[C_2mim][N(Tf)_2]$  using a 25 µm diameter Pt microdisk electrode with scan rates of 50 mV s<sup>-1</sup> (*solid line*) and 100 mV s<sup>-1</sup> (*dashed line*). Reprinted with permission from Bentley et al., *Anal. Chem.* 2014, *86*, 2073–2081 [15]. Copyright 2014, American Chemical Society

redox mechanisms in conventional molecular solvents [15]. Although it is possible to obtain the same information using chronoamperometry [55, 76, 77], the voltammetric convolution approach described here avoids the instrumental problems and ohmic ( $IR_u$ ) effects arising from the initially large currents encountered with potential-step methods.

# 5.4 Conclusions

The utility of several voltammetric methods has been evaluated for the purpose of quantifying the parameters (i.e., diffusivity, stoichiometric number of electrons, and/or bulk concentration), associated with a range of electroactive species in room-temperature ionic liquids. The application of conventional steady-state methods in this kind of medium is problematic under the highly viscous conditions that commonly are encountered, due to the difficulty in approaching a true steady-state under reasonable experimental conditions. The peak currents of dc cyclic voltammograms are sensitive to heterogeneous kinetics/uncompensated resistance, making analysis on the basis of the relationships outlined by the Randles–Sevcik equation problematic and while numerical simulation is relatively straightforward and represents a



**Fig. 5.10** Comparison of simulated (*open circles*) and experimental (*solid line*) cyclic voltammograms obtained from the oxidation of [Fe(Cp)<sub>2</sub>] (concentration determined by convolution voltammetry) in [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] using a 25 µm diameter Pt microdisk electrode with scan rates of (from *top* to *bottom*) 100 and 50 mV s<sup>-1</sup>. The parameters used in the simulations were  $D_{red} = 4.49 \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup>,  $D_{ox} = 4.20 \times 10^{-7}$  cm<sup>2</sup> s<sup>-1</sup>, c = 0.0105 M,  $k_s = 10$  cm/s,  $r_0 = 0.00133$  cm,  $\alpha = 0.5$ , T = 296 K, and  $E^0 = 0.179$  V. Reprinted with permission from Bentley et al., *Anal. Chem.* 2014, 86, 2073–2081 [15]. Copyright 2014, American Chemical Society

robust method of analysis; on some occasions it is severely hampered by mechanistic complexities or other uncertainties.

Semiintegral voltammetry, a convolution method specific to conditions under which mass transport occurs solely by semi-infinite planar diffusion, is a powerful and also robust analytical method which can be applied under highly viscous conditions to quantify the diffusivity. However, the fully planar diffusion requirement of semiintegration limits the use of this technique to conditions where background charging current is significant, making its subtraction essential for quantitative work. Fortunately, an extension of this method, known generally as convolution voltammetry, accommodates radial diffusion, allowing the experimental conditions to be tailored to minimize the charging current, thus avoiding the need to subtract the background contribution. Overall, the convolutive techniques discussed in this chapter provide powerful analytical tools which have great versatility, being applicable under experimental conditions where the direct use of conventional steadystate and transient voltammetry is severely limited.

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# Chapter 6 Small-Angle X-Ray Scattering of Ionic Liquids

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## 6.1 Introduction

As in most experimental techniques, an experimenter observes how a sample reacts to some kind of external stimulus. For example, in a simple electrochemical experiment, one applies a potential and observes a current response. Similarly, in SAXS, one exposes a sample to a beam of X-rays and measures the intensity, I, of the scattered X-rays as a function of the scattering angle,  $2\theta$ , shown in Fig. 6.1.

This is the basic concept of a small-angle scattering (SAS) experiment, whether X-rays or neutrons are being used. The fundamental difference between the two is that neutrons scatter from nuclei whilst X-rays scatter from electrons. With this in mind, the theory behind SAXS will be presented here, keeping in mind that the general theory can be applied to both, accounting only for the difference in the definition of scattering contrast.

With the increasingly high X-ray brilliance provided by synchrotrons around the world and the accessibility of bench-top SAXS instruments, we will only concern ourselves with X-rays. Regardless of how they are produced, the X-rays that interact with the sample are collimated (Fig. 6.1). Here, collimation means that the X-rays must propagate with a minimal amount of angular divergence so that when they interact with the sample, they do so at the same relative angle. The incident X-rays should be monochromatic, as polychromatic X-rays complicate analysis of the SAXS data, as we will show in the General Theory section below. However,

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Fig. 6.1 A simplified schematic showing a typical SAXS experiment showing the incoming and scattered X-rays from a sample

so-called pink beams can also be used to increase the incident flux of the X-rays, which have a wider spread of wavelengths (typically up to 10 %). This results in wavelength smearing of the data and can be treated with a priori knowledge of the beam profile. In most cases, the X-ray wavelengths are sufficiently monochromatic that wavelength smearing is negligible.

In this chapter, we aim to provide the reader with an understanding of how SAXS has been used to study a range of ionic liquid (IL) systems as well as the full potential that X-ray scattering experiments have in the study of ILs. For brevity, we will only present a brief introduction to SAS so that the reader can imagine a physical picture when looking at SAXS data, as well as understand both its potential and limits. A more comprehensive account of SAS analysis can be found in books by Guinier [1, 2], Glatter and Kratky [3], Giles [4], and (for biological macromolecules) Svergun [5], as well as review papers [6, 7]. Readers may also be interested in data reduction [8], corrections [9, 10], and analysis [11–17] work that is also very useful.

### 6.2 General Theory

## 6.2.1 Elastic X-Ray Scattering

Elastic X-ray scattering occurs when an incoming X-ray causes an electron to (briefly) accelerate, emitting a radially propagating X-ray of the same wavelength [18]. The resulting X-ray intensity scattered by a single electron depends on the polarization of the incoming X-rays and is given by the equations:

$$I_{\rm e} = r_{\rm e}^2 I_0 \cos 2\theta \quad (parallel) \tag{6.1}$$

$$I_{\rm e} = r_{\rm e}^2 I_0 \quad (perpendicular) \tag{6.2}$$

where  $r_e$  is the classical electron radius,  $I_0$  is the incoming intensity, and  $2\theta$  is the angle of intensity measurement [2]. In the small-angle regime,  $2\theta < 5^\circ$ , the  $\cos(2\theta)$  term does not deviate from one by more than a percent. Therefore, Eqs. (6.1) and (6.2) show that the polarization state of the X-rays does not affect the outcome of a SAXS experiment. However, the measured intensity should be normalized by  $I_e$  to obtain SAXS data on an absolute scale, if this is needed (recommended).

In general, SAXS data can be divided into two different types: diffraction in the small-angle regime and true small-angle scattering. The discrete diffraction peaks in the small-angle regime originate from ordered nanostructures, which are often found in ILs. The scattering angle where the diffraction peak reaches a maximum is related to a repeat distance, *d*, of an ordered phase. The SAXS data, on the other hand, usually vary smoothly with scattering angle and reflect the morphology and/ or microstructure of the scattering objects. In other words, diffraction peaks indicate the presence of crystalline or semi-crystalline phases, whereas SAS does not. The analyses of the two cases are different. Both will be discussed here, with emphasis on SAS analysis.

### 6.2.2 Data Reduction

Before one can analyze the raw scattering intensity, the data must be properly reduced and corrected. This can be a rather involved discussion and will only be briefly discussed here. More detail on data reduction and correction can be found in Glatter and Kratky [3] or an excellent review by Pauw [9]. Briefly, one has to calibrate the angle of measurement,  $2\theta$ , and the scaled intensity; large angles of measurement require additional geometrical and possibly polarization corrections (Eqs. 6.1 and 6.2). The angular calibration allows the experimenter to obtain the intensity as a function of  $2\theta$ . Common small-angle diffraction standards include silver behenate and rat-tail collagen for SAS measurements. In most cases, this is sufficient and the scaled intensity is not calibrated. However, when done properly [19], an absolute calibration of the intensity can provide the experimenter with information about the volume and contrast of the scattering objects, which may be important. especially when trying to identify unknown phases. In this case, one obtains the differential scattering cross section,  $\frac{\partial \Sigma}{\partial \Omega}(q)$ , which contains all of the

relevant SAS information. The magnitude of the scattering vector q is defined as  $q = 4\pi/\lambda \times \sin(\theta)$ , where  $\lambda$  is the X-ray wavelength and  $\theta$  is one-half of the scattering angle  $2\theta$ . In this chapter, we will follow the convention of using I(q), instead of  $\partial \Sigma$ 

$$\frac{\partial 2}{\partial \Omega}(q)$$

## 6.2.3 Diffraction

From a SAXS experiment, one can resolve ordered inhomogeneities within the sample. Specific to ILs, such ordering may be inherent to the IL itself, whether it be a consequence of the cation [20, 21], anion [22], or the aggregation of amphiphilic molecules in ILs [23, 24]. In these cases, the structural order is analyzed by resolving the repeat distance, d, of the phases. Such structural order is often a key feature of ILs, making SAXS an important technique for their study. This order is observed directly from the SAXS pattern as "peaks" in the  $I(2\theta)$  curve. These peaks correspond to the distance, d, of the ordered structure through Bragg's Law:

$$d = \frac{n\lambda}{2\sin\theta} \tag{6.3}$$

where  $\lambda$  is the wavelength of X-rays and *n* is an integer. Equation (6.3) has been used fruitfully in the study of ionic liquids using SAXS and wide-angle X-ray scattering (WAXS), which uses scattering profiles at larger scattering angles to resolve smaller distances. For n=1, Eq. (6.3) can also be written as  $d=2\pi/q$ , where *q* is the magnitude of the scattering vector at the center of the peak. We should note at this point that while the ordered distances, *d*, are directly obtained through Eq. (6.3), Bragg's law says nothing about the source of the ordering. However, because of the simplicity and ubiquitous application of Eq. (6.3) to SAXS in ILs, Bragg's law is often employed where better models should be used. A good example of this concerns ordered micelles, for which Eq. (6.3) is used to analyze the inter-micelle distance [25–27]. However, in these cases an analytical solution is readily available to model the SAXS data [28]. For this reason, we will focus mainly on SAXS analysis.

### 6.2.4 Fundamental SAXS Theory

As mentioned previously, SAXS provides information about the physical geometry of the system. for example, feature size, shape, and internal and/or external structure. With the assumption that  $\lambda$  is much smaller than the dimensions of the inhomogeneity in the sample, each scattered wave will constructively interfere with other scattered waves to some degree. The degree of constructive interference is determined by their relative phase,  $\varphi$ .

Figure 6.2 shows the scattering of an X-ray wave-front by two points in an inhomogeneity, separated by a vector,  $\mathbf{r}$ , where the scattered intensity is measured at a scattering angle,  $2\theta$ . When a monochromatic X-ray wave is scattered from different points in the inhomogeneity, the interference of the scattered waves will depend on the phase shift,  $\varphi$ , between the scattered and incident waves, which is given by equation:

$$\varphi = \frac{2\pi \left( \left( \mathbf{s} - \mathbf{s}_0 \right) \cdot \mathbf{r} \right)}{\lambda} = \mathbf{q} \cdot \mathbf{r}, \tag{6.4}$$



Fig. 6.2 A simplified diagram showing how two electromagnetic waves can either constructively or destructively interfere, depending on the angle of measurement (for a specific wavelength)

**s** and **s**<sub>0</sub> are unit vectors in the directions of the scattered and incoming waves, respectively, and the vector **q** is defined accordingly [1–3, 18]. Figure 6.2 also shows that the magnitude of **s**–**s**<sub>0</sub> is given by  $2\sin\theta$ , resulting in the conventional equation for  $|\mathbf{q}|(=q)$ :

$$q = 2\pi \frac{2\sin(\theta)}{\lambda} \tag{6.5}$$

where the factors  $2\pi$  and  $\lambda$  are included from Eq. (6.4). If the X-ray phase difference along the path between any two points is known, the resulting scattering amplitude from the two points in Fig. 6.2 can be calculated using complex notation:

$$A(\mathbf{q}) = \sum f_j e^{-i(\mathbf{q}\cdot\mathbf{r}_j)}$$
(6.6)

where  $f_j$  is the scattering power of a single electron *j*. The variable *f* is 1 for a free electron, but will not be the case near an adsorption edge [1–3, 18]. Thus, between Fig. 6.2 and Eq. (6.5), we can now relate real space dimensions to the scattering amplitude measured at a certain **q** value. At this point, **q** is a vector and not a scalar. However, it is important to note that the phase difference along the path of a vector, **r**, which is orthogonal to **q**, is 0 (Eq. 6.4). Thus, only the component of **r** parallel to **q** is relevant for scattering [3]. This is a particularly important concept for anisotropic systems where dimensions perpendicular to **q** do not affect the scattering intensity.

While Eq. (6.6) does relate the physical dimensions to the X-ray amplitude, it cannot be used directly because an X-ray scattering experiment measures scattering intensity (where scattering amplitudes are summed and multiplied by their complex conjugates), instead of scattering amplitude. The continuous distribution of electrons in the scattering object allows us to replace the summation in Eq. (6.6) with a scattering length density function,  $\rho(\mathbf{r})$ , and rewrite Eq. (6.6) as  $A(\mathbf{q}) = \int \rho(\mathbf{r}) e^{-i\mathbf{q}\cdot\mathbf{r}} dV$ ,

where the integral is taken over the scattering volume. The measured scattering intensity, I, will therefore be:

$$I(\mathbf{q}) = A(\mathbf{q})A(\mathbf{q})^* = \iiint \qquad \iiint \rho(\mathbf{r}_1)\rho(\mathbf{r}_2)e^{-i\mathbf{q}\cdot(\mathbf{r}_1-\mathbf{r}_2)}dV_1dV_2$$
(6.7)

where  $A^*$  is the complex conjugate of A, and  $\mathbf{r}_1$  and  $\mathbf{r}_2$  are two separate points in the sample. Equation (6.7) relates the measured scattering intensity,  $I(\mathbf{q})$ , to real space dimensions,  $\mathbf{r}$ . We can further simplify Eq. (6.7) by redefining  $\mathbf{r} = \mathbf{r}_1 - \mathbf{r}_2$  and introducing the auto-correlation function,  $\overline{\rho}^2(\mathbf{r})$  by the equation:

$$\overline{\rho}^{2}(\mathbf{r}) = \iiint \rho(\mathbf{r}_{1}) \rho(\mathbf{r}_{1} - \mathbf{r}) dV_{1}$$
(6.8)

where the function is integrated over the sample volume once. Combining Eq. (6.8) with Eq. (6.7), the scattering intensity can be written:

$$I(\mathbf{q}) = \iiint \overline{\rho}^2(\mathbf{r}) e^{-i\mathbf{q}\cdot\mathbf{r}} dV, \qquad (6.9)$$

where the function is again integrated over the sample volume just once. Equation (6.9) now provides the experimenter with a mathematical link between the scattering intensity and autocorrelation function of the scattering length density [3]. We derived Eq. (6.9) without making assumptions. However, this equation is not very useful because it contains vectors and imaginary numbers that are difficult to deal with analytically for many systems. By applying appropriate assumptions concerning the material system being studied, more useful forms of Eq. (6.9) can be derived and applied to extract physically meaningful parameters.

### 6.2.5 Scattering Inhomogeneities

At this point, we should point out an important aspect of SAXS—the scattering object, as exemplified in Fig. 6.2, needs to have a different electron density than that of its immediate surroundings in order to give a finite scattering intensity. The difference in electron density, however, can be either positive or negative, and the sign cannot be distinguished by SAXS alone. For example, the object in Fig. 6.2 could just as easily be a pore inside a matrix instead of a solid particle within a suspension. This ambiguity is a consequence of the well-known Babinet's principal of reciprocity [1]. For this reason, we will refer to the scattering inhomogeneities as such, instead of particles or pores.

### 6.3 SAXS Analysis

SAXS analysis is a very broad topic and contains within it a wide variety of ways to analyze the I(q) curve. In many cases, the type of applicable analysis depends on the system, and on the specific assumptions that can be made about the system. In this

chapter, we do not intend to cover all of the available SAXS analysis methods. Instead, we will provide an overview of the analysis methods that are relevant to ILs and offer some case examples. The goal is to familiarize the reader with fundamental aspects of SAXS. For analysis, we encourage the readers to use any one of the free SAXS software packages available [11, 12, 16, 29–31].

### 6.3.1 Common SAXS Assumptions

The first and most common assumption is that of *statistical isotropy*. It is assumed that there is no preferred orientation of the scattering inhomogeneities relative to the scattering vector,  $\mathbf{q}$ . As a general rule, this means that if we collect the scattering intensity from different sample orientations, we will get the same  $I(\mathbf{q})$  curve. This concept is illustrated in Fig. 6.3. For spherical shapes (far left), the inhomogeneities themselves are isotropic so they satisfy the assumption of statistical isotropy. If, however, these inhomogeneities are anisotropic (middle and far right), then they must be randomly oriented to be considered as statistically isotropic (far right). In the following sections, we will present some useful analytical techniques one can use when this assumption is valid.

The *dilute limit* assumption is also very common in SAXS analysis. This assumption requires that interaction or ordering between scattering inhomogeneities is negligible. We would strongly caution against making this assumption liberally. Instead,



Fig. 6.3 Illustrates the concept of statistical isotropy (*left* and *right*), while the *center* is anisotropic

we encourage using a priori knowledge of the system to determine the validity of this assumption. As a rule of thumb, if the inhomogeneity is evenly dispersed, its volume fraction needs to be less than a few percent to be considered "dilute."

*Centro-symmetry* assumes that the scattering inhomogeneities, themselves, are *centro-symmetric*. One can think of this as a shape-dependent assumption whereby a radial vector (from the center of mass of the inhomogeneity) has the same chord length within the inhomogeneity as a radial vector in the opposite direction. This is shown in Fig. 6.4 with a parallelepiped. Another *centro-symmetric* shape would be an ellipsoid of revolution.

### 6.3.2 Indirect Fourier Transformation Analysis

Indirect Fourier Transformation (IFT) Analysis is a method that has been applied in studies of protein stability in a hydrated choline di-hydrogen phosphate ionic liquid [32]. The IFT analysis can also be useful in identifying unknown phases, as well as understanding the link between real space and reciprocal space. This analysis assumes *statistical isotropy*, as well as the *dilute limit* [33].

If these assumptions are valid for a given system, then the phase factor in Eq. (6.9) can be averaged over all orientations and vectors replaced by scalars. The scattering intensity can be represented by the equation:

$$I(q) = V\overline{\eta^2} \int \text{PDDF}(r) \frac{\sin qr}{qr} dr = V\overline{\eta^2} \int \gamma_o(r) 4\pi r^2 \frac{\sin qr}{qr} dr \qquad (6.10)$$

$$\gamma_o(r) = \frac{\bar{\rho}^2(r)}{V\bar{\eta}^2} \tag{6.11}$$

$$\overline{\eta^2} = \left\langle \left(\rho - \overline{\rho}\right)^2 \right\rangle \tag{6.12}$$



Fig. 6.4 Diagram depicting the concept of centro-symmetry



Fig. 6.5 Log-log plot of the theoretical scattering intensity from a sphere 300 Å in diameter together with its PDDF function

where *V* is the total volume of the scattering inhomogeneities, PDDF(*r*) is the pair distance distribution function,  $\gamma_0(r)$  is the normalized correlation function,  $\rho$  is the scattering length density of the inhomogeneity,  $\overline{\rho}$  is the volume average scattering length density of the sample,  $\eta$  is the difference in scattering length densities, and  $\overline{\eta^2}$  represents the scattering contrast [3]. Though one might propose that the PDDF be calculated by taking the inverse Fourier transform of I(q), this is not advisable [3]. Instead, one can generate the PDDF function with a series of cubic spline functions with unknown coefficients. These unknown coefficients can then be varied to fit the raw I(q) data through Eq. (6.10). Of course, if a system cannot be considered *dilute*, the Generalized Indirect Fourier Transformation (GIFT) should be used instead of IFT [33].

Figure 6.5 shows both I(q) and the PDDF for a system of monodisperse spheres, 300 Å in diameter. Quantitatively, this is a good moment to discuss the units of  $\frac{\partial \Sigma}{\partial \Omega}(q)$  and PDDF. Such a system of monodisperse spheres would be represented by the equation:

$$\frac{\partial \Sigma}{\partial \Omega}(q) = NI_{\text{sphere}}(q) \tag{6.13}$$

where  $I_{\text{sphere}}(q)$  is the theoretical scattered intensity of a single sphere and N is the number of scatterers per unit volume. The resulting units are *always* cm<sup>-1</sup>. It follows then from Eq. (6.10) that the units for the PDDF are cm<sup>2</sup>. Equation (6.13) therefore shows, albeit for a simple case, the relationship between  $\frac{\partial \Sigma}{\partial \Omega}(q)$  and I(q). Of course,

more complex systems require slightly different relationships. Regardless, the units for  $\frac{\partial \Sigma}{\partial \Omega}(q)$  are always the same.

Qualitatively, one can see that the PDDF function approaches zero at 300 Å because of the finite size of the sphere. Other physically meaningful parameters can also be obtained from the PDDF, such as the radius of gyration,  $R_g$ , of the scattering population [3]. The radius of gyration,  $R_g$ , can be thought of as the root mean square distance from the center of the scattering inhomogeneity and will be discussed further in the following section.

## 6.3.3 Useful Approximations and Relationships

In the previous section, it was shown that the IFT could be used to analyze the entire (or a portion of the) SAXS curve (I(q) vs. q) to obtain physical information about a system. In this section, we will present quantitative approximations that can also be used to evaluate different portions of the I(q) curve. These approximations are extremely useful to an experimenter, particularly in the initial analysis where one needs to identify the source of the scattering. Here we will discuss portions of the I(q) curve representing different aspects of a structural inhomogeneity. Briefly, the Guinier approximations of the system. Power-Law decays in the I(q) curve can provide information about the surface of the inhomogeneity, as well as the shape of the inhomogeneity. Finally, we will discuss the scattering invariant, Q, which contains information about the total volume and contrast of the inhomogeneity.

#### 6.3.3.1 Guinier Approximation

The Guinier approximation provides information about volume parameters such as the particle size *via* the radius of gyration,  $R_g$ . The Guinier approximation assumes that the inhomogeneity is *dilute* and *centro-symmetric*, such that the single particle scattering intensity can be represented by the equation:

single particle 
$$I(\mathbf{q}) = \left[\eta \int \cos(\mathbf{q} \cdot \mathbf{r}) dV\right]^2$$
 (6.14)

where again  $\eta$  is the contrast. The Guinier approximation is valid only at very small  $(\mathbf{q} \cdot \mathbf{r})$ , where the  $\cos(\mathbf{q} \cdot \mathbf{r})$  can be approximated. If one considers only the magnitude of  $\mathbf{q}$  (whether this be a consequence of *statistical isotropy* or known

orientation of the inhomogeneity), the resulting approximation of the intensity at low q is:

$$I(q) \cong Ge^{\frac{-q^2 R_g^2}{3}}$$
 (6.15)

$$G = V^2 \overline{\eta^2} \tag{6.16}$$

where G is a constant containing  $\overline{\eta^2}$ , the electron density contrast between the particle and surrounding matrix and the inhomogeneity volume, V, and  $R_g$  is the radius of gyration [1, 3]. Equation (6.15) predicts a constant intensity at very low q, followed by a rapid decay proportional to  $e^{-q^2 R_g^2}$ , resulting in a "knee" in the scattering curve that is related to the size of the inhomogeneity. This "knee" is shown as the black dotted curve in Fig. 6.6. Note that Eq. (6.15) only describes the central portion of the I(q) curve that contains information about the volume parameters of the inhomogeneity. Also, from Eq. (6.15), the scattering intensity falls off quickly as  $qR_g$  term increases. This implies a reciprocal relationship between q and  $R_g$ . Therefore, for large values of  $R_g$ , one must obtain the scattering intensity I(q) at lower q values. Conversely, if one does not measure to low enough q values, little to no information about the volume parameters of an inhomogeneity can be resolved.



Fig. 6.6 Log-log plot of the scattering intensity from simple geometric shapes to illustrate the concept of multiple dimensions

As a general rule, to resolve the largest inhomogeneity size, *L*, one must measure the scattering intensity at *q* values of at least  $\pi/L$  [3] regardless of the model used to analyze the data. This is important to remember, if one is reporting sizes from SAXS data that were not measured. For example, micelles formed in ILs on the order of 1,500 Å cannot be resolved in a *q*-range that only goes down to 0.01 Å<sup>-1</sup> [34].

A least squares fit can be used to determine the  $R_g$  using Eq. (6.15); however, it is difficult for one to select the applicable *q*-range to fit. Alternatively, one can use a Guinier plot of  $\ln(I(q))$  vs.  $q^2$  to determine the  $R_g$  value. This is a simple and quick way to determine particle size. For example, in the photo-reduction of AgNO<sub>3</sub> in water-ionic liquid solutions, a Guinier plot was used to determine the size of the Ag nanoparticles as a function of composition and reduction time [35]. In this case, the Ag particles were approximated as spheres; thus the  $R_g$  is directly related to the radius of the particles following  $R_g = \sqrt{\frac{3}{5}} \times R$ , where *R* is the radius of the spheres.

In the case of a sphere, there is only one volume parameter: the radius, *R*. But what about shapes that have more dimensions, such as a rod, disk, or parallelepiped? In these cases, simple analysis can show that  $R_g$  is related to all the physical dimensions of the scattering object. For example, for a cylindrical rod of length *L* and  $\frac{R^2}{R^2}$ 

radius *R*, we have  $R_{\rm g} = \sqrt{\frac{R^2}{2} + \frac{L^2}{12}}$ . In practice, for particles with extreme shapes,

the scattering curve will show characteristics of two or more separated dimensions [36, 37]. An example can be found in Fig. 6.6. Here, in the case of rod and disk, the Guinier knees at  $q \sim 0.0009$  Å<sup>-1</sup> and  $q \sim 0.0005$  Å<sup>-1</sup> represent the cylindrical or discotic radius of gyration, respectively. Following these knees are power-law decays, followed by knees in the scattering curves that are associated with their smaller dimensions.

For simple geometric shapes, one can obtain each dimension separately by fitting Eq. (6.15) to the I(q) curve where each knee is observed. In these cases, one obtains a value of  $R_g$  and must use the appropriate relationship to obtain the actual dimension of the inhomogeneity [1, 3]. Therefore, the Guinier approximation can be used to determine the volume parameters of a dilute scattering inhomogeneity.

#### 6.3.3.2 Power-Law Decays

In Fig. 6.6, one will notice that for rods and disks, a power-law decay separates the two Guinier knees. Put simply, these power-law exponents in q can be associated with the presence of one-dimensional rods or two-dimensional disks at q values less than those associated with the smallest Guinier knee at high q. It is shown elsewhere that the intensity decays according to  $q^{-1}$  and  $q^{-2}$  for a rod and a disk, respectively [3]. These relationships are extremely useful since it would otherwise be difficult to determine whether a scattering inhomogeneity is rod-shaped or disk-shaped. It is, however, important to note that the presence of a finite distribution in size or significant shape distortion (bending) causes departures from these power-law slopes and that it is relatively rare to observe exact  $q^{-1}$  or  $q^{-2}$  exponents; higher exponents are more common.

#### 6 Small-Angle X-Ray Scattering of Ionic Liquids

In contrast to the Guinier approximation, the Porod approximation is derived for large  $(\mathbf{q} \cdot \mathbf{r})$ . Unlike the Guinier approximation, the Porod approximation is derived for small *r*-values near the surface. For a certain scattering object, Porod approximation gives rise to a general approximation for scattering at high *q*, whereas its corresponding Guinier approximation describes the knee at low *q*. Also, Porod approximation is valid only for a *statistically isotropic* system. The principal assumptions behind this approximation are that the surface is *smooth* and *well defined*; this means that the electron density function across the inhomogeneity surface must be a Heaviside (step) function and the surface itself is smooth [3]. The resulting approximation, at high *q*, is:

$$I(q) \cong Bq^{-4} \tag{6.17}$$

$$B = 2\pi \eta^2 S \tag{6.18}$$

where *B* is a constant proportional to the contrast and surface area [1, 3]. Equation (6.17) predicts a power-law decay in *q* of  $q^{-4}$  and shown in Fig. 6.7 as a straight line on a log–log plot of  $Iq^4$  vs. *q*. It should be pointed out that if the particle surface is not smooth or isotropic or the surface electron density function is not continuous, Eq. (6.17) would not be valid. These cases are discussed below.



**Fig. 6.7** Porod plot showing different power-law decays that are common in SAXS: interface with a well-defined electron density gradient (*blue curve*), Porod surface scattering (*red*), internal electron density fluctuations (*black*), surface fractal (*green*), Gaussian coil (*purple*), and mass fractal agglomerate (*orange*)

Though the Porod approximation has proven to be robust for many systems, deviations from this behavior are common and are thus briefly discussed here. Such deviations from Porod's law can be found in systems where the electron density function is continuous at the inhomogeneity surface (i.e., not a sharp boundary), the surface is rough (on the angstrom scale), or convoluted anisotropic inhomogeneities or mass fractals are present. These deviations can be described as either negative or positive deviations. In the former case, the scattering intensity at high *q* decreases more steeply than  $q^{-4}$  (e.g.,  $q^{-4.5}$ ), while positive deviations result in decays less than  $q^{-4}$  (e.g.,  $q^{-3}$ ).

Negative deviations from Porod decays (Fig. 6.7) can occur when the inhomogeneity has a diffuse interface, as opposed to a sharp, well-defined one. Such a system is commonly found in low-crystalline polymers where there is a gradual transition of  $\rho(r)$  at the phase boundary [3]. This phenomenon is also found in nanoparticle electrodeposition in deep eutectic solvents [38]. In this study, the observed negative deviations were associated with charge-neutralizing layers above particle ensembles on the surface.

These boundary gradients can be accounted for with only a slight modification to Eq. (6.17) [39]. Using the convolution property of Fourier Transforms, it can be shown that the scattering intensity (at high q) for an isotropic system can then be approximated as:

$$I(q) \cong \frac{B}{q^4} \left(1 - \sigma^2 q^2\right) \tag{6.19}$$

where *B* is the same as in Eq. (6.18) and  $\sigma$  is the thickness of the boundary over which the electron density gradient exists. Equation (6.19) is applicable for *isotropic systems* and assumes that the gradient can be described as the convolution of a step function and a Gaussian function, where the Gaussian function is approximated by a Taylor series expansion, though other functions can be used [40]. Similar relationships also exist for anisotropic systems [39].

Positive deviations from Porod's law are much more common in SAXS. We have already seen that scattering from anisotropic inhomogeneities can lead to power-law decays in the scattering intensity with q (Fig. 6.6). Others include but are not limited to electron density fluctuations within the inhomogeneity, polymers, surface fractals, and mass fractal agglomerates.

Spatial electron density fluctuations, within a phase, can cause positive deviations from Porod's law [41]. This effect is caused by electron density fluctuations that are small enough to interfere with the Porod scattering. This phenomenon has been reported for certain Al(OH)<sub>3</sub> gels, whereby the composition of the gel is the Al<sub>13</sub> polymer, which itself contains large fluctuations, resulting in a power-law decay of  $q^{-3.7}$  [41, 42]. While this phenomenon is rare, it is certainly possible in ILs that have a tendency to aggregate into complex structures [43]. This power-law decay is similar to surface fractal scattering, which is physically very different. Large molecules (i.e., polymers) may also lead to power-law decays, for example, a polymer with Gaussian statistics [44]. An example would be aggregation in ILs. The scattering intensity is given by the equation:

$$I(q) = 2 \frac{\left(e^{-R_{g}q} + R_{g}q - 1\right)}{\left(R_{g}q\right)^{2}}$$
(6.20)

where  $R_g$  is the average radius of gyration of the polymer. Strictly speaking, a polymer can be thought of as a special case of a one-dimensional rod that is randomly coiled. However, because the polymer is coiled, the scattering intensity, at high q, decreases according to  $q^{-2}$ , instead of  $q^{-1}$ , as shown in Fig. 6.7. Equation (6.21) is only correct for molecules with no self-avoidance. Polymers with self-avoidance will cause the intensity to decay closer to  $q^{-5/3}$  [45].

Another important class of morphology is fractal, which includes mass fractal and surface fractal. Although mass and surface fractals appear remarkably different, they share a common trace essential to fractal objects: self-affinity. Self-affinity means that the morphology of interest looks the same under different length scales, i.e., within certain limits, the essential geometric characteristics of a fractal object are unchanged by magnification.

For surface fractals, mathematically, this self-affinity is described by  $S \sim R^{ds}$  for surface fractals, where *R* is the scale of probing yardstick, *S* is the total surface area within the dimension specified by the yardstick, and  $d_s$  is the surface fractal exponent [46]. For an ordinary smooth object,  $d_s=2$ , consistent with a smooth surface being two-dimensional. For surface fractal dimensions, however,  $d_s$  can be non-integer and vary between 2 and 3, which then provides a quantitative measure of surface roughness.

Surface fractal analysis has been applied to the study of the breakdown of cellulose fibers using ILs, where it is shown that the IL pretreatment time influenced the surface morphology of the resulting biomass [47]. Such a surface is also common in glasses [48] and rocks [49] where the pore wall is rough as shown in Fig. 6.7. For surface fractals, it can be shown that the scattering intensity decays at high q by the equation:

$$I(q) = Bq^{d_s-6} \tag{6.21}$$

where *B* carries the same definition as in Eq. (6.18). Given that  $d_s$  varies between 2 and 3, surface fractal scattering is confined to power-law decays between  $q^{-3}$  and  $q^{-4}$ .

Mass fractal scattering, on the other hand, is associated with the structure of the inhomogeneities and not their surface. Physically, mass fractal scattering is observed when small particles agglomerate together to form a non-crystalline superstructure similar to that shown in Fig. 6.7. These structures are known to exist in aerogels, whereby particles are very close to each other but do not possess any order. The structure of these particles can be described as a fractal-like object [50]. The degree to which

the particles are packed can be expressed in terms of the mass density,  $\rho_{\rm m}$ , of the agglomerate:

$$\rho_{\rm m} \propto R_{\rm g}^{d_{\rm m}-3} \tag{6.22}$$

where  $R_g$  is the radius of gyration of the agglomerate and  $d_m$  is the mass fractal dimension, which ranges from 1 to 3. Therefore, as the value of  $d_m$  increases toward 3, the density,  $\rho_m$ , will also increase. Just as for regular inhomogeneities, the scattering intensity would show a typical Guinier knee at low q that corresponds to the  $R_g$  of the entire agglomerate. However, as q increases, it can be shown that the scattering intensity will decay according to:

$$I(q) \cong Bq^{-d_{\rm m}} \tag{6.23}$$

where the intensity decays according to the value of  $d_m$ , which can only be between 1 and 3 [50]. Scattering from agglomerates is well established in many systems that are prone to agglomeration.

## 6.3.4 Unified Equations

The Guinier and Porod approximations have proven to be robust for scattering inhomogeneities, but neither one can model the entire scattering curve. These approximations have been combined to describe the full I(q) curve for spheres, rods, disks, micelles, and intermediate objects [51]. A slightly more flexible unified equation has also been developed and will be briefly discussed here. Using both the Guinier approximation at low q and a power-law decay at high q, the scattering intensity can be represented by the equation:

$$I(q) = \sum_{i=1}^{N} (LQ_i + HQ_i)$$
(6.24)

$$LQ_{i} = G_{i}e^{\frac{-q^{2}R_{g_{i}}^{2}}{3}}$$
(6.25)

$$HQ_{i} = B_{i}e^{\frac{-q^{2}R_{gco}^{2}}{3}} \left(\frac{\left(erf\left(\frac{qR_{g_{i}}}{\sqrt{6}}\right)\right)^{3}}{q}\right)^{r_{i}}$$
(6.26)

where LQ<sub>*i*</sub> is the low *q* scattering contribution, HQ<sub>*i*</sub> is the high *q* scattering contribution, *i* is the level number, and  $P_i$  is the exponential power-law decay that dominates only the high *q* region, using the error function in Eq. (6.26). Using Eq. (6.24), one can model the scattering from a variety of systems or combination thereof by using



**Fig. 6.8** Log–log plot of the scattering intensity from a Gaussian distribution of spheres (*black circles*) and the associated Guinier approximation (*blue*), Porod approximation (*green*), and the unified equation (*red*)

multiple levels, *i*. An example of the unified equation is shown in Fig. 6.8 where Eq. (6.24) is used to model a size distribution of spheres. For more complicated objects, such as fractal agglomerates, different levels can be linked together with the  $R_{gCO}$ , which is used to terminate the high-*q* scattering in the case that the scattering intensity from another level dominates that portion of the I(q) curve; fractal agglomerates and anisotropic inhomogeneities are good examples of this [52]. The value of  $P_i$  in Eq. (6.26) would be 4, if Porod's law is valid or any of the previous mentioned decays [52]. However, one will note that the definition of *B* depends on the value of  $P_i$  chosen. For example, if the  $P_i$  equals 4, Eq. (6.18) can be used; different expressions must be used for different decays.

In practice, one can use Eq. (6.24) to model the scattering intensity to obtain information about the inhomogeneity size ( $R_g$ ), total volume or contrast (G), and surface or structure (B,  $P_i$ ). In certain cases, parameters obtained from Eq. (6.24) can be used to provide information about agglomerates [53], size distribution [54], or a two-phase system [55].

## 6.3.5 Invariant

In previous analyses, we have seen that the shape of the I(q) curve provides information about the physical dimensions of an inhomogeneity. When the relative scaling of the scattering intensity is important, one can use the invariant,  $Q_{inv}$ , to analyze changes in the total scattering volume or contrast of a system. Irrespective of the size, shape, or structure of the inhomogeneity,  $Q_{inv}$  can be calculated by the equation:

$$Q_{inv} = \frac{1}{2\pi^2} \int_0^\infty q^2 I(q) dq = CV \overline{\eta^2}$$
(6.27)

where *V* is the total volume of the scattering objects, and *C* would be a calibration constant that is normally acquired using an intensity calibration standard [3]. The only requirement of Eq. (6.27) is that the system be *statistically isotropic*. For anisotropic systems, a pseudo-invariant,  $Q_{\omega}$ , can also be used [56].

## 6.3.6 Composite Inhomogeneities, Form Factors, and Structure Factors

In Sect. 6.2.4, we saw that the total scattering amplitude can be calculated by simply summing all other amplitudes, with the weighted phase factor (Eq. 6.6). For a system of N particulate inhomogeneities, each at a position vector,  $\mathbf{P}_n$ , Eq. (6.6) can be modified to calculate the total scattering amplitude of these inhomogeneities by the equation:

$$A(\mathbf{q}) = \sum_{j} f_{j}(\mathbf{q}) e^{i(\mathbf{q}\cdot\mathbf{P}_{n})} \sum_{n} e^{i(\mathbf{q}\cdot\mathbf{r}_{j})}$$
(6.28)

where the second term is a summation over each particle, and the first term accounts for inter-particle displacements,  $\mathbf{P}_n$ . For known shapes, the second summation has an analytical solution. Therefore, if the second term can be replaced by the scattering amplitude of a single inhomogeneity, then the amplitude is equal to:

$$A(\mathbf{q}) = \sum_{n} V_n(R...) F_n(q, R...) e^{i(\mathbf{q}\cdot\mathbf{P_n})}$$
(6.29)

where  $V_n$  is the volume, R... is the volume parameters of the inhomogeneity, and  $F_n(q,R...)$  is the so-called form factor of the inhomogeneity. Assuming *statistical isotropy* leads to the well-known Debye Equation for composite inhomogeneities:

$$I(q, R...) = \sum I_{j}(q, R...) + 2\sum_{j} \sum_{n \neq j} A_{j}(q, R...) A_{n}(q, R...) \frac{\sin q P_{jn}}{q P_{jn}} \quad (6.30)$$

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$$A(q,R...) = V(R...)F(q,R...)$$

$$(6.31)$$

where  $P_{jn}$  is the magnitude of the vector that separates particle *j* from particle *n*. Equation (6.30) is a useful equation when one wants to calculate the scattering intensity of a collection of inhomogeneities. Note that if large distances,  $P_{jn}$ , separate the inhomogeneities, then the second term is zero and the total scattering intensity can be represented as the sum of the intensity of each inhomogeneity; in this case, the system is considered *dilute*.

In reality, small inhomogeneities measured by SAXS are not always in their dilute limit, making the second term in Eq. (6.30) necessary. We note that this second term is difficult to calculate directly. However, Eq. (6.30) can be rewritten, using a correlation function, g(P):

$$I(q,R...) = NI(q,R...) \left[ 1 + \frac{N}{V} \int (g(P) - 1) \frac{\sin qP}{qP} \right]$$
(6.32)

where *N* is the total number of inhomogeneities. One can further simplify Eq. (6.32) to a term for the inhomogeneities, *F*, and a term for their structure, *S*:

$$I(q, R...) = V^{2}(R...)F^{2}(q, R...)S(q, X...)$$
(6.33)

where V is the volume, F is the form factor, S is the structure factor, and X... represent the parameters that describe the structures of the inhomogeneities. Nowadays there is a wide variety of form factors and structure factors available [12, 57]. These analytical expressions are very simple, yet powerful, tools that the reader is strongly encouraged to review. While these analytical expressions provide a valuable link between the physical aspects of the system and the scattering intensity, it is important that they be used correctly. We will discuss a few notable examples below. However, it is impossible to discuss every case and the reader is encouraged to be aware of the assumptions that go into the form factor and structure factor they wish to use.

#### 6.3.6.1 Size Distribution and Anisotropic Inhomogeneities

For a dilute isotropic system, the contribution of each particle to the total scattering intensity is additive. When the distribution of inhomogeneities is known, the scattering intensity can be modeled as:

$$I(q) = CV\overline{\eta^2} \int D_n(R) V_p(R)^2 \left| F(q,R) \right|^2 dR$$
(6.34)



**Fig. 6.9** Log–log plots of the scattering intensity calculated from (1) a single 35 nm-diametered ellipsoid particle (*blue*) and (2) spheres with a Gaussian size distribution (*red*). The spherical mean diameter is 20 nm

where  $D_n$  is the number distribution of inhomogeneities of size, R,  $V_p$  is the particle volume,  $|F(q,R)|^2$  is the form factor, and k is a general constant that depends on the contrast and volume [3]. While Eq. (6.34) can be easily fit to an I(q) curve, how certain can one be of the resulting parameters? The answer to this question is that it depends on the data and model. For example, Fig. 6.9 is a plot of the intensity vs. q for a broad distribution of spheres and a single 350 Å ellipsoid with an aspect ratio of 0.3. The effects of polydispersity and particle shape on the scattering intensity are very similar, as both broaden the Guinier knee as well as dampen the oscillations at high q. Though particle shape and polydispersity may become distinguishable at extreme aspect ratios (i.e., disks and rods), both effects are indistinguishable if the system has inhomogeneities of moderate aspect ratios and an unknown distribution, as both traces in Fig. 6.9 are similar. One can imagine then that if both the size distribution and aspect ratio were fit simultaneously, there would be large uncertainties in the fit parameters. For this reason, an uncertainty analysis of the fit parameters should be performed. This can be accomplished by holding one of the fit parameters (i.e., parameter A) constant and fitting all other parameters and then looking at how

much the chi-square changes with different values of parameter A. This method is incorporated in the Irena package [11] for Igor Pro but can easily be accomplished in any least squares fitting routine.

Solving both the distribution and shape from a single 1–D I(q) curve is not possible without a priori knowledge of one or the other. In the case that the distribution is known through some other technique, the scattering curve can be fit to a system of inhomogeneities with either the same aspect ratio or with aspect ratio a function of size. Alternatively, if an aspect ratio is either assumed or known, the distribution can be solved for, directly, from the discretized form of Eq. (6.34). In this case, other methods such as the method of maximum entropy [58] can be used to determine the size distribution.

For a polydisperse system that contains inter-particle (inhomogeneity) interferences, Eq. (6.34) cannot be used by simple multiplication by the structured factor, as in Eq. (6.33). Although this has been used for significantly narrow distributions [37, 38, 59], there are better ways to properly account for structure in a polydisperse system. One such method, for relatively narrow size distributions, is by using the so-called *local monodisperse* approximation [60]. This approximation ignores the interference between different sized inhomogeneities and assumes that only likesized inhomogeneities interact.

$$I(q) = CV\overline{\eta^2} \sum D_n(R_j) V_p(R_j)^2 \left| F(q,R_j) \right|^2 S(q,R_{\text{HS}_j},v) \Delta R \qquad (6.35)$$

where  $S(q, R_{\text{HS}}, \nu)$  is the hard sphere structure factor [61]. This particular structure factor assumes that the inhomogeneities interact with a hard sphere radius,  $R_{\text{HS}}$ , and have a local volume fraction,  $\nu$ . For these "hard spheres," the potential energy of each particle (in normalized units) is everywhere one, except for within the hardsphere radius,  $R_{\text{HS}}$ , where it is infinite (i.e., the hard spheres are impenetrable) [61]. Equation (6.35) is just one example of how a structured-polydisperse system can be treated [62]. In addition, other structure factors have been derived for different cases, each with their own definition of the potential energy function acting between the inhomogeneities [12, 57].

### 6.3.7 Aggregation

Aggregation in ILs is a phenomenon by which either or both of the cations and anions aggregate together in solution to form local, highly charged phases. In these cases, aggregation is often described by the order in the system, which is observable by SAXS. On the other hand, when a third component is added (i.e., an amphiphilic molecule), other aggregated phases can form, which can also be observed with SAXS. Both of these cases will be discussed below. IL aggregation leads to a diffraction peak, arising from the ordered distances between phases. The observed peaks can then be used to understand the effect of different cations and anions. For example, it was shown that the ordering of 1-alkyl-3-methylimidazolium ILs depends on both the anion and the length of the alkyl chain [63]. While Bragg's law has been used extensively in this area to analyze the peak position(s), it is not adequate to interpret the entire SAXS curve, specifically, the shape of the inhomogeneities making up the individual phases. For this, structure factors must be used in Eq. (6.33) with the appropriate form factor. While no new analytical structure factors exist specifically for neat ILs, molecular dynamic simulations have been used to compare the simulated and observed structure factors in pyrrolidinium-based ILs [64]. These structure factors are not in readily useable analytical forms. However, they can be calculated numerically using Eq. (6.32). Finally, the structure factor of any system, on its own, can also be obtained through Eq. (6.33) by simply dividing the scattering intensity, I(q), by the form factor, if this is known a priori.

Aggregated phases, formed by the addition of third components, have also been studied in ILs. Often, these phases form micelles, which can easily be modeled by Eq. (6.35), using the appropriate form factor [28] and structure factor [65]. Using this approach, one can obtain the micelle size, hard sphere radius, chain aggregation number, and chain size [66]. However, this is not always possible because of the limited *q*-range available—a problem that is sometimes unavoidable depending on the instrument used.

In some cases Bragg's Law has been used in place of Eq. (6.35), to analyze the peak in the SAXS curve [67]. While this does provide information about the local order of the micelles, information, such as micelle size, is not provided. In other cases, the form factor for an ellipsoid has been used instead to resolve micelle size [68, 69]. In these cases, not all the micelle information was resolved from the SAXS data. However, for large micelles a significantly wide q-range is required to resolve the micelle size and individual chain dimensions using the appropriate form factor [28]. With a limited available *q*-range, this is just one example of how sometimes the simplest model is best. As stated previously, an uncertainty analysis on the fit parameters can also be useful.

### 6.3.8 Microemulsions

Models have been developed to describe the SAXS from microemulsions, which contain polar, nonpolar, and amphiphilic constituents [70]. There are a few different ways that one can analyze the SAXS from these systems. These approaches are reviewed here. Qualitatively, the Teubner-Strey phenomenological model accounts for a bi-continuous repeat distance, d, as well as the average length scale of the

polar/nonpolar domains,  $\xi$ , using only three fit parameters:  $a_2$ ,  $c_1$ , and  $c_2$  [70]. This model has found application in the study of ILs, which can either be polar or nonpolar. To this end, the Teubner-Strey equation has been used to characterize and compare microemulsions of ILs [71] and even magnetic ILs [72] as well as microemulsions formed with water. Scattering from these systems typically contains a peak in the intensity, characteristic of concentrated systems, as well as a decay in the scattering intensity of  $q^{-4}$ , which corresponds to surface scattering of the separate phases. These features are accounted for by the equations:

$$I(q) = \frac{8\pi / \xi c_2 V \eta^2}{a_2 + c_1 q^2 + c_2 q^4}$$
(6.36)

$$\xi = \left[\frac{1}{2} \left(\frac{a_2}{c_2}\right)^{1/2} + \frac{1}{4} \frac{c_1}{c_2}\right]^{-1/2}$$
(6.37)

$$d = 2\pi \left[ \frac{1}{2} \left( \frac{a_2}{c_2} \right)^{1/2} - \frac{1}{4} \frac{c_1}{c_2} \right]^{-1/2}$$
(6.38)

This equation has been applied successfully to many microemulsions, regardless of the concentration of the polar/nonpolar phase. However, in the case of dilute systems, the Teubner-Strey model does not reveal the size distribution of the inhomogeneities making up the dilute phase.

As pointed out by Klee et al., such a system can also be modeled using Eq. (6.33). This was accomplished by approximating the dilute phase as a polydisperse system of core-shell particles [37] and assuming a hard sphere structure factor; however, the effect of polydispersity on the structure factor was not accounted for [62]. As well, the GIFT analysis has also been used to verify the presence of a core-shell structure [73]. Ultimately, there is more than one single model that can accurately describe the SAXS in terms of the peak intensity, average size, and Porod scattering law. For example, a core-shell structure can correctly account for the shell of amphiphilic molecules at the surface of the microemulsion, which Eq. (6.36) cannot.

Yet another case for microemulsions is when colloidal particles are used to stabilize the emulsion, instead of amphiphilic molecules. To our knowledge, such a study has yet to be carried out for ILs. For such a system, an analytical scattering model that can account for the self-correlation of a spherical core and surfaceadsorbed particles has been developed [74]. Again, this model assumes that the system is in its dilute limit.

### 6.3.9 Monte-Carlo Simulations

A Monte-Carlo analysis may be required when analytical models are not available to analyze the scattering profile. In most cases, this happens because one or more assumptions in Sect. 6.3.1 cannot be met, which would otherwise allow for an analytical solution. In Small-angle scattering (SAS), a Monte-Carlo analysis includes the following steps: (1) random number generation within a sample volume, (2) assignment of the appropriate contrast to each point, and (3) numerical calculation of the scattering intensity [75]. In this section, a Monte-Carlo approach will be introduced, followed by one simple example.

The small-angle scattering can be calculated using the numerical forms of Eq. (6.7) or (6.14), depending on whether or not the system can be considered *centro-symmetric*. In all cases, the scattering intensity can be calculated using the numerical form of Eq. (6.7). If the system can be considered *isotropic*, the complex phase factor in Eq. (6.7) will be replaced by the "average" phase factor:  $\frac{\sin qr}{qr}$ . However,

this involves two summations, which for a large number of points can be computationally expensive. The calculation time can be reduced by effectively enlarging each point such that it occupies a larger volume. In this case, the numerical form of Eq. (6.7) would then be the Debye equation for composite particles (Eq. 6.30), where instead of points, objects of specific shape can be used [76].

In the case that the scattering inhomogeneity is a single *isotropic* object, it is possible to generate the PDDF, which can then be used to calculate the scattered intensity through Eq. (6.10). This is accomplished by first filling the object with randomly positioned points, followed by generating a histogram of distances, r, between each point. The resulting histogram is proportional to the PDDF and can then be used to calculate the scattered intensity or compared to the PDDF obtained from the raw data using IFT [76].

If one can assume *centro-symmetry*, the numerical form of Eq. (6.14) can be used to calculate the scattering intensity from systems that are anisotropic. Significantly lower calculation times can also be achieved because only one summation over the real space is needed at each **q** value. To illustrate how a realistic system can be modeled using this method, we will consider a system of spheres that have a Gaussian size distribution with a mean of 150 A and standard deviation of 15 A. Similar to Eq. 6.34, the scattered intensity of the system can be calculated by the equations:

$$I(\mathbf{q}) = C \sum I_i(q, R_i) D_{n_i}(R_i) \Delta R_i$$
(6.39)

$$I_{i}(\mathbf{q}) = \left[\sum \eta_{j} v_{p} \cos \mathbf{r} \cdot \mathbf{q}\right]^{2}$$
(6.40)

where  $\eta$  is the scattering length contrast of point *j*,  $\nu$  is the volume simulated by each point (equally, the inverse of the point density), and *C* is again a scaling factor.



**Fig. 6.10** Log–log plot showing the simulated SAS from a Gaussian distribution of spheres, having a mean radius of 150 A and standard deviation of 15 A. The scattered intensity is calculated from Eq. (6.39) (*circles*) and compared with the theoretical scattering (*black*), which was generated using the Irena package for Igor pro. In both cases, 50 spheres ranging in sizes between 4 Å and 15,000 Å (log binned) are used to simulate the distribution

Figure 6.10 is a log–log plot that compares the simulated scattered intensity with the analytical solution. One will note that large deviations between the Monte-Carlo curve and theoretical curve increase with increasing q. This can be improved by using more than the 10<sup>5</sup> points used in the simulation; this corresponded to a point density of 7 points per nm<sup>3</sup>. While there is no need to use Eq. (6.39) for a system of spheres, the real advantage of this approach is for anisotropic systems [77].

In section, the general Monte-Carlo approach to small-angle scattering has been presented. A Monte-Carlo simulation, however, involves careful consideration of more than just the fundamental equations behind it. In addition to the computational algorithm, the uniqueness of a feature shape [78] can be difficult to determine. Fortunately, there are software programs that address these issues [17]. There is also software in this field devoted to biological systems as well as other systems that cannot easily be analytically modeled [16].

## 6.4 Experimental

A typical SAXS experiment involves a sample and necessary optics that measure the scattered X-rays. Nowadays, with the accessibility of desktop SAXS machines and synchrotron radiation, the latter is taken care of by the manufacturer, technician, or beamline scientist. In this section, we will discuss practical aspects that the experimenter (as a user) should be concerned with. This entails planning and executing a SAXS experiment, followed by the subsequent data reduction and analysis.

### 6.4.1 Experimental Preparation

In a typical SAXS experiment, one has to first determine what sample geometry is necessary to achieve what one is looking for. For example, in most cases, one wants to look at phases in solution. These phases are typically *statistically isotropic* so it makes no difference what the sample orientation is relative to the incoming X-rays. In this case, a simple transmission geometry is sufficient to obtain the volume average dimensions of the scattering inhomogeneities. On the other hand, if there is reason to believe that scattering inhomogeneities are preferentially oriented near an interface, then a grazing transmission geometry should be considered [79]. A case example would be an electrochemical experiment whereby the system is exposed to an external electrochemical signal at the working electrode. These geometries are shown schematically in Fig. 6.11.

#### 6.4.1.1 Energy Selection

In some cases, for example, at a synchrotron, a user can perform their SAXS experiments at an energy that is optimal for their system. This is particularly useful when one has a weakly scattering system, due to either a small volume fraction or contrast. The optimal X-ray energy is one where no X-ray absorption edges are present and the measured scattering intensity is maximized. This requires some prior knowledge of the system, namely, the elemental composition and thickness of the sample. Once the composition is known, the scattering power,  $\rho^2(\lambda)$ , can be obtained.

In the case of ILs, the X-rays will need to pass through a sample holder that contains the liquid. In most cases, researchers use polyamide film windows for the X-rays to pass through. However, one should be careful with such windows because they scatter strongly at high q (~0.4 Å<sup>-1</sup>). Also, the longer the liquid path that the X-rays pass through, the greater the attenuation due to sample absorption, as given by the equation:

$$\mathrm{Tr} = e^{-\left(\left(\frac{\mu}{\rho}\right)\rho_s t_s\right)} \tag{6.41}$$



**Fig. 6.11** A schematic illustrating the difference in a Grazing Transmission (*top*) and Transmission (*bottom*) SAXS. The resolvable dimensions in each case are shown in *black* 

where  $\frac{\mu}{\rho}$  is the mass absorption coefficient for the material,  $\rho_s$  is its density, and  $t_s$  is the thickness through which the X-rays pass. To calculate Tr from Eq. (6.41), the experimenter should be able to provide  $\rho_s$  and  $t_s$  with reasonable accuracy. The mass absorption coefficient, however, depends on the composition and energy by the equation:

$$\frac{\mu}{\rho}(\lambda) = \sum \frac{\mu}{\rho}(\lambda)_i w_i \tag{6.42}$$

where  $w_i$  is the mass fraction of element *i* and  $\frac{\mu}{\rho}(\lambda)_i$  is its mass absorption coefficient.

Using tabulated values of each element's mass absorption coefficient, one can calculate the transmitted intensity, *I*, from the sample.



**Fig. 6.12** Plot the signal (*top*), detector efficiency (*black*), and transmission (*blue*) for a simple liquid cell filled with a 10 mM of Pt dissolved in a 2:1 urea:choline Cl<sup>-</sup> deep eutectic solvent with a 1 mm thickness. The scattering power,  $\rho^2$  of Pt is shown in the inset

The final ingredient in the optimization is the detector efficiency  $D(\lambda)$ , which must be obtained from the manufacturer. For a given scattering population, the final optimization is therefore:

Signal = 
$$\left[\rho^{2}(\lambda)D(\lambda)\operatorname{Tr}(\lambda)\right]$$
 (6.43)

The optimal energy is then taken to be the one that maximizes the left side of Eq. (6.29). Of course, because we are analyzing the elastically scattered X-rays, absorption edges should be avoided in a normal SAXS experiment; this can be observed in the function  $\rho^2(\lambda)$ . Figure 6.12 shows a case example of a simple cell that contains a deep eutectic solvent (DES) and is 1 mm thick. If, for example, we wanted to observe Pt nanoparticles, then the optimal energy would be approximately 16 keV, which will provide a high signal and is far enough away from any Pt absorption edge.

### 6.5 Future of SAXS and XPCS

In the earlier parts of this chapter, we have introduced the general principles of SAXS. It is worth noting, however, that SAXS is a *static* probe that can resolve the structural inhomogeneities within the specimen of interest. SAXS cannot capture the underlying cause for the structural development or alteration of a physical

system over time, i.e., dynamics. In this section, we will briefly introduce X-ray photon correlation spectroscopy (XPCS), a recently emerged technique that is both closely related to SAXS and capable of measuring nano-scale and micro-scale material dynamics.

XPCS probes the *dynamic* properties of matter by analyzing the temporal correlations between X-rays scattered by the sample. To achieve this, XPCS relies on the availability of coherent X-rays, which is not required for *static* SAXS measurements. Here, coherence refers to properties of X-rays that preserve the X-ray *phase* information commonly lost in conventional X-ray measurements. Preservation of the phase information enables temporally and spatially coherent interference.

Due to their stringent requirements on coherent X-rays, XPCS measurements cannot be performed using lab X-ray sources or even first- or second-generation synchrotron sources, where X-rays produced by these sources possess very low degrees of coherence. XPCS measurements were not possible until the operation of third-generation synchrotron sources, which have lower emittance and long straight sections of undulators that can achieve high X-ray brightness and a considerable degree of spatial coherence. The resulting partially coherent X-rays are several orders of magnitude more intense than previously available. Despite this, synchrotron undulator sources remain chaotic sources because of the spontaneous nature of the X-ray emission.

Overall, the characteristics of third-generation synchrotron sources have led to major progress in structural determinations of objects with low X-ray scattering or imaging contrast. Many groundbreaking discoveries in recent years [80–82] were facilitated by applications of coherent X-ray scattering, diffraction, and imaging techniques such as X-ray phase contrast imaging [83], X-ray holography [84], and coherent X-ray diffraction imaging [85]. More relevant to the topic of this chapter is the revolutionary development of the temporal probe of XPCS, which has made possible direct measurements of slow equilibrium and near-equilibrium dynamics in disordered systems.

From a technique point of view, in many aspects, XPCS is a natural translation of long-wavelength laser photon correlation spectroscopy (PCS), also known as dynamic light scattering (DLS), into the X-ray domain. Both XPCS and DLS share the same set of physical principles and exploit the coherence of their respective radiations by restricting the dimensions of the scattering sample volume to be similar to the coherent volume of the beam. The dynamic timescales of the monitored processes are acquired by analyzing the temporal correlations of photons scattered by the specimen [86].

There also exist key differences between XPCS and DLS. Visible light DLS, as a laser technique, suffers from two major limitations: resolvable size and adsorption. The wavelength of visible light ranges from 400 nm to 700 nm, which (from Eq. 6.5) necessarily restricts the collection of the scattering intensity to a very small scattering vector q. At the same time, the visible light scattering cross section is far



**Fig. 6.13** Frequency-scattering vector domains of available techniques for dynamic studies. The techniques in the map are Raman spectroscopy, Brillouin spectroscopy, inelastic neutron scattering (INS), inelastic X-ray scattering (IXS), neutron spin-echo spectroscopy, nuclear forward scattering (NFS), XPCS, ultrasmall-angle X-ray scattering-based XPCS (USAXS XPCS), and DLS [also known as photon correlation spectroscopy (PCS)]

greater than that for X-rays. Therefore, it is very difficult, if not impossible, for visible light DLS to probe the dynamics of optically opaque or highly absorbing media due to strong absorption and/or multiple scattering effects. XPCS, on the other hand, being an X-ray technique, is not subject to these limitations and offers an unprecedented capability to measure low-frequency ( $10^{-3}$  to  $10^{6}$  Hz) dynamics of structures in the range of 1–10,000 Å (as things stands currently). Figure 6.13 shows the frequency-wavevector range accessible to XPCS and DLS as well as other scattering-based techniques that are frequently used to study dynamics in disordered systems [87, 88].

Since its emergence less than two decades ago [89, 90], XPCS has made great strides in advancing many aspects of statistical physics and providing access to the slow dynamics of a wide range of physical events. Research areas that have benefitted considerably from XPCS include but are not limited to equilibrium dynamics of concentrated colloidal suspensions [90–95], glassy dynamics [96, 97],

atomic diffusion [98, 99], dynamical heterogeneities in soft matter [100, 101], critical fluctuations of liquid crystals [102, 103], near-equilibrium coarsening fluctuation in alloys [104] and weakly disturbed soft condensed matter systems [96, 105–107], and surface dynamics of fluidic and polymeric systems [108–114]. Most of these systems share some common traits, namely, the dynamical fluctuations happen on a length scale between nanometers and micrometers, and the dynamic timescale is greater than a microsecond.

The capabilities of XPCS have not been fully exploited by the ionic liquid research community, which may be attributed to two main reasons. Firstly, despite its rapid development, XPCS remains a highly specialized technique and its availability is limited to a handful of third-generation synchrotron facilities and X-ray free electron laser facilities around the world. Secondly, and perhaps more importantly, the current version of XPCS imposes a rather strict limitation on its detectable time resolution (1  $\mu$ s), and thus cannot detect dynamics faster than this limit. However, a significant effort is under way in the global synchrotron community to generate X-rays with much higher brightness and degree of coherence. This effort would allow sub-nanosecond time resolution for XPCS measurements, which will enable quantification of particle mobility in ionic liquids, as well as determination of the effects that various factors such as particle solvent interaction have on the equilibrium fluctuations of ionic liquids.

While it will take another few years for XPCS development to become fully capable of addressing problems central to the understanding of dynamic behavior in ILs, XPCS is already capable of revealing aspects of the fundamental properties of ILs. In the rest of this section, we will briefly introduce the fundamental theories behind XPCS. We will also present a couple of examples to illustrate the *current* capabilities of XPCS that are relevant to the IL research.

### 6.5.1 Theory

When a thin, disordered sample system is illuminated by coherent radiation, the coherent scattering gives rise to a random coherent diffraction pattern, also known as a "speckle pattern". Speckle patterns, which have been long known from laser scattering [115], were first exhibited in the X-ray regime by Sutton et al. in 1991 [116]. Since then, speckle patterns have been observed in a wide range of materials under coherent X-ray illumination [117–119]. The far-field coherent scattering intensity is given by the coherent superposition of scattering probability amplitudes:

$$I(\mathbf{q},t) = \left|\sum_{j} f_{j}(\mathbf{q}) e^{i(\mathbf{q}\cdot\mathbf{r}(t))}\right|^{2}$$
(6.44)

where **q** is the scattering vector, and  $f_j(\mathbf{q})$  is the scattering amplitude of the *i*th scatterer located at position **r** at time *t*. This summation takes place within the coherent volume, which is defined by the longitudinal coherent length and spatial coherent lengths of the given radiation. From a detection point of view, the measured intensity is an average of  $I(\mathbf{q},t)$  during the entire duration of data acquisition *T*. Distinct and sharp variations in intensities can only be captured when the data acquisition time is comparable to the inherent fluctuation timescale of the underlying material system. Otherwise, the measured intensity becomes an ensemble average, similar to intensity profiles acquired in a conventional SAXS experiment with incoherent illumination.

It is also worth noting that Eq. (6.44) assumes that the X-ray beam is fully coherent. As mentioned previously, the X-rays from a synchrotron undulator source are partially coherent in nature. It is often the case that the illuminated sample volume is greater than the coherent volume. The detected intensity therefore becomes the incoherent sum of a number of coherent scattering intensities from small volume elements, with each volume element having the same size as the coherent volume. Obviously, when the illuminated sample volume becomes too large compared with the coherent volume, the speckle pattern will be smeared out and we once again arrive at an intensity profile that resembles that from a conventional SAXS experiment discussed previously. To preserve the speckle pattern while allowing the maximum coherent flux, common practice at synchrotron beamlines is to use an aperture in front of the sample as a second coherent source [120–122]. The size of the aperture ideally needs to match the spatial coherent lengths. In reality, this requirement is normally relaxed and the aperture often has a size greater than that defined by the spatial coherent lengths, because XPCS is a photon-starved technique.

We illustrate a static speckle pattern from a colloidal suspension of gold nanoparticles in Fig. 6.14 [123]. The left panel shows a single coherent scattering speckle pattern, and the right panel shows the incoherent summation from 50 consecutive measurements, which, as discussed above, is analogous to data from a conventional incoherent SAXS measurement. Figure 6.14 clearly displays the distinctive differences between coherent and incoherent SAXS results.

If the spatial arrangement of the scattering features in the illuminated sample volume changes with time, the corresponding coherent speckle pattern will also change accordingly, following Eq. (6.44). The measurement of intensity fluctuations of the speckles can reveal the underlying dynamics of the sample, and forms the basis of XPCS. An example of the XPCS intensity fluctuation at one reciprocal vector is shown in Fig. 6.15.

The data reduction and analysis of a typical XPCS data of an equilibrium dynamic system is well documented [87, 124, 125]. The quantification of the equilibrium dynamic timescale is assisted by the normalized second-order intensity correlation function  $g_2(q,\tau)$ , which is defined by

$$g_{2}(q,\tau) = \frac{\left\langle I(q,t+\tau)I(q,\tau)\right\rangle_{t}}{\left\langle I(q,t)\right\rangle^{2}}$$
(6.45)

**Fig. 6.14** Coherent X-ray scattering pattern from a colloidal suspension of gold nanoparticles. *Left half* shows a single-shot coherent pattern, where distinct speckles are clearly visible. *Right half* shows a scattering ring obtained from a sum of 50 successive shots, which is smooth and largely resembles data from conventional SAXS experiments





**Fig. 6.15** Illustration of typical XPCS data. *Left panel* shows a simulated coherent speckle pattern. *Right panel* shows the fluctuation of the coherent scattering intensity from the highlighted pixel as a function time

where  $\tau$  is the time delay between two measurements, and  $\langle \rangle t$  denotes an ensemble average over all times.

It is also known that the normalized second-order intensity correlation function is related to the intermediate scattering function following

$$g_{2}(q,\tau) = 1 + \beta(q) \times \left| f(q,\tau) \right|^{2}$$
(6.46)

where  $\beta(q)$  is commonly referred to as the optical transfer function, and is related to the setup of the scattering instrument. For a fully coherent beam with no disturbance to the coherence from the optical elements,  $\beta(q) = 1$ .

The function,  $f(q,\tau)$ , is the time-dependent intermediate scattering function. It contains time-dependent spatial structural information, and can be attributed to scattering that arises from the non-periodic pair correlation function within the electron density function and it is further defined by

$$f(q,\tau) = \frac{S(q,\tau)}{S(q,0)} \tag{6.47}$$

Here S(q, 0) is the static structure factor, and  $S(q, \tau)$  is the time-dependent structure factor. In other words,  $f(q, \tau)$  can be seen as equivalent to the normalized dynamic structure factor in the time domain, which is fundamental in the description of dynamic behavior of condensed matter and is often the key parameter through which detailed comparisons between experiments and theories can be made. Access to this key parameter is the most important role of XPCS.

Depending on the underlying physical process that is responsible for the measured dynamics, the intensity correlation function  $g_2(q, \tau)$  [or intermediate scattering function  $f(q, \tau)$ ] can be analyzed using different models. For example, in the simplest case, when the scatterers undergo free diffusion (Brownian motion), the intermediate scattering function follows  $f(q,\tau) = \exp(-D_0q^2\tau)$ , where  $D_0$  is the diffusion coefficient. For simple monodisperse spherical objects,  $D_0 = k_{\rm B}T/6\pi\eta_{\rm s}r$ . Here  $k_{\rm B}$  is the Boltzmann constant, *T* is temperature, *r* is particle radius, and  $\eta_{\rm s}$  is the viscosity of the solvent. Therefore, XPCS measurements of dilute particle dynamics provide a direct probe of solvent viscosity, and when coupled with rheology experiments can help uncover the dynamic viscoelastic modulus of the solvent in the frequency domain.

We note that free diffusion is an exceptionally simple case. Most dynamic processes are more complicated and their intermediate scattering functions have to be treated accordingly and differently. Here we present another empirical and analytic form of the intermediate function that can be relevant to ILs, namely, the Kohlrausch–Williams–Watts (KWW) function  $g_2(t) = \beta \exp(-2(t/\tau)^{\gamma}) + 1$ . Here  $\tau$  is the characteristic relaxation time, and  $\gamma$  as an exponent indicates whether the decay is faster ( $\gamma > 1$ ) or slower ( $\gamma < 1$ ) than the exponential decay expected from a free diffusion.

### 6.5.2 Examples

#### 6.5.2.1 Example 1: Particle Dynamics

Recently, novel colloidal systems with ionic liquids as solvents have gained attraction because the colloidal nanoparticles allow fabrication of novel nanohybrid materials [126, 127], which can find applications such as in IL-based solid electrolytes [128, 129]. However, because ILs can act to modify the interparticle interactions between colloidal particles, the effects that different ILs have on the colloidal stability are not well understood [130]. To have a proper comprehension of the colloidal stability in ILs, it is critical to understand the dynamic behaviors of such colloids. XPCS, due to its suitable time and length scale, is unquestionably a technique that can offer a unique perspective to unveil the hidden mechanism governing the colloidal stabilities. While such studies do not yet exist, we will use the following example to illustrate the capabilities of XPCS in elucidating particle dynamics.

In colloidal suspensions, as colloidal particles move, they excite long-ranged flow in the fluid. Similarly, colloidal particles move in response to fluid motion. By generating and reacting to the local velocity of the fluid, colloidal particles experience hydrodynamic interaction, which, despite its long-recognized ubiquity, is not completely understood. Banchio et al. [93] studied the hydrodynamic interaction of concentrated ( $v \approx 0.14$ ), monodisperse fluorinated latex spheres of radius 82.5 nm in solvents of different NaCl concentrations. Due to the apparent high volume concentrations, the effective diffusion constant D(q) was obtained using a limiting form related to the intermediate scattering function, following  $D(q) = -1/q^2 \times \lim_{t \to 0} \partial(\log |f(q,t)|) / \partial t$ . The hydrodynamic interaction follows

 $H(q) = D(q)S(q)/D_0$ ; here S(q) is the static structure factor and  $D_0$  is the single particle diffusion constant in the dilute limit.

Figure 6.16 shows the q dependence of the static structure factor S(q), effective diffusion constant D(q), and the hydrodynamic interaction H(q) in a solvent with 0.5 mM NaCl. The structure factor was found to follow the Rogers-Young model, which describes standard macroion fluids of charge-stabilized spheres. More importantly, by comparing XPCS data with simulation results using a novel accelerated Stokesian Dynamics method, the authors found that there is no hydrodynamic screening present in low-salinity systems. Through this effort, the influence of many-body hydrodynamic interactions on the diffusion properties of charge-stabilized colloidal spheres was explained and quantified. This result may carry potential impact on the transport properties of complex colloidal particles suspended in various solvents of interest to industry, including ILs.

#### 6.5.2.2 Example 2: Surface Dynamics of Capillary Wave

ILs often possess peculiar molecular structure and composition, which can lead to unusual molecular packing. This also extends to the liquid/air interface of ILs, where a surface layer with a higher mass density than that of the bulk has been identified due to the low dimensionality at the free surface [131]. A subsequent question is on how this unusual packing affects the dynamics at the interface. To address this question, Sloutskin et al. conducted the first and the only XPCS investigation of ILs to date to probe the dynamics and critical damping of the capillary waves in ILs [132]. Due to the surface geometry, a grazing-incidence version of XPCS was employed, where the incidence angle of the X-rays was below the critical angle for total X-ray reflection so


**Fig. 6.16** Static structure factor S(q), short-time collective diffusion coefficient D(q), and hydrodynamic function H(q) for a suspension of charged latex spheres in a 0.5 mM NaCl solvent

that the surface dynamics on the top layer of the ionic liquid butylmethylimidazolium tetrafluoroborate ( $[C_4mim][BF_4]$ ) could be measured.

Similar to the transmission geometry, grazing incident intensity correlation function yields the dynamic structure factor. The dynamic structure factors of  $[C_4mim][BF_4]$  at different temperatures and reciprocal vectors are shown in Fig. 6.17. The experimental data reveal that capillary wave excitations at shorter wavelengths have higher frequencies, and capillary waves are over-damped at high *q* and low temperature. Moreover, it is found that in order to fully account for the line shape of the dynamic structure factor, both the homodyne and heterodyne components of the scattering have to be taken into account. Such findings are important to the understanding of the fundamental mechanic behaviors of ionic liquids, and can only be accessed through XPCS.



**Fig. 6.17** The grazing incidence dynamic structure factors for  $[C_4mim][BF_4]$  for (**a**) listed *qs* and (**b**) listed temperatures

## 6.6 Conclusion and Outlook

XPCS is a promising young technique that can monitor the dynamics of condensed matter on length scales shorter than that accessible to light scattering techniques. In spite of the tremendous progress made since its discovery, XPCS, being a signal-to-noise limited technique, has limited spatiotemporal resolution because of the relatively low degree of coherence in the X-ray beam generated by undulator sources at synchrotrons. This fact constrains its applications in many fields, including that of ILs. However, as we identified in this section, even at this stage, XPCS can contribute to the understanding of dynamics in concentrated colloidal particles in various ILs and surface dynamics of ionic liquids.

An important feature of XPCS is that the available time resolution scales as the square of the strength of scattering intensity, which is proportional to source brightness. For example, a 100-fold increase in brightness will provide a 10<sup>4</sup> increase in dynamic range, which in turn will enable nanosecond time and nanometer space resolution. This has already been achieved using X-ray free electron laser (XFEL)

facilities in the United States and Europe. However, access to XFEL is very limited. Currently, worldwide efforts are under way to upgrade the existing third-generation synchrotron facilities with multi-bend achromat lattices, which will provide orders of magnitude improvement in X-ray brightness and coherent flux. This upgrade, once completed, will allow XPCS measurements to a full spectrum of dynamic investigations of ionic liquids.

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# Part II Structure and Properties of Ionic Liquids Relevant to Electrochemistry

## Chapter 7 Room-Temperature Molten Salts: Protic Ionic Liquids and Deep Eutectic Solvents as Media for Electrochemical Application

Mérièm Anouti

## 7.1 Introduction

Ionic liquids (ILs) are room-temperature molten salts (RTMS) composed mostly of organic ions that may undergo almost unlimited structural variations. ILs and deep eutectic solvents (DESs) have been applied in various fields, such as electrolytes for lithium ion batteries, redox flow batteries (RFBs), electrodeposition, and electropolishing, and even in fuel cells. This chapter covers the newest aspects of H-donor ILs in applications where their transport properties (ion conductivity, diffusion, and viscosity) are exploited, for example, as electrochemical solvents for energy storage where conventional media, organic solvents (in batteries), or water (in supercapacitors) fail. Metal nanoparticles' (NPs) formulation and stabilization in H-donor RTMS with some unique size, shape, and properties are also discussed. In these decidedly different materials, a mixture with a molecular solvent shows electroactivity that is not exhibited in more traditional systems, creating huge potential for energy storage and electrocatalysis. The remarkable recent increase in the level of interest in RTMS (protic ionic liquids, PILs, and DESs) in academics and industry is illustrated by the rapid growth in the number of publications on the topic (Fig. 7.1), with more than a 100-fold increase observed over the period 2004 to 2014.

The first main objective of this chapter is to summarize the synthesis and physical properties of PILs and DESs and discuss their suitability as green solvents for different applications. The second main objective is to review the electrochemical applications of RTMS and discuss their advantages and disadvantages as electrolytes in comparison with an aprotic homologue for energy storage applications. I hope to generate interest in the wider community and encourage others to make use of proton-donor RTMS—PILs and DESs—in tackling scientific challenges.

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Fig. 7.1 Rapid growth of PIL and DES publications over the period 2000 to 2014; data obtained from a literature search using SciFinder scholar

## 7.2 Advances in Proton-Donor Room-Temperature Molten salts

### 7.2.1 Protic Ionic Liquids

ILs are organic salts with unusually low melting points, well below 100 °C [1, 2]. These substances have been suggested as potentially "green" replacements for traditional molecular solvents since some ILs are nonvolatile, nonflammable, thermally stable, and recyclable. Additionally, they open the path to novel methods that are not possible using classical solvents. Those formed by the transfer of a proton between a Brønsted acid and a Brønsted base form the protic subgroup now referred to as "Protic Ionic Liquids (PILs)" [3, 4].

$$HA + B = A^- + BH^+ \tag{7.1}$$

While one of the first IL described in 1914 by Walden was of "the protic type"  $[H_3NEt][NO_3]$  ethylammonium nitrate, conventionally called (NEA) (with a mp=12.5 °C), described in nearly all reviews on ILs [5], aprotic ILs largely dominate the open literature. Recently, there has been a resurgence of interest for these Protic ILs essentially because of their great potential for proton-transfer applications in fuel-cell technologies as an electrolyte in nonhumidified fuel-cell systems [6, 7]. In recent years, real progress has been made in the electrochemical application of PILs as media thanks to their proton activity [8, 9]. The physicochemical properties of pure PILs and their mixtures with protic and aprotic molecular solvents are now systematically studied as proton-conducting electrolytes. PILs are starting to emerge as useful materials owing to various potential applications [10]

including electrolytes in aqueous batteries, fuel cells, double-layer capacitors, and biosensors. There is, therefore, much promise of new and large application fields for PILs [11].

PILs differ from other types of ILs in that the ionic moiety is formed from the transfer of a proton [12]. However, neutral aggregates of PILs were hypothesized and later directly observed, both in the gas phase and at the PIL–solid interface [13]. Strong charge ordering can lead to a long-range order even in the presence of a solute and may arise from the competition among electrostatic, dispersion, and hydrogen-bonding interactions [14].

They present the advantage of being cost-effective and are easily prepared as their formation does not involve the formation of residual products. Different series of liquid crystalline have been isolated from the reaction of nitric, hydrochloric formic, and tetrafluoroboric acids with the corresponding alkylimidazoles, pyrrolidines, pyridines, or alkylamines. Those based on the imidazolium cation induce a specific stereoselectivity for the catalyzed Diels-Alder condensation reaction of cyclopentadiene and diethyl maleate [2, 15]. [The protonated Hünig base, [NHEt(i-Pr)<sub>2</sub>][CF<sub>3</sub>CO<sub>2</sub>], is reported to be an efficient medium for the nitration of arenes. Ohno and Yoshiwaza demonstrated for PILs prepared by neutralization of 1-alkylimidazoles the synergic effect between protonated alkylimidazoles and palladium, rhodium, or ruthenium catalysts observed in reactions where the presence of a proton is essential for good performance [16].

Many of these PILs involve very strong acids, such as  $H[N(Tf)_2]$ , H[NTf], etc., and hence the equilibrium (Eq. 7.1) is heavily shifted to the right, thus producing ILs as completely ionic salts.

The discussion concerning the labile proton and its acidity is still under debate [3, 17, 18]. It is possible to relate the acidity of PILs with their catalytic activities in different acid–base reactions. The efficiency of PILs as catalyzing media can further be improved by adding Brønsted acids. The strength of the added acid in a medium depends on the dissociation of acid and the stabilization of the conjugate base. Since different solvents solvate protons (H<sup>+</sup>) to different extents, the strength of an acid varies with the medium.

Because of the various specific and nonspecific interactions, ILs have a unique solvation behavior. However, it is difficult to correlate the solvation behavior of ILs with its solvent properties, such as polarity (normalized charge transfer  $E_T^N$ ) and relative permittivity ( $\varepsilon_r$ ) [19–21]. Determining pKa PILs values aims to understand the proton properties [3]. Since proton acidity is mainly defined by their solvation, an environment other than water results in different pKa IL values. Adams et al. showed recently that the role of the solvent in the PIL/solvent mixture turns out to be preponderant in the chemical equilibrium. They demonstrated that pKa PIL values depend on the medium and give information about the relative feasibility of the proton to interact with a given solute. Their results concluded that it is possible to predict hydrogen bond strength between the cation and the anion and, ultimately, the type of ionic network they form. This property is the key in the activity of PILs as shown by the Kumar group [3], who noted that the ability of PILs to promote



Fig. 7.2 Common cations in PILs

acidity is higher in [Hmim][HCO<sub>2</sub>] than other PILs: [Hmim]<sup>+</sup>>[Hpy]<sup>+</sup>>[HPyr]<sup>+</sup>. The observations drawn above are expected to be useful in synthesizing an efficient IL for acid catalysis. The most common cations for PILs are presented in Fig. 7.2.

## 7.2.2 Deep Eutectic Solvents

DESs are liquid media obtained by mixing, in certain ratios, a metal salt with a hydrogen bond donor (HBD), such as alcohol, amide, and carboxylic acid [22–27], as a complexing agent. This results in the formation of a eutectic mixture with a melting point temperature that is considerably lower than its original precursors, mainly due to the generation of intermolecular hydrogen bonds. The best glassforming composition in a simple binary eutectic system emphasizes the composition range between the eutectic and the medium points as shown in Fig. 7.3. DESs, thus, have gained great attention to replace current organic solvents and have been applied to many chemical processes.

At room temperature, a eutectic mixture can fall under ionic liquid; it has the general properties of ILs, such as nonvolatility, high fluidity, low melting temperature, high boiling temperature, and nonflammability [26, 28–32]. These eutectic mixtures are made up of organic salts, organic acids, organic neutral molecules, or inorganic salts, which is the only difference from the traditional ILs comprising cations and anions. In order to differentiate these eutectic mixtures from traditional ILs, they have been defined as DESs. However, they have their own special properties compared with aprotic ionic liquids (AILs). For instance, first, the synthesis of the eutectic mixture is simple. The pure state can be obtained only through mixing the two components together mechanically. Second, in a eutectic mixture, many



Fig. 7.4 Common DESs and NADESs

inorganic and organic chemicals are more soluble than in water. Even some "insoluble" metal oxides have been found to have significant solubility in a eutectic mixture. Third, it does not react with water and it is biodegradable, like the choline chloride/ urea eutectic mixture that has very low toxicity [31]. Figure 7.4 shows the most common DESs and natural DES (NADESs).

Similar combinations are also observed in plant secretions, and plants in drought or cold conditions. In fact, the ingredients for natural ILs and DESs are abundant in organisms [33]. Young et al. demonstrated in an exhaustive description of the NADESs that these compounds play important physiological roles as a third medium polar liquid in living cells and organisms [34]. For example, flower nectar liquid is composed mainly of sugars that are individual in their solid form at room temperature; however, in liquid form, the composition of this sugar mixture is similar to the proposed composition, a fructose–glucose–sucrose NADES [34], or to the components found in honey, composed of glucose and fructose. NADES components were also observed in desert plants of the *Selaginella* species and also in microorganisms, lichen, and various other organisms that can survive longer periods without water.

During the last decade, a series of novel and cheap complex systems based on lithium salt (LiX;  $X = [N(Tf)_2]$ ,  $[ClO_4]$ ,  $[CF_3SO_2]$ ) and organic compounds with an acylamino group (Urea, acetamide, glycol) [23, 33, 35–38] have been studied. A timeline of reported developments, both on applications and fundamental studies of deep eutectic solvents, is summarized in Fig. 7.5. The data indicate that complex systems are believed to be promising electrolytes for electrochemical devices due to their excellent thermal stability, low viscosity at room temperature, high ionic conductivity, and broad electrochemical stability. The Li[N(Tf)\_2]–acetamide composite was formerly chosen as the electrolyte applied in the energy storage application by Chen [39]. Thereafter, Anouti et al. demonstrated that *N*-methylacetamide (MAc) was able to decrease the melting point of a complex system containing a molten salt due to its "water-like" physical properties, e.g., a very high-dielectric constant and dipolar moment [40] can be considered as a good H-bond donor for the formulation



Fig. 7.5 Timeline of reported developments, both on applications and fundamental studies of deep eutectic solvents

of new DES-based electrolytes [40, 41]. We also demonstrated that each formulated DES-based electrolyte containing the MAc and a LiX salt ( $X = [NO_3]$ ,  $[N(Tf)_2]$ , or  $[PF_6]$ ) allows the realization of energy storage systems as LIBs or EDLC devices that show promising performances even at 80 °C. Interestingly, a discussion for the mechanism action of such electrolytes was centered on the mechanism of pore accessibility for non-solvated lithium ions in these media.

#### 7.2.3 Natural Ionic Liquids

As our mineral resources continue to be consumed at a prodigious pace, it is necessary now that the chemical industry adopts renewable natural sources as starting materials. Natural amino acids [42, 43] and their derivatives provide the most abundant renewable natural chiral pool and can form an efficient, practical, and facile precursor for the preparation of chiral compounds [44–47]. Nevertheless, current studies have also raised doubts over whether traditional ILs are genuine green reagents. For example, some ILs are volatile, combustible, and toxic and could exert negative effects on the environment [48]. Rogers and Voth reported that the decomposition of some ILs could form corrosive HF [49]. As far as we are concerned, the development of biological (Fig. 7.6), environmentally compatible, or biodegradable ILs or Natural Ionic Liquids (NILs) is of paramount importance [50].

At the same time, it is hard to prepare high-purity RTILs by conventional anion exchange reactions because the by-products, such as metal salts, were previously difficult to eliminate until pure RTILs were prepared by neutralization reactions of tertiary amines and organic acids. Furthermore, task-specific [51] and biodegrad-able [52–56] ionic liquids have an attractive future in green chemistry because their utilization will greatly reduce the risk to the environment.



Fig. 7.6 Lidocaine docusate: biological ILs, the third generation of ILs



Fig. 7.7 Biological ILs based on chitosan for biosensors and biocatalysis application

NILs chiral and biodegradable ionic liquids can be synthesized from natural amino acids [45]. Some characteristics of these RTILs, such as good miscibility with organic solvents, high ionic conductivities, and low glass transition temperatures (Tg), have been reported. For example, Chitosan is obtained by full or partial deacetylation of chitin (Fig. 7.7).

Carboxymethylated chitosan (CM-chitosan) has a similar molecular structure with amino acids and can be obtained by carboxymethylated reactions between chitosan and monochloroacetic acid [57]. Chitosan and CM-chitosan are attractive nontoxic, biocompatible, biodegradable, and film-forming biomaterials that can be used as biosensors and biocatalysis [58]. Despite a composite system based on chitosan and RTILs for electrochemistry applications presented by Lu et al. [59], to date, there are no other reports on the synthesis of ionic liquids composed of natural oligosaccharides. Furthermore, it will be helpful to improve the biocompatibility of ionic liquid by introducing CM-chitosan as an anion compound. Recently, RTIL based on 1-ethyl-3-methylimidazolium hydroxide,  $[C_2min][OH]$ , and CM-chitosan was prepared by a neutralization reaction (Fig. 7.7) [57].

## 7.3 Physicochemical Properties of H-donor RTMS

To design any process involving ILs on an industrial scale, especially in electrochemical process, some thermophysical properties must be known, such as viscosity, conductivity, and diffusivity. Furthermore, these experimental data provide useful fundamental information on molecular interactions and can also be applied to evaluate thermodynamic models [60–62]. These models provide better understanding of the nature of the molecular aggregation that exists in binary mixtures. However, the relatively high viscosities of pure ILs and to a lesser degree PILs compared to traditional solvents have resulted in limited commercial use to date. This problem is partially resolved by mixing ILs with water or organic solvents [63–66]. In fact, the main advantage of using binary mixtures (PIL + molecular solvent) is to decrease the viscosity and increase the conductivity of the solution, which leads to most ionic liquids used as electrolytes having conductivities less than those of water with added electrolyte, but comparable to those of organic solvents with added supporting electrolyte (e.g., acetonitrile containing 0.1 M Bu<sub>4</sub>NClO<sub>4</sub>). Since ILs are composed of ions, it is frequently assumed that they should have high conductivities. However, conductivity depends upon both the number of charge carriers and their motilities. The high viscosity and large size of the constituent ions of ILs result in reduced ion mobility and moderate conductivities.

## 7.3.1 Transport Properties and Ionicity Classification

#### 7.3.1.1 Conductivity

Conductivity determines the level of ohmic drop in voltammetric experiments. If the conductivity is too low, the voltammograms will be highly distorted. Among the most important properties of ILs is their conductivity for potential applications as electrolytes in electrochemical devices [67–69]. In the binary system where ILs are mixed with a molecular solvent (PIL+MS), solvent molecules separate the ions, and the mean distance between them depends on the IL concentration. The thermo-dynamic properties of such solutions are described by ion–solvent, ion–ion, and solvent–solvent interactions. This leads to various well-defined species present in the solution, such as free ions, complex ions, neutral ion pairs (ions of opposite sign are separated by the solvent molecule), or nondissociated neutral salt molecules (ions of the opposite sign are not separated by the solvent molecules).

As PILs can be mixed with molecular solvents, this provides new opportunities to study the conductivity of electrolyte solutions in salt-rich regions up to 15 mol.  $L^{-1}$ . Numerous studies concern the specific conductivity and viscosities of pure PILs [70–73], since it is desirable and of great importance to understand and predict the transport properties of PIL+molecular solvent solutions using classical and theoretical models.

The observed shape of the conductivity curve as a function of the solvent mole fraction follows the same trend for protic, aprotic, or deep eutectic solvents, as shown in Fig. 7.8 [74], which shows the change in conductivity following the addition of the solvents to  $[S_{111}][N(Tf)_2]$ ,  $[HN_{111}][N(Tf)_2]$ , and  $Li[N(Tf)_2]$  at 25 °C, respectively.

In this figure, the influence of the addition of the organic solvent, acetonitrile (ACN), gamma butyrolactone ( $\gamma$ -BL), and propylene carbonate (PC) is shown. The conductivity of each binary mixture increases quickly to reach a maximum conductivity in the solvent-rich region. Furthermore, it appears that all mixtures containing ACN have higher conductivity than those based on  $\gamma$ -BL; at the same time, all investigated PC solutions showed three times lower conductivities compared to ACN.



Fig. 7.8 Change in conductivity following the addition of solvents to  $[S_{111}][N(Tf)_2]$  (a),  $[HN_{111}][N(Tf)_2]$  (b), and  $Li[N(Tf)_2]$  (c) at 25 °C

Generally, PILs have higher conductivities compared with those based on the homologue AIL. This may be due to the contribution of labile hydrogen driven by the Grotthuss mechanism [75]. In the case of DESs (Fig. 7.8c) [40], the strong interaction between N-methylacetamide (NMA) and the ion pair explains ion mobility and conductivity. The similarity between the graphs  $\sigma = f(xs)$  reported for each RTMS indicates that the mechanisms of the charge transport must be similar for all investigated IL+solvent binary mixtures. When the solvent is added to an IL, the charge density, as well as the viscosity of the solution, is reduced. At solvent concentrations close to the maximum conductivity, the effect of dilution by the solvent is dominant.

#### 7.3.1.2 Viscosity

Viscosity is influenced by several parameters. With respect to the anion, higher basicity, size, and capacity to form hydrogen bonds increase the IL viscosity. Moreover, due to the acid/base character of PILs, their viscosity is highly dependent on hydrogen bonds between ions [76–78]. In general, AIL viscosity is higher than their homologue PILs. The viscosity at 25 °C of the  $[HN_{222}][N(Tf)_2]$  has been



reported as ~ 39 mPa · s [74]. This value is similar to that value measured for  $[S_{222}]$  [N(Tf)<sub>2</sub>] [74, 79] (33 mPa · s at 25 °C). Both sulfonium AIL and ammonium PIL with homologous structures have lower viscosities than those reported for pyrrolidinium or imidazolium [N(Tf)<sub>2</sub>]<sup>-</sup>-based ILs, which have viscosities generally between 50 and 100 mPa · s at 25 °C [80].

At 25 °C, the viscosity values of different DESs reported in the literature range from 50 mPa s to 5,000 mPa, for example, viscosity up to 500 mPa  $\cdot$ s is reported in the case of the equimolar oxalic acid/choline chloride DES system [23, 81, 82]. In general, at 25 °C the DES viscosity values are similar to those observed in the case of classical ILs. In other words, DES viscosity is high and is strongly affected by the selection of the solvent and salt driven by their structures that determine the nature of intermolecular interactions between the molecules and ions in solution as shown in Fig. 7.9 [41].

For example, the high viscosity of the acetamide-based DESs is mainly due to the Coulombic interactions between the Li<sup>+</sup> cation and the carbonyl group, as well as between the amide group and the [N(Tf)<sub>2</sub>] anion (Fig. 7.9). The relatively high viscosity, compared to traditional solvents, can also be interpreted as a decrease in conformational degrees of freedom in solution due to the stable trans-structure of the N-methylacetamide. Takano and Nakamura showed that the trans-state is more stable than the cis-state by 2.8 kcal mol<sup>-1</sup>. Thus, van der Walls interactions are more stable, reinforcing the friction between species [83]. The influence of the addition of the organic solvent, acetonitrile (ACN), gamma butyrolactone ( $\gamma$ -BL), and propylene carbonate (PC), on the rheological properties of ILs can be analyzed by the rheological approach. In general, the viscosity of electrolytes varies with concentration C according to the Jones–Dole equation [84, 85]

$$\frac{\eta}{\eta_0} = 1 + A\sqrt{C} + BC \tag{7.2}$$

where  $\eta$  and C are, respectively, the viscosity and concentration of the solution and  $\eta_0$  is the viscosity of the solvent. *A* and *B* are Jones–Dole coefficient values: the slope (*B*) and ordinate (*A*) are deduced from a plot of the reduced viscosity

$$\frac{\left(\frac{\eta}{\eta_0}-1\right)}{\sqrt{C}} = f\left(\sqrt{C}\right).$$
 A is generally independent of concentration, C, and B is related

to the effect of the ions on the structure of the solvent. B is generally interpreted as a measure of the structure-forming and structure-breaking capacity of an electrolyte

in solution [86–88]. A positive value of the *B* coefficient indicates a structureforming effect, and a negative value shows a structure-breaking effect. In a comparative study concerning sulfonium AILs and ammonium PILs, negative B values were obtained for both AILs and PILs in mixture with  $\gamma$ -BL and ACN, while positive B values was obtained in the case of ILs/PC mixtures [74]. This result can be interpreted as a structure-breaking effect on the addition of these ILs to  $\gamma$ -BL and ACN and as a structure-forming effect on the addition of these ILs to PC. In the same solvent, this effect is more pronounced with the aprotic IL [S<sub>111</sub>][N(Tf)<sub>2</sub>] than with the protic [HN<sub>111</sub>][N(Tf)<sub>2</sub>]. Therefore, the structure-forming capability of the sulfonium cation is higher than that observed for the equivalent ammonium IL. This is probably due to the size of the sulfonium cation and to the fact that the sulfur d-orbitals may be able to interact with the solvent through a coordinative bond. Finally, for each salt, the *B* values vary according to the nature of the solvent in the following order: PC> $\gamma$ -BL>ACN.

The addition of water in PIL solutions decreases drastically the viscosity of the media compared to the viscosity of pure PILs. For example, the viscosity of pure [HPyr][HSO<sub>4</sub>] is close to 156.3 cP, whereas when mixed with water, the equimolar composition has a viscosity close to 33 cP. Additionally, for high concentrations of PILs ( $x_{IL}$ >0.5), anion choice also affects dramatically the solution viscosity [89]. This effect is driven by the fact that the HSO<sub>4</sub>-based PIL is around nine times more viscous than PIL containing the [CF<sub>3</sub>CO<sub>2</sub>] anion. For a lower PIL mole fraction, such a difference tends to decrease, since the viscosity of each aqueous solution tends to converge toward the viscosity of pure water. The dependence of the viscosity deviations from ideality,  $\eta^{E}$ , ( $\eta^{E} = \eta - (x_1 \eta_1 + x_2 \eta_2)$ ) as a function of the PIL mole fraction composition,  $x_{PIL}$ , expresses the modification of ionic association by the addition of water (7.2) in PILs (7.1).

For example, Fig. 7.10 shows that  $\eta^{E}$  is positive over the entire composition range in the case of the ([HPyr][CF<sub>3</sub>CO<sub>2</sub>]+H<sub>2</sub>O) binary mixture, with a small amplitude, whereas, for the ([HPyr][HSO<sub>4</sub>]+H<sub>2</sub>O) binary mixture, the deviation is negative with a high amplitude 14 times higher than the maximum viscosity deviation value reported for the fluorinated anion [89]. In fact, the strong ionic association and the hydrophobicity of the fluorinated anion could explain the low impact of the addition of water on the viscosity of the trifluoroacetate-based PIL solution. In contrast, the acidic equilibrium of [HSO<sub>4</sub>] anion and water promotes a drastic change in viscosity.

#### 7.3.1.3 Ionicity and Diffusion

One way of assessing the ionicity of ILs, RTMSs, or DESs is to use the classification diagram based on the Walden rule [90, 91]. The Walden rule relates to the ionic mobility represented by the equivalent conductivity  $\Lambda$  ( $\Lambda = \sigma/C$ ) to the fluidity  $\eta^{-1}$  of the medium through which the ions move [71, 92]. Figure 7.13 shows the variation of log ( $\Lambda$ ) versus log(1/ $\eta$ ) at various temperatures from 20 to 80 °C in the case of the Li[N(Tf)<sub>2</sub>]/MAc system at *x* Li[N(Tf)<sub>2</sub>]=1/4 compared to those reported by our group in the case of the pyrrolidinium nitrate PIL [HPyr][NO<sub>3</sub>] and its mixture with



**Fig. 7.10** Viscosity deviations from ideality,  $\eta^{E}$ , as a function of the PIL mole fraction composition,  $x_{PIL}$  for the aqueous mixture [HPyr][HSO<sub>4</sub>] and [HPyr][CF<sub>3</sub>CO<sub>2</sub>] ([HPyr]=[Pyrr]). Reproduced from [89] with permission from Elsevier

propylene carbonate [40]. The ideal line is obtained on the basis that ions have mobility that is determined only by the viscosity of the medium and that the number of ions present in the equivalent volume is that indicated by the salt composition, i.e., all ions contribute equally. The position of the ideal line is established using aqueous KCl solutions at a high dilution. The results obtained in Fig. 7.11 indicate that the LiX-based DESs are a superionic liquid and these solutions become more "ionic" according to the Walden classification with temperature [40]. This observation can be linked, as discussed above, to the low pseudo energy of the viscous flow value associated with this solution, which further suggests the predisposition of this mixture for use as an electrolyte for energy storage application.

Several authors have then used self-diffusion coefficients determined by Pulsedgradient spin-echo NMR (PGSE-NMR) to calculate the molar conductivity ( $\Lambda_{NMR}$ ) according to the Nernst–Einstein equation [63, 93, 94]

$$\Lambda_{_{NMR}} = \frac{F^2 \Big[ D_{_{C^+}} + D_{_{A^-}} \Big]}{RT}$$
(7.3)

where *F* is the Faraday constant, *R* is the universal gas constant, and  $D_{\text{cation}}$  and  $D_{\text{anion}}$  are the self-diffusion coefficients obtained by PGSE-NMR from the translational motion (self-diffusion) of the NMR-sensitive nuclei observed. Thus, the  $\Lambda_{\text{NMR}}$  values were derived from the assumption that all diffusing species detected during the



**Fig. 7.11** The Walden rule for the ionicity of Walden plot  $\log(\Lambda)$  versus  $\log(\eta^{-1})$  of the Li[N(Tf)<sub>2</sub>]/MAc DES at  $x_{\text{LiTFSI}} = 1/4$ : *filled circle* and Pyrrolidinium nitrate protic ionic liquid [HPyr][NO<sub>3</sub>] and its mixture with propylene carbonate ([HPyr][NO<sub>3</sub>]+PC) binary mixtures as a function of the temperature at  $x_{\text{PIL}} = 0.25$ : *filled triangle*, 0.10; *open square*, 0.22; *filled square*, 0.30; *Reverse filled triangle*, 0.50; *open diamond*, 0.80; *open circle*, 1. Reproduced from [40] with permission from Elsevier

PGSE-NMR measurements contribute to the molar conductivity. On the other hand, the  $\Lambda_{cond}$  values can be evaluated by the migration of charged species under an electric field. In the presence of neutral ion pairs, the  $\Lambda_{NMR}$  values were expected to differ from those determined by conductivity ( $\Lambda_{cond}$ ) [75]. In order to calculate the molar conductivity, it was necessary to take into account all mobile species: the mobile proton ( $H^+$ ), the cation ( $C^+$ ), and the anion ( $A^-$ ) as in the following equation:

$$\Lambda_{NMR} = \frac{F^2}{RT} \left[ \left( 1 - \alpha \right) D_{C^+} + \alpha \left( D_{H^+} \right) + D_{A^-} \right]$$
(7.4)

where *T* is the absolute temperature, *F* is Faraday's constant, and  $\alpha$  a parameter ranging from 0 to 1 according the dissociation of pyrrolidinium cation.

For the sake of comparison, the experimental conductivities  $\Lambda_{cond}$ , as well as  $\Lambda_{RMN}$  for anion, cation, and proton for the ([HPyr][CF<sub>3</sub>CO<sub>2</sub>]+H<sub>2</sub>O) binary system, have been also plotted in the same graph, illustrated in Fig. 7.12 [75]. We can be shown that, at a low composition range (i.e., ww < 50 % w/w), irrespective of the choice of the  $\alpha$  value (e.g.,  $\alpha = 1$  or  $\alpha = 0$ ),  $\Lambda_{cond}$  was found to be similar to the calculated  $\Lambda_{NMR}$  values. In fact, in this case, ions provide the major contribution to diffusion in the solution. However, for a higher composition range (i.e., ww > 50 % w/w), it is not the case since certain discrepancies have been found between the calculated



**Fig. 7.12** Experimental conductivities  $\Lambda_{cond}$ , as well as calculated  $\Lambda_{RMN}$  for anion, cation, and proton for the ([HPyr][CF<sub>3</sub>CO<sub>2</sub>]+H<sub>2</sub>O) binary system as function of mass fraction. Reproduced from [75] with permission from Elsevier

and experimental diffusion values. In other words, for such concentrations, diffusion in solution is certainly driven by the ion pairs, as well as by neutral species, which renders the Nernst equation invalid for the high composition range (i.e., ww > 50 % w/w). The cation self-diffusivity was then decomposed into two contributions, which corresponded to the cation self-diffusivity contributions of the single ion (D<sub>Pyrr+</sub>) and the ion pair (D<sub>PyrrA</sub>), respectively. Apparently, at a low composition range, both corresponding curves are almost similar because the contribution of the Grotthuss is low [95].

## 7.3.2 Structural Properties and Application to Materials Chemistry

#### 7.3.2.1 Self-Assembled Structures in PILs

In recent years, it has been established that many ILs are nanostructured, possessing populations of cations and anions that are ordered on specific length scales [96]. This nanostructure typically occurs due to segregation of the ionic liquid into polar and nonpolar domains. Ionic liquid cations usually consist of an ionic and an alkyl component which, similar to amphiphile self-assembly, drives the segregation.



Fig. 7.13 DRX profiles for the double diamond (Pn3m) symmetry system formed by the monoolein (50.8 wt%) / ethanolammonium formate [ $H_3N(CH_2CH_2OH)$ ][ $HCO_2$ ] system at 25 °C

Meanwhile, self-assembly in ILs and their application to materials chemistry have been emerging as a promising area of research. Although ILs exhibit smaller cohesive energy compared to water [97, 98], the formation of ordered molecular assemblies has been demonstrated for bilayer membranes [60, 99–101] and low-molecular weight ionogels [102]. PILs and water mixtures have been shown to display unique physicochemical properties, which are different from the pure counterparts [103–105]. They relate to the formation of solvent clusters and continuous superstructures [106] in binary aqueous IL mixtures, which vary depending on the component chemical structures of IL, composition of the binary mixtures, and physical conditions, such as temperature.

Several PILs, including ethyl ammonium nitrate, have been found to have intermediate range ordering, consisting of polar and nonpolar domains analogous to those observed in amphiphilic self-assembly processes. Greaves et al. reported an absence of such structure in ethanolammonium formate,  $[H_3N(CH_2CH_2OH)]$  $[HCO_2]$ , and correlated this lack of ordering of the ions as an influential factor in small molecule amphiphile self-assembly [107, 108]. In contrast, highly structured PILs have an increased propensity toward amphiphile solubilization as show in Fig. 7.13. By consequence higher concentrations of amphiphile are required to form self-assembled structures.

Observed changes in the physicochemical and micellar properties of the pyrrolidinium imidazolium or alkylammonium alkylcarboxylates protic ionic liquid surfactants in mixtures with water can be linked to the nature of the cation. Figure 7.14 shows, for example, lamellar patterns bilayer system of diisopropylammonium octanoate in water (50 % w/w). By comparison with classical anionic surfactants having inorganic counterions (Li<sup>+</sup>, Na<sup>+</sup>...), these monomers exhibit a higher ability to aggregate in aqueous solution, demonstrating their potential applicability as a surfactant.



**Fig. 7.14** (a) TEM of  $[NHEt(i-Pr)_2][C_9H_{19}CO_2]$  in water (50 % w/w); bar = 50 nm. (b) The Bragg peaks by SAXS of lamellar patterns bilayer system

#### 7.3.2.2 Application of PILs Structuring Reductive Media to Nanoparticle Synthesis

Understanding of ordered self-assembling phenomena in binary PIL–water systems has been largely lagging behind. The formation of clusters and continuous structures of PIL molecules in aqueous systems and their influence on molecular self-assembly are of pivotal importance not only for fundamental science but also for their wide range of technological applications.

For example, thanks to their "organized" and tunable structure, ILs-based media have already been reported in the literature as predisposed to the synthesis of different nanomaterials [109] including silver, gold, ruthenium, iron, and platinum nanoparticles [110].

Recently, a facile method for the formation of mono-dispersed metal nanoparticles (NPs) at room temperature from  $M^{(III)}Cl_3$  (with M=Au, Ru, Mn, Fe, or V) in different media based on N,N-dimethylformamide (DMF) or water solutions containing a PIL, namely the octylammonium formate and the bis (2-ethyl-hexyl)ammonium formate, was presented [111, 112].

These PILs present redox-active structuring properties that influence their interactions with selected molecular compounds (DMF or water), as well as the shape and the size of formed metal NPs in these solutions. Figure 7.15 shows the different shape and size of gold and Pt NPs obtained in a water–octylammonium formate mixture.

By the same approach employing low-energy sputtering, several groups generated novel electrolytes comprising nanoparticle dispersions within ionic liquids [113]. These studies also afforded the unique opportunity to investigate nanoscale growth mechanisms occurring within the IL. Cyclic voltammetry and electrochemical impedance spectroscopy analyses revealed that when the IL contained a substantial fraction of sub-nanometer-sized particles, the double-layer capacitance was increased

AuCl<sub>3</sub>/water instantly after 10 mn After 15 mn After 20 mn

**Fig. 7.15** Mono-dispersed colorless nanoparticles. (**a**) Gold NPs in aqueous bis(2-ethyl-hexyl) ammonium formate. (**b**) Gold NPs in octylammonium formate (OAF). (**c**) Vanadium NPs in bis(2-ethyl-hexyl)ammonium formate + dimethylformamide. (**d**) Pictures showing the various stages of the gold NPs' formation by adding fresh solution of AuCl<sub>3</sub> dissolved in DMF and bis(2-ethyl-hexyl)ammonium formate + water solution over the time

by close 200 %, concomitant with a bulk electrolyte resistance decrease of 70 % with respect to a gold-free control. These promising results reveal an anomalous capacitance increase and low internal resistance for nanoparticle-in-IL dispersions, suggesting intriguing potential as electrolytes for next-generation Electrical Double-Layer capacitors (EDLCs), fuel cells, and sensors. A very large potential development in the nanomaterial domain is expected in the PIL structured domain.

## 7.3.3 Electrochemical Stability and Metal Protection Against Corrosion in RTMS

Electrolytes for electrochemical devices should resist reduction and oxidation and exhibit a larger electrochemical window. The electrochemical stability of RTMS is generally measured by cyclic voltammetry at room temperature recorded in a three-electrode cell configuration using a platinum, gold, or vitreous carbon electrode as the working electrode, and Ag/AgCl (saturated in solvent) for triethylammonium formate PILs (Fig. 7.16a) or Li for DESs based on lithium salt (Fig. 7.16b) as the reference electrode.

The stability window of PILs ranges from 1.5 to 5.0 V according to the acidity of ammonium cation and the stability of the anion. In general, reversible and small peaks observed in the case of the PILs-based system, as shown in Fig. 7.18, is attributed to the presence of water (>1,000 ppm).



**Fig. 7.16** Electrochemical stability of RTMS measured by cyclic voltammetry. Triethylammonium formate PILs (**a**) and DESs based on lithium salt (**b**)

The cathodic limit observed in an ionic liquid is generally due to the reduction of the ammonium cations [114, 115]. Such a reduction proceeds by the CE mechanism: first, the deprotonation of ammonium cation occurred (Eq. 7.5), followed by the reduction of the proton (Eq. 7.6). For the anodic limit, the ammonium could, in this case, be oxidized in the presence of oxygen.

$$\mathbf{R}_{3}\mathbf{N}\mathbf{H}^{+} \leftrightarrows \mathbf{E}\mathbf{t}_{3}\mathbf{N} + \mathbf{H}^{+} \tag{7.5}$$

$$\mathrm{H}^{+} + \mathrm{le}^{-} \leftrightarrows 1/2\mathrm{H}_{2} \tag{7.6}$$

In oxidation, the anion associated with the PILs is oxidized. In the case of carboxylates, the relatively low potential (1.5 V (vs. Ag/AgCl) mechanism proceeds according to the Kolbe reaction followed by the formation of dimers, whereas the oxidation of the alkyl radical at more anodic potential can be leading to products deriving from the carbocation, named the non-Kolbe reaction. The mechanism is described as follows:

$$\mathbf{R}\mathbf{C}\mathbf{O}\mathbf{O}^{-} - \mathbf{l}\mathbf{e}^{-} \leftrightarrows \mathbf{R}^{-} + \mathbf{C}\mathbf{O}_{2} \tag{7.7}$$

$$2\mathbf{R} \rightleftharpoons \mathbf{R} - \mathbf{R} \tag{7.8}$$

$$\mathbf{R}^{-} - \mathbf{l}\mathbf{e}^{-} \leftrightarrows \mathbf{R}^{+} \leftrightarrows \mathbf{products}$$
 (7.9)

The electrochemical stability window of the Lithium-based DESs on Pt is generally from 4.5 to 5.5 V [41]. The cathodic limit shown by these electrolytes was significantly higher, comparable to that observed for aprotic ionic liquid (see Fig. 7.16b). Furthermore, the anodic limit was comparable to electrolytes containing the X<sup>-</sup>anion for lithium salt LiX as  $[NO_3]$  or  $[N(Tf)_2]$  anions. Considering these results, each DES appears to display an electrochemical stability window (ESW) large enough to be used as an electrolyte for the energy storage systems as described below.



**Fig. 7.17** Cyclic voltammograms of the Al electrode in  $[HN_{222}][N(Tf)_2]$  at 20 °C (**a**) and scan rate: 5 mV s<sup>-1</sup>. SEM images of aluminum current collectors after cycling in Li[N(Tf)<sub>2</sub>]–MAc at x<sub>Li+</sub>=0.20, inset: after cycling in 0.3 M Li[N(Tf)<sub>2</sub>] in PC. Reproduced from [41] with permission from the PCCP Owner Societies

The native passive  $Al_2O_3$  layer existing on the metal surface provides protection against corrosion. It is well known that, depending on the nature on the electrolyte anions, this passive layer can be broken down leading to aluminum corrosion at a high potential. The [N(Tf)<sub>2</sub>] anion shows a corrosive effect on the aluminum collector, corroded around 3.8 V vs. Li/Li<sup>+</sup> when the Li[N(Tf)<sub>2</sub>] electrolyte was contained in lithiumion batteries (LIBs) or electrochemical double-layer capacitor (EDLC) systems [116–119] with an aluminum-coated positive electrode. Therefore, it is very important before any use of RTMS as an electrolyte to control its effect on aluminum corrosion.

Aluminum's corrosive behavior was evaluated in several PILs, for example,  $[N(Tf)_2]^-$ -based PILs [120]. Figure 7.17 shows cyclic voltammograms of an aluminum electrode in  $[HN_{222}][N(Tf)_2]$  from the first to the fourth cycle [120]. The first cycle illustrates a hysteresis loop initiated at about 0.25 V vs. Ag with a large irreversible current peak (1 mA cm<sup>-2</sup>) at about 1.1 V vs. Ag. For the second cycle, and the following, the initiation potential of the hysteresis loop was significantly shifted to the more anodic side (1.25 V vs. Ag), while the current sharply decreased (0.1 mA cm<sup>-2</sup>). Al passivation could be achieved in this PIL electrolyte from the second cyclic voltammogram.

Figure 7.17b shows SEM images of an aluminum current collector of the LFP electrode cycled in a cell containing DESs based on  $\text{Li}[N(\text{Tf})_2]$  taken at the end of the cycling [41]. As shown, the current collector displayed a quite uniform morphology, and only some residues were visible. In comparison, the inset presents the collector cycled in 0.3 M  $\text{Li}[N(\text{Tf})_2]$  in PC, displaying holes of different sizes and depth distributed all over the surface of the sample.

These holes were generated from the strong corrosion process occurring during the cycling in electrolytes containing the  $[N(Tf)_2]$  anion, which is able to solubilize  $Al[N(Tf)_2]_3$  formed at the surface of the collector [117], as illustrated in Fig. 7.18. From these observations, it appears evident that the  $Li[N(Tf)_2]$  DESs-based electrolyte displays the ability to prevent aluminum corrosion and can be considered as a suitable electrolyte.



**Fig. 7.18** Corrosion mechanism in organic solvent based on  $Li[N(Tf)_2]$  as electrolytes. The dissolution and desorption of Al-complex formed not occurring in RTMS

## 7.4 Application of H-Donor RTMS as Electrolytes in Energy Storage

Accordingly, investments for the exploitation of renewable energy resources are increasing worldwide, with particular attention to wind and solar power energy, which are the most mature technologies. The intermittence of these resources requires high-efficiency energy storage systems. Electrochemical systems, such as batteries and supercapacitors that can efficiently store and deliver energy on demand in stand-alone power plants, as well as provide power quality and load leveling of the electrical grid in integrated systems, play a crucial role in this field. Indeed, the advantage of using electrochemical storage systems has been demonstrated for both wind and photovoltaic technologies [121, 122]. The efficacy of batteries in integrated systems is directly related to their content in energy efficiency and their lifetime. Indeed, in virtue of their high value of energy efficiency, lithium batteries are expected to provide an energy return factor higher than that assured by conventional batteries, e.g., lead-acid batteries [123-127]. Supercapacitors have attracted increasing interest because of their high-power storage capability, which is highly desirable for applications in electric vehicles (EVs) and hybrid electric vehicles (HEVs) [128–133]. Supercapacitors can be coupled with fuel cells or batteries to deliver the high power needed during acceleration and to recover energy during braking. In this section, we describe the latest developments regarding the use of H-Bond donor RTMS application in supercapacitors and batteries focusing on the use of lithium-based DESs and PILs.

## 7.4.1 Use of H-Bond Donor for Supercapacitors: Advantage and Limitations

Electrical double-layer capacitors are well known for their good power performance and extreme stability in terms of life cycle. Activated carbons (ACs) are the most commonly used electrode materials for EDLC applications because of their relatively low cost and large surface area compared to other carbon-based materials. Another factor that influences supercapacitor properties is the selected electrolyte.

Currently, aqueous solutions have been mostly utilized [134]. However, the drawback of the aqueous electrolyte-based supercapacitor is also obvious mainly

due to the narrow cell voltage ( $\Delta E \approx 1$  V) and low energy  $E = \frac{1}{2}C_{sp}\Delta V^2$  ( $C_{sp}$  is the

specific capacitance and  $\Delta V$  is the operating voltage). Organic electrolytes and AILs have a higher breakdown voltage, but have greater resistance. The advantages of a higher cell voltage are therefore usually countered by the greater resistance. Another factor limiting the use of aqueous media is temperature. Today, manufacturers typically specify an operational temperature range from -40 to 70 °C for capacitors based on ACN or PC. In this context, PILs have naturally attracted a great deal of attention due to their suitable properties.

#### 7.4.1.1 Application of PILs as Electrolytes for Supercapacitors

PIL-based electrolytes exhibit intermediate conductivity compared to conventional electrolytes (especially in ACN) and AILs, but they might have interesting conductivity at low temperatures [135]. Additionally, some works have indicated that in PIL-based electrolytes, ruthenium oxide [136], as well as activated carbon [137], might exhibit pseudo-capacitance due to the labile proton in PILs, which participates on the fast redox reactions at the electrode/electrolyte interface. Taking into account these properties, PILs could be interesting electrolyte candidates in order to use them as electrolytes for supercapacitors.

Cyclic voltammograms and galvanostatic curves obtained using activated carbon in neat PILs as well as in their mixture (Fig. 7.19) demonstrate that PIL-based



**Fig. 7.19** (a) Cyclic voltammograms for three-electrode cell with activated carbon in neat  $[HN_{222}]$  [N(Tf)<sub>2</sub>] with Ag wire as a reference electrode at a scan rate of  $\nu = 5$  mV s<sup>-1</sup>. Reproduced from [120] with permission from the PCCP Owner Societies; and (b) In [HP<sub>444</sub>][BF<sub>4</sub>] with (x<sub>CH3CN</sub>=0.86) at a scan rate of  $\nu = 100$  mV s<sup>-1</sup>. Reproduced from [139] with permission from Elsevier

supercapacitors might exhibit good cycling stability (over 30,000 cycles) [138] and an interesting performance in a rather broad range of temperatures.

The mixture solvent- $[HN_{111}][N(Tf)_2]$  (solvent=PC,  $\gamma$ -BL, or ACN) can be successfully used at temperatures as low as -30 °C and -40 °C, while the solvent-free supercapacitor containing the PIL  $[HN_{222}][N(Tf)_2]$  is able to feature stable performance in the temperature range from 10 to 60 °C. At the same time, when PILs with low-water content are used in combination with AC containing few surface groups, such supercapacitors do not exhibit any evident pseudo-capacitive behavior in comparison with phosphonium-based PILs, as shown in Fig. 7.19b. Taking into account these results, PIL and activated carbon-based supercapacitors appear as stable devices, but, due to their lower operative voltages in comparison to conventional organic solvents, their energy appears lower than that possible using organic electrolytes or aprotic ILs.

#### 7.4.1.2 Parameters Influencing the Storage Mechanism According to PILs

Several parameters can govern the storage mechanism in the EDLC for PILs according to the electrolytes/material couple. First, a reduction of the ammonium cation in the presence of an activated carbon electrode is presumably linked to electronic transfer kinetics. Reactions in which electron and proton transfer is performed have been described either by two distinct steps, Electron Proton Transfer or Proton Electron Transfer (EPT or PET), or in the same concerted step, Concerted Proton Electron Transfer (CPET) [140–142]. Contrary to simple proton or electron transfer, CPET is more complicated and the coupling at the activated carbon /molecule (cation) interface influences the process both thermodynamically and kinetically.

In a concerted mechanism (Fig. 7.20), the electrons and protons are transferred in the same step; this mechanism is defined by only one transition state,



Fig. 7.20 Concerted mechanism of electrons and protons transferred to the activated carbon linked to the Cosmo volume and (Pyrrolidinium (HPyr) or diisopropylethylammonium  $[NHEt(i-Pr)_2]$  cation polarizability in PILs

and consequently, it avoids high-energy reaction intermediates. However, microscopically, the kinetic description is not the same for both processes. The electron transfer is governed by both intramolecular cation and also solvent reorganization. Consequently, potential energies of reactants (here, cations) and products (here, hydrogen and amine) can be described by the internal deformations (variation of both bond lengths and angles) and external structuration of systems (solvent reorganization) as illustrated in Fig. 7.20.

Two other parameters influence the electrolyte behavior in the EDLC system: the van der Waals volume of ions, which must adapt itself to the material porosity, and their polarizability (Fig. 7.22). These two parameters are correlated, e.g., the volume of the [NHEt(i-Pr)<sub>2</sub>] cation (207.37 Å<sup>3</sup>) is twice that of the pyrrolidinium cation (106.01 Å<sup>3</sup>), but at the same time, [NHEt(i-Pr)<sub>2</sub>]<sup>+</sup> displays higher polarizability (Fig. 7.22), which allows better distortion in order to adapt its size to the carbon pore size [143]. Thus, [NHEt(i-Pr)<sub>2</sub>]<sup>+</sup> counterbalances its larger volume by its higher polarizability. This believable hypothesis linking reduction stability limit to the geometry and the volume of cations could explain the different behavior observed in Fig. 7.21.

#### 7.4.1.3 Specific Behavior of DESs as Electrolytes for Supercapacitors

This "superionicity" behavior of DESs based on N-methylacetamide and lithium ion used as electrolytes for EDLC at an activated carbon explains their good cycling ability (Fig. 7.22a), observed by cyclic voltammetry and galvanostic charge–discharge methods, with high up to 380 F g<sup>-1</sup> at elevated voltage and temperature, i.e.,  $\Delta E$ =2.8 V and 80 °C for the Li[N(Tf)<sub>2</sub>]–MAc mixture at, for example, x<sub>Li</sub>=0.25 (Fig. 7.22b) [144].

The electrochemical resistances ESR (equivalent series resistance) and EDR (equivalent diffusion resistance) evaluated using electrochemical impedance spectroscopy (EIS) measurements clearly demonstrate that according to the nature of the anion, the mechanism of ion adsorption can be described by pure double-layer adsorption at the specific surface, or by the insertion of desolvated ions into the



**Fig. 7.21** Three-electrode cyclic voltammograms of a PVDF-AC electrode in  $[NHEt(i-Pr)_2]$  $[N(Tf)_2]$  (**a**) and  $[HPyr][N(Tf)_2]$  (**b**), with Ag wire as pseudo-reference, at 5 mV s<sup>-1</sup>, at 30 °C



**Fig. 7.22** (a) Three-electrode cyclic voltammograms of activated carbon in  $\text{Li}[N(\text{Tf})_2] - \text{MAc}$  ( $x_{\text{Li}+}=0.25$ ) at scan rate 5 mV s<sup>-1</sup>. (b) Specific capacitance calculated according to

$$\left(C_{sp} = \frac{2\int idt}{\Delta E.m}; i \text{ is applied current}, \Delta E \text{ is the tension voltage and m is the active mass of } Ac$$

for  $\Delta E$  = 2.6 V. Reprinted with permission from [142] with permission from the American Chemical Society

ultramicropores of the activated carbon material. Insertion of lithium ions is observed by the presence of two reversible peaks in the CVs when the operating voltage exceeds 2 V (Fig. 7.22) [144, 145]. The decreasing capacitance of symmetric AC/AC systems despite good efficiency can be interpreted by the imbalanced mass of carbon electrodes caused by important lithium insertion at the negative electrode and by saturation of the positive electrode by anions; both mechanisms prevent, in fact, the system being operational.

Considering the promising properties, especially their cost, hazard, and the risks of these DESs series, their introduction as safer electrolytes could represent an important challenge for the realization of environmentally friendly EDLCs operating at high temperatures. The study of the original ions' adsorption mechanism of desolvated lithium ions provides an interesting opportunity for fundamental studies even beyond the applicative interest of DESs as electrolytes for supercapacitors.

## 7.4.2 Application of the PILs for Lithium Ion Batteries

"Due to the high value of the energy content, lithium ion batteries have triggered the growth of the market of popular devices, such as mobile phones, laptop computers, MP3s, and others. Indeed, lithium ion batteries are today produced in billions of units per year [146, 147].

At first sight, the electrochemical process which drives the lithium ion battery appears quite simple, apparently consisting of the reversible exchange of lithium ions
between two electrodes. However, in practice, the operation of this battery requires the mastery of key side processes. Accordingly, worldwide research and development efforts are directed toward the replacement of the present battery components with materials having higher performance in terms of energy, power, cost, reliability, lifetime, and safety.

Approaches to reach this goal are focused along two main lines:

- Replacement of graphite and of lithium cobalt oxide with alternative, higher capacity, lower cost anode and cathode materials;
- Replacement of the organic carbonate liquid electrolyte solutions with safer and more reliable electrolyte systems.

Among the electrolytes proposed so far, those based on aprotic ILs appear to be very promising since their introduction can improve both the safety as well as the operative temperature range of the use of LIBs [148–150]. Nevertheless, the performance of IL-based LIBs still needs to be improved in order to be fully competitive with that of the conventional electrolytes. Moreover, the cost of ILs might also represent an obstacle for the introduction of these electrolytes in LIBs.

#### 7.4.2.1 Use of PILs as Electrolytes in Li-Ion Batteries

Recently, the Anouti and Balducci groups reported for the first time the use of PILs as electrolytes for LIBs [151]. The investigated electrolytes consisted of a solution containing PIL  $[HN_{222}][N(Tf)_2]$  and the lithium salt Li $[N(Tf)_2]$  (1 M). Considering all beneficial properties of PILs, easy to synthesize and cheaper than aprotic liquids, conductivity comparable to that of aprotic ILs, and electrochemical stability window large enough to allow the realization of LIBs containing LFP as cathode and Lithium Titanium Oxide (Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> (LTO)) as anode, the PIL-based electrolyte allows the realization of devices able to deliver capacities comparable with those possible with the aprotic IL-based electrolyte as shown in Fig. 7.23 by constant-current charge–discharge behavior [151].



Fig. 7.23 (a) Charge–discharge voltage profiles of an LFP cathode and LTO anode and (b) discharge capacity of LIBs containing 1 M Li[N(Tf)<sub>2</sub>] in [HN<sub>222</sub>][N(Tf)<sub>2</sub>] at 0.1 C, 1 C, and 10 °C

The performance of PILs for LIBs certainly needs to be improved. Nevertheless, the results of this work clearly show that PILs can be successfully introduced in LIBs. Considering the beneficial properties (and the cost) of these ILs, such introduction could represent an important contribution for the realization of safer and environmentally friendly LIBs.

#### 7.4.2.2 Use of DESs as Electrolytes in Li-Ion Batteries

Considering that the presence of labile proton does not prevent the use of PIL-based electrolytes in lithium-ion batteries, it was therefore possible to imagine the possibility of using more broadly the "H-bond Donors" as electrolytes replacing those based on alkylcarbonates. The successful introduction of DESs-based lithium salts is an illustration of this new way of research into electrolytes replacing conventional organic solvents.

Recently, Anouti et al. demonstrated that these electrolytes have good compatibility with both electrodes ( $Li_4Ti_5O_{12}$  and  $LiFePO_4$ ) [40, 41]. Tested cells show good electrochemical performances in term of specific capacitance, rate, and cycling ability, indicating that the  $Li[N(Tf)_2]/MAc$  DES can be a promising electrolyte for EDLCs and LiBs applications, especially for those requiring high safety and stability.

As shown in Fig. 7.24, the LiFePO<sub>4</sub> electrode displays the typical voltage profile, the plateau corresponding to the lithium insertion–extraction at around 3.45 V vs. Li/ Li<sup>+</sup>; the difference between the charge and the discharge voltage plateau is exceptionally small. Obviously, the presence of water affects the specific capacity of the electrode: the lower the water content, the higher the capacity. Nevertheless, the presence of different amounts of water does not seem to have a significant effect on the voltage plateau. This is surprising because in general electrolytes for batteries do not work in



**Fig. 7.24** (a) Constant-current charge–discharge profiles of LFP electrode in LiX–NMAc.  $X = NO_3$ ,  $[N(Tf)_2]$  (TFSI), PF<sub>6</sub>; NMAc is the N-methylacetamide. (b) Comparative discharge capacity and efficiency as obtained during tests carried out at a 1 C rate and 60 °C. Reproduced from [41] with permission from the PCCP Owner Societies

the presence of traces of water exceeding 20 ppm. Here, the amount of water is evaluated at 500 ppm, which does not prevent the function of electrode LFP. These observations are considered in light of free residual water or water attached by H-bonding. In DESs and PILs, the presence of a labile proton does not necessarily imply a hydrogen potential with the standard reaction of free water molecules.

# 7.5 Conclusion

This chapter presents an overview of PILs and DESs and discusses the possibility of employing them as electrolytes for renewable energy storage as lithium ion batteries and supercapacitors and for utility-scale load leveling applications. Use of ILs as electrolytes for energy storage application is provided, building on the feasibility of replacing ILs with DESs in the near future, based on recent publications on the topic. H-Bond donor RTMS may offer significant advantages over their generally more volatile organic molecular solvent counterparts. This kind of ionic liquid possesses several inherent advantages, such as cheap raw materials, simple preparation procedures, and better biocompatibility. For example, PIL properties, prepared by the proton-transfer reaction between the base and proton-donor acid, are easy to tune for target electrochemical application because of the diversity of bases and proton donors that are available. PILs often have high intrinsic conductivities-similar to aqueous solvents with added supporting electrolytes—resulting in simplified experimental arrangements. Many RTMS with selected ions have wide electrochemical windows (dictated by the high stability of the cation and anion) without requiring the presence of a labile proton.

PILs and DESs also have reductive structuring properties contributing to their ability to solubilize a wide range of polar and nonpolar species as precursors of metallic nanoparticles. All the above advantages, together with the competitive performance, make H-bond RTMS a strong candidate for future electrolyte development for energy storage systems. The RTMS-based electrolyte allows the realization of devices, lithium ion batteries, redox flow, and supercapacitors to deliver capacities comparable with those possible with organic solvent- or aprotic IL-based electrolytes. Especially, DESs show unusual solvent properties for metal oxide, inorganic salts, and solid organic compounds, which could make these binary eutectic mixtures the new medium for electrochemical application in the future. However, drawbacks include the high viscosity of DESs, resulting in small diffusion coefficients at ambient temperatures, and the hydrophilic properties of PILs, which limit their generalization.

The performance of RTMS and their purification certainly needs to be improved and the investigation of their potentialities should be continued. Nevertheless, the newest aspects addressed by the research community clearly conclude that RTMS can be successfully introduced in the energy storage application. Considering the beneficial properties (and the cost) of these media, such introduction could represent an important contribution for the realization of safer and environmentally friendly systems. 7 Room-Temperature Molten Salts...

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# Chapter 8 Task-Specific Ionic Liquids for Electrochemical Applications

Hua Zhao

# 8.1 Introduction

Ionic liquids (ILs) have been widely examined as solvents, additives, or catalysts in a variety of applications including organic catalysis [1–5], inorganic and materials synthesis [6], biocatalysis [7–12], electrochemistry [13], pharmaceutical chemistry [14], polymerization [15, 16], and engineering fluids [17–19]. The physicochemical properties of ILs are tunable through a careful selection of a variety of different cations and anions and a rational combination of ion pairs. More interestingly, cations and/or anions can be further functionalized to form so-called task-specific ionic liquids (TSILs). The notion of TSILs carrying specific functionality tailored for particular applications has proven visionary, and a variety of different functional groups have been grafted onto ILs [20–22]. In particular, there is an exponential growth in constructing new TSILs as electrolytes for electrochemical applications. This chapter focuses on a critical discussion of some major types of TSILs and their electrochemical properties and applications.

# 8.2 Ether/Thioether- and Hydroxyl/Thiol-Functionalized ILs

# 8.2.1 General Physical Properties

Our recent review has captured some key physical properties of ether- and alcoholfunctionalized ILs [22]. The inclusion of alkyloxy or alkyloxyalkyl groups in ILs often lowers the melting points ( $T_m$ ) [23–26]. Additionally, the lowering of the

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glass transition point,  $T_g$ , is observed in ILs with no  $T_m$  [23, 27, 28]. The likely explanation for the observed  $T_m$  and  $T_g$  depression due to the ether group incorporation is that the high chain flexibility predominates over the high polarity of the ether group [23]. The complete disappearance of crystallinity and the decrease in  $T_m$  of ILs are caused by both the higher rotational freedom of ether chain and the reduced lattice energy of ILs.

The inclusion of ether groups in IL cations often results in a reduction in viscosity. Molecular dynamic simulations indicate that the low viscosity stems from the less effective assembly between more flexible ether chains, which leads to less aggregation/interaction of the chains of neighboring cations rather than any change on ionic pairing [29]. Studies by Raman-induced Kerr spectroscopy [30, 31] show that the larger ionic volume of ether substitution induces a weaker interionic interaction; however, the ether group itself causes a stronger interionic interaction but is of more flexible nature having a faster reorientation than the alkyl group. Based on the density data, the Lee group [32] suggested that the highly flexible alkoxy chains increase the total free volume, which boosts the transport of adjacent molecules and leads to a lower viscosity. On the other hand, the grafting of hydroxyl groups to the cation typically increases the IL viscosity [33]. The hydroxyl groups likely contribute to an intermolecular hydrogen-bond network leading to a higher viscosity [34–36].

Short-chain-ether-functionalized ILs are usually less thermally stable than their corresponding alkyl-substituted analogues [23, 24, 27, 37, 38], most likely due to the weakened cation-anion electrostatic interaction freeing the anions to act as nucleophiles. However, imidazolium ILs containing very long ether chain (7–16 oxygen atoms) have shown a higher thermal stability than alkyl-substituted salts, e.g., [mPEG16-Me-Im]I (containing 16 oxygen atoms) has a higher decomposition temperature ( $T_d$ ) of 284 °C as compared to that of [C<sub>2</sub>mim]I (264 °C) [39]. This was explained by the enhanced intermolecular interactions in the ILs carrying a long ether chain: despite the reduction in electrostatic interaction between the cation and anion due to the shielding of ether chain, strong van der Waals interactions are expected to exist between the polar ether chains. Additionally, due to the wrapping of long ether chain around the cation [40], the nucleophilic attack on the imidazo-lium ring leading to degradation may be hindered.

A higher solvent polarity is generally observed for ether-/hydroxyl-functionalized imidazolium ILs than those of non-functionalized ILs based on solvatochromic measurements [33, 41, 42] and dielectric constants [43]. The addition of hydroxyl or alkoxy group to the cation remarkably increases the hydrophilicity of ILs [44–46]. Imidazolium ILs form an extended hydrogen-bonded network in both solid and liquid states, with a main contributor being the C-2 hydrogen of the imidazolium ring [47, 48]. The strength of these H-bonds is more dependent on the type of anions than the oxygen functionalization of side chain [27] even though multiple oxygen atoms in the IL side chain can serve as H-bond acceptors for solute molecules.

#### 8.2.2 Electrochemical Properties

The ionic conductivity of an IL is mainly controlled by its viscosity (known as the Walden plot), density, formula weight, and size of the cation and anion [49]. Due to the lower viscosities of ether-functionalized ILs, these liquids tend to have higher specific conductivities at 25 °C than alkyl-substituted ILs, such as [CH<sub>3</sub>OCH<sub>2</sub>CH<sub>2</sub>-Et<sub>2</sub>-MeN][N(Tf)<sub>2</sub>] (2.6 mS/cm) vs. [Bu-Et<sub>2</sub>-MeN][N(Tf)<sub>2</sub>] (1.6 mS/cm) and  $[CH_3OCH_2CH_2-Et_2-MeN][CF_3BF_3]$  (3.0 mS/cm) vs.  $[Bu-Et_2-MeN][CF_3BF_3]$ (2.1 mS/cm) [23]. Another excellent example was illustrated by Donato et al. [50] as: [Me(OCH<sub>2</sub>CH<sub>2</sub>)<sub>3</sub>-mim][BF<sub>4</sub>] vs. [C<sub>10</sub>mim][BF<sub>4</sub>] (0.874 mS/cm vs. 0.337 mS/cm at 25 °C), and [MeOCH<sub>2</sub>CH<sub>2</sub>-mim][BF<sub>4</sub>] vs. [C<sub>4</sub>mim][BF<sub>4</sub>] (0.950 mS/cm vs. 0.00124 mS/cm at 25 °C). The same conductivity increase trend was observed for ether-functionalized ILs based on imidazolium cations [38], pyrrolidinium, piperidinium, oxazolidinium, or morpholinium cations [24], phosphonium and ammonium cations [25, 51, 52], as well as guanidinium cations [53, 54]. Belhocine et al. [55] prepared a series of seven-member ring azepanium-based ILs (Scheme 8.1) and found the incorporation of alkoxyalkyl group results in a reduction in viscosities and an increase in conductivities. In addition, cyclic voltammetry indicated very wide electrochemical windows (5.0-6.5 V) of azepanium ILs, implying their high potential as electrolytes. Although [C<sub>2</sub>mim]I showed a high ionic conductivity at temperatures above 50 °C, long ether chain-grafted ILs exhibited an even higher conductivity at room temperature than that of [C<sub>2</sub>mim]I, which is attributed to the lower viscosity and better solvation of I<sup>-</sup> anions in ether-derived ILs. In addition, these ether-functionalized ILs displayed higher resistance against cathodic reduction than alkyl-substituted ILs due to the protective wrapping of long ether side chain around the cation [39]. Therefore, these ether-functionalized imidazolium iodides are potentially ideal electrolytes for electrochemical devices such as dyesensitized solar cells (DSSCs). However, when introducing two, three, or four ether groups to the quaternary ammonium salts, lower conductivities (and similar/higher viscosities) were observed over ammonium salts carrying no or one ether group [56,57]. But if the incorporation of more than one alkoxy group to the IL cation leads to a viscosity reduction, an increase in conductivity is expected [52]. The reasonable explanation to this could be the stronger van der Waals interactions for larger



 $\label{eq:result} \begin{array}{l} \mathsf{R} = \mathsf{butyl} \\ \mathsf{hexyl} \\ \mathsf{CH}_3\mathsf{OCH}_2\mathsf{CH}_2 \\ \mathsf{CH}_3\mathsf{OCH}_2\mathsf{CH}_2\mathsf{OCH}_2\mathsf{CH}_2 \\ \mathsf{X} = \mathsf{CF}_3\mathsf{COO} \\ \mathsf{CF}_3\mathsf{SO}_3 \\ \mathsf{N}(\mathsf{Tf})_2 \end{array}$ 

Scheme 8.1 Azepanium ILs

cations and lower cation symmetry. On the other hand, the ether functionalization and a lower viscosity do not always lead to higher conductivity. For example, methoxymethyl ethyl dimethylammonium tetrafluoroborate ([CH<sub>3</sub>OCH<sub>2</sub>-Et-Me<sub>2</sub>N] [BF<sub>4</sub>]) is considered a poor ion conductor based on the Walden plot because this IL has an order of magnitude lower conductivity than ideal [58].

The electrochemical stability is also affected by the incorporation of ether groups. Grafting one or multiple short-chain ether groups in quaternary ammonium, cyclic quaternary ammonium, or sulfonium ILs generally leads to reduced electrochemical stability, but with the electrochemical windows still being sufficiently high (usually >4.0 V) for practical uses as electrolytes [23–26, 28, 51, 57, 59]. For example,  $[Me(OCH_2CH_2)_3-mim][BF_4]$  has a smaller electrochemical window than  $[C_{10}mim]$ [BF<sub>4</sub>] (1.23 V vs. 2.00 V at 25 °C); [MeOCH<sub>2</sub>CH<sub>2</sub>-mim][BF<sub>4</sub>] also has a smaller electrochemical window than  $[C_4 mim][BF_4]$  (1.01 V vs. 1.66 V at 25 °C) [50]. Chen et al. [52] argued that the incorporation of a second alkoxy group to the quaternary ammonium cation caused no negative impact on the electrochemical stability of the resulting ILs. The electrochemical potential windows of quaternary ammonium salts tend to be wider than that of the imidazolium type [51]. The electrochemical stability of guanidinium ILs was not affected greatly by the incorporation of ether groups [53, 54]. Liao et al. [60] observed that the grafting of an ether group (-CH<sub>2</sub>OCH<sub>2</sub>CH<sub>2</sub>CH<sub>2</sub>CH<sub>3</sub>) at the C-2 position of 1-propyl-3-methylimidazolium could improve its reduction stability and achieve a very low solid electrolyte interfacial resistance. Furthermore, Jin et al. [61] synthesized 26 ether-functionalized trialkylimidazolium ILs at the C-2 position carrying  $[N(Tf)_2]^-$  anions and found most of them have viscosities lower than 90 mPa s at 25 °C, conductivities as high as 3.02 mS/cm, a better thermal stability than ILs with alkoxy substituents at the Nposition, as well as wide electrochemical windows (>4.2 V). Chai et al. [62] prepared a series of ether-functionalized trialkylimidazolium ILs (methyl or ethyl group at the C-2 position) carrying  $[N(Tf)_2]^-$  anions and reported that 26 ILs have viscosities lower than 100 mPa s (with the lowest value being 54.4 mPa s) at room temperature and these ILs have wide electrochemical windows greater than 4.3 V. Interestingly, when studying the effect of water in two ether-functionalized imidazolium ILs on cyclic voltammetry measurements using a platinum electrode, Migliorini et al. [63] observed diminished cathodic currents in [Me(OCH<sub>2</sub>CH<sub>2</sub>)<sub>3-</sub> mim][CH<sub>3</sub>SO<sub>3</sub>] with as little as 0.19 mM of water, and extremely reduced charge transfer processes (for both cathodic and anodic) in [MeOCH<sub>2</sub>CH<sub>2</sub>-mim][CH<sub>3</sub>SO<sub>3</sub>] containing 0.19-1.1 mM water. It was suspected that a new species was produced between imidazolium ILs and water, which blocked the active sites of the platinum electrocatalyst. Despite its unknown identity, this species was speculated to be formed by the hydrolysis of the imidazolium cation with the release of protons. Measurements of pH confirmed the increase of proton concentration in these ILs with the addition of water. Liu et al. [64] prepared a number of ether-functionalized ILs based on ammonium cations and carborane anion [nido-7,8-C<sub>2</sub>B<sub>9</sub>H<sub>12</sub>]<sup>-</sup> and found these ILs have low conductivities (the highest value being 233 µS/cm) due to high viscosity, and low electrochemical stability due to relatively high reactivity of the anion at the anode at voltages greater than 1 V. Lang and Kohl [65] suggested that the oxygen position in ether-functionalized ILs also influences the electrochemical

stability, for example, [(EtOMe)EtMe<sub>2</sub>N]Cl has a much lower reductive stability (1 mA/cm<sup>2</sup> at -0.6 V vs. Ag/AgCl) than [(MeOEt)EtMe<sub>2</sub>N]Cl (-1.78 V).

Yeon et al. [66] reported that some hydroxyl-functionalized imidazolium and morpholinium ILs (paired with  $[BF_4]^-$ ,  $[PF_6]^-$ , or  $[N(Tf)_2]^-$ ) also have some superb electrochemical properties:  $[HOCH_2CH_2-mim]^+$  type ILs have wide electrochemical windows in the range of 5.4–6.4 V and ionic conductivities ranging from 2.1 to 4.6 mS/cm at 25 °C; hydroxyl-functionalized morpholinium ILs have large electrochemical windows (5.2–6.2 V) as well but much poorer conductivities (0.00066– 0.087 mS/cm at 25 °C) due to the high viscosities of these liquids. Pinkert et al. [34] reported that hydroxyl-containing protic ammonium ILs of acetate or formate have conductivity values ranging from  $4.8 \times 10^{-4}$  to 2.3 S/m at 5–75 °C, which suggests that their Walden products (molar conductivity×viscosity) are comparable to aprotic ILs. Interestingly, Wu et al. [36] indicated that hydroxyl-functionalized pyrrolidinium and piperidinium ILs [with  $[N(Tf)_2]^-$  as anions] exhibit wider potential windows than those of corresponding ether-functionalized ILs.

## 8.2.3 Electrochemical Applications

In the early 1980s, ether-functionalized ILs were synthesized and investigated as alternative ambient-temperature electrolytes, such as methoxyethyl ethyl dimethylammonium tetrafluoroborate ([CH<sub>3</sub>OCH<sub>2</sub>CH<sub>2</sub>-Et-Me<sub>2</sub>N][BF<sub>4</sub>],  $T_m = 13$  °C and  $T_{\rm g}$ =-98 °C) [67], and methoxymethyl ethyl dimethylammonium tetrafluoroborate  $([CH_3OCH_2-Et-Me_2N][BF_4], T_m = -16 \ ^{\circ}C \text{ and } T_g = -115 \ ^{\circ}C) [68].$  In the 1990s, much attention was focused on the incorporation of cationic or anionic units on PEGs to produce the liquid state of the ion conductive polymers (cation-tethered PEG, aniontethered PEG, or their mixtures), and many of these studies have been reviewed elsewhere [13, 69]. To demonstrate this concept, the Ohno group [70, 71] attached sulfonamide, ethylimidazolium, or sulfonate groups to the ends of PEG oligomers (MW ranging from 150 to 2,000) resulting in viscous liquids (Scheme 8.2). However, their mixtures exhibited drastically decreased  $T_{g}$  and increased ionic conductivity. For example, for PEG-150 with sulfonamide groups,  $T_{\rm g}$  decreased from 3.2 to -61.6 °C and its ionic conductivity increased about 105 times to 0.0612 mS/cm at 50 °C after mixing with PEG-150 with appended ethylimidazolium groups. Similarly, Dickinson et al. [72] described the preparation of viscous molten salts containing either polyether-tailed 2-sulfobenzoate or polyether-tailed triethylammonium as counterions of ruthenium hexamine, metal trisbipyridines, metal trisphenanthrolines, and ionic forms of aluminum quinolate, anthraquinone, phthalocyanine, and porphyrins and measured their ionic conductivities and cyclic voltammetry property.

The most common application of oxygen-functionalized ILs is as *electrolytes for lithium batteries* due to their low viscosities, high conductivities, and reasonably high electrochemical stability [53, 56, 57, 73, 74]. The Quartarone group [75] prepared composite electrolytes based on PVdF-HFP [poly(vinylidene fluoride-co-hexafluoropropene)] gelled with a 0.41 mol/kg solution of Li[N(Tf)<sub>2</sub>] in *N*-methoxyethyl-*N*-methylpyrrolidinium bis(trifluoromethanesulfonyl)imide; when





using a mesoporous silica as the filler (vs. HiSil<sup>TM</sup>-based membrane), a higher lithium transference number, a more stable electrochemical interface, and better cycling performances were observed. Consequently, the Li/LiFePO4 cells with this composite film showed satisfactory charge/discharge capacity, discharge efficiency close to unity, as well as low capacity losses at medium C-rates for 180 cycles. Alternatively, the Gerbaldi group [76] revealed a different approach to prepare new electrolyte membranes for Li-based cells: in situ single-step free radical photo-polymerization of dimethacrylic oligomers with up to 60 wt% *N*-methoxyethyl-*N*-methylpyrrolidinium bis(trifluoromethanesulfonyl)imide. This method combines the advantages of polymer electrolytes swollen by conventional organic liquid electrolytes with the non-flammability, high thermal, and electrochemical stability properties of ILs. Accordingly, a satisfactory ionic conductivity (0.1-1 mS/cm) and electrochemical properties are obtained over a wide temperature range. They further studied the polymer electrolyte membranes in lab-scale cells with LiFePO<sub>4</sub> as the cathode and Li metal as the anode, resulting in good charge/discharge capacities, Coulombic efficiency close to unity, and low capacity loss at medium C-rates. Han et al. [77] synthesized eight ammonium-based ILs carrying multiple ethoxyethyl groups and observed these ILs have low viscosities (79-135 mPa s at 25 °C) and high conductivities (1.0-2.8 mS/cm at 25 °C). In addition, these ILs could dissolve a high amount of lithium salt (>1.60 mol/kg), and the resulting binary electrolytes display a Li<sup>+</sup> ion transference number  $(t_{1i})$  of 0.6–0.7. These functionalized ILs are also electrochemically stable (electrochemical windows ranging 5.42-5.73 V), affording the Li deposition/stripping at room temperature. These favorable properties indicate the high potential of these ILs as electrolytes for Li (or Li-ion) batteries. Chai et al.

[62, 78] synthesized several ether-functionalized pyrazolium ILs containing bis(trifluoromethylsulfonyl)imide anions and found these ILs have conductivities in the range of 1.6–3.31 mS/cm at 25 °C and a wide electrochemical window of 4.4– 4.6 V; therefore, these ILs could be used as electrolytes for lithium battery, where a high chemical stability against lithium metal was observed for these electrolytes, and a good capacity and cycle property at the current rate of 0.1 C were obtained for Li/ LiFeO<sub>4</sub> cells constructing with IL electrolytes without additives. Ferrari et al. [79] prepared two ether-functionalized ILs (i.e., [MeOCH<sub>2</sub>CH<sub>2</sub>-mim][N(Tf)<sub>2</sub>] and  $[Me(OCH_2CH_2)_2 - mim][N(Tf)_2]$ ) and found both ILs are thermally stable and have lower viscosities than alkyl-substituted [C4mim][N(Tf)2]; more notably, both ILs have electrochemical stability windows wider than 5 V. When the new ILs containing  $Li[N(Tf)_2]$  were mixed with ethylene carbonate/diethyl carbonate (EC/DEC, 1:1 v/v) as electrolytes in Li/LiFePO<sub>4</sub> cells, the capacity retention higher than 92 % was achieved at C rate lower than 0.2 C. However, in such systems, the electrochemical stability windows were still under 4 V and the cycling behavior of Li cells was not found that N.N-diethyl-N-methyl-Nimproved. Nakamoto et al. [80] (2-methoxyethyl)ammonium bis(trifluoromethanesulfonyl)amide exhibits a high stability against electrochemical oxidation over 4 V vs. Li/Li<sup>+</sup> for battery applications and a high O<sub>2</sub> redox reversibility; therefore, it could be a promising electrolyte for nonaqueous lithium-oxygen (Li-O<sub>2</sub>) batteries.

In addition, ether-functionalized ILs have shown their unique roles as electrolytes in electric double-layer capacitors (EDLCs) and dye-sensitized photoelectrochemical solar cells (DSSCs). EDLCs do not rely on chemical reactions for charging and discharging electricity as do rechargeable batteries, but physically store energy via the electric double layer. Generally, EDLCs have a longer lifetime and higher power density than rechargeable batteries. In addition to their high performance, EDLCs are environmentally benign devices because heavy metal materials are not required. The purpose of using ILs in EDLCs is to further improve their energy density and high-temperature stability. Sato et al. [81] noticed that an ether-grafted IL, [CH<sub>3</sub>OCH<sub>2</sub>CH<sub>2</sub>-Me-Et<sub>2</sub>N][BF<sub>4</sub>], has a wide potential window (6.0 V) and a high ionic conductivity (4.8 mS cm<sup>-1</sup> at 25 °C). Subsequently, an EDLC was constructed by a pair of activated carbon electrodes with this IL as the electrolyte. At a working voltage of ~2.5 V, the EDLC exhibited a higher capacity above room temperature and a better charge-discharge cycle durability at 100 °C than a conventional EDLC using an organic liquid electrolyte such as [Et<sub>4</sub>N][BF<sub>4</sub>] in propylene carbonate. Higashiya et al. [82] prepared oxygen-containing spirobipyrrolidinium salts (Scheme 8.3) for potential applications as electrolytes in EDLCs. This group observed that introducing an oxygen atom (and alkyl groups to break the symmetry) to the spirobipyrrolidinium ring led to a reduction in melting points and viscosities of the resulting ILs. Meanwhile, these new salts retained a high electrochemical stability: the potential window ranged from 5.9 to 7.3 V (0.65 M in acetonitrile), and the conductivity (2.0 M in acetonitrile) varied from 48 to 55 mS cm<sup>-1</sup>.

Pandey et al. [83] designed new EDLC cells by using multiwalled carbon nanotube (MWCNT) electrodes and polymer electrolyte films comprising of PEG (MW~ $6\times10^5$ ), Li(CF<sub>3</sub>SO<sub>3</sub>) or Mg(CF<sub>3</sub>SO<sub>3</sub>)<sub>2</sub>, and [C<sub>2</sub>mim][CF<sub>3</sub>SO<sub>3</sub>].





 $X = CH_2 \text{ or } O \qquad R_1 = H, \text{ Me or Et}$  $R_2 = H \text{ or Me} \qquad R_3 = H \text{ or Me}$  $A = BF_4, BF_3C_2F_5, Tf_2N$ 

Although PEG chains were not covalently attached to the IL cation, the polymer electrolytes showed ionic conductivities of ~0.1 mS/cm at room temperature and the electrochemical stability window of ~4 V. These new EDLC cells with Mg-and Li-based polymer electrolytes exhibited specific capacitance values of 2.6–3.0 and 1.7-2.1 F/(g of MWCNT), respectively, and the Mg-based polymer electrolyte performed slightly better than the Li-type.

An ether-functionalized IL, 3-[2-(2-methoxyethoxy)ethyl]-1-methyl-imidazolium iodide, was used as the liquid electrolyte in a DSSC. However, the efficiency of liquid electrolyte was found inferior to those of sol-gel electrolytes [84]. The Lin group [85] attached different PEG methyl ether chains (PEG-150, 350, 550, and 750) to 1-methylimidazole to form ILs as electrolytes for DSSCs. They found that a longer PEG chain resulted in an increased apparent diffusion coefficient of triiodide, an improved dye regeneration rate, lower charge transfer resistance of triiodide reduction, and a higher ionic conductivity despite the higher solvent viscosity. Yang et al. [86] used PEG-1000-functionalized 1-methylimidazolium and ether-functionalized iodide mixed with 1-alkyl-3-methylimidazolium iodides as electrolytes for DSSCs. These new electrolytes showed high ionic conductivities and a large apparent diffusion coefficient for triiodide, particularly with the further addition of N-methylimidazole. Zheng et al. [87] constructed dye-sensitized solar cells using pyrazolium iodide as iodide source and ether-functionalized pyrazolium ILs as solvents and achieved a maximum of 1.7 % efficiency, photo-voltage of 0.557 V, and photocurrent density of 6.3 mA/cm<sup>2</sup> using the electrolyte concentration of 0.1 M I<sub>2</sub> and 1 M 1-(2-methoxyethyl)-2-ethylpyrazolium iodide in 1-(2-methoxyethyl)-2-ethylpyrazolium bis(trifluoromethylsulfonyl)imide without additives at 100 mW/cm<sup>2</sup>.

The functionalized ILs have also been used in various *electrodes*. Gao et al. [88] added 1-(3-chloro-2-hydroxy-propyl)-pyridinium acetate into carbon paste as a binder to prepare so-called carbon IL electrode, which was used for the voltammetric determination of adenosine-5'-monophosphate (5'-AMP). The new electrode enhanced the oxidation peak currents, resulting in a strong oxidation peak of 5'-AMP with the oxidation peak potential of 1.38 V at pH 4.0 Britton–Robinson buffer. The same group [89] also mixed 1-(3-chloro-2-hydroxypropyl)-3-methylimidazolium tetrafluoroborate in the carbon paste to construct a carbon paste electrode, which was applied in the sensitive detection of adenosine-5'-diphosphate (ADP). They found

the new electrode exhibits notable redox catalysis effect on the oxidation of ADP with a high selectivity and a low detection limit of  $3.23 \,\mu mol/L$ . Yu et al. [90] synthesized imidazolium-based ILs functionalized by different groups such as hydroxyl, nitrile, carboxyl, and thiol and further employed these ILs in the construction of chitosan/IL composites, which was used as flexible templates for the preparation of Au/Pt nanostructures deposited in situ on the surface of composites via electrodeposition. The resulting chitosan/IL-Au/Pt biosensors for  $H_2O_2$  reduction exhibit a high sensitivity and selectivity, low detection limit, and short response time; the functional groups of ILs influence the electrocatalytic activity of nanocomposites. The Detellier group [91] incorporated hydroxyl-functionalized ILs of different sizes in the interlayer spaces of kaolinite to prepare new nanohybrid materials based on clay minerals. The interlayer distances of the grafted materials could be controlled by the encapsulation of different ILs; as a result, the voltammperometric detection of anions with different sizes (thiocyanate, sulfite, and ferricyanide ions) could be accomplished based on the anion exchange capacity of the new nanomaterials by using glassy carbon electrodes coated with a thin film of the modified kaolinite.

KCl-type salt bridges have limited uses for samples with low ionic strength; however, newer salt bridges constructed from hydrophobic ILs are capable of overcoming this restriction [92]. Specifically, an ether-functionalized phosphonium IL, tributyl(2-methoxyethyl)phosphonium bis(pentafluoroethanesulfonyl)amide, exhibited stable liquid junction potentials when in contact with aqueous solutions with low ionic strength (as low as 1  $\mu$ M), and thus is a foreseeable electrolyte for salt bridges in accurate determination of pH and other single ion activities [93]. In addition, this IL has a low solubility in water (0.2 mM at room temperature) and is more chemically stable in alkaline solutions than tetraalkylphosphonium salts.

#### 8.2.4 Thiol/Thioether Functionality (Also See Review [94])

Lee et al. [95] demonstrated the formation of self-assembled monolayers (SAMs) of thiol-grafted imidazolium ILs on a gold surface and observed the strong influence of IL anions on the surface hydrophobicity and wettability. Furthermore, the same group [96] reported that SAM surfaces coated with these ILs on a gold electrode exhibited a selective electron transfer toward redox-probe molecules: that is, the electron transfer was observed in the presence of  $Fe(CN)_6^{3-}$  but not in the case of  $Ru(NH_3)_6^{3+}$ . Similarly, Rong et al. [97] immobilized a thiol-functionalized imidazolium IL on the surface of a gold electrode via Au–S bonds and observed more intense and stable electrochemiluminescence (ECL) for the luminol-O<sub>2</sub> system at the Au–IL and water interface. Itoh et al. [98] reduced a disulfide-functionalized imidazolium salt to thiol with in situ formation and stabilization of Au nanoparticles (NPs) (see Scheme 8.4). The thiol-IL-stabilized Au NPs were water soluble and stable against Brønsted acids (such as HCl, HBr, and HBF<sub>4</sub>). However, when either HI or HPF<sub>6</sub> was added, agglomeration of nanoparticles along with a color change of the solution was observed, signifying potential applications in optical sensors for anions.



Scheme 8.4 Au NP stabilization using a thiol-functionalized IL

Torriero et al. [99] synthesized thioether-functionalized ILs based on imidazolium, tetrazolium, and benzolium cations and various anions (i.e.,  $[N(Tf)_2]^-$ ,  $[CF_3SO_3]^-$ ,  $[R_2PO_4]^-$ ,  $Cl^-$ , and  $[PF_6]^-$ ) and found the potential windows (<3.94 V) of these ILs are narrower than common ILs due to the presence of thioether groups. A pyrrolidinium IL incorporating a thioether-functionalized chain was prepared, and its polarity ( $E_T^N$ ) and three Kamlet–Taft parameters were determined [100]. This study suggested that the thioether-containing IL has a lower polarity and  $\alpha$  value (H-bond acidity), but a higher  $\pi^*$  value (dipolarity/polarizability) than alkyl- and cyano-substituted ILs. Lesniewski et al. [101] constructed a gold–carbon nanoparticulate film electrode from oppositely charged conductive particles using a layerby-layer approach and observed that the use of a thiol-functionalized imidazolium salt as nanoparticle stabilizer (instead of amino groups) required no protonation during the assembling process.

## 8.3 Carboxyl-Functionalized ILs

Zhao et al. [102] suggested that the incorporation of an ester group onto an IL cation increases the solvent's H-bond acidity due to the weakly acidic  $\alpha$ -protons next to the ester group. Methylcarboxyl or cyano group substituted imidazolium ILs were investigated as electrolytes in lithium batteries [103]. Imidazolium, pyridinium, pyrrolidinpiperidinium, morpholinium, and quaternary ammonium ium, salts of  $[N(Tf)_2]^-$  functionalized with carboxyl groups were used in the selective dissolution of metal oxides and hydroxides [104]. Activity coefficients at infinite dilution of various organic compounds in two ester-functionalized ILs (1-methacryloyloxyhexyl-3-methylimidazolium bromide and 1-acryloyloxypropyl-3-methylimidazolium bromide) were measured by the inverse gas chromatography (GC) method [105]. Lu et al. [106] constructed a new electrochemical sensor by printing indium tin oxide (ITO) on electrodes (working, counter, and pseudo-reference electrode), followed by coating a thin layer of  $[H-betaine][N(Tf)_2]$  (Scheme 8.5) on the ITO electrode. The thin IL layer serves as both an electrolyte and a medium for selectively dissolving

Scheme 8.5 Structure of protonated betaine bis(trifluoromethylsulfonyl) imide

Scheme 8.6 Propylene carbonate-functionalized piperidinium RTIL





Wang et al. [107] covalently attached a carboxylic acid-functionalized IL, 1-(methylcarboxylic acid)-3-octylimidazolium bis(trifluoromethylsulfonyl)imide, to an oxidized boron-doped diamond (BDD) surface via an esterification reaction; the IL-modified electrode was found capable of selective electron transfer toward positive and negative redox species: Fe(CN)<sub>6</sub><sup>4-</sup> was detected on the IL-modified BDD interface, but surface-adsorbed Ru(NH<sub>3</sub>)<sub>6</sub><sup>3+</sup> was not detected. Tsuda et al. [108] prepared a piperidinium IL ( $T_g$ =-24.3 °C) functionalized with propylene carbonate (see Scheme 8.6) as potential electrolyte for energy-storage devices (ESD) because of its high thermal stability and lithium metal deposition ability, although this IL exhibited a high viscosity (~29,000 mPa s at 40 °C) and low conductivity (0.007 mS/cm at 40 °C). Deng et al. [109] suggest that the incorporation of an ester functionality to the alkyl chain of pyridinium or ammonium cations ([N(Tf)<sub>2</sub>]<sup>-</sup> as anions) increases the viscosity by fivefold for pyridinium ILs and twofold for ammonium ILs at 20 °C.

Baek et al. [110] prepared pyrrolidium-based ILs carrying different substituents including butyl, butyronitrile, pentenyl, and methyl butyrate (Scheme 8.7). The nitrile- and ester-functionalized ILs show higher viscosities and lower conductivities than the other two. Their potential windows (vs. Li/Li<sup>+</sup>) fall in the range of 4.19–4.97 V and are primarily dependent on the oxidation power of the functional group on cations. It was also found that the peak currents at the reduction on the graphite electrode were 100 times stronger in butyl- and pentenyl-substituted ILs than in nitrile- and butyrate-functionalized ILs.







# 8.4 Amine-Functionalized ILs

The Niu group [111, 112] prepared IL-functionalized single-walled carbon nanotubes (SWNTs) by the amidation between carboxylic acid-containing SWNT and an amine-terminated IL (1-propylamine-3-methylimidazolium bromide), followed by coating the modified SWNT on the surface of glassy carbon electrode (GCE). Glucose oxidase was immobilized on the new GCE by an anion exchange process. They further observed a high bioactivity of immobilized glucose oxidase in the bionanocomposite, as well as a linear amperometric response within 0-20 mM glucose during the electrochemical detection of glucose. Following this study, Gao and Zheng [113] designed a glucose biosensor using an amine-functionalized IL through several steps (Scheme 8.8): (a) the formation of IL-SWNT by the amidation between 1-ethylamine-2,3-dimethylimidazolium bromide and SWNT, and the coating of IL-SWNT on the surface of GCE; (b) electrochemical deposition of gold nanoparticle (GNP) onto IL-SWNT to produce GNP-IL-SWNT nanocomposite; (c) the coating of 1-ethylamine-2,3-dimethylimidazolium bromide on the surface of GNP to prepare IL-GNP-IL-SWNT nanocomposite; (d) the immobilization of glucose oxidase on the new nanocomposite via anion exchange. This glucose oxidase-modified electrode exhibited a superb electrocatalytic activity to the reduction of glucose with a detection limit of  $0.8 \,\mu$ mol/L (S/N=3). The IL layers on the SWNT and GNP are believed to facilitate the electron transfer between glucose oxidase and the electrode.

Also following the Niu's study [112], another group [114] immobilized cytochrome c onto SWNTs, which was covalently modified by 1-propylamine-3methylimidazolium bromide and then coated on GCE, for the electrochemical detection of hydrogen peroxide. The new biosensor showed a wide linear response



Scheme 8.8 Illustration of glucose oxidase-modified electrode using amine-functionalized IL

range of almost four orders of magnitude of  $H_2O_2$  (4.0×10<sup>-8</sup> M to 1.0×10<sup>-4</sup> M) as well as a low detection limit of  $1.3 \times 10^{-8}$  M (based on S/N=3). In addition, the biosensor also has a high selectivity, satisfactory reproducibility, and long-term stability. Li et al. [115] modified graphene nanosheets by 1,3-di(4-amino-1-pyridinium) propane tetrafluoroborate via a covalent attachment of amino groups and epoxy groups in an alkaline solution. The functionalized nanosheets were fabricated onto glassy carbon electrode along with hemoglobin via cross-linking with chitosan and glutaraldehyde. This biosensor enables a direct electron transfer and bioelectrocatalytic reaction of immobilized hemoglobin, leading to a pair of reversible redox peaks of hemoglobin and bioelectrocatalytic detection of  $H_2O_2$  with a high stability, reproducibility, and selectivity.

# 8.5 Nitrile (or Cyano)-Functionalized ILs

Egashira et al. [116] prepared a nitrile-functionalized IL named [CTMA][N(Tf)<sub>2</sub>] (CTMA = N.N.N.V.cyanomethyl trimethyl ammonium) and found its conductivity is in the order of 10<sup>-4</sup> S cm<sup>-1</sup> at 35 °C (its m.p.), which is lower than that of alkylsubstituted IL. Their further examinations on the lithium deposition/dissolution in 0.2 M Li[N(Tf)<sub>2</sub>]/[CTMA][N(Tf)<sub>2</sub>] electrolytes suggest a better cycle behavior than using the Li electrolyte based on a non-functionalized IL. A likely explanation is the formation of a protective film on the lithium surface. The Deng group [117] produced a number of nitrile-functionalized imidazolium, pyridinium, and quaternary ammonium ILs containing different anions (Cl<sup>-</sup>,  $[BF_4]^-$ ,  $[PF_6]^-$ ,  $[N(CN)_2]^-$ , and  $[N(Tf)_2]^-$ ); their data indicated that the incorporation of cyano group leads to increased viscosities, decreased conductivities, lower toxicity, and higher electrochemical windows (as high as 5.8 V). The likely reason is that the inclusion of cyano group induces conformational changes of the imidazolium groups and the enhancement in hydrogen-bonding interactions. As suggested earlier by Back et al. [110] in Scheme 8.7, the nitrile- and ester-functionalized pyrrolidium-based ILs show higher viscosities and lower conductivities than alkyl and pentenyl-substituted analogues; the nitrile-type IL has the widest potential window (4.97 V). Siriwardana et al. [118] synthesized nitrile-functionalized methimazole-type ILs by a two-step route (Scheme 8.9): alkylation of



Scheme 8.9 Preparation of nitrile-functionalized methimazole-type ILs

2-mercapto-1-methylimidazole with 2-chloroacetonitrile or 2-chloropropionitrile, and anion metathesis with  $Li[N(Tf)_2]$ . The resulting ILs have lower potential windows (2.94–3.09 V, glassy carbon electrode) than  $[C_2mim][N(Tf)_2]$  (4.51 V).

# 8.6 Zwitterionic ILs

Nguyen et al. [119] synthesized several imidazolium-based zwitterionic salts functionalized by a propylsulfonate group at C-3 position and an ester group at C-1 or C-2 position. In particular, grafting an ester group at the C-2 position of the imidazolium ring substantially improved the electrochemical stability of zwitterionic salts, and when these zwitterionic salts were used as additives for lithium battery electrolytes, their cycling performance was also improved compared with those containing a zwitterionic salt with an ester group at C-1 and a hydrogen or methyl group at C-2. For example, cycle performance tests suggested that the initial cell capacity was mostly retained for up to 100 cycles at 0.5 C when 2.5 wt% of 2-(acetoxymethyl)-1-butylimidazolium-3-propylsulfonate was mixed with the model electrolyte comprising ethylene carbonate (EC), dimethyl carbonate (DMC), and ethylmethyl carbonate (EMC) at 1:1:1 (v/v/v) ratio. Rondla et al. [120] observed the liquid crystal behavior of SO<sub>3</sub><sup>-</sup>-functionalized imidazolium zwitterionic salts (Scheme 8.10), which tend to align perpendicularly on a glass surface due to the hydrogen-bonding interaction between the glass surface and hydrophilic  $SO_3^-$  group as well as the high local symmetry surrounding the S atom. Adding lithium salt to these zwitterionic salts decreases the melting temperature while increases the clearing temperatures, resulting in room-temperature liquid crystals and high anisotropic lithium ion conductivity. These room-temperature liquid crystals could become target ion carriers in the electrochemical applications.

# 8.7 Polymerized ILs

ILs containing alkene groups could be polymerized and turned into valuable polyelectrolytes. Earlier studies on the subject have been reviewed [121]; herein we provide several recent examples. The Niu group [122] constructed a new  $H_2O_2$ -detecting electrolyte by fabricating multilayer ultrathin films of polyelectrolyte-functionalized



Scheme 8.10 SO3--functionalized imidazolium zwitterionic salts

Scheme 8.11 Polyelectrolytefunctionalized IL



Scheme 8.12 IL monomer for synthesizing poly(ionic liquid)

IL (Scheme 8.11) and Prussian blue (PB) nanoparticles onto indium-tin oxide conductive glass using the electrostatic layer-by-layer assembly technique. The new electrolyte exhibits an excellent reproducibility, high stability, and sensitivity (up to  $10^{-7}$  M) for the amperometric measurement of H<sub>2</sub>O<sub>2</sub>. The Guo group [123] polymerized 3-ethyl-1-vinylimidazolium tetrafluoroborate on ordered mesoporous carbons (OMCs), which became the support material for the deposition of ultrafine Pt nanoparticles via self-assembly; the functionalized OMCs were used to construct a new  $H_2O_2$  sensor with a linear range of 0.1  $\mu$ M–3.2 mM. In addition, this new  $H_2O_2$ sensor has a high sensitivity of 24.43 µA mM<sup>-1</sup> and a low detection limit of 0.08 µM. To accurately determine epinephrine (an important catecholamine neurotransmitter), Wu et al. [124] designed an epinephrine sensor by fabricating an ITO electrode with a chitosan film through the electrodeposition of multiwalled carbon nanotubes coated with a polymerized IL (POIL), poly(3-ethyl-1-vinylimidazolium tetrafluoroborate), in the presence of epinephrine as the template. The new sensor shows a linear response to epinephrine in the range of  $0.2 \,\mu\text{M}$  to  $0.67 \,\text{mM}$ , and a low detection limit of 60 nM (at an S/N of 3). In addition, the electrode exhibits a high reusability and good reproducibility and stability.

0

Jia et al. [125] constructed ionic polymer-coated nanofibrous membranes through grafting poly(ionic liquid) brushes (Scheme 8.12) onto the electrospun SiO<sub>2</sub> nanofiber surface using atom transfer radical polymerization (ATRP) method. They further demonstrated the potential applications of functionalized membranes as an anion-directed molecular gating system and also a membrane with electroactivity via simple counteranion exchange of the attached poly(ionic liquid) brushes.



Weber et al. [126] synthesized and characterized poly(styrene-*b*-4-vinylbenzylalkylimidazolium bis(trifluoromethanesulfonyl)imide) (alkyl = CH<sub>3</sub>, *n*-C<sub>4</sub>H<sub>9</sub>, *n*-C<sub>6</sub>H<sub>13</sub>) diblock copolymers (2.7–17.0 mol% POIL) (Scheme 8.13). They further obtained comparable values of conductivity (~0.1 mS cm<sup>-1</sup> at 150 °C) for lamellar samples of copolymers with similar compositions but different imidazo-lium alkyl groups; however, the ionic conductivity of copolymers could be related to the POIL composition and the corresponding morphology (0.01 mS cm<sup>-1</sup> for 8.6 mol% POIL and 0.1 mS cm<sup>-1</sup> for 17.0 mol% POIL at 150 °C).

Díaz et al. [127] designed Polymer Electrolyte Membrane Fuel Cells (PEMFC) using two different types of membranes based on protic ILs: (a) Nafion membranes impregnated with 1-methyl-3-(4-sulfobutyl)imidazoliumbis(trifluoromethylsulfonyl) imide ([HSO<sub>3</sub>-Bu-mim][N(Tf)<sub>2</sub>]) or 1-butyl-3-(4-sulfobutyl)imidazolium trifluoromethanesulfonate ([HSO<sub>3</sub>-Bu-bim][CF<sub>3</sub>SO<sub>3</sub>]), (b) membranes based on the polymerization of 1-(4-sulfobutyl)-3-vinylimidazolium trifluoromethanesulfonate ([HSO<sub>3</sub>-Bu-vim][CF<sub>3</sub>SO<sub>3</sub>]). Their measurements suggested that Nafion membranes impregnated with [HSO<sub>3</sub>-Bu-bim][CF<sub>3</sub>SO<sub>3</sub>] gave the current density of 217 mA/cm<sup>2</sup> and maximum power of 44 mW/cm<sup>2</sup> under anhydrous conditions at 25 °C and [HSO<sub>3</sub>-Bu-vim][CF<sub>3</sub>SO<sub>3</sub>] polymerized electrolytes produced the current density of 154 mA/cm<sup>2</sup> and maximum power of 33 mW/cm<sup>2</sup> at the same condition.

# 8.8 Other Cation-Functionalized ILs

Szot et al. [128] constructed an electrode based on indium-tin oxide with a controlled amount of conductive nanoparticles by combining the sol containing trimethoxysilyl-functionalized IL (Scheme 8.14) and carbon nanoparticles modified with phenyl sulfonate anionic groups. They found that the new electrode could be used as a reversible sponge for  $Fe(CN)_6^{3-}$  anions because of the presence of imidazolium functional groups. In addition, 2,2'-azino-bis(3-ethylbenzothiazoline-6sulfonate) anion as an enzyme mediator could be irreversibly accumulated on the electrode; the modified electrode shows the catalytic property in O<sub>2</sub>-saturated aqueous solution containing laccase. The same group [129] further designed a second electrode by replacing sol with a methanolic suspension of silicate submicroparticles



with appended imidazolium functional groups. This group found that following the adsorption of bilirubin oxidase, electrodes constructed from sol and carbon nanoparticles show modest bioelectrocatalytic activity toward dioxygen reduction at pH 4.8.

Weaver et al. [130] synthesized several ferrocene-functionalized phosphonium ILs carrying  $PF_6^-$  or  $OTs^-$  anions and found the apparent diffusion coefficients for electron transport and for the IL counterions are similar to one another. These ferrocenated phosphonium ILs show similar electron transport properties as those redox ILs based on the combinations of redox groupings with imidazolium and with short-chain polyether functionalities. Forgie et al. [131] prepared a ferrocenyl-substituted imidazolium IL (Scheme 8.15). In its neat form, this IL has a high viscosity and low conductivity. However, after mixing with ethylene carbonate–diethyl carbonate solvent, the electrolytic solutions exhibit reasonable viscosity and conductivity and could be used an additive in lithium battery electrolytes in standard coin cells with a metallic Li anode and a  $Li_4Ti_5O_{12}$  cathode.

The Cheng group [132] designed a catechol-functionalized imidazolium salt (Scheme 8.16) and coated it on screen-printed carbon electrode (SPCE) to construct an electrochemical sensing probe for dihydronicotinamide adenine dinucleotide (NADH). The new probe has a high electrocatalytic activity at 0.32 V for the oxidation of NADH in pH 7.0 buffer solutions and a low detection limit (S/N=3) of 0.4  $\mu$ M. Weng et al. [133] synthesized sulfone-functionalized imidazolium ILs (Scheme 8.17) and found that these ILs are highly compatible with Li/Li<sub>1.1</sub>(Ni<sub>1/3</sub>Co<sub>1/3</sub>Mn<sub>1/3</sub>)<sub>0.9</sub>O<sub>2</sub> (NCM) cathode material in Li battery.

N(Tf)<sub>2</sub>-



Scheme 8.18 Iodoarenefunctionalized imidazolium IL

The Fuchigami group [134] prepared a new iodoarene-functionalized imidazolium IL (Scheme 8.18) and used it as a mediator for indirect electrochemical fluorination of organic compounds in a HF-based IL. The viscous IL-type mediator limits its mobility, which allows the efficient indirect electrochemical fluorination in a simple undivided cell (vs. conventional mediatory systems).

# 8.9 Anion-Functionalized ILs

As discussed earlier, most ether/hydroxyl-functionalized ILs are cation-modified; however, there are also examples where the functionality is incorporated into the anion's structure. For example, ionic melts formed by pairing polyether-tailed 2sulfobenzoate with ruthenium hexamine, metal trisbipyridines, or porphyrin derivatives allow direct microelectrode voltammetry in the undiluted material [72]. Activity coefficients at infinite dilution for 1-butyl-3-methyl-imidazolium 2-(2-methoxyethoxy) ethyl sulfate were measured and these data were analyzed for the separation of hexane/benzene mixtures [135]. Zhuang et al. [136] synthesized a metal-containing IL, [(C<sub>10</sub>H<sub>21</sub>)<sub>2</sub>-benzimidazolium]<sub>2</sub>[Cd<sub>2</sub>Cl<sub>6</sub>] (m.p. 80 °C) and used it as a binder and electrocatalyst in constructing a bulk-modified carbon paste electrode. The new electrode was shown to be highly effective for the reduction of hydrogen peroxide and bromate at a lower detection limit. The same group [137] further constructed a new carbon paste electrode with another metal containing IL,  $[(C_4H_9)_2$ -benzimidazolium][FeCl<sub>4</sub>] (m.p. 70 °C), achieving excellent electrocatalytic activities toward nitrite and bromate reduction with a detection low limit and high sensitivity (0.01  $\mu$ M and 100.58  $\mu$ A  $\mu$ M<sup>-1</sup> for nitrite and 0.01  $\mu$ M and 83.11  $\mu$ A  $\mu$ M<sup>-1</sup> for bromate detection, respectively). Qiao et al. [138] prepared tungstatefunctionalized imidazolium ILs [Rmim]<sub>2</sub>[WO<sub>4</sub>] (R=C<sub>6</sub>H<sub>13</sub> or C<sub>12</sub>H<sub>25</sub>) and found these new ILs have higher viscosities and lower conductivities than those carrying anions of PF<sub>6</sub><sup>-</sup> and CH<sub>3</sub>SO<sub>3</sub><sup>-</sup>. Cyclic voltammograms suggested these functionalized ILs have electrochemical potential windows of about 4 V. Su and Cheng [139]



R

R = H, or Me

0

S

deposited  $[C_4 mim]_3[Fe(CN)_6]$  onto a screen-printed carbon electrode, followed by the addition of a second layer of poly(3-(aminopropyl)trimethoxysilane) sol–gel. The new electrode shows a highly stable redox couple, and in strongly acidic solutions, the reduction of nitrite could be achieved with a low detection limit and high sensitivity also without the interference of dissolved oxygen and common salts.

1-Methyl-3-octyl-imidazolium diethyleneglycolmonomethylether sulfate (ECOENG 48 M) was studied as the solvent for the Suzuki cross-coupling of phenylboronic acid and 4-bromoacetophenone [140]. 1-Ethyl-3-methylimidazolium 2-(2-methoxyethoxy) ethylsulfate was used as a solvent for the extraction of linalool from citrus essential oil [141]. Klein et al. [142] prepared quaternary ammonium salts (including choline salts) of an oligoether carboxylate (2,5,8,11-tetraoxatridecan-13-oate) (Scheme 8.19) with a  $T_g$  of -60 °C and viscosities in the range of 260–840 mPa s at 25 °C; these organic liquids exhibit significantly lower viscosities, higher conductivities, and higher polarities than alkali oligoether carboxylates. Enomoto et al. [143] synthesized several room-temperature ILs carrying fluorosulfate anions, i.e.,  $[C_2mim][SO_3F]$ ,  $[C_2mim][(FO_2SOH)OSO_2F]$ , and  $[C_2mim]$ [(FO<sub>2</sub>SOH)<sub>2</sub>O<sub>2</sub>SOF] and found that they have low viscosities (46.6 mPa s, 9.2 mPa s, and 5.1 mPa s at 25 °C, respectively) and high conductivities (10.8 mS cm<sup>-1</sup>, 30.8 mS cm<sup>-1</sup>, and 43.2 mS cm<sup>-1</sup> at 25 °C, respectively) but different electrochemical windows (4.3 V, 2.0 V, and 2.2 V for glassy carbon electrode). The lower electrochemical stability of the latter two ILs is due to H<sub>2</sub> evolution at the cathode limits.

Liu et al. [144] synthesized a series of new asymmetric ether-functionalized imide anions, (fluorosulfonyl) (polyfluorooxaalkanesulfonyl)imides (Scheme 8.20) pairing with different oniums, such as 1,3-dialkylimidazolium, quaternary alkyl (or ether-functionalized alkyl)ammonium, *N*-alkyl-*N*-methyl-pyrrolidinium, and -piperidinium. Scheme 8.20a-based ILs usually exhibit higher thermal stabilities,







Scheme 8.20 Functionalized anions-(fluorosulfonyl)(polyfluorooxaalkanesulfonyl)imides

lower viscosities (as low as 56 mPa s at 25 °C), higher conductivities (as high as 3.44 mS/cm at 25 °C), wider electrochemical windows (up to 6.35 V), and superior capability for enabling reversible Li deposition/striping than Scheme 8.20b-based analogues. Zheng et al. [145] measured the densities, viscosities, and electrical conductivities of Lewis acidic 1-butyl- and 1-hydrogen-3-methylimidazolium chloro-aluminate ILs and suggested their wide applications as electrolytes and catalysts.

It is also known that ILs with cyano-containing anions often have low viscosities (some even below 20 mPa s at room temperature) and high conductivities, such as dicyanamide  $[N(CN)_2]^-$  [146, 147], tricyanomethanide  $[C(CN)_3]^-$  or TCM<sup>-</sup> [148, 149], tetracyanoborate  $[B(CN)_4]^-$  [150, 151], and thiocyanate  $[SCN]^-$  [152]. Weingarth et al. [153] further established that the electrochemical stability of these ILs follows a decreasing order of  $[C_2 \text{mim}][B(CN)_4] > [C_2 \text{mim}][N(CN)_2] > [C_2 \text{mim}][C(CN)_3]$ .

#### 8.10 Deep Eutectic Solvents

Recently, the Abbott group [154–156] demonstrated that a mixture of solid organic salt and a complexing agent forms a liquid at temperatures below 100 °C, so-called "deep eutectic solvents" (DES), or "deep eutectic ILs" (DEILs). A typical example is mixing choline chloride (m.p.=302 °C, 2-hydroxyethyl-trimethylammonium chloride) and urea (m.p. = 133 °C) at a 1:2 molar ratio resulting in a room-temperature liquid ( $T_{\rm f}$ =12 °C) [154]. In addition to their applications in chemical and enzymatic reactions [22, 157], choline-based eutectic solvents are widely used in electrodeposition and electropolishing of metals [158-160], which has been reviewed for several types of eutectics [161-163]. A recent example by Mele et al. [164] illustrates the preparation of nanowires via electrodeposition in DES through a two-step strategy: (a) potentiostatic electrodeposition of an Au-Mn alloy in eutectic choline chloride/ urea (1:2); (b) electrochemically controlled oxidation of Au-Mn deposits, forming simultaneously the nanoporous gold support and the functional Mn-oxide decorating the nanopores. The specific capacity of nanoporous gold-supported nanostructured Mn-oxide was found higher than that of unsupported electrodeposited Mn-oxide nanowires based on the cyclic voltammetry measurements.

# 8.11 Summary

ILs with a variety of different functionalities have been developed for electrochemical applications. These ILs can be customized to have a wide range of viscosities, conductivities and electrochemical stability by incorporating different take-specific functional groups and making various ion pairs. In addition, the non-volatility and high chemical/thermal stability of ILs make them ideal and versatile electrolytes for many electrochemical applications. A new trend is to combine the task-specific ILs and nanomaterials for constructing novel sensors. There is still a need for further understanding of structure/functionality–property–application relationship, especially more data on physicochemical properties of task-specific ILs. Acknowledgments The author acknowledges the supports provided by the Henry Dreyfus Teacher-Scholar Award (2012), ACS-PRF (54875-UR9), NIH MBRS-RISE grant (1R25GM096956), and NIH NIBIB contract award (HHSN268201200011C).

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# **Chapter 9 Polymeric Ion Gels: Preparation Methods, Characterization, and Applications**

Maitane Salsamendi, Laurent Rubatat, and David Mecerreyes

# 9.1 Introduction

Ion gels or ionogels are a relatively new type of gels where the liquid phase, percolating throughout the solid phase, is an ionic liquid (IL). Ion gels are unique since they combine some properties and overcome others of well-known gels such as hydrogels, where the liquid phase is water, or organogels, where the liquid phase is an organic solvent. The properties given by the ionic liquids such as the high ionic conductivity and a wide electrochemical stability window are preserved in the ion gels, making them suitable and very attractive soft solid materials for electrochemists [1-5]. Additionally, the negligible vapor pressure, the nonflammability, and the thermal stability of the liquid phase of ionic liquids will permit a use of ion gels at elevated temperatures, up to 400 °C in some reported cases. Ion gels are formed by an ionic liquid component and a gelator also named solid phase which can be polymeric or nonpolymeric, organic or inorganic. There are two clear ion gel families which depend on the chemical nature of the solid phase, inorganic or organic, i.e., polymeric. Whereas many works and recent reviews have been dedicated to ion gels where the solid phase is based on inorganic sol-gel materials, here, we will focus on the use of polymers to develop ion gels.

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Fig. 9.1 Schematic representation of the applications of ion gels

In this chapter, a general overview of ion gels and their applications, mainly focused on electrochemical technologies, will be presented. The chapter will start with a general definition of ion gels and their preparation methods. Then we will describe the properties and advantages of ion gels, and finally their various applications. It is worth to stress that both ionic liquids and polymers offer unlimited chemical versatility; therefore, ion gels are a unique platform to design original materials [1]. Interestingly, the solid-like behavior enlarges the broad array of applications of ionic liquids. Applications of ion gels are illustrated in Fig. 9.1, which include electrolytic membranes for batteries, fuel cells, solar cells, actuators, electrochemical sensors, biosensors, supercapacitors, separation and catalytic membranes, or drug release.

## 9.2 Gels: Basic Definition and Classifications

Thomas Graham used the term "gel" in 1861 for the first time, and nowadays it is a common household item which is easily identified by the simple "inversion test": if the material is able to support its own weight without falling out when a pot is turned upside down, it is considered as a gel [6, 7]. However, as Dorothy Jordan Lloyd noted in 1926, gels are "...easier to recognize than to define." The generally accepted definition is that given by Flory in 1974, which is the next: A gel is a two-component, colloidal dispersion with a continuous structure with macroscopic

dimensions that is permanent on the timescale of the experiment and is solid-like in its rheological behavior [8, 9].

Even though gels are predominantly liquid in composition (typically 99 % by weight, the other 1 % is the gelator), it remains a solid, i.e., a jelly-like material that does not flow [10]. By changing the nature or the concentration of the gelator (gelling component) it is possible to modify and tune the physical properties of the material. This way, a myriad of materials with different characteristics have been recognized to form gels. In a general way, gels can be classified in two major groups: (1) the physical gels, when the internal three-dimensional network is cross-linked through weak and reversible interactions (e.g., hydrogen bonds, hydrophobic interactions, van der Waals forces, etc.), and (2) the chemical gels, when the cross-links result from covalent bonding. The term supramolecular gel, which is intensively used in recent years, refers to some of the so-called physical gels where the gelating agents make use of noncovalent interactions to form the gel.

Depending on the fluid component used to form the gel, they were classified as *organogels* or *hydrogels* [11]. When water is the liquid component, the gel is named hydrogel [12], whereas the organogel term is used when the liquid is an organic solvent [13]. More recently, ion gels were proposed as an additional type of gel where the liquid phase is an ionic liquid, immobilized in a three-dimensional network presenting a solid-like behavior. Ion gels have some of the properties of hydrogels since they are ionic in nature and they usually have some inorganic components in the structure (ionic liquid's anions). However, they also have some properties similar to organogels due to the chemical nature of the ionic liquid cation. Furthermore, ion gels present some unique properties such as the low vapor pressure and thermal stability of the liquid phase and wide electrochemical applications [2]. Due to these facts, they have been classified as a new type of gel which complements the terms hydrogels and organogels.

#### 9.3 Preparation Methods of Polymeric Ion Gels

In recent years, many studies have been carried out in order to fabricate ion gels with polymers. Preparation methods of ion gels can be classified into three main techniques as described in Fig. 9.2. These preparation methods include (i) swelling of a polymer in an ionic liquid, (ii) by a solution cast or solvent mediated method, or (iii) by in situ polymerization and cross-linking of monomers inside ionic liquids [2, 14].

**Swelling a Polymer in an Ionic Liquid** Two main preparation approaches are classified here. First, ion gels can be prepared by immersing a given polymer membrane (cross-linked or not) in an ionic liquid which is able to penetrate the membrane and swell the polymer without dissolving it. This synthetic method is limited by the choice of the polymer and the ionic liquid used, and the composition of the ion gel is determined by the maximum swelling capacity of the polymer [14–16]. In a typical example, Doyle et al. prepared Nafion-based ion gel membranes by using two different ionic liquids as swelling agents, 1-butyl-3-methylimidazolium trifluoromethanesulfonate [C<sub>4</sub>mim][CF<sub>3</sub>SO<sub>3</sub>] and 1-butyl-3-methylimidazolium tetrafluoroborate [C<sub>4</sub>mim][BF<sub>4</sub>] [17].



Fig. 9.2 Schematic representation of the different methods for ion gels' preparation

In the second approach, a polymer (usually a biopolymer such as gelatin, agarose, or a block copolymer) is dissolved in an ionic liquid at a given temperature. Then the polymer solution in ionic liquid is cooled down and an ion gel is formed. Due to this preparation procedure, these types of ion gels present thermo-reversible transitions. In a preparation example, Barreriros and coworkers reported the dissolution of gelatin in ionic liquids at temperatures higher than 35 °C to prepare ion jelly materials upon cooling [18]. A similar approach was used by Singh et al. using the biopolymer Agarose [19]. On the other hand, Lodge and coworkers pioneered

the development of ion gels using block copolymers as gelators. Thus, poly(*N*-isopropyl acrylamide-*b*-ethylene oxide-*b*-*N*-isoppopyl acrylamide) PNIPAm-PEO-PNIPAm triblock copolymer was mixed with 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] ionic liquid [20]. 10 % of the block copolymer was directly dissolved in the ionic liquid. The mixture was viscous liquid at room temperature; however, after cooling down to ~15 °C it became a transparent ion gel. Interestingly, a reversible gel transition was observed upon cooling–heating cycles between 5 and 50 °C. Similarly, Lodge and coworkers reported thermo-reversible ion gels based on 20 wt% of poly(styrene-b-ethylene oxide-b-styrene) and 80 wt% of [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] [21].

Solution Cast Method This preparation method of ion gels consists on the mixture of a given polymer and the IL together with a cosolvent to form a homogeneous dissolution, which is subsequently casted and dried to remove the solvent [22-26]. By this method, different types of polymers and ionic liquids can be mixed in different proportions, controlling and adjusting the properties of the final ion gels [14]. However, the limitation of this method is that the weight percent of ionic liquid is usually limited and some incompatibility problems between ionic liquids and polymers could appear. In a typical example, Shalu et al. studied the preparation of poly(vinylidene fluoride) PVdF-HFP copolymer-based ion gels by increasing the amount of ionic liquid  $[C_4 mim][BF_4]$  [27]. Briefly, a desired amount of PVdF-HFP was dissolved in acetone under stirring at 50 °C. Afterward, different amounts of ionic liquid (from 0 to 90 wt%) were added and stirred for 2-4 h at the same temperature until the solution of PVdF-HFP and ionic liquid became viscous. After casting it into Petri dishes and removing the solvent, rubbery films of the ion gel were obtained. The maximum conductivity value obtained was  $1.6 \times 10^{-2}$  S cm<sup>-1</sup> for the membrane containing 90 % of ionic liquid at room temperature. The textural changes of the PVdF-HFP/SN network and phase changes from crystalline to amorphous nature provided more free volume for ease of ion transport. However, in most cases, incompatibility and segregation of the ionic liquid from the ion gel with time are observed. To avoid this ionic liquid leaching problem, Marcilla et al. proposed the use of polymeric ionic liquids as a very compatible polymer matrix to prepare ion gels [28].

**Polymerization–Cross-linking of Monomers in Ionic Liquids** By this method, the in situ one-step synthesis of ion gels is carried out by mixing all reactants (monomer, initiator, cross-linking agent) in an ionic liquid. The polymerization can be carried out thermally or using UV light in the presence of a photoinitiator. The compatibility between the polymer matrix and the ionic liquid used as a solvent is crucial to obtain ion gels since the loss of miscibility during polymerization may be a limitation in gel forming [2]. In this regard, vinyl monomers have been intensively studied since many of them show high compatibility with different ionic liquids [29–31]. This way, transparent, mechanically strong, and highly conductive polymer electrolyte films have been obtained. Watanabe and coworkers reported for the first time the in situ radical polymerization of a vinyl monomer 2-hydroxyethyl methacrylate (HEMA) in an ionic liquid 1-butylpyridinium tetrafluoroborate [C<sub>4</sub>py][BF<sub>4</sub>] leading to a conductivity of  $10^{-3}$  S cm<sup>-1</sup> [30]. Later, the same group has studied the polymerization of methyl

methacrylate in 1-ethyl-3-methyl imidazolium bis(trifluoromethane sulfonyl)imide  $[C_2mim][N(Tf)_2]$  [31]. The monomer was chosen according to the compatibility of the vinyl monomer and the ionic liquid used, since acrylonitrile, styrene, HEMA, and acrylamide were incompatible after being polymerized.

This method is very versatile and can be applied to many different monomer/ionic liquid combinations [32]. For instance, Isik et al. recently reported for the first time ion gels which were fully composed of low toxicity and biocompatible ionic liquids [33]. Ion gels containing 40 % of cholinium lactate methacrylic monomer and 60 % of cholinium lactate ionic liquid were synthesized by photopolymerization. The effect of additional ethyleneglycol dimethacrylate (4 %) as a cross-linker was explored and found to be responsible for the reduction in the transparency and the improvement of the ion gel's integrity. As a very different example, cyclic carbonate network polymers were synthesized using dual functional cyclic carbonate methacrylate (CCMA) monomer [34]. Due to the high compatibility between the ionic liquid and the cyclic carbonate network, transparent, flexible, and stable ion gels were obtained, which contained high ionic conductivity (up to  $10^{-3}$  S cm<sup>-1</sup> at ambient temperature).

Hybrid ion gels, which are constituted by a combination of organic and inorganic materials synthesized by a sol-gel method, have attracted the interest of many researchers due to the mechanical strength that inorganic materials can provide to the gel. Although this chapter is mainly focused on organic materials, some examples should be mentioned. In 2010, Vioux and coworkers reported some work on hybrid sol-gel ion gels [35, 36]. In this type of ion gels, the three-dimensional network is formed by the condensation of alkoxysilanes such as tetraethoxy silane (TEOS) (instead of monomer polymerization). For instance, they carried out the synthesis of homogeneous and transparent PMMA-silica ion gels, fabricated from a copolymer based on MMA and methacryloxypropyltrimethoxysilane (MPTMS), then the ionic liquid [C<sub>4</sub>mim][N(Tf)<sub>2</sub>] was added, and finally a solution of tetraethoxy silane (TEOS) was incorporated to the mixture. Gelation of the hybrid ion gel occurred within 1 h and the aging continued for 14 days. In this system, the silica nanofiller covalently bonded to the polymer chains, which provided mechanical strength to the ion gel, while the ionic liquid was responsible for the flexibility and ionic conductivity of the material. High ionic liquid loadings have been described, close to 90 wt%, which contained the same ionic conductivity as the pure ionic liquid, and no leaching was observed. More recently, Noor et al. suggested that the mechanism of ionic liquid immobilization in the silica network is based on the hydrogen bonds formed between the anion of the ionic liquid (BF<sub>4</sub><sup>-</sup>) and the hydroxyl group of the silica [37]. As a result, they obtained solid-state electrolytes with high loading of ionic liquid (up to 97 %).

#### 9.4 Properties of Ion Gels

Ion gels are soft-solid materials formed by two components: (i) an ionic liquid and a (ii) polymeric cross-linking component. The intimate contact between the ionic liquid and the solid-like network provides an intrinsic hybrid character to the ion gel. Ion gels usually present the unique properties of the ionic liquid, such as thermal stability, negligible vapor pressure, nonflammability, electrochemical and chemical stability, or high ionic conductivity [38, 14]. Furthermore, the polymer network is responsible for the solid-like behavior. The properties of the ion gel can be infinitely tuned by changing the chemical structure of the polymer network, the ratios, cross-linking degree, or modifying the type of ionic liquid. The main properties that characterize ion gels are the ionic conductivity and their mechanical and rheological properties as described below.

#### 9.4.1 Ionic Conductivity

The good ionic conductivity is one of the most interesting properties of ion gels when being used as electrolytic membranes in several electrochemical devices. The ionic conductivity of the ion gel can be easily controlled by adjusting the content of the ionic liquid and the type of polymer in the membrane. Indeed, by increasing the amount of ionic liquid the ionic conductivity can be enhanced. This was very well illustrated by Marcilla et al., who reported several ion gels with conductivities varying from  $10^{-7}$  to  $10^{-2}$  S cm<sup>-1</sup> depending on the poly(ionic liquid) to ionic liquid ratio [39]. However, an excess of ionic liquid can cause poor mechanical stability and ionic liquid leaching, especially when the ionic liquid and the polymer are not totally compatible [14, 37]. Yang and coworkers have prepared ion gel membranes of PVdF-HFP with different concentrations of 1-butyl-4-methylpyridinium bis(trifluoromethanesulfonyl)imide [C<sub>4</sub>mβpy][N(Tf)<sub>2</sub>] through solution-casting method [40]. The highest ionic conductivity obtained was  $2.01 \times 10^{-4}$  S cm<sup>-1</sup> with 33.3 wt% of ionic liquid (See Fig. 9.3).

The ionic conductivity of the gel membranes is usually lower than that of the pure ionic liquid, confirming the molecular level blending of the solid network and the ionic liquid. Pandey and Hashmi observed that the ionic conductivity of 1-ethyl-3-methylimidazolium tris(pentafluoroethyl) trifluorophosphate [C<sub>2</sub>mim] [FAP] was reduced from  $3.6 \times 10^{-3}$  S cm<sup>-1</sup> to  $1.7 \times 10^{-3}$  S cm<sup>-1</sup> after blending it in 20 wt% of PVdF-HFP [41]. However, the addition of salt LiPF6 in [C<sub>2</sub>mim][FAP]/PVdF-HFP provided a slight enhancement in the conductivity value ( $2.6 \times 10^{-3}$  S cm<sup>-1</sup>), probably due to high Li<sup>+</sup> ion mobility in the polymer electrolyte. On the other hand, the potential window of the ion gel was slightly reduced after the addition of salt from ~4.5 V (from -2.2 to 2.3 V) to ~4 V (from -2.0 to 2.0 V), but still it was sufficient to use them in supercapacitor applications.

#### 9.4.2 Mechanical and Rheological Properties

The local interactions between ILs and the solid phase of the gel have been addressed from different perspectives as functions of the systems in the case of the polymeric ion gels, the main observable effect is the plasticizing effect of the IL on the



**Fig. 9.3** (a) Photograph of the as-prepared ionic liquid gel polymer electrolyte. (b) Conductivity of the ion gel with various weight percentages of  $[C_4m\beta py][N(Tf)_2]$  systems. (c) Temperature dependence of the ionic conductivity for  $[C_4m\beta py][N(Tf)_2]/Li[N(Tf)_2]/PVdF$ -HFP polymer electrolytes containing 33.3 wt%  $[C_4m\beta py][N(Tf)_2]$  from 0 to 80 °C [40]

polymer leading usually to a glass transition lower than the polymer one and higher than the IL one [42, 29]. In a typical example, Jiang et al. have studied the decrease in glass-transition temperature (Tg) of pure PMMA from 107.5 to 23.5 °C with an increase of the mass fraction of the ionic liquid 1-butyl-3-methylimidazolium hexa-fluorophosphate [C<sub>2</sub>mim][PF6] from 0/10 to 5/5 of [C<sub>4</sub>mim][PF6]/[MMA] [29].

On the other hand, the mechanical and rheological properties of ion gels are important factors to be considered according to the targeted applications. Nagasawa et al. studied the properties of the ion gels consisting of several ionic liquids and the N,N'-(trans-cyclohexane-1,4-diyl)-dibenzamide-based polymer with different anions (CDBA6-X), bis(trifluoromethanesulfonyl)amide (CDBA6-N(Tf)<sub>2</sub>) or bis(fluorosulfonyl)imide (CDBA6-FSI) among others [43]. The rheological properties are summarized in Fig. 9.4, demonstrating the quasi-solid behavior of the ion gel since (storage moduli) G' is greater than (loss moduli) G'' for the entire range of frequencies (Fig. 9.4a). In Fig. 9.4b, a strain-induced collapse of the gel state above the critical strain region with a dramatic decrease of the G' value is shown. However, G' increased when the concentration of CDBA6-N(Tf)<sub>2</sub> increased, reaching values of  $1 \times 10^5$  Pa at 50 g/L. Regarding the mechanical properties of those ion gels, despite the fact that noncovalent networks were obtained (physical gel), they exhibited very good mechanical strength.



**Fig. 9.4** Rheological data of the CDBA6-N(Tf)<sub>2</sub>/[C<sub>2</sub>mim][N(Tf)<sub>2</sub>] and CDBA6-FSI/[C<sub>2</sub>mim] [FSI] ionogels. (**a**) Frequency sweeps of three samples of the ionogels with different concentrations. (**b**) Strain amplitude sweeps (strains at 0.1 Hz). (**c**) Step strain measurement (0.1 %  $\leftrightarrow$  100 %) of the CDBA6-FSI/[C<sub>2</sub>mim][FSI] ionogel (20 g/L). Step strain measurement was a continuous one (three cycles). (**d**) The chemical structure and pictures of the ion gel [43]

Highly stretchable and transparent ion gels have been reported such as the ones presented by Chen, Suo, and coworkers polymerizing acrylic acid in 1-ethyl-3-methylimidazolium ethylsulfate  $[C_2mim][EtSO_4]$  [44]. The ion gel exhibited a Young's modulus of  $3.1 \pm 0.6$  kPa, fracture strength of  $7.4 \pm 0.4$  kPa, and a fracture stretch of  $4.6 \pm 0.3$ . Furthermore, the relatively small hysteresis was observed in the cyclic stretch–stress curves after hundreds of cycles of loading and unloading. In the initial cycles, the Young's modulus decreased and became stable after 150 cycles. Therefore, good mechanical reversibility was observed. More stretchable solid electrolytes were reported by Wallace and coworkers [45]. These ion gels, which were PMMA networks with polyethylene glycol diacrylate cross-linker swollen by 1-ethyl-3-methylimidazolium bis(trifluoromethanesulnofyl)imide [C<sub>2</sub>mim][N(Tf)<sub>2</sub>], were elastically stretched more than 500 % of their original length and they exhibited larger than 1.5 MPa of tensile breaking strength.

On the other hand, confinement effects can be observed and are intensively studied exclusively on inorganic ion gels, where the confinement of the IL within the nanopores of the gel solid phase can alter significantly the physicochemical properties of the IL, such as phase transitions (appearance and disappearance of transition) and molecular dynamics as well. Nevertheless, the dynamical effects appear to be localized on the ion–wall interface preserving the liquid behavior of the IL until extreme confinement. The significative confinement effects, including enhancement in luminescence emission, observed in inorganic ion gel are reported in the review [2].

# 9.4.3 Morphology

The association of block copolymers with ionic liquids opens an unlimited number of combinations to be explored and exploited. ABA triblock copolymers have been already successfully used to immobilize a large amount of ionic liquids leading to unique ion gel with controlled morphologies, containing only few percent by volume of polymers. Indeed, due to the selective solubility of the blocks in the ionic liquid (only block B is soluble) the macromolecules can self-assemble to provide a highly elastic solid with typical mesh sizes in the range of 10–100 nm [1]. Using an appropriate nonsoluble block, temperature can be used as an external stimulus to provoke the solubility and then induce a reversible solid to liquid transition which can be of interest for material processing [46].

T. Russell, J. Watkins, and coworkers have reported a study on cross-linked ABA block copolymer combined with ionic liquids to obtain self-assembled ionic gels presenting decoupled ionic conductivity and mechanical strength [47]. Indeed, poly(propylene oxide)–poly(ethylene oxide)–poly-(propylene oxide) (PPO–PEO–PPO) block copolymers with cross-linkable end groups were blended with [C<sub>4</sub>mim] [PF<sub>6</sub>] ionic liquid. Interestingly, the chosen IL selectively solubilized the PEO block, promoting the copolymer microphase separation (which were otherwise disordered or weakly ordered). According to the small-angle scattering results, differ-

ent morphologies were achieved: cylindrical aggregates of PPO arrayed in a hexagonal pattern in the PEO/IL matrix and, at higher IL concentration, a bodycentered cubic (BCC) morphology of PPO spheres in a PEO/IL matrix are observed. The authors conclude that the microphase separation does not affect the ionic conductivity, but it can be used to increase the mechanical stability by isolating phaseselective cross-linkers from the ion-conducting phase.

Block copolymers can be also associated with a lower amount of ILs leading to membrane-like materials such as reported by R. Segalman and coworkers using poly(styrene-block-2-vinylpyridine) blended with the ionic liquid imidazolium bis(trifluoromethane)sulfonimide  $[Im][N(Tf)_2]$  [48]. In this system, polystyrene (PS) is not soluble in the ILs. As demonstrated by small-angle X-ray scattering, the composite materials exhibit a variety of controlled morphologies, including lamel-lae, hexagonally close-packed PS cylinders, body-centered cubic PS spheres, face-centered cubic PS spheres, or disordered PS micelles, which allows us to propose lyotropic phase diagrams [48]. It has been shown that the nanostructure does not significantly impact the conductivity of the membranes, possibly due to the continuity of the conducting phase [25].

Recently, Lodge and coworkers have used a triblock terpolymer, poly[isopreneb-(styrene-co-norbornenylethylstyrene)-b-ethylene oxide] (INSO), to blend with 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide  $[C_2mim][N(Tf)_2]$ [49]. The structural characterization revealed the continuous morphologies trapped by the chemical cross-linking of the PS blocks presenting both the conductive and the high modulus domains. The conductivity measurement revealed that the ion conductivity in the PEO domains was much lower than the value measured with PEO homopolymer; this point was attributed to the potential conducting pathways' dead ends or to the presence of isolated conducting domains resulting from the solvent-casting procedure.

#### 9.5 Applications

Most of the applications of ion gels are found as solid electrolytes in electrochemical devices. Ion gels combine two properties such as the ionic conductivity provided by the ionic liquid and the solid-like behavior which gives access to all-solid devices facilitating the preparation and security of most electrochemical devices. Indeed, the main drawback of liquid electrolytes (aqueous, organic, or ionic liquid-based) in electrochemical devices is the need of additional encapsulation, which can be overcome by the use of ion gels-based electrolytic membranes. Those ion gel solid electrolytes can be then used in batteries, fuel cells, solar cells, electrochemical sensors, biosensor, actuators, or supercapacitors. Although this chapter will mainly focus on electrolytic membranes, other promising applications of ion gels such as separation membranes, catalytic membranes, or drug release in biomedicine will be also mentioned.

### 9.5.1 Batteries

A battery is an energy-storage device that transforms chemical energy into electrical energy and supply electrical energy via terminals/contacts [50, 51]. In the last decades, the demand for energy-storage and portable devices has increased all over the world; therefore, the production of batteries grew considerably [52]. The lithium-ion secondary (rechargeable) batteries have become the most studied candidates among other types of batteries. They play an important role in modern society since they are the power system for sustainable vehicles, portable computers, cameras, mobile phones, medical instrumentations, as well as electrochemical storage systems in renewable energy plants [53]. However, cycling performances, costs, operational temperature, and safety are still major issues to be improved or resolved. In this perspective, all-solid batteries can be a major progress with ion gels as promising candidate for that purpose.

Electrolytic membranes based on ion gels which use poly(vinylidene fluoride)hexafluoro propylene (PVdF-HFP) as copolymer matrix have been intensively studied [54, 55, 22, 56]. Hofmann et al. have reported an ionic liquid-based polymer gel electrolyte for lithium ion batteries prepared by combining a conducting salt (Lithium bis(trifluoromethylsulfonyl)azanide), the PVDF-HFP, different types of ionic liquids, and additives. The conductivity of the gel electrolytes varies with the ionic liquid used and values up to 1-2 mS/cm were obtained (See Fig. 9.5) [57]. Li Libo et al. have studied the increment of conductivity in the electrolytic membrane when increasing the concentration of a given ionic liquid [40, 58]. Furthermore, Fernicola et al. have prepared membranes with 60, 70, and 80 % of lithium saltionic liquid (Li salt-IL) mixture to give conductivity values in the order of 10<sup>-4</sup> S cm<sup>-1</sup> and an electrochemical stability window in the range of 1.8–4.5 V vs Li<sup>+</sup>/Li [52]. The Li salt–IL mixture acts as a plasticizer for the polymer matrix, suppressing the crystallinity of the electrolytic membrane. The ionic conductivity increased with the Li salt-IL content and the temperature, reaching 10<sup>-2</sup> S cm<sup>-1</sup> at 110 °C. Unexpectedly, a significant enhancement in the Li transference number was observed when passing from the liquid to the membrane electrolyte system.

Recently, electrospun fibrous membrane of P(VdF-HFP) has been prepared and electrochemically activated by incorporating lithium (bis(trifluoromethylsulfonyl) imide) complexed with different ionic liquids 1-ethyl-3-methylimidazolium (bis(trifluoromethylsulfonyl)imide) [C<sub>2</sub>mim][N(Tf)<sub>2</sub>], 1-propyl-3-methylimidazolium (bis(trifluoromethylsulfonyl)imide) [C<sub>3</sub>mim][N(Tf)<sub>2</sub>], or 1-butyl-3-methylimidazolium (bis(trifluoromethylsulfonyl)imide) [C<sub>4</sub>mim][N(Tf)<sub>2</sub>], or 1-butyl-3-methylimidazolium (bis(trifluoromethylsulfonyl)imide) [C<sub>4</sub>mim][N(Tf)<sub>2</sub>], or 1-butyl-3-methylimidazolium (bis(trifluoromethylsulfonyl)imide) [C<sub>4</sub>mim][N(Tf)<sub>2</sub>], or 1-butyl-3-methylimidazolium (bis(trifluoromethylsulfonyl)imide) [C<sub>4</sub>mim][N(Tf)<sub>2</sub>] [59, 60]. Interconnected fibrous structure of the membrane presented fibers with large surface area and high porosity. Due to this unique structure of the membrane, high ionic conductivity (>2.4×10<sup>-3</sup> S cm<sup>-1</sup>) was achieved at 25 °C. The excellent electrochemical characteristics of these fibrous ion gels allow the fabrication of safer lithium batteries with improved performance.

Another approach to obtain ion gels-based membranes for lithium batteries is to use polymeric ionic liquid (PIL) as polymer host and incorporate ionic liquid and



**Fig. 9.5** (a) Structures of the ionic liquids. (b) Photograph of gel polymer electrolyte with a diameter of 13 mm and a thickness of 200  $\mu$ m. (c) Conductivity Arrhenius plots of four gel polymer membranes. The data are obtained from impedance spectroscopy at 10–50 °C. (d) Composition, conductivity data, and ECW of gel polymer electrolytes with varied ionic liquids. *mp* melting point, *ECW* electrochemical window; electrodes, stainless steel/stainless steel; first cycle; v=25 mV/s; T=50 °C; potential range, E vs Stainless Steel=± 4 V [57]

lithium salt [61–63]. The use of PILs as matrices in ionic liquid-based polymer electrolytes presents some advantages comparing with other polymer hosts: (1) Good chemical affinity between PILs and ILs affording stable polymer electrolytes. (2) Electrochemical stability and the ionic character of PILs make them good candidates as electrolyte hosts. (3) As usual in ion gel-based electrolytes, PIL-based membranes are easy to process. Appetecchi et al. have reported the synthesis of electrolytic membrane using poly(diallyldimethylammonium)-bis(trifluoromethanesulfonyl)imide as a polymer host, *N*-alkyl-*N*-methylpyrrolidinium-bis(trifluoromethanesulfonyl)imide as ionic liquid, and Li[N(Tf)<sub>2</sub>] as a lithium salt [39]. The electrolytic membrane obtained has presented good mechanical properties with high chemical stability even after prolonged storage times in contact with lithium anode, and it was thermally stable up to  $300 \, ^{\circ}$ C. These membranes exhibited room temperature ionic conductivity above  $10^{-4}$  S cm<sup>-1</sup> with an electrochemical stability window up to 5.0 V vs Li<sup>+</sup>/Li, time-stable interfacial resistance values, and good lithium stripping/plating performance.

Early work on polymer electrolytes indicated that polyethylene oxide (PEO) is a promising candidate as a host for lithium salt in relation to its ability to solvate Lithium cation [64–66]. This is attributed to its flexible ethylene oxide segments and ether oxygen atoms, which have a strong donor character and solvate lithium

cations. However, the major drawback of PEO-based polymer electrolytes is the ionic conductivity at ambient temperatures. The introduction of room temperature ionic liquids, such as *N*-alkyl-*N*-methylpyrrolidinium bis(trifluoromethanesulfonyl)-imide, into the polymer electrolyte (PEO-Li[N(Tf)<sub>2</sub>]) resulted in an increase of more than one order of magnitude in ionic conductivity at room temperature, which was attributed to the plasticizing effect of the ionic liquid. For instance, in the case of N-butyl-N-methyl-pyrrolidinium to lithium cation  $[C_4mPyr]^+/Li^+$  ratio of 3.22, the ionic conductivity reaches  $2 \times 10^{-4}$  S cm<sup>-1</sup> at 40 °C.

Moreover, other polymers have also been studied in the synthesis of ion gel-based membranes. Stepniak has reported membranes obtained by in situ photopolymerization of a mixture of ethoxylated bisphenol A diacrylate (bisAEA4) and 0.4 M solution of Li[N(Tf)<sub>2</sub>] in N-methyl-N-propylpiperidinium bis(trifluoromethanesulfonyl) imide  $[C_3mpip][N(Tf)_2)$  [67]. It is worth stressing that the photopolymerization technique is a suitable method for synthesizing porous gel polymer electrolytes, due mainly to the ease and rapidity of processing. Stable, porous, and flexible membranes were characterized to give 0.64 mS cm<sup>-1</sup> of ionic conductivity at 25 °C and good electrochemical stability (4.8 V). Charge-discharge test of the lithium-ion battery using  $Li_4Ti_5O_{12}$  (LTO) as anode with ionic liquid gel polymer electrolyte (IL-GPE) exhibited a good specific capacity of 124 mAh g<sup>-1</sup> and 110 mAh g<sup>-1</sup> at C/20 and C/5, respectively. Furthermore, gel polymer membranes of polyacrylonitrile and poly(methyl methacrylate) (PAN/PMMA) incorporating room-temperature ionic liquids have been reported [68, 69]. The ionic conductivity of the membrane with  $[C_4 mPyr][N(Tf)_2]$  is  $3.6 \times 10^{-3}$  S cm<sup>-1</sup> at room temperature, and the capacity of LiFePO<sub>4</sub> in the cell Li/GPE/ LiFePO<sub>4</sub> is 139, 134, 120, and 101 mAh g<sup>-1</sup> at the charge/discharge rate of 0.1, 0.2, 0.5, and 1C, respectively, remaining unchanged after ten cycles for each rate.

#### 9.5.2 Fuel Cells

A fuel cell is an electrochemical conversion device that has a continuous supply of fuel such as hydrogen, natural gas, or methanol and an oxidant such as oxygen, air, or hydrogen peroxide [51, 70]. The most promising commercial applications of fuel cells appear to be as a stationary power for central and dispersed power stations and as mobile power for portable electronics devices and automobiles. Fuel cells offer a rather clean electrical power generation; they are quiet in operation and can be more efficient in the conversion of energy in a fuel into power than gasoline engines or utility thermal power plant.

Proton exchange membrane fuel cells (PEMFCs) are considered to be promising candidates; however, several factors, such as cost, reliability, good proton conductivity, durability, and the ability to operate at temperatures higher than 120 °C, are major challenges in the commercialization of PEMFCs [71]. Operating above 120 °C offers significant advantages such as reduced CO poisoning at the anode, increased energy efficiency, improved heat rejection, improved quality of waste

heat, and easy water management. In this regard, the polymer electrolyte membrane, which acts as a charge carrier for protons, a separator for the reactant gases, and an electronic insulator that prevents electrons from passing through, is a key component to be developed [72, 73]. Water management in the PEM is crucial and challenging since polymers usually require water to promote proton mobility between both electrodes, and above 100 °C, this water is evaporating, reducing the activity of the fuel cells. Thus, there is a researching interest to develop protonconducting electrolytes that do not require hydration for proton conduction.

Ion gels are good candidates to be used as electrolytic membranes in PEMFCs, where the ionic conductivity of the membrane depends on the concentration of the ionic liquid, on the conductivity of neat ionic liquid, and on the polymer's nature. The good miscibility of the polymer and ionic liquid is crucial while preparing membranes with sufficient ionic conductivity for PEMFC applications. Ionic liquids fall into two general classes: aprotic (with applications in lithium batteries, dye-sensitized solar cells, thermo-electrochemical cells) and protic, which are less studied in general due to the reactivity of the active proton, but this feature makes them of significant interest to be used in fuel cell electrolytes [74]. However, the good affinity between the polymer and the ionic liquid plays the most significant role, together with the nature of the polymer, in ionic conductivity. As an example, Schauer et al. have studied membranes with two relatively similar ionic liquids, 1-butyl-3-methylimidazolium trifluoromethanesulfonate [C4mim][CF3SO3] and 1-ethylimidazolium trifluoromethanesulfonate [C<sub>2</sub>mim][CF<sub>3</sub>SO<sub>3</sub>], respectively, aprotic and protic [73]. Both ionic liquids had very similar affinities to given polymers, and similar ionic conductivities were measured in the ionic liquid-polymer membranes.

Different polymers have been studied in combination with ionic liquids to synthesize gel polymer electrolytic membranes for PEMFCs. Perfluorosulfonated acid (PFSA)-based polymers, such as Nafion, are the most studied ones for this purpose. These polymers are mechanically, thermally, and chemically stable and have very high proton conductivity [75]. However, its conductivity drops at temperatures higher than 100 °C due to water evaporation, which has an important role in proton conduction. Díaz et al. prepared membranes based on Nafion with protic ionic liquids, such as 1-butyl-3-(4-sulfobutyl)imidazolium trifluoromethanesulfonate [HSO<sub>3</sub>-bmim] [CF<sub>3</sub>SO<sub>3</sub>] or 1-methyl-3-(4-sulfobutyl)imidazolium bis(trifluoromethanesulfonyl) imide [HSO<sub>3</sub>-bmim][N(Tf)<sub>2</sub>], for their use as electrolytes in PEMFCs under anhydrous conditions [76]. These membranes achieve current densities of 217 mA/cm<sup>2</sup> and a maximum power of 44 mW/cm<sup>2</sup> under anhydrous conditions at 25 °C. Mališ et al. investigated the influence of humidity and the temperature on the PVdF-HFP and Nafion-based membranes' conductivity after mixing the polymers with [C<sub>4</sub>mim] [CF<sub>3</sub>SO<sub>3</sub>] or [C<sub>2</sub>mim][CF<sub>3</sub>SO<sub>3</sub>] [77]. All membranes showed relatively high ionic conductivity, which increases with increasing temperature. Under dry conditions, the conductivity of the Nafion membrane itself drops to zero, while in combination with ionic liquids no conductivity drop was observed. The conductivity stability has to be attributed mainly to the ionic liquid effect. On the other hand, in a humidified atmosphere the conductivity of the Nafion-based membrane is higher than in dry conditions, and a protic ionic liquid increases the content of water in the membrane. In this regard, the



**Fig. 9.6** (a) A photograph of SPI-2.27 composite membrane. (b) Arrhenius plots of ionic conductivities for [dema][CF<sub>3</sub>SO<sub>3</sub>] and SPI/[dema][CF<sub>3</sub>SO<sub>3</sub>] composite membranes based on (i) SPI-1.51 (IEC=1.51 meq  $g^{-1}$ ) and (ii) SPI-2.27 (IEC=2.27 meq  $g^{-1}$ ) [78]

lowest conductivity was achieved for the combination of aprotic ionic liquid,  $[C_4mim]$  [CF<sub>3</sub>SO<sub>3</sub>], and a hydrophobic fluoroelastomer, PVdF-HFP.

Moreover, sulfonated polyimides (SPIs) have been used to prepare polymer electrolyte membranes for nonhumidified fuel cells by the addition of a protic ionic liquid, diethylmethylammonium trifluoromethanesulfonate [dema][CF<sub>3</sub>SO<sub>3</sub>] (See Fig. 9.6) [78, 79]. The uniform, tough, and transparent membranes have good thermal stability (>300 °C) and ionic conductivity (>10<sup>-2</sup> S cm<sup>-1</sup> with an ionic liquid content higher than 67 %) under anhydrous conditions. A current density higher than 240 mA cm<sup>-2</sup> is achieved with a maximum power density of 100 mW cm<sup>-2</sup> at 80 °C when using a membrane in the H<sub>2</sub>/O<sub>2</sub> fuel cell operation under dry conditions.

Many other polymers, such as poly(ether ether ketone) (PEEK), polybenzimidazole derivative containing benzofuranone moieties (PBI-O-Ph), or poly(vinyl alcohol) (PVA),

have been used in order to prepare electrolytic membranes for fuel cells in combination with protic or aprotic ionic liquids [80–86]. Jothi et al. have synthesized a polymer membrane based on sulfonated poly(ether ether ketone) (SPEEK) and halogen-free ionic liquids containing imidazole cations of 1-ethyl-3-methylimidazolium,  $[C_2mim]^+$ , and anions of diethyl phosphate [87]. The composite membranes had good conductivity in the range of 1.25–3.16 mS cm<sup>-1</sup> at 145 °C under anhydrous environment, and the fuel cell including SPEEK/50 % ionic liquid membrane gave a maximum power density of 203 mW/cm<sup>2</sup> at the same temperature.

Alkaline polymer electrolyte fuel cells (APEFCs): two of the major limitations of PEMFCs are the use of expensive platinum-based catalysts and also the cost of PEM [88, 89]. Therefore, alkaline polymer electrolyte fuel cells have received a great attention, which presents several advantages, such as lower activation loss in alkaline medium, facile cathode kinetics permitting the use of abundant low-cost metal catalysts (Ni, Fe, Ag, etc.), and decreased oxidant reduction overpotential at high pH, thereby increasing the efficiency. The anion exchange membrane, which acts as an electrolyte to transport anions from cathode to anode, is one of the key components of alkaline fuel cells. Lin et al. have reported the photocopolymerization of ionic liquid monomer, 1-vinyl-3-methylimidazolium iodide [Vmim][I], with styrene and acrylonitrile in the presence of 2–10 % cross-linker divinylbenzene to obtain a membrane which was converted to their OH<sup>-</sup> forms by exchanging the iodide with hydroxide anions [90]. The membranes had hydroxide ion conductivities above  $10^{-2}$  S cm<sup>-1</sup> at room temperature and excellent chemical stabilities in high pH media at 60 °C, fulfilling the basic conductivity and chemical stability requirements [91].

### 9.5.3 Solar Cells

A solar cell is an energy production device that converts the energy of light into electricity. Dye-sensitized solar cells (DSSC) are proposed as an alternative to costly Si-solar cells, in which the electrolyte plays an important role alongside the porous  $TiO_2$  electrode. Many studies have been reported with the objective of getting solar cells using inorganic gelators-based ion gels with promising results. Briefly, it can be found that silica, TiO<sub>2</sub>, Al<sub>2</sub>O<sub>3</sub>, and ZnO nanoparticles or carbon nanotube (CNT) layers in combination with ionic liquids give ion gels for solar cells high efficiency as well as excellent stability [92–95]. Moreover, a combination of polymers with inorganic particles has also been reported as a candidate material for ion gels. Forsyth and coworkers studied poly(hydroxyethyl methacrylate-cotetraethylene glycol diacrylate) poly(HEMA-co-TEGDA) photopolymerized in I<sub>2</sub>containing ionic liquid as a gel electrolyte for DSSCs [96]. TiO<sub>2</sub> nanoparticles were used as a photoinitiator and a cogelator in gel forming. The results from DSSCs assembled using the ionic liquid-based polymer gel electrolyte showed energy conversion efficiency of 3.9 % at 1 sun (AM 1.5) and 5.0 % at 0.39 sun illumination. However, this chapter will focus on organic ion gel electrolytes.

The most studied polymer electrolytes for solar cells are based on PEO or PVdF. An electrolytic membrane based on PEO and an ionic liquid 1-methyl-3propylimidazolium iodide (PMII) has been reported as a novel candidate for DSSC since it has good ionic conductivity  $(3.56 \times 10^{-4} \text{ S cm}^{-1} \text{ when } 200 \text{ wt\%}$  of ionic liquid) as well as iodide anion which is beneficial for redox couple formation (I<sup>-</sup>/I<sub>3</sub>) [97]. More recently, M. Forsyth and coworkers studied PEO-PVdF-based polymer electrolytes in combination with alkyl imidazolium iodide-functionalized silica (SiO<sub>2</sub>-imI) to assemble a DSSC. The ionic conductivity of  $1.07 \times 10^{-4} \text{ S cm}^{-1}$  and a power conversion efficiency of 3.83 % were obtained under air mass 1.5 solar spectrum illumination at 100 mW cm<sup>-2</sup> with 8 wt% of SiO<sub>2</sub>-imI composite polymer electrolyte [98]. Soni et al. have investigated polymer gel electrolytes for DSSCs [99]. Indeed, PEO/PPO-based amphiphilic block copolymers were combined with 1-butyl-3-methylimidazolium iodide [C<sub>4</sub>mim][I] and iodide to synthesize a highly ordered polymer gel to be used in DSSCs and a 2.1 % solar to electricity conversion efficiency was achieved using a specific ruthenium-based dye D907.

Beyond the conventional polymers, polymeric ionic liquids-based gel polymer electrolytes have been also reported for solar cell applications. Azaceta et al. used poly(1vinyl-3-alkylimidazolium) iodide polymers mixed with 1-methyl-3-propylimidazolium iodide to formulate polymer electrolytes, which showed ionic conductivities in the range of 10<sup>-3</sup> to 10<sup>-7</sup> S cm<sup>-1</sup> at room temperature [100]. As expected, this ionic conductivity depends on the ionic liquid content. Finally, they prepared solar cells with an area of 1 cm<sup>2</sup> using mentioned polymer gel electrolytes to yield a maximum light-to-electricity conversion efficiency of 3.73 %. Continuing with poly(ionic liquid)-based gel electrolytes, poly(1-butyl-3-vinylimidazolium) bromide [PBvim][Br] and poly(1butyl-3-vinylimidazolium) bis(trifluoromethanesulfonyl)imide [PBvim][N(Tf)<sub>2</sub>] were dissolved at room temperature in ionic liquids to form gel electrolytes without using any volatile organic solvent [101]. Figure 9.7a shows the J-V curves of the fabricated DSSCs with mentioned poly(ionic liquid)s and poly(styrene-co-acrylonitrile) to compare. The cells based on [PBvim][N(Tf)<sub>2</sub>] gel electrolyte showed a maximum efficiency of 4.4 % under simulated air mass 1.5 solar spectrum illumination at 100 mW cm<sup>-2</sup> as well as higher long-term stability. Furthermore, bis-imidazoliumbased poly(ionic liquid) electrolytes for DSSCs were reported [102]. Indeed, poly(1butyl-3-vinylimidazolium-3-hexyl)imidazolium bis(trifluoromethanesulfonyl)imide  $[PBvim][C_6im][N(Tf)_2]_2$  electrolytes have been prepared and used for the fabrication of organic solvent-free quasi-solid-state DSSCs to obtain an efficiency of 5.92 % under the simulated air mass 1.5 solar spectrum illumination at 100 mW cm<sup>-2</sup>, which is higher than that of monocationic polymer gel electrolyte.

### 9.5.4 Supercapacitors

Electrochemical capacitors, also referred as supercapacitors or ultracapacitors, store energy using either ion adsorption (electrochemical double-layer capacitors EDLCs) or fast surface redox reactions (pseudocapacitors). In recent years, they have



**Fig. 9.7** The J–V curves of DSSCs containing liquid electrolytes, Poly(St-AN), [PBvim][Br], and [PBvim][N(Tf)<sub>2</sub>]-based electrolytes (polymer contents: 25 wt%) (**a**) Under simulated AM 1.5 solar spectrum irradiation at 100 mW cm<sup>-2</sup>. (**b**) In the dark [101]

received much attention, mainly due to their high-power density, long life cycle ( $\sim 10^5$  to  $10^6$  charge–discharge cycles), and fast charging (few seconds) [51, 103–106]. However, one of the main drawbacks of current capacitors is the use of aqueous or organic electrolytes, and with that the supercapacitors can show narrow cell voltage (limited to ~ 1.2 V) or high flammability and toxicity [41]. Ion gels are suitable electrolytes to avoid these inconveniences as they have wider electrochemical potential window and thermal stability.

In order to obtain ionic liquid-based gel polymer electrolytes, several polymer or copolymer matrices have been used, such as poly(vinylidene fluoridehexafluoropropylene) PVdF-HFP, poly(methyl methacrylate) PMMA, polystyrenepoty(ethylene oxide) PS-PEO, poly(vinyl alcohol) PVA, or polyacrylonitrile PAN [41, 45, 107–109]. As an example, recently Pandey and Hashmi prepared an ionic liquid gel polymer electrolyte based on 1-ethyl-3-methylimidazolium tris(pentafluoroethyl) trifluorophosphate [C<sub>2</sub>mim][FAP] and PVdF-HFP copolymer that exhibits an excellent thermal stability, a wide electrochemical window of ~4.4 V (from -2.2 to 2.2 V), and a high ionic conductivity of  $\sim 2 \times 10^{-3}$  S cm<sup>-1</sup> at room temperature [103]. Solid-state supercapacitors based on multiwalled carbon nanotube (MWCNT) electrodes and ion gel electrolytes have been fabricated; a good cycling performance with~82 % capacitance retention after 10,000 charge-discharge



**Fig. 9.8** (a) Temperature dependence of ionic conductivity of the ionic liquid gel polymer electrolyte film. Inset: The corresponding log ( $\sigma$  T<sup>1/2</sup>) vs 1/(T – T<sub>0</sub>) plot. (b) Cyclic voltammetry curves of EDLC cells at different scan rates. On the graph, there is a picture of a transparent and free-standing gel polymer electrolyte film. (c) Variation in the capacitance values of the EDLC cells [110]

cycles was achieved. Furthermore, the modified MWCNT electrodes show a specific capacitance of ~76 F g<sup>-1</sup> and the supercapacitors show specific energy and specific power of ~17.2 Wh kg<sup>-1</sup> and ~18.9 kW kg<sup>-1</sup>, respectively. The synthesis of 1-ethyl-3-methylimidazolium tetracyanoborate [C<sub>2</sub>mim][B(CN)<sub>4</sub>] and PVdF-HFP copolymer-based ion gel used as an electrolyte in EDLCs has been also reported [110]. The ion gel showed excellent thermal stability up to 310 °C, an electrochemical window of ~3.8 V, and a high ionic conductivity of ~9×10<sup>-3</sup> S cm<sup>-1</sup> at room temperature (See Fig. 9.8). The EDLCs show single electrode-specific capacitance values of ~34.4 F g<sup>-1</sup> and the specific energy and specific power of the capacitor are ~3.5 Wh kg<sup>-1</sup> and ~4.2 kW kg<sup>-1</sup>, respectively.

Besides the most common lithium ion-conducting gel polymer membranes, magnesium ion-conducting systems have also been reported to be used in electrochemical power storage devices, including EDLCs [111]. 1-ethyl-3-methylimidazolium trifluoromethanesulfonate  $[C_2mim][CF_3SO_3]$  and PVdF-HFP copolymer-based electrolytes were prepared to be used in an EDLC which contains activated charcoal

(AC) electrodes. By the incorporation of magnesium salt and ethylene carbonatepropylene carbonate cosolvent to the electrolyte, an important improvement was achieved on the properties of EDLCs. Indeed, 136 F g<sup>-1</sup> of the optimal capacitance value of AC was measured, which corresponds to the specific energy and power density of ~18.8 Wh Kg<sup>-1</sup> and ~6.67 kW kg<sup>-1</sup>, respectively. On the other hand, by the addition of graphene nanosheets as an ionic conducting promoter to the common ionic liquid gel polymer electrolytes, an improved electrochemical behavior can be obtained: smaller internal resistance, higher specific capacitance, cycling stability, and better rate performance, as well as good thermal stability up to 400 °C [112].

Ion liquid-based gel polymer electrolytes in combination with electronically conducting polymer-based electrodes, such as PEDOT, have been studied to prepare supercapacitors [113, 114]. For instance, Pandey et al. have characterized devices with specific PEDOT electrode capacitance of ~154.5 F g<sup>-1</sup>, maximum specific energy of 6.5 Wh kg<sup>-1</sup>, and specific power of 11.3 kW kg<sup>-1</sup>.

Ion gels play an important role to obtain all-solid-state flexible, stretchable, and lightweight supercapacitors, which are very interesting energy-storage devices for many applications [115, 45]. Kang et al. have fabricated flexible supercapacitors using bacterial nanocellulose papers coated with carbon nanotubes as electrodes and an ion gel based on PS-PEO-PS triblock copolymer with an ionic liquid 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide, as electrolyte [109]. While the hydrophobic PS unit of the membrane ensured good adhesion to the carbon nanotube electrode via van der Waals interactions, the PEO block retained a hydrophilic ionic liquid in the ion gel system. A flexible energy-storage device was successfully fabricated and used to light a yellow light-emitting diode.

#### 9.5.5 Actuators

In recent years, polymer actuators have attracted much attention for applications in robotics or medical devices due to their soft motion, simple structure, flexibility, and lightweight. In particular, ionic electroactive polymer actuators (polymer-metal composite actuators, conductive polymer actuators, and carbon nanotube actuators), which are driven by migration or diffusion of ions, exhibit a large deformation with low voltage application (<5 V) [116–118]. However, the main drawback arises when working in dry conditions, especially due to solvent evaporation. In this respect, ion gels have been studied as promising electrolytic membranes for this type of actuators. Fukushima, Aida, and coworkers were pioneers to report bucky-gel actuators fabricated through layer-by-layer casting. The actuators were ready to work without the need of further encapsulation [119-122]. In a typical example, the ion gel is composed of an ionic liquid, such as [C<sub>2</sub>mim][N(Tf)<sub>2</sub>], and PVdF-HFP copolymers. The gel is then placed between two bucky-gel-electrode layers containing singlewalled carbon nanotubes (SWCNT). They observed that the curvature of the actuator is proportional to the voltage applied and the thickness of the device; i.e., at a given voltage, thinner actuator's curvature is larger than the thicker ones.

Apart from conventional PVdF-HFP copolymer, other polymers were used to prepare actuator ion gels. For instance, Watanabe and coworkers have fabricated polymer actuators using ion gel electrolytes that contained 1-ethyl-3methylimidazolium bis(trifluoromethanesulfonyl)amide  $[C_2 mim][N(Tf)_2]$  and polystyrene–block-poly(methyl methacrylate)–block-polystyrene triblock copolymer (PS-b-PMMA-b-PS) synthesized by successive atom-transfer radical polymerizations (ATRPs) [38]. PS is not compatible with  $[C_2mim][N(Tf)_2]$ , while PMMA phase can be dissolved in the ionic liquid to form an ion conduction pathway. This leads naturally to the self-assembly of PS-b-PMMA-b-PS copolymers in the ionic liquid giving them gel properties. Indeed, the affinity and repulsion of the polymer blocks to  $[C_2mim][N(Tf)_2]$  forced the formation of PS sphere domains that served as physical cross-linking points, as observed by the atomic force microscope (Fig. 9.9a). This ion gel electrolyte exhibits high ionic conductivity (> $10^{-3}$  S cm<sup>-1</sup>) at room temperature and was used for a trilaminar ionic polymer actuator sandwiched between two carbon composite electrodes. After applying low voltages to the actuator, less than 3 V, it is softly bent toward the anodic side. The same authors have studied other polymers, such as sulfonated polyimides (SPIs) or polyethersegmented polyurethaneurea (PEUU), in ion gel electrolyte formation for polymer actuators [123]. SPIs provide strength to the electrolyte due to the rigid aromatic backbone, and the counter-cations make it compatible with ionic liquids. As a result,



**Fig. 9.9** (a) Chemical composition of triblock ion gel electrolyte and the membrane picture obtained by AFM; (b) Arrhenius plots of ionic conductivity and displacement of ion gel actuators for the ion gels containing 20 % of  $[C_2mim][N(Tf)_2]$  but different block lengths [38]

the SPI/IL exhibited favorable mechanical properties (elastic modulus >10<sup>7</sup> Pa) together with a high ionic conductivity ( $10^{-3}$  S cm<sup>-1</sup>). The best trilaminar actuator obtained using SPI/IL ion gel electrolyte, reported in the literature, exhibits a relatively large displacement and high-speed response, keeping 80 % of the initial displacement even after more than 5,000 cycles [124].

# 9.5.6 Emerging Applications: Electrochemical Sensors, Optoelectronic Devices, Bioelectronics, Gas Separation Membranes, Catalytic Membranes, Drug Releases

Ion gels are finding more and more applications in different areas than the ones described before. In this section, we describe some of the most interesting emerging application areas of ion gels.

Electrochemical Sensors, Optoelectronic Devices, and Bioelectronics In the field of sensors, membranes based on poly(vinyl chloride) (PVC), ionic liquid 1-butyl-3-methylimidazolium hexafluorophosphate [C<sub>4</sub>mim][PF<sub>6</sub>], and polyazacycloalkane as ionophore were synthesized by Coll et al. and used in ion-selective electrodes as they exhibited a selective response to the hydrophilic anion sulfate [125]. Later on, Shvedene et al. have fabricated more polymer membranes for selective electrodes containing PMMA or PVC and ionic liquids [126]. The ionic liquid works as both plasticizer and ion-responsive media, and the electrodes obtained demonstrated good and stable response to ions (cations and anions). Those sensors were successfully designed to detect detergents. On the other hand, and mainly due to a biocompatibility of ionic liquids with biomolecules and enzymes, ion gels have been studied for biosensors applications [127, 128]. For instance, a film based on Nafion and a hydrophobic ionic liquid [C<sub>4</sub>mim][PF<sub>6</sub>] that can be used to immobilize and entrap horseradish peroxidase (HRP) and still retain its biological activity has been reported [129]. Therefore, it can be used for biosensors and biocatalysis applications as well.

Recently Owens and coworkers, who are pioneers in using ion gels for *bioelectronics*, have reported ion gels-assisted electrodes for applications in long-term cutaneous recordings [130]. They fabricated electrodes with gold and PEDOT:PSS, which were coated with ion gels. The ion gel decreased impedance at the interface with human skin, and they maintained a steady value over several days, making them suitable for a noninvasive, long-term monitoring of human electrophysiological activity (Fig. 9.10).

*Electrochromic devices* based on ion gels have been reported by Diamond and coworkers [131, 132]. The phosphonium ionic liquid was functionalized by a viologen molecule in order to achieve an electrochromic material, which was at the same time part of the electrolyte in an ion gel. The coloration efficiency of the device was 10.72 cm<sup>2</sup> C<sup>-1</sup> and of relatively fast switching kinetics (221 s to obtain 95 % of absorbance) when compared with other electrochromic ionic liquids (up to 18,000 s).



**Fig. 9.10** Schematic representation of the electrode positions on an arm. The working electrode (Ionic liquid gel+PEDOT:PSS/Au dry electrode) and counter electrode (C.E.) were placed on the forearm, 5 cm away from each other. The reference electrode (R.E.) was placed on the arms, 30 cm away from the W.E. [130]

Recently Lodge, Frisbie, and coworkers have used block copolymer-based ion gel to prepare flexible, low-voltage, emissive *displays* on plastic [133]. The patterned ion gels contain redox-active luminophores and triblock copolymer of polystyrene–block-poly(methyl methacrylate)–block-polystyrene, where the solvophobic poly styrene end blocks associate form micelles in 1-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide [ $C_2$ mim][N(Tf)<sub>2</sub>].

**Gas Separation Membranes** The electrolytic properties of ion gels and their applications in electrochemical devices are already widely explained; however, the ability of ionic liquids to dissolve a wide range of species, gases among others, make them suitable also for other types of applications, such as separation membranes.  $CO_2$ ,  $CH_4$ ,  $C_2H_6$ ,  $C_2H_4$ ,  $O_2$ , and  $N_2$  are some of the gases that can be dissolved in ionic liquids [134].  $CO_2$  is one of the most common and well-known global warming driver, which can be captured by ionic liquid-based membranes [135]. For instance, PVdF and  $[C_4mim][BF_4]$ -based polymeric membranes have been studied to remove acid gases such as  $H_2S$  and  $CO_2$  from crude natural gas, in which the permeability coefficient was increased when the ionic liquid content increased [136, 137].

**Catalytic Membranes** Ion gel membranes have been reported to be used as catalytic membranes or as a reaction media in biocatalysis. Liu et al. have reported the encapsulation of horseradish peroxidase (HRP) into an ionic liquid  $[C_4mim][BF_4]$ -based silica sol–gel matrix [138]. The specific activity of HRP enhanced dramatically, about

30-fold greater than that in silica gel without ionic liquid, and an excellent thermal stability of HRP was obtained after immobilizing it in ionic liquid-based matrix. It was suggested that the ionic liquid was responsible for the stabilization and protection of the immobilized HRP.

**Ion Gels for Drug Release** Ion gels that are able to lose gradually the ionic liquid are promising candidates to be used for drug release. Therefore, these ion gels operate in contrast to those described previously, i.e., ionic liquid leaching is required and controlled [2]. It has been demonstrated that ionic liquids can dissolve compounds with pharmaceutical activity that are insoluble or poorly soluble in the common aqueous or organic solvents, making them a promising alternative for drug solubility [139–141].

#### 9.6 Summary and Outlook

The aim of this chapter was to give a general overview of ion gels and more in detail the use of polymer-based ion gels in electrochemical applications. Therefore, the first part of the chapter provides the definition and properties of ion gels, as well as preparation methods, such as swelling a polymer in an ionic liquid, solution casting, or direct polymerization of monomers in an ionic liquid.

Within the last 10 years, there has been a growing interest for polymer-based ion gels, probably due to the association of unique properties and their promising use in many applications, especially in electrochemical devices. Ion gels have been reported in this chapter revealing that through the polymer chemical structure and the ionic liquid fraction, (i) first the morphology of the gel can be controlled and (ii) second the mechanical properties and the ionic conductivity can be tuned independently. Without doubt, the richness, in terms of physicochemical properties, of ionic liquids and polymers makes this type of ion gels very attractive for future researches. Considering the mentioned properties of ion gels, the applications have been reported in the second part of the chapter, which are mainly focused on energy electrochemical devices. However, it is worth to mention the new properties such as biocompatibility of some ionic liquids that can be used to fabricate ion gels with applications in sensors or bioelectronics.

The intimate relationship between ion transport and the three-dimensional polymeric network has been addressed for specific polymer/ionic liquids, but is still not fully understood in detail and should definitely be mapped as a function of composite components. This again opens up a vast field of research, extremely challenging in terms of control of the morphologies and measure of the local ion dynamics toward the investigation of the ions' confinement effects in organic ion gels. Indeed, the use of multifunctional polymers such as block copolymers can provide additional functionalities to the ion gel (electron conductor, photoresponsive, etc.) or selective affinity with the ionic liquids, leading to the association of new properties or achieving original controlled morphologies.

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## **Chapter 10 Structural Aspect on Li Ion Solvation in Room-Temperature Ionic Liquids**

Kenta Fujii, Shiro Seki, Hiroyuki Doi, and Yasuhiro Umebayashi

### **10.1 Introduction**

As is well recognized now, room-temperature ionic liquids (ILs) possess many advantages for electrochemistry due to their unique properties such as high ionic conductivity, wide electrochemical window, good chemical and thermal stabilities, non-flammability, and non-volatility. So, ILs have been widely applied to chemical synthesis and separation fields as a green solvent and also new electrolyte for electrochemical devices such as Li secondary batteries [1-4]. The ILs generally consist of bulky organic cations such as 1-alkyl-3-methylimidazolium [C<sub>n</sub>mim]<sup>+</sup>, N-alkyl-N-methylpyrrolidinium  $[C_n Pyr]^+$ , quaternary ammonium, etc., and inorganic and/ or organic anions such as tetrafluoroborate  $[BF_4]^-$ , hexafluorophosphate  $[PF_6]^-$ , and bis(trifluoromethylsulfonyl)imide  $[N(Tf)_2]^-$ . Therefore, the physicochemical properties of a solvent can be easily controlled by changing a combination of cation and anion, which is one of advantages in ionic liquid chemistry. In electrochemical applications,  $[N(Tf)_2]^-$  and its analogue bis(fluorosulfonyl)amide  $[FSI]^-$  have so far been widely used as the anion of ILs. These anions combined with  $[C_n mPyr]^+$  or *N*-methyl-*N*-(2-methoxyethyl)ammonium [DEME]<sup>+</sup> are well utilized for Li battery applications using ILs, which is ascribed to stable formation of solid electrolyte interface (SEI) [5–10]. Furthermore, other electrochemical device applications

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(field effect transfer [11, 12] and electric double layer [13]) have been reported, particularly in FSI-based ILs.

In development of ILs for electrochemical devices such as Li secondary batteries, it is important to reduce the viscosity, because a lower viscous solvent leads to a higher ionic conductivity and transport properties. Therefore, several low viscous ILs have been synthesized and proposed up until now [14–18]. Here, we focus on FSI-based ILs, which is well known as one of low viscous ILs. [FSI]<sup>-</sup> has a similar molecular structure to  $[N(Tf)_2]^-$ , i.e., the CF<sub>3</sub> groups of  $[N(Tf)_2]^-$  are only substituted by F atoms. In spite of similar molecular structure between [FSI]- and  $[N(Tf)_2]^-$ , it is established that the FSI-based ILs show a significantly lower viscosity than the  $N(Tf)_2$ -based ones [5, 6, 19]. For example, the viscosity of [C<sub>2</sub>mim] [FSI] is 17 mPa s, which is appreciably lower than that of  $[C_2 mim][N(Tf)_2]$ , 28 mPa s. In general, the addition of Li salt to solvent IL leads to the increase in the viscosity. Indeed, the viscosity of N(Tf)2-based ILs significantly increases with the addition of Li[N(Tf)<sub>2</sub>] salt. Interestingly, the increase in the viscosity of FSI-based ILs with the addition of Li[FSI] salt is appreciably small relative to the corresponding [N(Tf)<sub>2</sub>] system [19], resulting in excellent performance of electrochemical devices using the FSI-based ILs. Tsuzuki et al. reported temperature dependence of the viscosity of  $[C_2 mim][FSI]$  and  $[C_2 mim][N(Tf)_2]$  with the corresponding Li salts [19]. The viscosity strongly depends on temperature in the  $[N(Tf)_2]$  system, and then the relative viscosity, i.e.,  $\eta$ (neat IL)/ $\eta$ (IL with 0.32 mol kg<sup>-1</sup> Li salt), largely changes from 1.4 (10 °C) to 1.9 (80 °C). On the other hand, there is no or less temperature dependence of the relative viscosity for the FSI system, and the extent is very small within 0.1 in the same temperature range. The ionic conductivity and ionic diffusion have been also reported. The self-diffusion coefficients of ions (Li<sup>+</sup>, IL cation and anion) in the FSI-based IL solutions were investigated in detail by both experimental and theoretical methods and compared with those in the [N(Tf)<sub>2</sub>]based ones at a microscopic level [19-21]. Here, note that such dynamic properties of IL systems are strongly related to the static liquid structure and Li ion solvation. We have therefore studied conformational isomerism and liquid structure in neat FSI- and [N(Tf)<sub>2</sub>]-based ILs by using Raman/IR spectroscopic and X-ray/neutron scattering experiments and theoretical calculations [22-36]. Particularly, it is indispensable to elucidate solvation structure of Li ion in the ILs as the fundamental knowledge on understanding Li ion reactivity and mobility, which plays a key role for improving Li ion battery performance at the molecular level. In this chapter, we describe our recent works on Li ion solvation structure in the [FSI]- and [N(Tf)<sub>2</sub>]based ILs and discuss their difference and similarity from the structural aspects.

## 10.2 Liquid Structure of Neat ILs

Solvation of metal ion in electrolyte solutions strongly depends not only on the metal ion–solvent interactions but also on the solvent–solvent interactions and/or liquid structure in the bulk [37–40]. When a metal ion is introduced into a solvent, (1) the metal ion destroys the solvent structure to create isolated solvent molecules

around it as the first step and then (2) the metal ion is solvated with the isolated solvent molecules to form a solvation cluster as the second step. The liquid structure in the bulk is thus effective for metal ion solvation, particularly in the former step. So, we firstly describe about liquid structure of neat ILs (mainly,  $[C_2mim][FSI]$  and  $[C_2mim][N(Tf)_2]$ ) to deeply understand Li ion solvation in the IL systems.

For investigation of static liquid structure in the bulk ILs, it is well known that X-ray and neutron scatterings (or diffractions) are one of powerful tools to directly determine the interaction distance between ions. Furthermore, computer simulations are also useful to investigate a detailed static structure at the atomistic level, and thus often combined with X-ray/neutron experimental data. Soper et al. firstly applied such combination of experimental and simulation data to the structural investigation of ILs, i.e., the large-angle neutron diffraction with empirical potential structure refinement (EPSR) based on Monte-Carlo simulations [41, 42]. We also reported liquid structure of various IL systems such as imidazolium- [27, 32, 35], pyrrolidinium- [26, 43], and ammonium [30, 44]-based ILs studied by large-angle X-ray scattering or high-energy X-ray diffraction (LAXS and HEXRD, respectively) with the aid of molecular dynamics (MD) simulations. In general, the liquid structure and ion-ion interaction obtained from X-ray/neutron experiment or computer simulation study are discussed in terms of radial distribution function given by Furrier transformation of the structure factor, S(q) where q denotes the scattering vector. Figure 10.1a shows X-ray radial distribution functions,  $G^{exp}(r)$ s as the form of  $r^2[G(r) - 1]$  for [C<sub>2</sub>mim][FSI] [36] and [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] [35] observed by HEXRD experiments. The HEXRD measurements were performed by using highenergy X-ray diffraction apparatus of BL04B2 beam line at SPring-8 (Japan Synchrotron Radiation Research Institute, JASRI, Japan) [45–47], and their details (instruments and data corrections) are described in our previous work [26, 35]. As can be seen in this figure, the experimental  $r^2[G^{exp}(r) - 1]$  exhibits the sharp and broad peaks at r < 3 Å and r > 5 Å, respectively, for both [C<sub>2</sub>mim][FSI] (solid line, black) and  $[C_2 mim][N(Tf)_2]$  (solid line, gray). The sharp peaks at r < 3 Å are mainly assigned to the intramolecular interactions of cation and anion, whereas the three broad peaks at around 5, 9, and 15 Å to the intermolecular interactions of cationcation, anion-anion, and cation-anion components [27, 35]. The peak centered at around 5 Å can be assigned to the first neighboring cation-anion interactions, which are discussed below in detail. On the other hand, two broad peaks at around 9 and 15 Å may be originated from the long-range correlations between ions (including cation-anion, cation-cation, and anion-anion) in the second and the third neighbor regions. Here, note that the peak positions of 9 and 15 Å are slightly shorter for the  $[C_2 mim][FSI]$  than for the  $[C_2 mim][N(Tf)_2]$  due to smaller anion size of  $[FSI]^-$  than  $[N(Tf)_2]^-$ . In this long r-range, the peak intensities or oscillations in the  $r^2[G^{exp}(r) -$ 1] for the  $[C_2mIm][FSI]$  are significantly weaker than those for the  $[C_2mIm][N(Tf)_2]$ . This implies that the extent of the long-range ordering or structuredness is lower in the FSI system than in the  $[N(Tf)_2]$  one. Figure 10.1b shows X-ray weighted radial distribution functions derived from MD simulations,  $G^{MD}(r)$ s [36]. It is clear that the observed  $G^{\exp}(r)$ s are well represented by the theoretical  $G^{MD}(r)$ s for both systems. The total  $G^{MD}(r)$  can be deconvoluted into intra- and intermolecular components, i.e.,  $G^{\text{MD}}_{\text{intra}}(r)$  and  $G^{\text{MD}}_{\text{inter}}(r)$ . The  $G^{\text{MD}}_{\text{inter}}(r)$  is composed of three partial  $G^{\text{MD}}_{\text{inter}}(r)$ s



**Fig. 10.1** X-ray radial distribution functions as a form of  $r^2[G(r)-1]$  for neat [C<sub>2</sub>mim][FSI] (*black*) and [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] (*gray*) obtained by (**a**) HEXRD experiments and (**b**) MD simulations [36] and [62]

for cation–anion, anion–anion, and cation–cation components, which are shown in Fig. 10.2. In the partial  $G^{\text{MD}}_{\text{inter}}(r)$ s for the [C<sub>2</sub>mim][FSI] system, the cation–anion correlation in the first neighboring sphere (3–7 Å) is mainly composed of the peaks at 3.4, 4.5, and 5.6 Å. The 3.4 Å peak corresponds to the closest atom–atom interaction in this system, which is mainly ascribed to the carbon (imidazolium ring)– oxygen ([FSI]) interaction [36]. The same is applied to the [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] system, i.e., the closest carbon (imidazolium ring)–oxygen ([N(Tf)<sub>2</sub>]) interaction appears at around 3.4 Å. The partial  $G^{\text{MD}}_{\text{inter}}(r)$  for the cation–anion component also has the broad peak centered at 11 Å, which corresponds to the cation–anion interaction in the second neighbors. For the anion–anion components, the broad correlations appear at around 8 Å as the first peak. The cation–cation correlations are also found at around 8 Å in the  $G^{\text{MD}}_{\text{inter}}(r)$ , although they are significantly weak in the intensity. This is because [C<sub>2</sub>mim]<sup>+</sup> is constructed by H, C, and N atoms with small X-ray scattering factor, *f*, unlike [FSI]<sup>-</sup> with large ones of F and S. It is thus concluded that



**Fig. 10.2** Partial  $G^{\text{MD}_{inter}}(r)$ s for the C<sub>2</sub>mim–FSI (*red*), FSI–FSI (*blue*) and C<sub>2</sub>mim–C<sub>2</sub>mim (*gray*) interactions derived from MD simulations, together with the corresponding total  $G^{\text{MD}_{inter}}(r)$  (*black*) [36]

the anion–anion correlations mainly contribute to the 8.5 Å peak observed in the total  $G^{\exp}_{inter}(r)$ , whereas the cation–cation ones less contribute to the total  $G^{\exp}_{inter}(r)$ .

With regard to the first neighboring cation-anion interaction, we further analyzed the MD results to evaluate space distribution function, SDF. Figure 10.3a shows SDF for  $[FSI]^-$  (center of mass) around C<sub>2</sub>mim cation, calculated with the MD trajectories [36]. It is easily found in this figure that [FSI]<sup>-</sup>s distribute above and below the imidazolium ring plane and near to the C4 and the C5 carbons. The coordination number, n(r) of [FSI]<sup>-</sup>s around the C<sub>2</sub>mim cation, is estimated to be 3.8 (approximately 4). With an increase in the probability density from 1.5 to 2.4, the distribution of [FSI]- still remained above and below the imidazolium ring, whereas that near to C4 and C5 positions disappeared (Fig. 10.3b). This means that the potential surface of the interaction between [FSI]<sup>-</sup> and [C<sub>2</sub>mim]<sup>+</sup> is deeper at above and below the imidazolium ring than at C4 and C5 positions. Here, note that the H of C2 position of the imidazolium cation is capable of forming a hydrogen bonding interaction with the anion in the ILs composed of smaller-size anions such as Cl, Br, and BF<sub>4</sub> [48]. In FSI system, however, no significant probability of [FSI]<sup>-</sup> is found to the direction of C2-H bond in the SDF. It is thus expected that the hydrogen bonding C2-H···O ([FSI]<sup>-</sup>) cannot be formed in [C<sub>2</sub>mim][FSI] due to bulkiness of anion. For [C<sub>2</sub>mim][N(Tf)<sub>2</sub>] system (Fig. 10.3c, d), we can see that the [C<sub>2</sub>mIm]<sup>+</sup> is also surrounded by four anions in the first neighbor region, and the orientation is also similar to the  $[C_2mim][FSI]$  system. From these results, we can propose that there is no significant difference in the closest cation-anion interactions between [FSI] and [N(Tf)<sub>2</sub>]systems in terms of static structure, although the size of [FSI]<sup>-</sup> is appreciably smaller than that of  $[N(Tf)_2]^-$ .



**Fig. 10.3** Space distribution functions, SDFs for center of mass of  $[FSI]^-$  around  $[C_2mim]^+$ . The colored clouds represent the isoprobability surfaces of (**a**) 1.5 and (**b**) 2.4 larger probability density relative to the bulk one. The SDFs for the N(Tf)<sub>2</sub> system with (**c**) 1.5 and (**d**) 2.4 larger probability density are also shown [36]

### 10.3 Li Ion Solvation: Raman Spectroscopic Study

As mentioned in Introduction, lithium batteries using ILs as an electrolyte have been studied in terms of the development of high-energy density battery with high safety. The battery performances such as current density and charge–discharge reactivity at electrolyte/electrode interface are closely related to the ionic conductivity in ILs and the redox reaction and the desolvation behavior of Li ion at the interface, respectively. Here, note that they are directly and/or indirectly influenced by the Li ion solvation, i.e., the solvation number of IL anions bound to Li ion and the strength of Li ion–IL anion interactions. Therefore, the Li ion solvation structure in ILs has been widely investigated by both experimental [49–52] and theoretical [53–55] techniques.



**Fig. 10.4** *Top*: LiFSI salt concentration dependence of Raman spectra observed for the [C<sub>2</sub>mim] [FSI] solutions in the frequency range of (**a**) 680–800 cm<sup>-1</sup> and (**b**) 1,160–1,260 cm<sup>-1</sup> at 298 K. *Bottom*: Typical curve fitting results for the solutions (0.772 mol kg<sup>-1</sup> LiFSI concentration) in the range of (**c**) 680–800 cm<sup>-1</sup> and (**d**) 1,160–1,260 cm<sup>-1</sup> [59]

We also studied the [FSI]- and [N(Tf)<sub>2</sub>]-based IL solutions including Li ion by Raman/IR spectroscopy and quantum calculations to elucidate the Li ion solvation structure [56–59]. Figure 10.4a shows typical Raman spectra in the range of 680– 800 cm<sup>-1</sup> observed for [C<sub>2</sub>mim][FSI] solutions containing Li[FSI] salt (0–0.772 mol kg<sup>-1</sup>). At Li[FSI]=0 mol kg<sup>-1</sup> (neat IL), [C<sub>2</sub>mim][FSI] exhibits a main peak at 731 cm<sup>-1</sup>, which can be assigned to the  $\nu_{\rm s}$ (N–S) vibration of [FSI]<sup>-</sup> (free [FSI]) [24]. The Raman band at 731 cm<sup>-1</sup> is gradually weakened with increasing Li[FSI] concentration, and then the higher-shifted band at 744  $cm^{-1}$  is intensified. The same behavior is observed in the [N(Tf)<sub>2</sub>]-based RTILs [56, 57, 60, 61], i.e., Raman band of  $[N(Tf)_2]^-$  at around 740–750 cm<sup>-1</sup> is weakened and shifted to the higher frequency with increasing metal ion concentration. According to our previous work [56, 57, 60, 61], the former band is assigned to the  $[N(Tf)_2]^-$  in the bulk (free  $N(Tf)_2$ ) and the latter to the  $[N(Tf)_2]^-$  bound to  $Li^+$  ion (bound  $[N(Tf)_2]$ ). Thus, in the FSI system, it is concluded that the observed 731 and 744 cm<sup>-1</sup> bands are originated from free and bound [FSI], respectively. Figure 10.4b shows Raman spectra of the  $\nu_{\rm s}$ (S–O) vibration of [FSI]<sup>-</sup> in the range of 1,220–1,230 cm<sup>-1</sup>. The Li[FSI] concentration dependence of the  $\nu_s$ (S–O) vibration is similar to that of the  $\nu_{\rm s}$ (N–S) vibration described above, indicating that the Raman band at lower frequency side is originated from the free FSI and that at higher one from the bound FSI. To discuss the spectral variations in detail, in general, the observed Raman spectra are deconvoluted into some single bands by using curve fitting analysis. Typical results examined in the range of 680-800 and 1,150-1,280 cm<sup>-1</sup> are shown in Fig. 10.4c, d, respectively. As can be seen in these figures, both Raman spectra observed for Li[FSI]=0.177 mol kg<sup>-1</sup> solution are well explained in terms of the free and bound [FSI] (solid gray and blue lines) and some [C<sub>2</sub>mim] (bashed line) components. With an increase of the salt concentration, the free [FSI] bands centered at 731 and 1.220 cm<sup>-1</sup> decrease and the bound bands at 744 and 1.228 cm<sup>-1</sup> intensify without appreciable change in peak frequency and half width at half maximum. By analyzing the integrated intensity of the free band extracted, the number of [FSI]<sup>-</sup>s solvated to Li<sup>+</sup> ion can be estimated, as follows.

The integrated intensity,  $I_{\rm f}$ , of free [FSI] in the bulk is given as  $I_{\rm f} = J_{\rm f} m_{\rm f}$ , where  $J_{\rm f}$ and  $m_{\rm f}$  stand for the Raman scattering coefficient and the concentration, respectively, of free [FSI]. By taking into account a mass balance equation,  $m_f = m_T - m_b = m_T - m_r$  $nm_{\rm Li}$ , where  $m_{\rm T}$ ,  $m_{\rm b}$ ,  $m_{\rm Li}$  denote concentrations of total [FSI], bound [FSI], and Li<sup>+</sup> ion, respectively, and n is the number of [FSI]<sup>-</sup> bound to the Li<sup>+</sup> ion. As the result, we obtain the following equation:  $I_f/m_{Li} = J_f(m_T/m_{Li} - n)$ . Plots of  $I_f/m_{Li}$  values against  $m_{\rm T}/m_{\rm Li}$  give a straight line with the slope (=J<sub>f</sub>) and the intercept (=-J<sub>f</sub>n), which is shown in [59]. The solvation number, n, is thus obtained according to n = -slope/intercept and was estimated to be 3.0(1) and 2.9(1) at 731 and 1,220 cm<sup>-1</sup> bands, respectively, at 298 K. This suggests that Li ion is solvated with three [FSI]-s in the [C<sub>2</sub>mim][FSI] at 298 K. The solvation number of Li ion in the [N(Tf)<sub>2</sub>]-based ILs was also estimated in the concentration range of  $LiN[(Tf)_2] < 1 \text{ mol } dm^{-3}$  by the similar analysis [56–58]. According to our Raman spectroscopic study with the aid of DFT calculations, the Li ion is solvated with two [N(Tf)<sub>2</sub>]-s acting as a bidentate ligand, resulting in a tetrahedrally four-coordinated structure with O atom of two bidentate  $[N(Tf)_2]$ -s. We can point out here that the n (=3) in [FSI] system significantly differs from the n (=2) in [N(Tf)<sub>2</sub>] system. To discuss a possible solvation structure of Li ion in the [FSI] system, we extended our Raman study to the temperature dependence of the *n*.

Figure 10.5 shows temperature dependence of the solvation number, *n* values for the Li[FSI]/[ $C_2$ mim][FSI] system, together with those for the Li[N(Tf)<sub>2</sub>]/[ $C_2$ mim]



**Fig. 10.5** Temperature dependence of the solvation number, *n*, of Li ion in  $[C_2mim][FSI]$  estimated by using Raman bands at 1,220 cm<sup>-1</sup> (*red*) and 727 cm<sup>-1</sup> (*blue*), together with that in  $[C_2mim]$  [N(Tf)<sub>2</sub>] (*black*) [59]

 $[N(Tf)_2]$  one. In the [FSI] system, the *n* gradually decreases with increasing temperature. This indicates that the solvated  $[FSI]^-$  around Li ion are liberated to the bulk at high temperature to decrease the *n* from 3 (298 K) to 2.5 (370 K). On the other hand, there is no temperature dependence on the solvation number in the  $[N(Tf)_2]$  system, i.e., the *n* value is almost a constant at any temperature examined here. This implies that the desolvation of bidentate  $[N(Tf)_2]^-$  ligand coordinated to Li ion does not occur or is very difficult in the  $[N(Tf)_2]$  system. From these results, we can propose that the Li ions in the  $[C_2mim][FSI]$  coexist as  $[Li(FSI)_3]^{2-}$  and  $[Li(FSI)_2]^-$  at high temperature. Furthermore, it is expected that the  $[Li(FSI)_3]^{2-}$  complex involves both bidentate and monodentate  $[FSI]^-$ s that strongly and weakly coordinated to Li ion, respectively, resulting in the desolvation of weakly coordinated monodentate  $[FSI]^-$  from the  $[Li(FSI)_3]^{2-}$  complex at high temperature.

The temperature dependence of the n value can be quantitatively analyzed to give an equilibrium constant, K, with regard to the [FSI] desolvation process by assuming the following equilibrium equation [59].

$$\begin{bmatrix} \text{Li}(\text{FSI})_3 \end{bmatrix}^{2^-} = \begin{bmatrix} \text{Li}(\text{FSI})_2 \end{bmatrix}^- + \begin{bmatrix} \text{FSI} \end{bmatrix}^-$$
  
$$K = \begin{bmatrix} \text{Li}(\text{FSI})_2 \end{bmatrix}^- / \begin{bmatrix} \text{Li}(\text{FSI})_3 \end{bmatrix}^{2^-} = (3-n) / (n-2)$$



Fig. 10.6 Most stable optimized geometry of (a)  $[Li(FSI)_3]^{2-}$  and (b)  $[Li(N(Tf)_2)_2]^{-}$  complexes in gas phase [59]

The thermodynamic parameters of enthalpy, entropy, and Gibbs free energy ( $\Delta H^{\circ}$ ,  $\Delta S^{\circ}$ , and  $\Delta G^{\circ}$ ) for the equilibrium are also estimated from the relationship of  $\Delta G^{\circ} = -RT \ln K$  and  $\Delta G^{\circ} = \Delta H^{\circ} - T\Delta S^{\circ}$ , i.e., van't Hoff plots for the equilibrium reaction. By using the *n* values obtained from 1,220 cm<sup>-1</sup> Raman band (filled circles colored with red in Fig. 10.5), the  $\Delta H^{\circ}$  and  $T\Delta S^{\circ}$  (298 K) are evaluated to be 35(2) kJ mol<sup>-1</sup> and 29(2) kJ mol<sup>-1</sup>, respectively.

According to our ab initio calculations, the possible model of  $[\text{Li}(\text{FSI})_3]^{2-}$  complex has been proposed [59], which is shown in Fig. 10.6a. In the calculation, we examined the geometry optimizations for four types of the complexes:  $[\text{Li}(\text{monodentate FSI})_2(\text{bidentate FSI})_1]^{2-}$ ,  $[\text{Li}(\text{monodentate FSI})_1(\text{bidentate FSI})_2]^{2-}$ ,  $[\text{Li}(\text{monodentate FSI})_1(\text{bidentate FSI})_2]^{2-}$ , and  $[\text{Li}(\text{bidentate FSI})_3]^{2-}$ . As the results, the most stable geometry is obtained for the  $[\text{Li}(\text{monodentate FSI})_2(\text{bidentate FSI})_1]^{2-}$ . As can be seen in the picture, the Li ion interacts with the oxygen atoms of  $[\text{FSI}]^-$ s and the coordination number is 4, which is similar to the  $[\text{Li}(\text{bidentate N}(\text{Tf})_2)_2]^-$  complex (Fig. 10.6b). The interaction energy of the Li-monodentate FSI in the  $[\text{Li}(\text{monodentate FSI})_1]^{2-}$  complex is appreciably weaker than that of the Li-bidentate FSI. The calculated interaction energies using the geometry shown in Fig. 10.6a are -444.3 and -560.6 kJ mol<sup>-1</sup> for the monodentate and bidentate [FSI]^-s, respectively. This supports Raman spectroscopic results described above, i.e., the monodentate [FSI]^- preferentially desolvates from the first solvation shell of the Li ion.

# **10.4** Atomistic Solvation Structure of Li Ion in ILs: HEXRD and MD Simulation Study

Figure 10.7a shows the experimental radial distribution function as a form of  $r^2[G(r) - 1]$  observed for LiFSI in [C<sub>2</sub>mim][FSI] solutions by HEXRD measurements. The peaks at around 5 (4.5 and 5.5), 9, and 15 Å can be fully assigned to the



**Fig. 10.7** X-ray radial distribution functions as a form of  $r^2[G^{exp}(r)-1]$  for (**a**) [Li] $x_{Li}[C_2mim]$   $(1-x_{Li})[FSI]$  and (**c**) [Li] $x_{Li}[C_2mim](1-x_{Li})[N(Tf)_2]$  solutions obtained by HEXRD experiments. (**b**) and (**d**) show the corresponding normal  $G^{exp}(r)$ s to easily see the closest Li<sup>+</sup>–O (anion) interactions shown by *arrows* [59] and [62]

intermolecular interactions [26, 36, 59]. It is found that the peak intensities at 4.5 and 5.5 Å increase with increasing Li[FSI] salt concentration. They are mainly originated from the correlations in the [Li(FSI)<sub>3</sub>]<sup>2-</sup> complexes and the closest [C<sub>2</sub>mim]<sup>+</sup>– [FSI]<sup>-</sup> interactions, which is discussed below in detail. Focusing on the broad peaks at around 9 Å, the peak intensity at 8 Å decreases but that at 11 Å increases with increasing salt concentration. The same is also found in the corresponding [N(Tf)<sub>2</sub>] system (Fig. 10.7c). The variations in the [N(Tf)<sub>2</sub>] system are ascribed to the long-range anion–anion interactions in the bulk and in the [Li(N(Tf)<sub>2</sub>)<sub>2</sub>]<sup>-</sup> complex [62]. Therefore, in the FSI system, it is expected that the formation of [Li(FSI)<sub>3</sub>]<sup>2-</sup> affects the radial distribution function at both of the short and long ranges. Here, we note the closest atom–atom interactions in the [Li(FSI)<sub>3</sub>]<sup>2-</sup> complex, particularly Li<sup>+</sup>–O



**Fig. 10.8** Pair distribution functions,  $g^{\text{MD}}(r)$ s for the Li<sup>+</sup>–X (O, S, and N) correlations in  $[\text{Li}]x_{\text{Li}}[C_2\text{mim}](1-x_{\text{Li}})$ [FSI] ( $x_{\text{Li}}=0.27$ ) at 298 and 398 K [59]

(FSI) interactions. Figure 10.7b, d shows the radial distribution functions,  $G^{exp}(r)$ s (normal form) for the [FSI] and  $[N(Tf)_2]$  systems, respectively. In general, it is quite difficult to observe the Li<sup>+</sup>-X correlations in the Li ion solvation structure in the solutions by an X-ray scattering technique due to a smaller X-ray scattering ability of Li ion. However, by using HEXRD with high r-resolution, we can find the Li<sup>+</sup>-O (FSI) interactions in the  $G^{exp}(r)$ . The closest Li<sup>+</sup>–O interaction in the [Li(FSI)<sub>3</sub>]<sup>2–</sup> complex appears at 1.94 Å and increases in intensity with an increase of Li salt concentration. The distance of 1.94 Å is consistent with the averaged Li<sup>+</sup>–O distance (1.97 Å) obtained by the present ab *initio* calculations for the [Li(monodentate FSI)<sub>2</sub>(bidentate FSI)<sub>1</sub>]<sup>2-</sup> (see Fig. 10.6). Similarly, the Li<sup>+</sup>–O interaction is also experimentally observed in the corresponding  $Li[N(Tf)_2]/[C_2mim][N(Tf)_2]$  system. The Li<sup>+</sup>–O distance is 1.86 Å in the  $[N(Tf)_2]$  system, which is slightly shorter than that in the FSI system. The difference in the Li+-O interactions between [FSI] and  $[N(Tf)_2]$  systems can be explained in terms of the solvation number *n* in the Li complexes, i.e., the larger n=3 in the [FSI] system than in the [N(Tf)<sub>2</sub>] one (n=2) leads to the longer atom-atom distance in the first coordination sphere of the Li ion.

The solvation structure at the atomistic level can be also investigated by MD simulations to give important evidence from theoretical aspect. Figure 10.8 shows the atom–atom pair correlation functions,  $g^{MD}(r)$  for the Li<sup>+</sup>–X (X=O, S, and N within [FSI] anion) derived from MD simulations. At 298 K, the Li<sup>+</sup>–O in the  $g^{MD}(r)$  is clearly found as a closest atom–atom correlation at 1.84 Å. The integral area intensity of the 1.84 Å peak that corresponds to the coordination number of O around Li<sup>+</sup> in the first neighboring is 3.7 (approximately 4). This suggests that Li ion is coordinated with four oxygen atoms within [FSI]<sup>-</sup>s to form a tetrahedral-like structure. The Li<sup>+</sup>–S correlation locates at 3.20 Å and the integrated value is also near to 4 (3.98). Here, note that the there are two peaks of the Li<sup>+</sup>–N correlation at 3.72 and 4.19 Å in the  $g^{MD}(r)$ . The former can be assigned to the bidentate [FSI]<sup>-</sup> solvated to the Li ion, whereas the latter to the monodentate [FSI]. The integrated

intensity ratio of the monodentate  $[FSI]^-$  to the bidentate one is estimated to be 1.97. This means that the monodentate and bidentate  $[FSI]^-$ s in the first solvation shell of the Li ion coexist as mono:bi=2:1. These results are completely consistent with those obtained from the Raman spectroscopy and ab initio calculations as described above. It is found in the  $g^{MD}(r)$ s at high temperature (Fig. 10.8, 398 K) that the coordination numbers of O, S, and N decrease to 3.44, 3.71, and 2.91, respectively. We thus found that the desolvation of  $[FSI]^-$  in the solvation sphere of Li ion evidently occurs at high temperature, which strongly supports Raman spectroscopic study.

### 10.5 Conclusion

Raman spectroscopy and high-energy X-ray diffraction with the aid of theoretical calculations are quite useful to elucidate Li ion solvation structure in ionic liquid systems. The molecular structure of  $[FSI]^-$  is similar to that of  $[N(Tf)_2]^-$  one; however, the Li ion solvation in the FSI-based ILs is largely different from that in the  $N(Tf)_2$ -based ILs. The difference in the Li ion solvation affects the physicochemical properties such as viscosity and ionic conductivity for the ILs containing Li ion. We believe that structural investigations at the molecular level presented in this chapter are important and helpful to understand electrochemical applications using ILs, for example, Li battery performances.

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## Symbols and Abbreviations

## **Ionic Liquid Abbreviations**

## Cations

[Hmim] <sup>+</sup>	1-Methylimidazolium		
[C <sub>1</sub> mim] <sup>+</sup>	1,3-Dimethylimidazolium		
[C <sub>2</sub> mim] <sup>+</sup>	1-Ethyl-3-methylimidazolium		
[C <sub>2</sub> dmim] <sup>+</sup>	1-Ethyl-2,3-dimethylimidazolium		
[C <sub>3</sub> mim] <sup>+</sup>	3-Methyl-1-propylimidazolium		
[C <sub>3</sub> dmim] <sup>+</sup>	2,3-Dimethyl-1-propylimidazolium		
[C <sub>4</sub> mim] <sup>+</sup>	1-Butyl-3-methylimidazolium		
[C <sub>4</sub> dmim] <sup>+</sup>	1-Butyl-2,3-dimethylimidazolium		
$[C_4C_4im]^+$	1,3-Dibutylimidazolium		
[C <sub>5</sub> mim] <sup>+</sup>	3-Methyl-1-pentylimidazolium		
[C <sub>6</sub> mim] <sup>+</sup>	1-Hexyl-3-methylimidazolium		
[C <sub>8</sub> mim] <sup>+</sup>	3-Methyl-1-octylimidazolium		
[C <sub>10</sub> mim] <sup>+</sup>	1-Decyl-3-methylimidazolium		
[dC <sub>18</sub> im] <sup>+</sup>	1,3-Dioctadecylimidazolium		
[HOCH <sub>2</sub> CH <sub>2</sub> -mim] <sup>+</sup>	1-(2-Hydroxyl)ethyl-3-methylimidazolium		
[MeOCH <sub>2</sub> CH <sub>2</sub> -mim] <sup>+</sup>	1-(2-Methoxy)ethyl 3-methylimidazolium		
[Me(OCH <sub>2</sub> CH <sub>2</sub> ) <sub>2</sub> -mim] <sup>+</sup>	1-(2-Methoxyethoxy)ethyl)-3-methylimidazolium		
[Me(OCH <sub>2</sub> CH <sub>2</sub> ) <sub>3</sub> -mim] <sup>+</sup>	1-(2-(2-Methoxy)ethoxy)ethyl)-3-methylimidazolium		
[HSO3-Bu-mim]+	1-Methyl-3-(4-sulfobutyl)imidazolium		
[HSO <sub>3</sub> -Bu-bim] <sup>+</sup>	1-Butyl-3-(4-sulfobutyl)imidazolium		
[HSO <sub>3</sub> -Bu-vim] <sup>+</sup>	1-(4-Sulfobutyl)-3-vinylimidazolium		
[vmim] <sup>+</sup>	3-Methyl-1-vinylimidazolium		
$[C_4 vim]^+$	3-Butyl-1-vinylimidazolium		
$[C_8 vim]^+$	3-Octyl-1-vinylimidazolium		
[C <sub>12</sub> vim] <sup>+</sup>	3-Dodecyl-1-vinylimidazolium		

$[C_{18}vim]^+$	3-Octadecyl-1-vinylimidazolium		
[C <sub>22</sub> vim] <sup>+</sup>	3-Docosyl-1-vinylimidazolium		
$[C_2C_4OOC_2im]^+$	3-(4-Ethoxy-4-oxobutyl)-1-ethylimidazol-3-ium		
[C <sub>2</sub> PhC <sub>2</sub> im] <sup>+</sup>	1-Ethyl-3-phenethylimidazol-3-ium		
[C <sub>3</sub> PhC <sub>3</sub> im] <sup>+</sup>	3-(3-Phenylpropyl)-1-propyl-1H-imidazol-3-ium		
[C <sub>3</sub> PhOC <sub>3</sub> im] <sup>+</sup>	3-(4-Phenoxybutyl)-1-propyl-1H-imidazol-3-ium		
[FcC <sub>1</sub> mim] <sup>+</sup>	1-(Ferrocenylmethyl)-3-methylimidazolium		
[Amim] <sup>+</sup>	1-Allyl-3-methylimidazolium		
[HPyr] <sup>+</sup>	Pyrrolidinium		
[C <sub>1</sub> HPyr] <sup>+</sup>	1-Methylpyrrolidinium		
[C <sub>3</sub> mPyr] <sup>+</sup>	1-Methy-1-propylpyrrolidinium		
[C <sub>4</sub> mPyr] <sup>+</sup>	1-Butyl-1-methylpyrrolidinium		
[C₅mPyr] <sup>+</sup>	1-Methyl-1-pentylpyrrolidinium		
[C <sub>3</sub> bPyr] <sup>2+</sup>	1,1'-(Propane-1,3-diyl)bis(4-methylpyridinium)		
$[C_4 bPyr]^{2+}$	1,1'-(Butane-1,4-diyl)bis(4-methylpyridinium)		
[C <sub>3</sub> mpip] <sup>+</sup>	1-Methyl-1-propylpiperidinium		
[C <sub>4</sub> mpip] <sup>+</sup>	1-Buthyl-1-methylpiperidinium		
$[C_2C_6pip]^+$	1-Ethyl-1-hexylpiperidinium		
[HP <sub>444</sub> ] <sup>+</sup>	Tributylphosphonium		
$[P_{1444}]^+$	Tributylmethylphosphonium		
$[P_{4444}]^+$	Tetrabutylphosphonium		
$[P_{66614}]^+$	Trihexyl(tetradecyl)phosphonium		
[H <sub>3</sub> NEt] <sup>+</sup>	Ethylammonium		
[HN <sub>111</sub> ] <sup>+</sup>	Trimethylammonium		
[HN <sub>222</sub> ] <sup>+</sup>	Triethylammonium		
[N <sub>1114</sub> ] <sup>+</sup>	Butyltrimethylammonium		
$[N_{1116}]^+$	Hexyl(trimethyl)ammonium		
[N <sub>2,2,1,m</sub> ] <sup>+</sup>	<i>N</i> , <i>N</i> -diethyl- <i>N</i> -methyl- <i>N</i> -(2-methoxyethyl)ammonium		
[N <sub>2224</sub> ] <sup>+</sup>	Butyl(trimethyl)ammonium		
[N <sub>2 2 2 6</sub> ] <sup>+</sup>	Hexyl(trimethyl)ammonium		
[N <sub>3 3 3 p</sub> ] <sup>+</sup>	Trimethylphenylammonium		
$[N_{4444}]^+$	Tetrabutylammonium		
[N 4446] <sup>+</sup>	Tributyl(hexyl)ammonium		
$[N_{6666}]^+$	Tetrahexylammonium		
[N <sub>66614</sub> ] <sup>+</sup>	Trihexyl(tetradecyl)ammonium		
$[N_{1888}]^+$	Methyl(trioctyl)ammonium		
[N <sub>8 8 8 8</sub> ] <sup>+</sup>	Tetraoctylammonium		
[N <sub>1 12 12 12</sub> ] <sup>+</sup>	Tridodecylmethylammonium		
[CTMA] <sup>+</sup>	<i>N,N,N,N</i> -cyanomethyl trimethyl ammonium		
[dema]+	Diethylmethylammoium		
[dmea]+	Dimethylethylamine		
[DEME] <sup>+</sup>	N-methyl-N-(2-methoxyethyl)ammonium		
[NHEt(i-Pr) <sub>2</sub> ] <sup>+</sup>	N,N-diisopropylethylamine		

· · · · ·		
$[H_3N(CH_2CH_2OH)]^+$	Ethanolammonium	
$[H_2N(CH_2CH_2OH)_2]^+$	Bis(2-hydroxyethyl)ammonium	
$[(HOCH_2CH_2)N_{111}]^+$	Choline	
[CH <sub>3</sub> OCH <sub>2</sub> CH <sub>2</sub> -Et-Me <sub>2</sub> N] <sup>+</sup>	(2-Methoxy)ethyl ethyl dimethylammonium	
[CH <sub>3</sub> OCH <sub>2</sub> CH <sub>2</sub> -Et <sub>2</sub> -MeN] <sup>+</sup>	(2-Methoxy)ethyl diethyl methylammonium	
[Bu-Et <sub>2</sub> -MeN] <sup>+</sup>	Butyl diethyl methylammonium	
[Hpy] <sup>+</sup>	Pyridinium	
$[C_4 py]^+$	1-Butylpyridinium	
[C₄mβpy] <sup>+</sup>	1-Butyl-3-methylpyridinium	
[C <sub>8</sub> py] <sup>+</sup>	1-Octylpyridinium	
$[C_{18}py]^+$	1-Octadecylpyridinium	
[HmimSC <sub>4</sub> ] <sup>+</sup>	1-Methyl-2-butylthiolonium	
$[S_{111}]^+$	Trimethylsulfonium	
[S <sub>221</sub> ] <sup>+</sup>	Diethyl(methyl)sulfonium	
[S <sub>222</sub> ] <sup>+</sup>	Triethylsulfonium	
[CDBA6] <sup>+</sup>	N,N'-(trans-cyclohexane-1,4-diyl)-dibenzamide	
[H-betaine] <sup>+</sup>	Betainium	
[PD] <sup>3+</sup>	1,3,5-Tris(3-((ferrocenylmethyl)amino)	
	pyridiniumyl)-2,4,6-triethylbenzene	
$[(N_{111})(N_{112})BH_2]^+$	(Trimethylamine)-(dimethylethylamine)dihydroborate	

## Anions

[FSI]-	Bis(fluorosulfonyl)imide
[BETI]-	Bis(perfluoroethylsulfonyl)imide
$[N(Tf)_2]^-$	Bis(trifluoromethylsulfonyl)imide
$[C_4C_4N]^-$	Bis(nonafluorobutylsulfonyl)imide
[NTf] <sup>-</sup>	Brifluoromethanesulfonate
$[N(CN)_2]^-$	Bicyanamide
[C(CN) <sub>3</sub> ] <sup>-</sup>	Tricyanomethanide
[PF <sub>6</sub> ] <sup>-</sup>	Hexafluorophosphate
[NO <sub>3</sub> ] <sup>-</sup>	Nitrate
[B(CN) <sub>4</sub> ] <sup>-</sup>	Tetracyanoborate
$[BF_4]^-$	Tetrafluoroborate
$[CF_3BF_3]^-$	Trifluoromethyltrifluoroborate
[BSB] <sup>_</sup>	Bis(salicylate[2-])borate
[TFPB] <sup>-</sup>	Tetrakis(3,5-trifluoromethylphenyl)borate anion
[SCN]-	Thiocyanate
[HCO <sub>2</sub> ] <sup>-</sup>	Formate
$[CF_3CO_2]^-$	Trifluoroacetate
[CH <sub>3</sub> CO <sub>2</sub> ] <sup>-</sup> or [Ac] <sup>-</sup>	Acetate
[C <sub>9</sub> H <sub>19</sub> CO <sub>2</sub> ] <sup>-</sup>	Decanoate

[CF <sub>3</sub> SO <sub>3</sub> ] <sup>-</sup>	Trifluoromethanesulfonate
[CH <sub>3</sub> SO <sub>3</sub> ] <sup>-</sup>	Methanesulphonate
[HSO <sub>4</sub> ] <sup>-</sup>	Hydrogen sulfate
[MeSO <sub>4</sub> ] <sup>-</sup>	Methylsulphate
[EtSO <sub>4</sub> ]⁻	Ethyl sulphate
$[C_8H_{17}SO_4]^-$	Octylsulfate
[FAP]-	Trifluorotris(pentafluoroethyl)phosphate
$[R_2PO_4]^-$	Dialkylphosphate
[Me <sub>2</sub> PO <sub>4</sub> ] <sup>-</sup>	Dimethylphosphate
[(EH) <sub>2</sub> PO <sub>4</sub> ] <sup>-</sup>	Bis(2-ethylhexyl)phosphate
[TPTP]-	Tris(pentafluoroethyl)trifluorophosphate
[(i-C <sub>8</sub> )PO <sub>2</sub> ] <sup>-</sup>	Bis(2,4,4-trimethylpentyl)phosphinate
[DPP]-	Diphenylphosphate
[DBP]-	Dibutylphosphate
[EtPO <sub>3</sub> H] <sup>-</sup>	Ethylphosphonate
$[(i-C_4)_2 PS_2]^-$	Diisobutyldithiophosphinate
$[(OC_2)_2PS_2]^-$	O,O'-diethyldithiophosphate
[OH]-	Hydroxide
[I]-	Iodide
[Cl]-	Chloride
[CS]-	Camphorsulfonate
[SiF <sub>6</sub> ] <sup>2-</sup>	Hexafluorosilicate
[SbF <sub>6</sub> ]⁻	Hexafluoroantimonate
[Cu <sub>2</sub> Cl <sub>3</sub> ] <sup>-</sup>	Copper chloride
$[Cu_2Br_3]^-$	Copper bromide
[AlCl <sub>4</sub> ] <sup>-</sup>	Tetrachloroaluminate
[tos] <sup>-</sup>	Tosylate
[Adip] <sup>2-</sup>	Adipate
[Succ] <sup>2–</sup>	Succinate

## **Chemical Abbreviations**

AA	Ascorbic acid	
AC	Activated carbons	
ACN	Acetronitrile	
Au	Gold	
γ-BL	Gamma butyrolactone	
Bu <sub>4</sub> N	Tetrabutylammonium	
Cc+	Cobaltocenium	
Chi	Chitosan	
cis-Mn	cis-[Mn(CN)(CO) <sub>2</sub> [P(oph) <sub>3</sub> ](DPM)] (DPM = Ph <sub>2</sub> PCH <sub>2</sub> PPh <sub>2</sub>	
cis-W	cis-[W(CO) <sub>2</sub> (DPE) <sub>2</sub> ] (DPE <sub>5</sub> Ph <sub>2</sub> PCH <sub>2</sub> CH <sub>2</sub> PPh <sub>2</sub> )	

(continued)
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CNTs	Carbon nanotubes		
Ср	Cyclopentadienyl		
DEC	Diethyl carbonate		
DMC	Dimethyl carbonate		
DMF	Dimethyl formamide		
DmFc	Decamethylferrocene		
DMSO	Dimethyl sulfoxide		
EAN	Ethylammonium nitrate		
EC	Ethylene carbonate		
EMC	Ethylmethyl carbonate		
Fc	Ferrocene		
Fc <sup>+</sup>	Ferrocenium		
FTO	Fluorine-doped tin oxide		
HOPG	Highly ordered pyrolytic graphite		
ITO	Indium tin oxide		
LTO	Lithium titanium oxide		
MAc	N-methylacetamide		
MEA	Monoethanolamine		
MeCN	Acetonitrile		
MWCNT	Multiwall carbon nanotubes		
NADH	Nicotinamide adenine dinucleotide		
NHC	N-heterocyclic carbenes		
OMCs	Ordered mesoporous carbons		
PC	Propylene carbonate		
	Polycarbonate		
PEDOT	Poly(3,4-ethylenedioxythiophene)		
PEG	Polyethylene glycol		
PS	Polystyrene		
Pt	Platinum		
PVA	Polyvinyl alcohol		
PVF	Polyvinylferrocene		
RE	Rare earth		
SAPG	Stress-annealed pyrolytic graphite		
scCO <sub>2</sub>	Supercritical carbon dioxide		
SWCNT	Single wall carbon nanotubes		
trans-Mn	$trans-[Mn-(CN)(CO)_2{P(oph)_3}(Ph_2PCH_2PPh_2)]$		

## **Abbreviations**

AC	Alternating current
AFM	Atomic force microscopy
AIL	Aprotic ionic liquid
	(continued)

ANS	Analyte	
ATR	Attenuated total reflectance	
BDD	Boron doped diamond	
bp	Boiling point	
CGT	Complexed gas technology	
CILEs	Carbon ionic liquid electrodes	
СР	Conducting polymer	
CPE	Carbon paste electrodes	
CPET	Concerted proton electron transfer	
CV	Cyclic voltammetry	
CVD	Chemical vapor deposition	
DES	Deep eutectic solvents	
DLC	Diamond-like coatings	
DLS	Dynamic light scattering	
DRIFTS	Diffuse reflectance infrared Fourier-transform spectroscopy	
DSSC	Dye-sensitized photoelectrochemical solar cells	
E-ALD	Electrochemical atomic layer deposition	
E-ALE	Electrochemical atomic layer epitaxy	
ECC	Electrocapillary curve	
ECL	Electrochemiluminescence	
ECM	Electrocapillary maximum	
EDL	Electrical double layer	
EDLC	Electric double layer capacitors	
EDR	Equivalent diffusion resistance	
EDX	Energy dispersive X-ray	
EE	Electrochemical mechanism with sequential electron transfer	
EIS	Electrochemical impedance spectroscopy	
EPT	Electron proton transfer	
EQCM	Electrochemical quartz crystal microbalance	
ESR	Equivalent series resistance	
ESW	Electrochemical stability windows	
ET	Electron transfer	
EVs	Electric vehicles	
EW	Electrochemical potential windows	
FTIR	Fourier transform infrared spectroscopy	
GC	Glassy carbon	
HBD	Hydrogen bond donor	
HER	Hydrogen evolution reaction	
HEVs	Hybrid electric vehicles	
HFCs	Hydrogen fuel cell	
HOR	Hydrogen oxidation reaction	
IDE	Interdigitated electrode	
IL, RTIL	Ionic liquid	

(continued)		
ILEs	Ionic liquid-based electrolytes	
IL-G	Ionic liquid-graphene composite film	
IR	Infrared spectroscopy	
IRRS	Internal reference redox systems/internal reference redox scale	
IS	Immittance spectroscopy	
JCPDS	Joint committee on powder diffraction standards	
LED	Light-emitting diode	
MBE	Molecular beam epitaxy	
MEP	Molecular electrostatic potential	
MFT	Mean field theory	
mp	Melting point	
NADES	Natural deep eutectic solvents	
NHE	Normal hydrogen electrode	
NMR	Nuclear magnetic resonance	
NP	Nanoparticle	
OCP	Open circuit potential	
OER	Oxygen evolution reaction	
OLEs	Organic solvent-based electrolytes	
OPD	Overpotential deposition	
ORR	Oxygen reduction reaction	
OX <sub>ANS</sub>	Oxidised redox component of the ANS	
OX <sub>IRRS</sub>	Oxidised redox component of the IRRS	
QRE	Quasi-reference (or pseudo-reference) electrodes	
PDDF	Pair distance distribution function	
PEMFC	Polymer electrolyte membrane fuel cells	
PET	Proton electron transfer	
PFIL	Polyelectrolyte-functionalized ionic liquid	
PILs	Protic ionic liquids	
ppb	Part per billion	
ppm	Part per million	
PVD	Physical vapor deposition	
PZC	Potential of zero charge	
RDE	Rotating disk electrode	
RED <sub>ANS</sub>	Reduced redox component of the ANS	
RED <sub>IRRS</sub>	Reduced redox component of the IRRS	
RFB	Redox flow batteries	
rpm	Revolutions per minute	
RRDE	Rotating ring-disk electrode	
RTMS	Room-temperature molten salts	
SAS	Small angle scattering	
SAXS	Small angle X-ray scattering	
SCE	Saturated calomel electrode	
SECM	Scanning electrochemical microscopy	

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SEM	Scanning electron microscopy
SFG	Sum frequency generation spectroscopy
SHG	Second harmonic generation
SPCE	Screen-printed carbon electrode
STM	Scanning tunneling microscope
STS	Scanning tunneling spectroscopy
ToF-SIMS	Time-of-flight secondary ion mass spectrometry
TSIL	Task-specific ionic liquids
UHV	Ultrahigh vacuum
UMEs	Ultramicroelectrodes
UPD	Underpotential deposition
UV	Ultraviolet
UV-Vis	Ultraviolet-visible
VOCs	Volatile organic compounds
VSFS	Vibrational sum frequency spectroscopy
WAXS	Wide angle X-ray scattering
XFEL	X-ray free electron laser
XPCS	X-ray photon correlation spectroscopy
XPS	X-ray photoelectron spectroscopy
XRD	X-ray diffraction
ZIL	Zwitterionic liquid

## Roman Symbols

А	Electrode area
a	Microdisk electrode radius
ai	Activity of ions
В	Porod scaling factor
С	Capacitance
	Coulomb
с	Bulk ionic concentration (also referred as <i>C</i> )
C_	Concentration of anion
C <sub>+</sub>	Concentration of cation
$C_0$	Capacitance at the minimum (PZC)
C <sub>d</sub>	Double layer capacitance
$C_{\rm sp}$	Specific capacitance
D	Diffusion coefficient
$D_0$	Diffusion coefficient of an oxidised redox component
$D_n(R)$	Number distribution function
D(q)	Effective diffusion constant
$D_{\rm R}$	Diffusion coefficient of a reduced redox component

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	<b>D</b> 00.1
$D(\lambda)$	Detector efficiency
d	Tip-substrate distance
	Electrolyte density
	Repeat distance
$d_{\mathrm{i}}$	Diameter of an ion
$d_m$	Mass fractal dimension
$d_s$	Surface fractal dimension
е	Charge on the electron
Е	Energy
	Potential
E'	Electric field of the visible and infrared incoming beams
E <del>o</del> '	Formal potential (also referred as $E^{0'}$ )
$E_{1/2}$	Measured or expected half-wave potential in voltammetry
$E_{1/4}$	Potential where $I/I_d = 1/4$
$E_{3/4}$	Potential where $I/I_d = 3/4$
$E_{\mathrm{a}}$	Activation energy
$E_{\rm end}$	Ending potential in a voltammetric scan
$E_{\mathrm{m}}$	Mid-point potential
$\Delta E_{ m m}$	Distance between the $E_m$ of two redox processes
$E_{\mathrm{T}}^{\mathrm{N}}$	Normalized charge transfer
$\Delta E_{ m p}$	Peak-to-peak potential separation
$E_{\rm rev}$	Reversing potential in a voltammetric scan
$E_{\rm start}$	Starting potential in a voltammetric scan
F	Faraday constant-the number of coulombs per mole of electrons ( $F = 96485 \text{ C mol}^{-1}$ )
F(q,)	Form factor
f	Scattering power of a free electron (excluding anomalous effects)
$f_0$	Fundamental frequency
$\Delta f$	Frequency shift
G	Guinier scaling factor
$\Delta G^{\circ}$	Gibbs free energy
g	Gravitational force
$g_2(q,\tau)$	Normalized second order intensity correlation function
$H^{\circ}$	Enthalpy
H(q)	Hydrodynamic interaction
h	Hour
Ι	Faradaic current (also referred as <i>i</i> )
Іо	Incident intensity flux
Id	Current under diffusion control
Ie	Intensity scattered by a single electron
Ip	Peak current (also referred as $i_p$ )
I(q)	Measured intensity from a small angle scattering experiment
i <sub>ss</sub>	Steady-state mass transport limited current (also referred as $I_L$ )
i <sub>T</sub>	Tip current

J	Raman scattering coefficient
j	Current density (also referred as J)
Κ	Binding constant
$k^{0'}$	Heterogeneous charge transfer rate constant (cm <sup>2</sup> s)
k <sub>B</sub>	Boltzmann constant
K <sub>cross</sub>	Equilibrium constant for a simple outer-sphere second-order cross-reaction
$k_{\rm cross}$	Rate constant for a simple outer-sphere second-order cross-reaction
<i>k</i> <sub>d</sub>	Homogeneous rate constant for "forward" reaction (the unit depends on reaction order)
L	Dimension of any inhomogeneity
Μ	Convolved/semiintegrated current
$M_{ m L}$	Mass transport limited convolved/semiintegrated current
т	Mass transfer coefficient
$\Delta m$	Mass changes
Ν	Number density of scatterers
n	Number of moles of electrons
	Integer
Р	Pressure
	Real space vector between two inhomogeneities
Q	Charge
$Q_{\rm inv}$	Scattering invariant
q	Scattering vector
R	Resistance
	Universal gas constant (8.314 J K <sup>-1</sup> mol <sup>-1</sup> )
	Radius
R <sub>ct</sub>	Charge transfer resistance
R <sub>g</sub>	Radius of gyration
Rg <sub>CO</sub>	Radius of gyration cutoff (unified equation)
$R_{\rm HS}$	Hard sphere radius
R <sub>s</sub>	Solution resistance
$R_{\rm u}$	Uncompensated resistance
r	Real space vector between two points
	Radial distance from the center of an electrode (cm)
$r_0$	Electrode radius
r <sub>g</sub>	Radius of the sheath
S	Surface area
	Siemens
$S^{\circ}$	Entropy
$S(q,\ldots)$	Structure factor
<i>s</i> , <i>s</i> <sub>o</sub>	Unit vector of scattered and incoming X-rays, respectively
T	Temperature
Tg	Glass transition temperature
$T_{\rm m}$	Melting point
Tr	Transmission

ts	Material thickness
V	Voltage (also referred as $U$ )
ν	Particle volume fraction
$\nu_{\rm p}$	Volume occupied by a single point
W	Warburg element
w	Mass fraction
x	Distance from a planar electrode
<i>x</i> <sub>2</sub>	Distance between the electrode surface and the inner Helmholtz plane

## Greek Symbols

α	Electron transfer coefficient
$\beta(q)$	Optical transfer function
γ	Decay exponent
γs	Interfacial tension
$\gamma_{\rm o}(r)$	Normalized auto-correlation function
ε	Dielectric constant
	Permittivity
$\mathcal{E}_{\mathrm{r}}$	Relative permittivity
η	Efficiency of the process
	Viscosity
$\eta^{-1}$	Fluidity
$\overline{\eta^2}$	Square of the volume average contrast
Λ	Molar conductivity
λ	Wavelength of light (nm)
$\mu_q$	Quartz shear modulus,
μΙρ	Mass absorption coefficient
υ	Scan rate
ρ	Scattering length density
$ ho_{ m q}$	Quartz density
$ ho_s$	Mass density of a material
$ar{ ho}^2$	Auto-correlation of scattering length density function
$\rho^2(\lambda)$	Scattering power (includes absorption)
$\sigma$	Ionic conductivity
	Standard deviation
τ	Cell time constant
	Time delay between two measurements
$\phi$	Phase
ω	Electrode angular velocity

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